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FINAL REPORT ON THE OXIDATION OF
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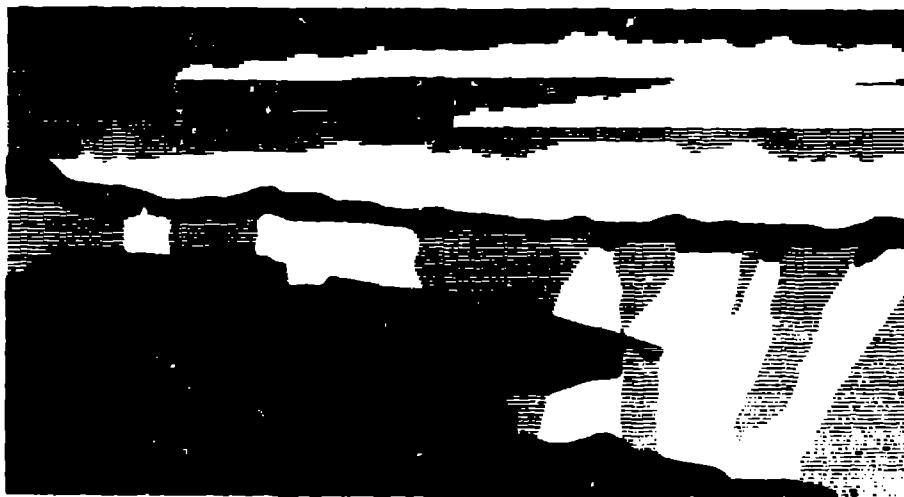
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PREFACE

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This report has been reviewed by the Public Affairs Office (PA) and is releasable to the National Technical Information Service (NTIS). At NTIS, it will be available to the general public, including foreign nationals.

This report has been reviewed and is approved for public release.

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**FINAL REPORT
ON THE
OXIDATION OF ENERGETIC MATERIALS IN SUPERCRITICAL WATER**

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LIST OF ABBREVIATIONS

AP	Ammonium Perchlorate
BTTN	1,2,4-Butanetriol Trinitrate
CARS	Coherent Anti-Stokes Raman Spectroscopy
DA&C	Data Acquisition and Control
DAC	Digital to Analog Converter
DRE	Destruction and Removal Efficiency
ft	Foot
FTIR	Fourier-Transform Infrared
g	Gram
GC-MS	Gas Chromatography-Mass Spectroscopy
HMX	Cyclotetramethylene Tetranitramine
HPLC	High Performance Liquid Chromatography
id	Inside Diameter
in	Inch
mL	Milliliter
MPa	Mega Pascals
NC	Nitrocellulose
NG	Nitroglycerine
NM	Nitromethane
NQ	Nitroguanidine
OB/OD	Open Burning/Open Detonation
od	Outside Diameter
PEP	Propellants, Explosives and Pyrotechnics
PETN	Pentaerythritol Tetranitrate
psia	Pounds Per Square Inch Absolute
psig	Pounds Per Square Inch Gage
RDX	Cyclotrimethylene Trinitramine
SCWO	Supercritical Water Oxidation
TNT	2,4,6-Trinitrotoluene
UDMH	1,1-Dimethylhydrazine
YAG	Yttrium Aluminum Garnet
µm	Micrometer (10⁻⁶ Meters)

SECTION I

INTRODUCTION

A. OBJECTIVE

The objective of this project was to determine the suitability of oxidation in supercritical fluids (SCO), particularly water (SCWO), for disposal of propellants, explosives, and pyrotechnics (PEPs).

The SCO studies of PEPs addressed the following issues:

- The efficiency of destruction of the substrate.
- The products of destruction contained in the effluent.
- Whether the process can be conducted safely on a large scale.
- Whether energy recovery from the process is economically practicable.

The information essential for process development and equipment design was also investigated, including issues such as practical throughput of explosives through a SCWO reactor, reactor materials and corrosion, and models for process design and optimization.

B. BACKGROUND

1. Need for Alternative Disposal Methods

Traditional methods for disposing of PEPs have been open burning or open detonation (OB/OD); however, regulatory agencies are likely to prohibit OB/OD because of the uncontrolled air emissions and soil contaminations. Likewise, controlled incineration carries a liability for air pollution because large quantities of NO_x are produced in the conventional combustion chemistry of PEPs and because the course of combustion of PEPs is generally erratic and characterized by recurrent process upsets. Soil and ground water have already been contaminated with PEPs through normal operations at manufacturing plants and military bases. Incineration can be used for decontamination of these soils, with the associated liability for air pollution, but few satisfactory and economic methods exist for ground water decontamination. A clear need exists for improved disposal and destruction methods.

2. Supercritical Water Oxidation (SCWO)

In SCWO, the waste is generally mixed with an oxidant (oxygen, air, or hydrogen peroxide) in water at pressures and temperatures above the critical point (374 °C and 22.13 MPa). Under these conditions, water is a fluid whose densities are high enough that reasonable process throughput can be achieved, but whose transport properties are like those of a gas, allowing rapid, homogeneous chemical reaction. Supercritical water is a unique solvent medium in which oxidation can take place at lower temperatures than incineration, thus limiting the production of NO_x and char. The reaction is entirely enclosed in a pressure vessel at concentrations low enough that the heat of reaction is absorbed by the solvent. As a result, the temperature can be maintained at any desired level (typically in the range 400-650 °C). Oxidation occurs rapidly, on the time scale of seconds to minutes, and produces simple products (ideally CO₂, H₂O, and N₂).

In principle, any organic compound -- that is, any compound composed of carbon and other elements such as hydrogen, nitrogen, phosphorus, sulfur, and the halogens -- can be completely oxidized to relatively innocuous products. Because water is the reaction medium, the process can be used for a variety of organic wastes containing water, or for water contaminated with organic compounds. The optimum concentration of organics in water will vary with the heat of oxidation of the particular organic compounds present and the engineering design of the apparatus. An engineering consideration in the design of a plant is the range of organic concentrations that generates enough heat to maintain the reaction, but not more heat than can readily be removed from the processing vessel. Pure or highly concentrated organic wastes can be diluted with water, whereas fuel or other organic wastes can be added to dilute aqueous wastes. Other factors that influence the engineering design include the residence time in the reactor (determined by the chemical kinetics of oxidation of the waste), the physical state of the waste and its oxidation products, and the quantity of waste to be processed.

A schematic for the SCWO process is shown in Figure 1. The waste, oxidant, and fuel (if needed) are compressed, preheated, mixed, and injected into the reactor where the waste is (ideally) converted into H₂O, CO₂, N₂, salts, and insoluble solids. Reactor pressures typically range from 25 to 35 MPa (3700 to 5100 psia). Solid, liquid, and gaseous effluents are separated, depressurized, and (if needed) postprocessed. All effluents can be contained and collected for testing before release to the environment. Unreacted oxygen can be segregated and recycled, and energy can be recovered and used to heat incoming waste.

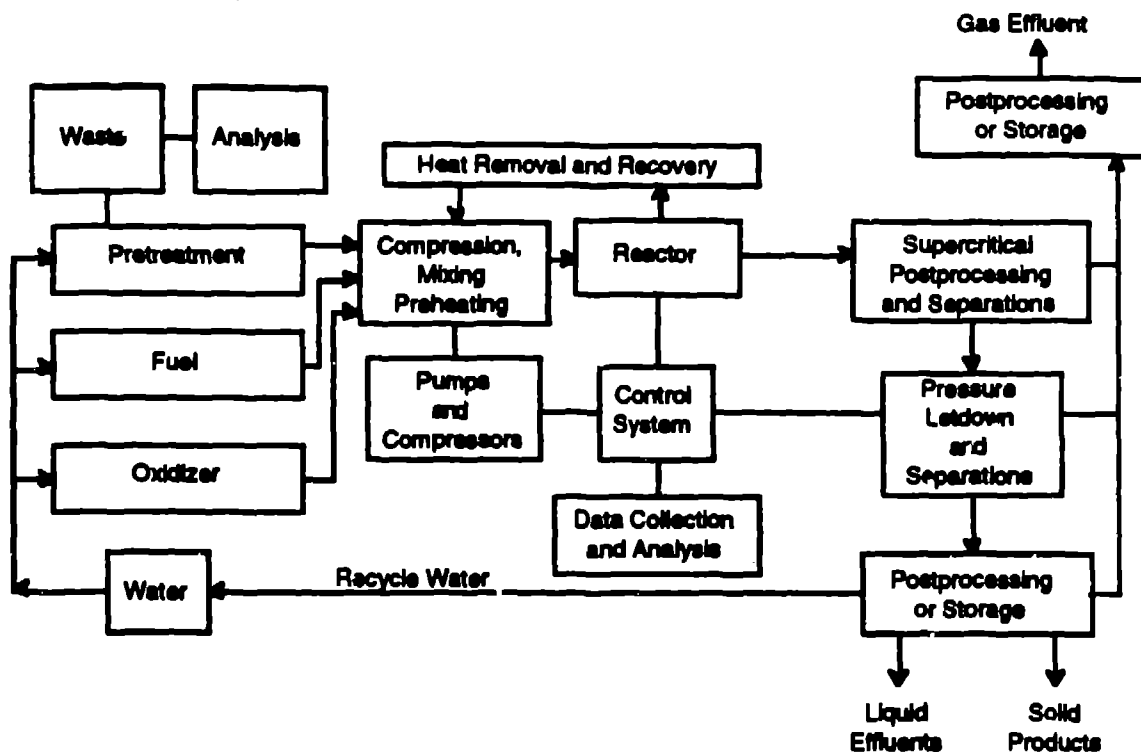


Figure 1. SCWO Process Schematic.

A great range of scale appears to be possible for supercritical water oxidation plants. Standard pressure-vessel technology can be used to provide small mobile units or permanent medium-sized surface installations for processing of laboratory or manufacturing wastes. Plants with very large capacities have also been proposed, in which a cylindrical heat exchanger and reaction vessel are placed in the ground by use of oil-field drilling and well-completion technology.

Operation of an SCWO unit for the treatment of explosive wastes would need to be controlled remotely. The details for full-scale operation (site preparation, facility needs, utilities) will depend on the waste being treated and the particular design of the reactor (i.e., tube, vessel, in-ground, etc.). A more complete description of the operation of full-scale SCWO units, including materials throughput, mass balances, and equipment design, can be found in several reports (References 7, 8).

An SCWO reactor that could be used for demonstration purposes is schematically outlined in Figure 2. Flow capacity of this unit would be 20 gallons/hour and it would process water containing up to 20 percent organic content by weight. For comparison, the capacity of a

medium-sized, full-scale unit is envisioned to be 10 to 100 times larger, depending on the specific waste stream. This demonstration unit would be used to evaluate design concepts for a full-scale unit, pre- and post-processing technologies for each different waste type, and process controls. It would provide information concerning the effectiveness of the treatment process (e.g., destruction efficiencies, products of SCWO, etc.), wear and useful lifetime of equipment components, health and safety considerations, and operation and maintenance requirements.

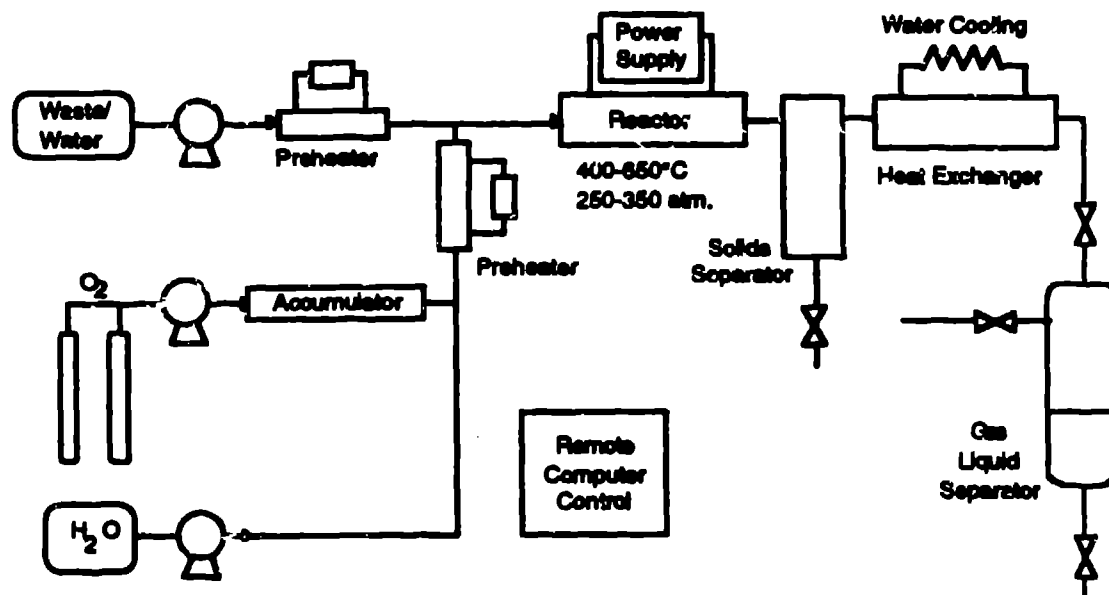


Figure 2. Simplified Schematic of Demonstration SCWO Treatment Unit.

3. Results of Past SCWO Studies: Demonstrated Performance

The principle of SCWO has been successfully demonstrated. Supercritical water oxidation has exhibited high destruction and removal efficiencies (DREs) for a broad range of common solid and liquid wastes, including such difficult examples as chlorinated aromatic solvents (References 1-6). These same studies have indicated that the major reaction products are water, carbon dioxide, and inorganic salts. Traces of carbon monoxide and nitrous oxide were also observed. Nitrous oxide can be efficiently converted into nitrogen and oxygen by venting through an inexpensive, commercially available catalyst. Less detailed but promising results were also reported for 2,4-dinitrotoluene, which is structurally related to several of the substrates in this study.

A wide variety of compounds have been successfully oxidized. These include simple hydrocarbons and oxygenates, chlorinated organics and aromatics, nitro-organic compounds, pharmaceuticals and biopharmaceuticals, dioxin-contaminated soil, fermentation wastes, and municipal and industrial sludges (References 3-7). Table 1 lists a number of compounds for which destruction efficiencies have been measured. The SCWO process has been operated successfully in the presence of many inorganic compounds (Table 2) and has been used to process a number of complex wastes (Table 3). In addition, such inorganic compounds as perchlorate and nitrate salts have been destroyed in supercritical water with greater than 99.9 percent efficiency.

Although the principle of SCWO has been successfully demonstrated on many classes of wastes, it has not been (before this work) applied to energetic materials. Issues that remain unresolved include the safety of the process, kinetics of decomposition, reaction products (the nitrogen chemistry in particular is not known), effects of high salt concentrations such as aluminum and chloride salts expected to be produced with most propellant formulations, introduction of energetic materials into a SCWO reactor at practical concentrations and the effects of corrosion on reactor materials.

4. Readiness for Demonstration

Industrial, governmental, and university participants at a workshop sponsored by the U. S. Air Force Engineering and Service Center, held at Los Alamos in August of 1989, decided that no fundamental impediments exist to the application of supercritical water oxidation processes to ultrahazardous materials under appropriately controlled conditions. There was, however, general agreement that several practical difficulties will require additional research and development. These areas include the handling of solids, materials problems relating to corrosive wastes, the handling of high-risk wastes (e.g., highly radioactive mixed wastes), and the handling of energetic materials. Since then, progress has been made on problems associated with the handling of solids and explosives. Although work has been done on the corrosion problem, no successful solution has yet been fully demonstrated. Corrosion problems may need to be resolved for specific waste streams before a full-scale plant is implemented, although they are not severe enough to delay demonstration of the technology.

TABLE 1. CHEMICALS TREATED BY SUPERCRITICAL WATER OXIDATION AND TYPICAL DESTRUCTION EFFICIENCIES^a

Chemical Name	Destruction Efficiency, %
Ammonia	>99.71
Ammonium Perchlorate	>99.9
Arochlors (PCBs)	>99.995
Biphenyl	99.97
Carbon Tetrachloride	>96.53
Chlorinated Dibenzo- <i>p</i> -dioxins	>99.9999
Chloroform	>98.83
2-Chlorophenol	>99.997
<i>o</i> -Chlorotoluene	>99.998
Cyclohexane	99.97
DDT	99.997
Dextrose	99.6
4,4'-Dichlorobiphenyl	99.993
1,2-Dichloroethylene	99.99
2,4-Dinitrotoluene	99.9998
Ethylene Glycol	>99.9998
Fluorescein	>99.9992
Hexachlorocyclohexane	>99.9993
Hexachlorocyclopentadiene	99.99
HMX ^b	>99.9
Methyl Ethyl Ketone	99.993
Nitrobenzene	>99.998
Nitroguanidine ^b	>99.9
Nitromethane ^b	>99.9
PETN ^b	>99.9
RDX ^b	>99.9
Tetrachloroethylene	99.99
TNT ^b	>99.9
Trichlorobenzenes	99.99
1,1,1-Trichloroethane	>99.99997
1,1,2-Trichloroethane	>99.981
<i>o</i> -Xylenes	99.93

^a(References. 1-6).

^bThis study.

TABLE 2. INORGANIC COMPOUNDS PROCESSED THROUGH SUPERCRITICAL WATER OXIDATION REACTOR^a

Alumina	Magnesium Phosphate
Ammonium Chloride	Magnesium Sulfate
Ammonium Sulfate	Mercuric Chloride
Boric Acid	Potassium Bicarbonate
Bromides	Potassium Carbonate
Calcium Carbonate	Potassium Chloride
Calcium Chloride	Potassium Sulfate
Calcium Oxide	Silica
Calcium Phosphate	Sodium Carbonate
Calcium Sulfate	Sodium Chloride
Fluorides	Sodium Hydroxide
Heavy Metal Oxides	Sodium Nitrate
Hydrochloric Acid	Sodium Nitrite
Iron	Sodium Sulfate
Iron Oxide	Soil
Lithium Sulfate	Sulfur, Elemental
Magnesium Oxide	Titanium Dioxide

TABLE 3. COMPLEX WASTES TREATED BY SUPERCRITICAL WATER OXIDATION^a

Adumbran	Human Waste (black and gray water)
<i>Bacillus stearothermophilus</i>	Ion Exchange Resins
(Heat-Resistant Spores)	(Styrene-Divinyl Benzene)
Bran Cereal	Malaria Antigen
Carbohydrates	Olive Oil
Casein	Paper
Cellulosics	Protein
Coal	Sewage Sludge
Coal Waste	Soybean Plants
Corn Starch	<i>Sulfolobus acidocaldarius</i>
Diesel Fuel	Surfactants
<i>E. coli</i>	Transformer Oil
Endotoxin (Pyrogen)	Yeast

^a(References. 1-6).

5. Comparison to Other Technology: Projected Performance

Compared to other available technologies, supercritical water oxidation is applicable to a broader range of waste types. It can be used to treat pure organics, contaminated soils and water, sludges, and some inorganics. It appears to be economically competitive with other technologies used for aqueous wastes containing 1 to 20 percent organic matter. Since the SCWO process is completely contained, emissions can be controlled and, at present, public concern should not delay obtaining operating permits. The complexity of the technology is comparable to incineration, so with proper engineering and process controls, qualified technicians should be able to operate and maintain an SCWO unit.

Incineration is a nonspecific alternate method for destroying organic materials. Incineration can be operated at a relatively low cost, but requirements for extensive emission controls and difficulties associated with controlling processes and obtaining permits can negate potential advantages. Supercritical water oxidation takes place at a much lower temperature (about 500 °C) than incineration and in a completely contained system. Almost no oxides of nitrogen are expected at these low temperatures, and the effluent is completely contained and controlled. Supercritical water oxidation can be applied to water containing 20 percent or less organic waste. By comparison, incineration is not as cost effective at these concentrations. Cost estimates for developing technologies, such as SCWO at full scale, are inherently uncertain and should be considered cautiously. The cost of SCWO of wastes has been estimated in several studies (References 6-8). For treating a ton of dry organic material, the costs are estimated to be between \$300 and \$600 per ton depending on the size of the SCWO treatment unit (Reference 8).

Other methods under development that may apply to explosive wastes include oxidation by hydrogen peroxide and/or ozone with ultraviolet (UV) radiation, electrochemical oxidation, and oxidation or thermolysis in molten salts. In two-phase systems such as these, concentration gradients across phase boundaries and mass transfer of oxygen limit the rate and extent to which compounds can be completely destroyed. A supercritical fluid is a single phase allowing complete mixing; thus, reaction rates are not diffusion limited. A preliminary cost comparison of these oxidation processes prepared by the Energy and Environmental Analysis Group at Los Alamos National Laboratory estimates the costs for the UV processes for contaminated water at 10 to 100 times less per gallon of water than for SCWO. However, these technologies are limited to low (<1000 ppm) concentrations of organics. Concentrated wastes would need to be diluted. In addition, these methods usually require special pretreatment of the waste water, thereby increasing costs.

6. Regulatory and Public Acceptance of the Technology

The Environmental Protection Agency (EPA) has informally stated that supercritical water oxidation is not considered to be incineration. Thus it will probably be permitted under 40 CFR 264, Part X. If supercritical water oxidation units become an integral part of a manufacturing process, the EPA will not consider the unit to be a treatment facility, implying that wastewater and air discharge permits are sufficient. In a demonstration of SCWO technology in New York State, MODAR Corporation obtained a permit under the New York State Environmental Conservation Law, Article 27, Title 7, Part 360, and approval from the EPA to treat polychlorinated biphenyls (PCBs) under 40 CFR 761.60(e). The waste analysis plan and trial test plan were developed to comply with the Resource Conservation and Recovery Act (RCRA) regulations cited in 40 CFR 265.402(a)(2). A second demonstration by MODAR at a chemical plant in Pennsylvania did not require similar permits (because PCBs were not being treated) and the effluent was sent to the plant's water treatment facility.

Supercritical water oxidation has only recently come to the public's attention. Published essays presenting favorable views of the technology by the New York Times and Associated Press have recently appeared in newspapers nationwide. Negative public opinion is not anticipated.

C. SCOPE

This project seeks to examine the behavior of 13 energetic substrates under conditions of SCWO to provide the DREs of the substrates, to determine the optimum conditions for maximizing the DREs, and to ensure safe operation. These substrates are

- Ammonium perchlorate (AP)
- 1,2,4-Butanetriol trinitrate (BTTN)
- Cyclotrimethylene trinitramine (RDX)
- Cyclotetramethylene tetranitramine (HMX)
- Nitrocellulose (NC)
- Nitroglycerine (NG)
- Nitroguanidine(NQ)
- Nitromethane (NM)
- Nitrogen tetroxide (N₂O₄)

Pentaerythritol tetranitrate (PETN)
2,4,6-Trinitrotoluene (TNT)
Hydrazine (N₂H₄)
1,1-Dimethylhydrazine (UDMH).

Products of destruction are identified and measured. Experimental results are evaluated to determine whether the reaction products are environmentally acceptable. If possible, the overall kinetics of oxidation of the substrates are quantified. Practical issues related to process development have also been explored. Corrosion studies to determine the suitability of various reactor materials are reported. Methods for achieving practical throughput of explosives through a SCWO reactor have been explored, including introducing explosives into the reactor either in a co-solvent or as a water slurry and pretreatment of explosives using base hydrolysis. Many aspects of the SCWO process have been modeled and the results are reported here, from the chemical kinetics of the oxidation reactions to fluid flow, heat transfer and process plant balance. Finally, safety studies have determined the detonation sensitivity characteristics of PEPs in supercritical water systems.

D. REPORT ORGANIZATION

This final report summarizes the progress that has been made reaching the goals of this project. It includes

- Design, construction and operation of SCWO reactors used for explosives,
- Development of experimental procedures for determining DREs, products of destruction from SCWO reactions, and optical *in-situ* probing of SCWO reactions.
- Discussion of DREs and products of reaction for AP, RDX, HMX, NG, NQ, NM, PETN, TNT, N₂H₄, and UDMH,
- Examination of process techniques for introducing high concentrations of PEPs into SCWO reactors,
- Development of kinetic models for elucidating chemical reactions in supercritical fluids,
- Development of equations of state that better describe supercritical fluid properties, and
- Reaction of nitrates with organics in supercritical water.

To keep the size of this report manageable, the results of hundreds of experiments have been analyzed and summarized in the 52 tables presented in the following sections.

SECTION II

EXPERIMENTAL APPROACH

This section describes the reactors used to destroy high-energy materials through supercritical fluid oxidation/reduction processes, and the analytical methods used to measure product species. We have constructed, tested, and operated two linear flow reactors, one of which contains a corrosion-resistant gold lining, a flow reactor heated in a fluidized sand bath, and microbatch reactors for investigating the energetics of slurries. We will present a generalized description for each of the experimental reactors and the corresponding operational procedures. The specific experimental conditions under which the destruction measurements were performed will be presented in the results and discussion sections. The optical techniques, coherent anti-Stokes Raman spectroscopy (CARS) and normal Raman spectroscopy, to be used as probes of reaction kinetics, will also be discussed in these sections.

A. LINEAR REACTORS

Bench-scale linear flow reactors have been developed to destroy explosives in supercritical water. A schematic of the linear reactors is shown in Figure 3; a photograph is shown in Figure 4. Solutions of oxidizer and/or explosive are introduced at high pressure into the reactor by constant-flow, high-performance liquid chromatography (HPLC) (LDC Analytical, Constametric 3200) pumps. The explosives are typically in water at less than half their solubility limit or decomposed in water as the result of prior hydrolysis reactions. Check valves are placed in each line to prevent backstreaming in case of pump failure. Fuel and oxidizer are either premixed before being pumped or are introduced separately. In either case, mixing is completed before reaching the heated section of the reactor. The central core of the reactor is heated to a controlled temperature by six heaters in parallel consisting of hollow brass tubes wrapped with MgO₂-insulated Nichrome® wire. The temperature is maintained by regulating the current through the heating wire with Omega CN9000 series microprocessor temperature controllers. The temperature of each of these heaters can be varied independently; however, for all experiments described in this report the temperature of each heated section was kept the same. The temperature is monitored with six K-type (chromel-nickel), sheathed thermocouples in close proximity to the reactor core. A water-cooled heat exchanger at the exit cools the reacted mixture to room temperature. The cooled effluent is passed through a 7- μ m filter for removal of any particulate matter before reducing the pressure to ambient with a let-down valve.

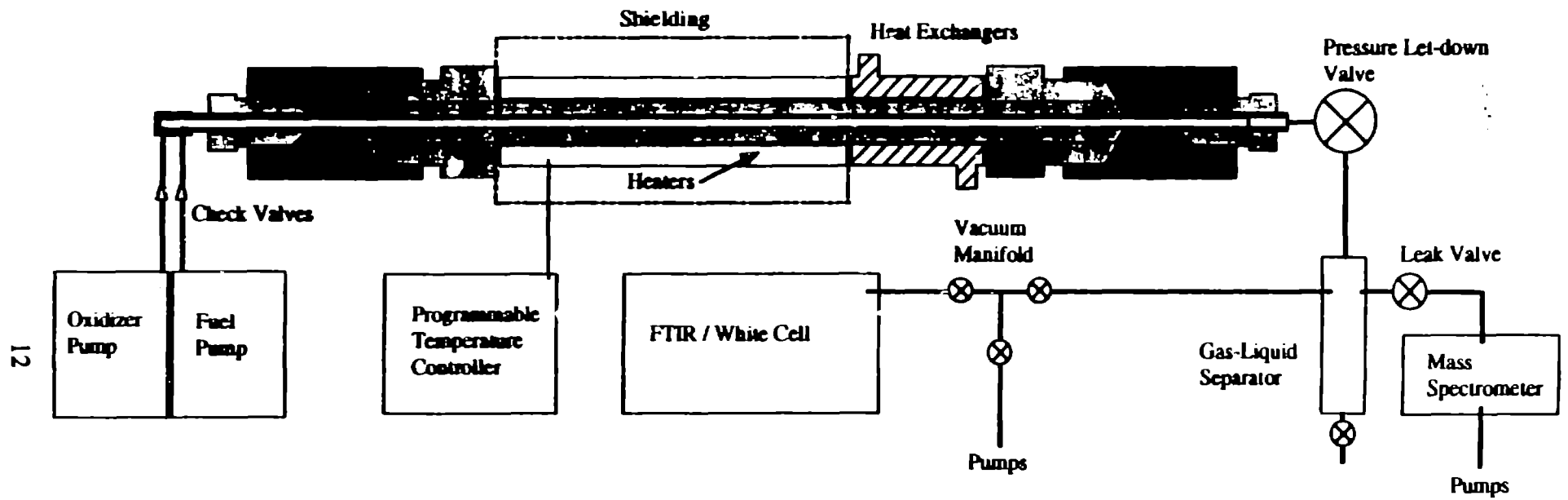


Figure 3. Schematic of linear flow reactor coupled to gas-liquid separator, pumping manifold, and pathways to gas analyses.



Figure 4: Photograph of the Linear Reactor

Gas and liquid effluents at ambient temperature and pressure then enter a gas-liquid separator (Figures 5, 6). The liquid effluent is removed from the bottom for *ex-situ* quantitative analysis as described in Section II.H.2, while the gas-phase products are expanded into a multipass White cell and analyzed with a Perkin-Elmer 1760-X Fourier-transform infrared (FTIR) spectrometer. A small portion of the gas also passes through a leak valve into a UTI quadrupole mass spectrometer for measurement of the gases N₂, O₂, and H₂.

The high-temperature portion of one of our linear reactors is constructed out of C-276, a nickel alloy. The C-276 alloy was chosen because of its known strength and resistance to corrosion at high temperatures. Even so, under some reaction conditions we have seen considerable corrosion. To overcome this problem, a second reactor was constructed containing a 316 stainless steel sheath with a gold liner (Figure 7). A seal was made with the gold liner by flaring one end of the gold tube and compressing it between tapered high-pressure fittings. The liner is open at the exit of the reactor, creating a static supercritical region between the liner and stainless core. The gold liner protects all high-temperature sections of the reactor. All "taper seal" high-pressure fittings, and most other components obtained from High Pressure Equipment Co., are manufactured from 316 stainless steel and rated to a minimum of 4080 atm. Table 4 compares the composition of 316 stainless steel, C-276, and Inconel 625 alloys.

TABLE 4. COMPOSITION OF REACTOR MATERIALS

	Ni%	Cr%	Mo%	Fe%	W%	Co%	Mn%	C%	Si%	Other%
C-276	59.5-	14.5-	15.0-	4.0-	3.0-	2.5	1.0	0.01	0.08	.048
	51.0	16.5	17.0	7.0	4.5					
Stainless Steel 316	10.0-	16.0-	2.0-	61.8-	---	---	2.0	0.08	1.0	.075
	14.0	18.0	3.0	68.8						
Inconel 625	62	21.5	9.0	5.0	---	---	---	0.1	0.5	1.9

The C-276 reactor core is 64 in. long by 0.083 in. inside diameter (id) (1.6 meters x 0.33 millimeter), and the gold-lined stainless steel reactor is 55 in. x 0.103 in. (1.4 meters x 0.04 millimeter). These dimensions provide a heated volume of 5.7 mL and 7.4 mL, respectively. Using an empirical equation of state for supercritical water (Reference 9), we estimate a residence time of 5-150 seconds, depending on flow rate (typically 1-8 grams/minute) and temperature (400-600 °C) at a pressure of 340 atm. At higher temperatures, the density of water drops significantly, decreasing residence times. Figure 8 shows the results of an experiment to characterize

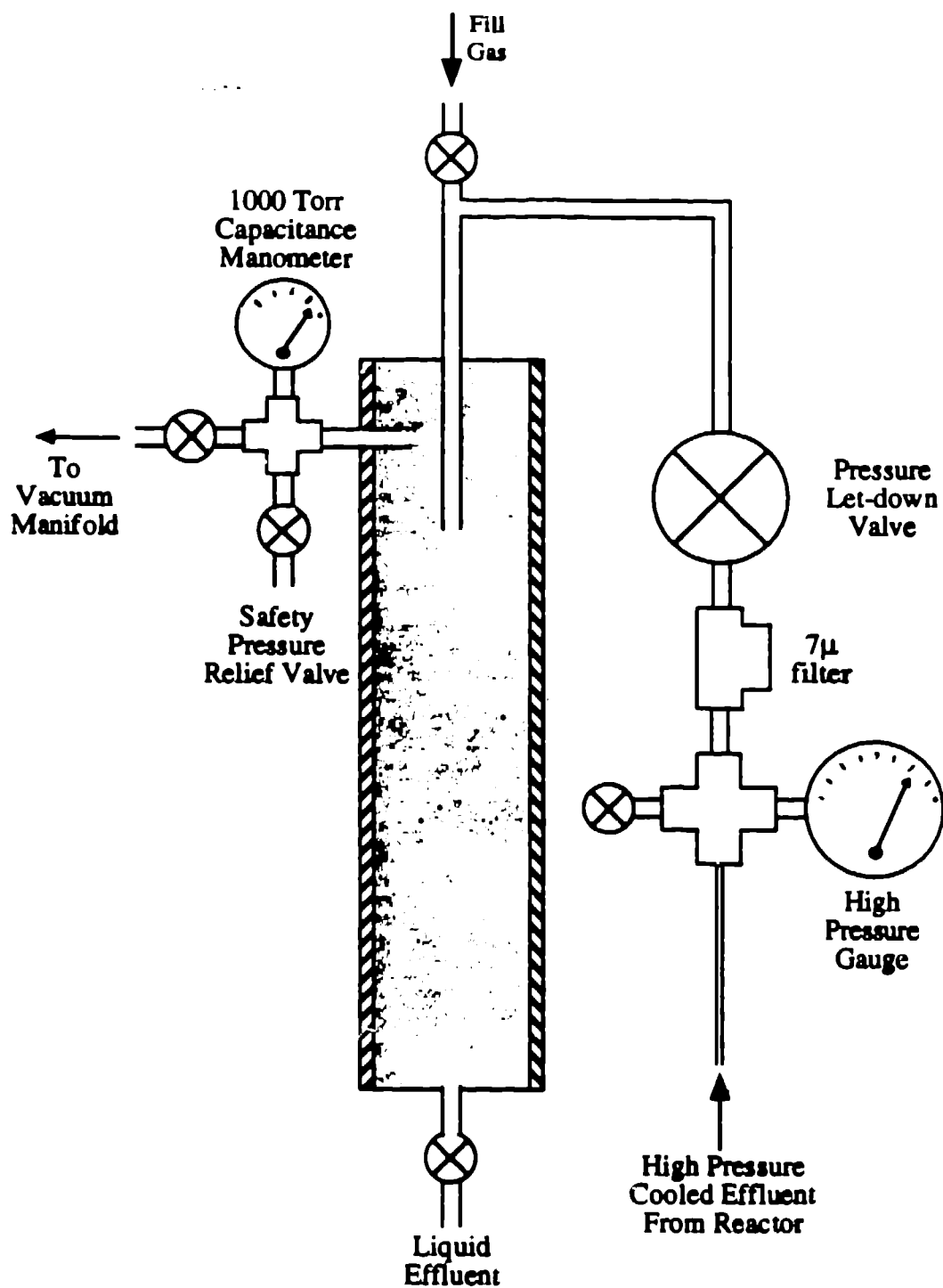


Figure 5. Detailed diagram of the gas-liquid separator. Cooled effluent is passed through a filter before pressure let-down. System is then pressurized with a buffer gas, and gaseous effluent is expanded into the White cell and mass spectrometer leak valve. The liquid effluent is removed through bottom valve.



Figure 6 Photograph of the Gas-Liquid Separator

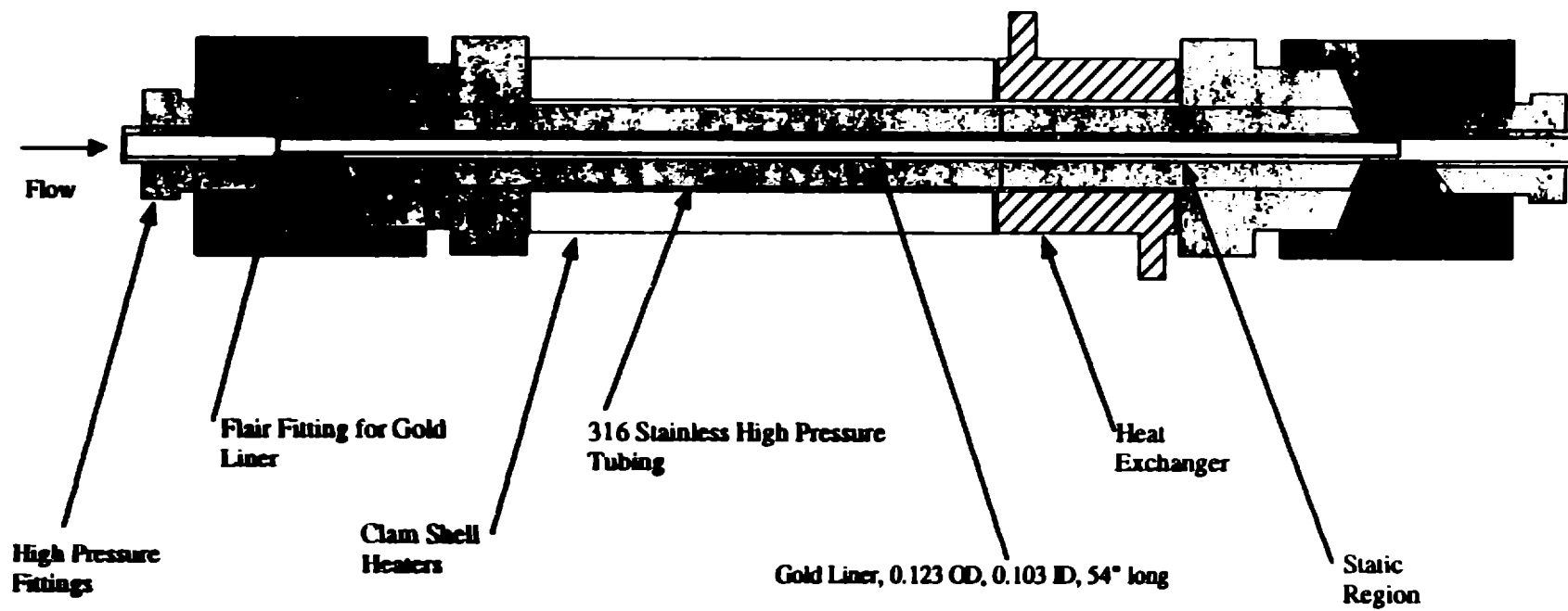


Figure 7. Detailed diagram of gold-lined reactor. The drawing is not to scale.

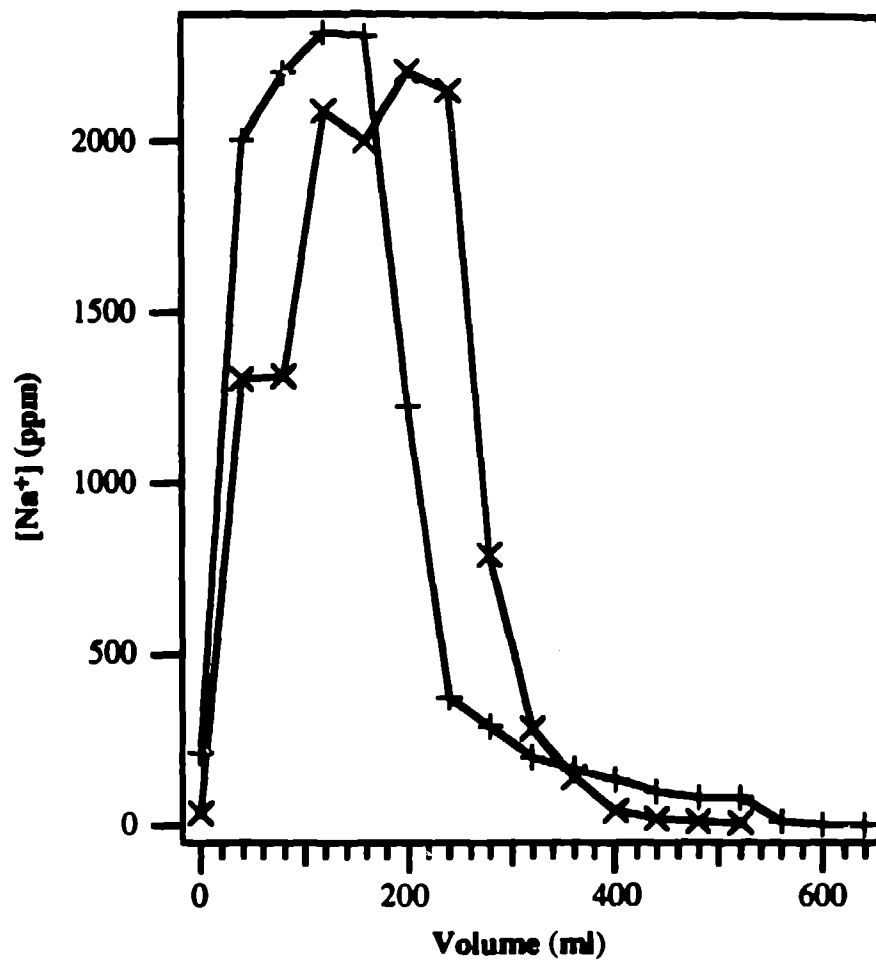


Figure 8. Sodium concentration versus volume flowed through reactor for a 200 ml aliquot of 2500 ppm NaCl solution at (x) room temperature and (+) 600 °C.

the flow through the linear reactors. A fixed volume (200 mL) of NaCl solution (2500 ppm) was pumped through the reactor at a rate of 4 mL/minute at room temperature and at 600 °C. Samples were collected every 10 minutes. The sodium ion concentration was measured by atomic absorption spectroscopy. The room-temperature trace in Figure 8 appears broader, which is typical of laminar flow with substantial axial diffusion. The narrower 600 °C trace indicates that the flow is becoming more plug-like. Most of the broadening in the high-temperature run is probably occurring in the cool regions of the reactor. However, since this reactor is not used for kinetics studies, completely developed plug flow is not critical.

Typical experiments begin by flowing deionized water through the reactor as it is brought up to temperature (400 - 600 °C). The deionized water is exchanged for solutions of explosive and/or oxidant mixtures. Aliquots of liquid effluent, including the flush, are collected continuously until the experiment is complete. The reactor is then rinsed with deionized water and the rinse effluent is also collected for analysis. Liquid effluent is analyzed for any residual explosives, inorganic and organic constituents, and corrosion products. The tracer studies suggest that for experiments with constituents that remain soluble, the volume of effluent analyzed will be only slightly greater than the volume injected into the reactor due to a slight dilution. However, if reaction products precipitate out of the SCW phase, they may appear in the effluent during the cool-down or flushing phase (see below). The gas effluent is allowed to accumulate in the gas/liquid separator until pressures between 10-200 torr above the water vapor pressure are reached. This volume of gas is expanded into the White cell of the FTIR and pressurized to 600 torr with He for reasons discussed in Section II.H.1.a.

B. FLUIDIZED SAND BATH REACTOR

For experiments measuring the kinetics of reactions, a coiled, tubular reactor in a fluidized sand bath was used. Figure 9 shows a schematic and Figure 10 shows a photograph of the fluidized sand bath reactor used to examine the kinetics of reactions in supercritical water. Thus far the reactor has been used primarily for the study of nitrate reactions. The reactor consists of two preheater tubes, each having a volume of 7 mL, which combine at reaction temperature in a mixing tee. The reactor tube (a C-276 alloy, 6.35 millimeters outside diameter (od) x 2.12-millimeters id, volume of 13.1 mL) leads from the mixing tee to a chilled water heat exchanger. Seven thermocouples are used to monitor surface temperatures on the preheaters and the reactor. Thermocouples are in contact with the fluid at the mixing tee and after the chilled water heat exchanger. Temperature profiles indicated the reactor tubing is isothermal to within 1 °C at reaction temperatures (450 °C to 525 °C).

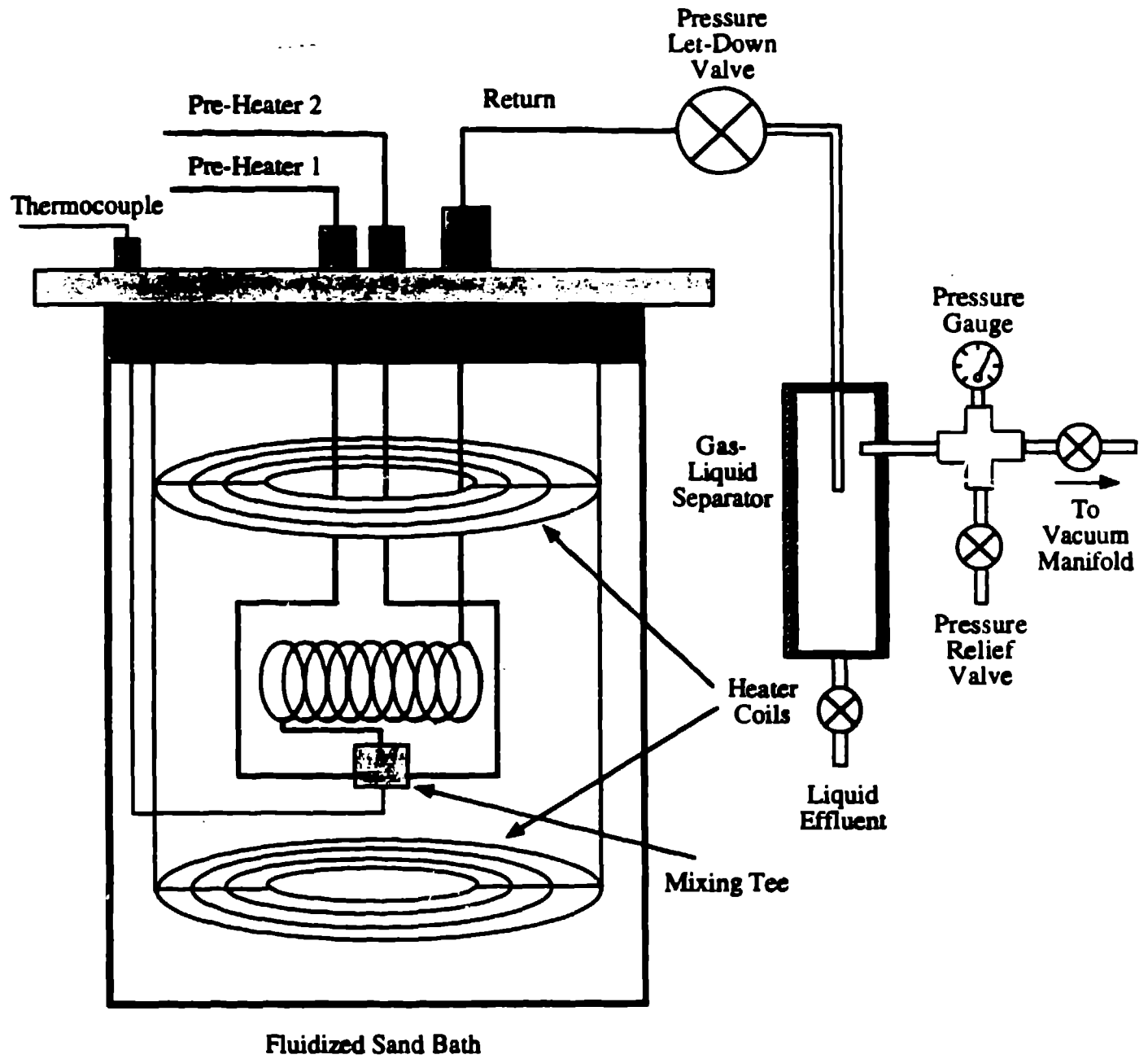


Figure 9. Schematic of sand bath reactor coupled to the gas-liquid separator.



Figure 10: Photograph of the Sand Bath Reactor

The reaction quench is rapid, occurring within 0.25 mL of tubing. The reactor is operated in ranges where Reynolds numbers (> 2100) indicate that flow should be turbulent. Two HPLC pumps provide flow rates up to 10 mL/minute for the oxidant and organic feed solutions. Experiments are started by circulating deionized water through the apparatus at the desired experimental pressure. While the deionized water circulates, the fluidized sand bath is brought to temperature using its internal and auxiliary heaters. The internal heaters are controlled with a feedback controller, while auxiliary heaters are controlled with a variable transformer. When the desired experimental temperature is reached, the water feed streams are changed to oxidant and fuel feed solutions. A stopwatch marks this time. After 20-30 minutes, effluent sampling is initiated. When sampling is completed at one residence time, pump flow rates are adjusted to provide a new residence time. At the new residence time, the system is allowed to equilibrate for 20-30 minutes, and sampling at the new residence time is initiated. At each temperature and residence time, feed and total flow rates are measured. When all experiments are completed, the heaters to the fluidized sand bath are turned off, and a continuously recycled water rinse of the apparatus is started. This water rinse serves to collect water-soluble species that adhered to apparatus walls. Water rinses are conducted for 12-16 hours.

For all temperatures and residence times, three sets of four liquid samples are collected for analyses. One sample is used for pH measurement, while the others are analyzed for aqueous nitrogen and carbon species and corrosion products. Gas samples are collected for analysis by gas chromatography (GC) and Fourier transform infrared (FTIR) spectroscopy. Ion chromatography is used to measure nitrite and nitrate concentrations. An ion-specific electrode is used to determine ammonia concentrations. Metal concentrations (Cr, Na, Mo, Fe, Ni) are measured by atomic absorption (AA) spectrophotometry, while gas chromatography is used to determine methanol concentrations.

C. BATCH REACTOR

Two microbatch reactors are used for investigation of the dissolution of solid explosives and propellants in water during the transition through the critical point (Figures 11, 12). Although numerous designs were considered and tested, the two designs that proved most useful were a constant-volume reactor and an optically accessible reactor. These reactors permit the introduction of a slurry of explosives that can be heated to 600 °C and pressurized to 10,000 psi (680 atm) in a controlled manner. The reactors are made of 316 stainless steel and have a total volume of 200 μ L each. The estimated (and observed) pressure rise was far below the maximum rating. For safety purposes, the computer, video monitor, and all experimental personnel can be located remotely

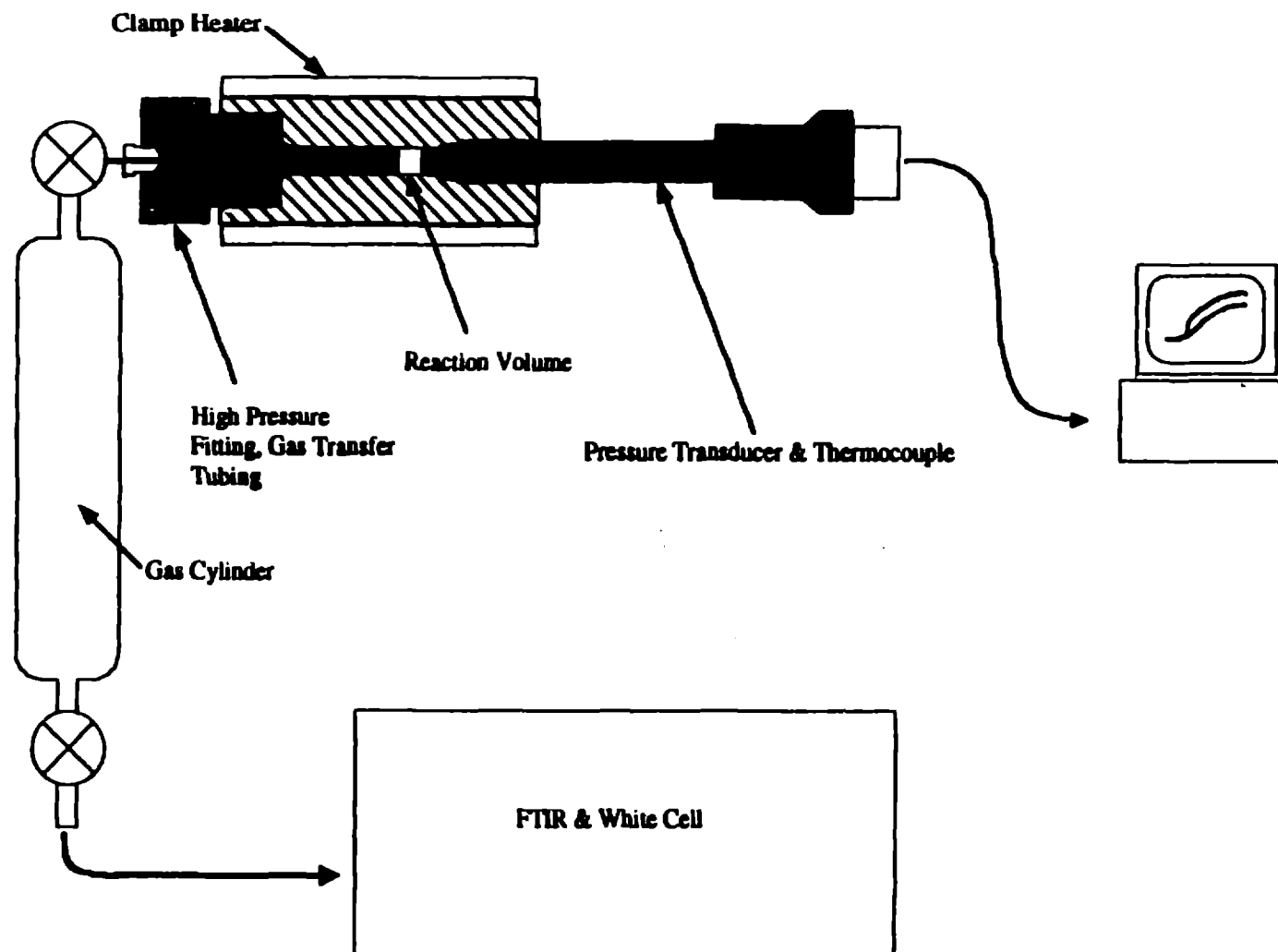


Figure 11. Schematic of the batch reactor experimental setup. The reaction volume used was 200 μl , but can be varied up to 2 ml. After completing the experiment, the reactor volume is expanded into the evacuated gas cylinder for subsequent analyses by FTIR.



Figure 12: Photograph of the Batch Reactor

behind a protective barrier. Kevlar® shielding was also used to cover the reactor area during experiments.

The optically accessible reactor allows visual inspection of the slurry as the reactor is slowly brought up to temperature and pressure and also provides the potential for the spectroscopic monitoring of SCW reactions and the dissolution of explosives. This design features two opposing diamond windows that permit backlighting of the sample and observation through the opposite window. The cell is pressurized with a pressure intensifier using water as the pressure-coupling fluid. A high-resolution CCD camera is used to visually monitor the reactor interior.

Both cells are heated using nickel-chromium wire and a Variac® connected to line current. The temperature is measured with a K-type thermocouple placed directly in the reaction volume and pressure is monitored with a Heise pressure gauge. The pressure and temperature data are recorded on a Macintosh® computer. Gas products are expanded into a stainless cylinder and examined by FTIR spectroscopy using procedures described in Section II.H.1.a.

D. TRANSPORTABLE WASTE DESTRUCTION UNIT

The largest-capacity SCWO reactor we have used for studying the destruction of explosives is a two-gallon-per-hour transportable waste destruction unit. A schematic of the unit is shown in Figure 13 and a photo is shown in Figure 14. The purpose of this unit is to evaluate process and design issues and to develop an experience base on operability. Although not specifically designed for kinetics studies, it also has that capability. The unit can use oxygen, air, or hydrogen peroxide as the oxidant. It is designed to provide a basic system into which various reactor configurations can be inserted. The basic system uses a supply-and-mixing subsystem to provide a mixed feed for the reactor and a cool-down and pressure let-down subsystem for postprocessing the reactor effluent. Currently, the cool-down/let-down subsystems do not include solids-handling components. The unit is designed to meet or exceed ASME mechanical standards and allows all critical operations to be carried out remotely. The system fits on a framework that is roughly 5 ft. x 12 ft. x 4 ft. high (1.6 meters x 3.7 meters x 1.3 meters), and it can be picked up as a unit and transported on a truck or trailer. For initial testing with high concentrations of explosives, this feature will allow the unit to be located at an explosives firing site. The total height of the unit varies with the reactor, which is mounted on the top of the 4-foot high framework. The external supplies required are 120 volts AC and 220 volts AC three-phase electrical power, 160-psi compressed air, and roughly one gallon per minute of cooling water.

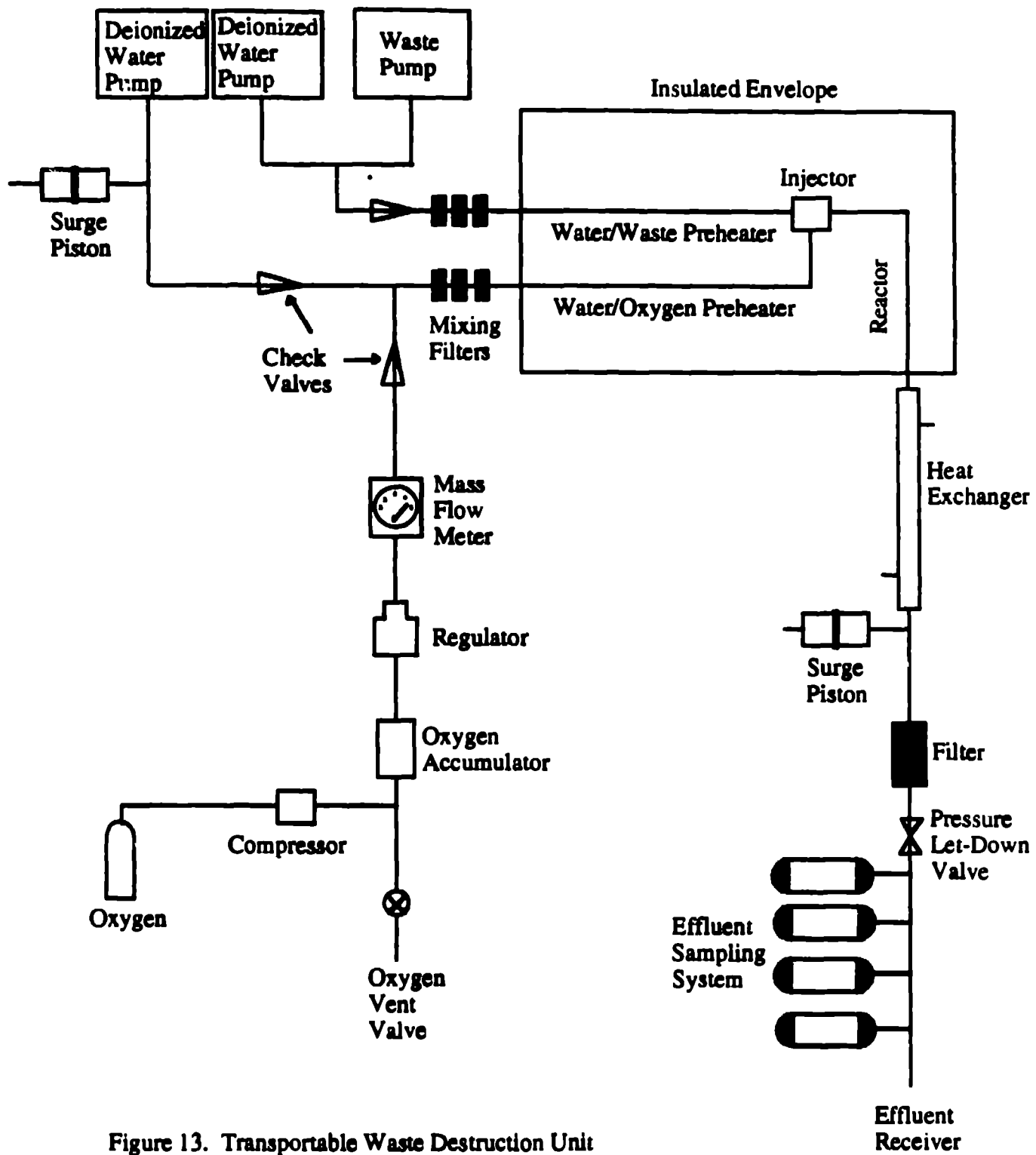


Figure 13. Transportable Waste Destruction Unit



Figure 14: Photograph of the Transportable Waste Destruction Unit

The supply and mixing subsystems include fluid supply reservoirs, pumps to bring the fluids to operating pressure at the desired flow rate, and devices for mixing fluids before they enter the reactor. A 50-gallon supply tank can be used for water or aqueous-waste feed to the system. The feed is pumped to the reactor operating pressure of about 4000 psi by a Milton Roy duplex metering pump. The maximum capacity of this pump is 2.2 gallons/hour, but the nominal operating flow is 1.1 gallons/hour. The duplex pump contains two pistons, operating 180° out of phase to reduce pulsations. There is still, however, a considerable amount of surge in the output. This surge is dampened by piston accumulators on the water line near the pump and just before the let-down valve.

A concentrated organic stream or a stream of dilute explosives can be introduced into the pressurized water line by a separate metering pump. Currently, a Milton Roy HPLC metering pump with a maximum output of 10 mL/minute is used. The waste is injected into the water and passed through a filter to promote mixing. The waste/water stream is then heated before being combined with the oxidizer.

Oxygen is supplied from standard 2000-psi bottles located on the rig. The oxygen is regulated to 1500 psi and is fed into a Haskel double-acting two-stage gas booster, in which it is compressed to the operating pressure of about 4500 psi. Oxygen from the booster is collected in a 2-liter reservoir. A high-pressure regulator controls the oxygen pressure at 4300 psi, with a variation of 20 to 50 psi. A Linde mass flow meter is used to measure the oxygen flow rate. The output from this meter is used by the data acquisition system to control the oxygen flow via a pneumatically actuated control valve. After going through a check valve, the oxygen is injected into a water stream and is passed through a filter for further mixing. The oxygen/water stream is then heated before it is mixed with the waste.

The present reactor is made from welded Inconel 625 tubing, 0.188 in. (0.13 millimeter) id by 0.308 in. (1.03 millimeter) od. The desired operating temperature of the mixed fluids is achieved by direct electrical resistance heating of two separate 12-ft. (4-meter) preheaters. For each preheater, the heating is done in two parallel electrical circuits. Electrical power is provided to each preheater by separate Hewlett Packard 6469-C DC power supplies rated at maximum current of 300 amps at a maximum voltage of 36 volts. The flows from the waste/water and oxygen/water preheaters are combined. Oxidation occurs in a 6-ft. (2-meter) insulated tube (Inconel 625, 0.188 in. id by 0.308 in. od) following the mixing region. Thirty-five thermocouples are attached to the outside of the preheaters and reactor to measure surface temperatures.

After leaving the reactor, the process stream is cooled using a single-pass, counterflow, coaxial-tube heat exchanger. The cooled effluent passes through a single let-down valve, where its pressure is reduced to atmospheric. The let-down valve controls the reactor operating pressure. After the let-down valve, the effluent enters an array of sampling bottles. The entire flow can be diverted to a given bottle for a period of time. The sampling valves are controlled remotely. When the effluent is not being sampled, it passes into a product tank.

Data acquisition, control, and monitoring are accomplished with a Hewlett Packard 3852A data acquisition and control unit and a Macintosh IIfx desktop computer. A digital voltmeter, three 20-channel multiplexers (scanners), a 4-channel digital-to-analog converter (DAC), and a 10-relay actuator are used for data acquisition and control. The DAC channels provide continuous control of the two control valves (oxygen flow and pressure let-down) and the two DC power supplies. The scanners are used to sample the voltages from the pressure transducers, thermocouples, oxygen flow meter, power supplies and two power supply current-shunt voltages. During a test all data are recorded and displayed. If needed, the data from a test can be replayed at a later time.

A more complete description of a similar version of this reactor can be found in Los Alamos report number LA-12216-MS.

E. ONE-GALLON PER HOUR REACTOR SYSTEM

The one-gallon per hour (1 gph) reactor system is a continuous-flow system with a tubular reactor. The system consists of a waste/water feed and pressurization sub system, an oxygen feed and pressurization subsystem, a preheater/reactor subsystem, a cooling subsystem, and a pressure letdown and sampling subsystem. For monitoring and control of the system there is a remote data acquisition and control (DA&C) system. A photograph of the entire system is shown in Figure 15.

The waste/water feed and pressurization subsystem consists of a pair of 6-gallon plastic feed tanks with a remotely-actuated switching valve between them, a feed pump, and a pulsation



Figure 15: Photograph of 1 gallon per hour unit

dampener. A photograph of this subsystem is shown in Figure 16. In operation one feed tank contains pure deionized water and the other contains a slurry of explosive (or explosive simulant) in water. A recirculating pump is provided for the slurry tank to keep solids from settling out on the tank bottom. The switching valve is used to select feed from one or the other feed tank as desired. This valve is an electric-motor-driven three-way Parker ball valve. The pressurizing feed pump is an American Lewa diaphragm pump capable of delivering up to 2 gallons per hour of liquid at pressures to 5500 psia. The pump is driven by a 220 Vac, three-phase electric motor, which is remotely actuated using a 110 Vac relay. Pump capacity control is accomplished with a manual stroke adjustment, although a remotely-controlled stroke actuator is available. The surge suppresser is a cylindrical accumulator with a floating piston. One end of the accumulator is attached to the process fluid downstream of the main feed pump, and the other end is charged with a trapped volume of nitrogen. The gas end is charged to about one-half of anticipated system operating pressure when there is no system pressure and is then valved off so that the piston is roughly in the mid position during operation. The system is essentially undamped until the system pressure reaches the nitrogen charging pressure. All fittings and lines between the pump and the preheater are high-pressure rated 316 stainless steel components. The lines are 0.250 in. od by 0.083 in. id and are kept as short and straight as possible to prevent appreciable accumulation of solids.

The oxygen supply and pressurization system consists of a bank of conventional 2200 psi oxygen bottles with regulator, a remotely-actuated oxygen supply shutoff valve, an oxygen compressor, an oxygen accumulator, an oxygen feed shutoff valve, an oxygen feed pressure regulator, an oxygen flow meter, an oxygen flow control valve and a check valve. A photograph of this subsystem is shown in Figure 17. Oxygen feed pressure is supplied by a double-acting, two stage, intercooled Haskel Gas Booster, which can boost the oxygen from bottle pressures as low as 200 psi up to 4500 psi at flow rates of 20 slm (standard liters per minute) or more. Typical oxygen flow rates in operation are 5-10 slm. The gas booster is driven by compressed nitrogen gas from a standard 50,000 scf trailer, but any clean compressed air or nitrogen of about 100 psig or higher can be used. In operation, the oxygen supply pressure is not allowed to drop below about 1100 psia to prevent excessive use of drive gas. The booster is equipped with a pilot valve which turns the booster on when the outlet pressure drops below 4350 psia and turns it off when the outlet pressure goes above 4500 psia. These limits are adjustable, but it is difficult to reduce the "deadband" below this 150 psi level. Since it is not feasible to obtain a steady flow from the booster, a 2-liter oxygen accumulator is provided at the booster exit. This capacity results in booster operation about every 3-5 minutes for nominal oxygen flow rates.



Figure 16: Photograph of waste-water feed and pressurization subsystem

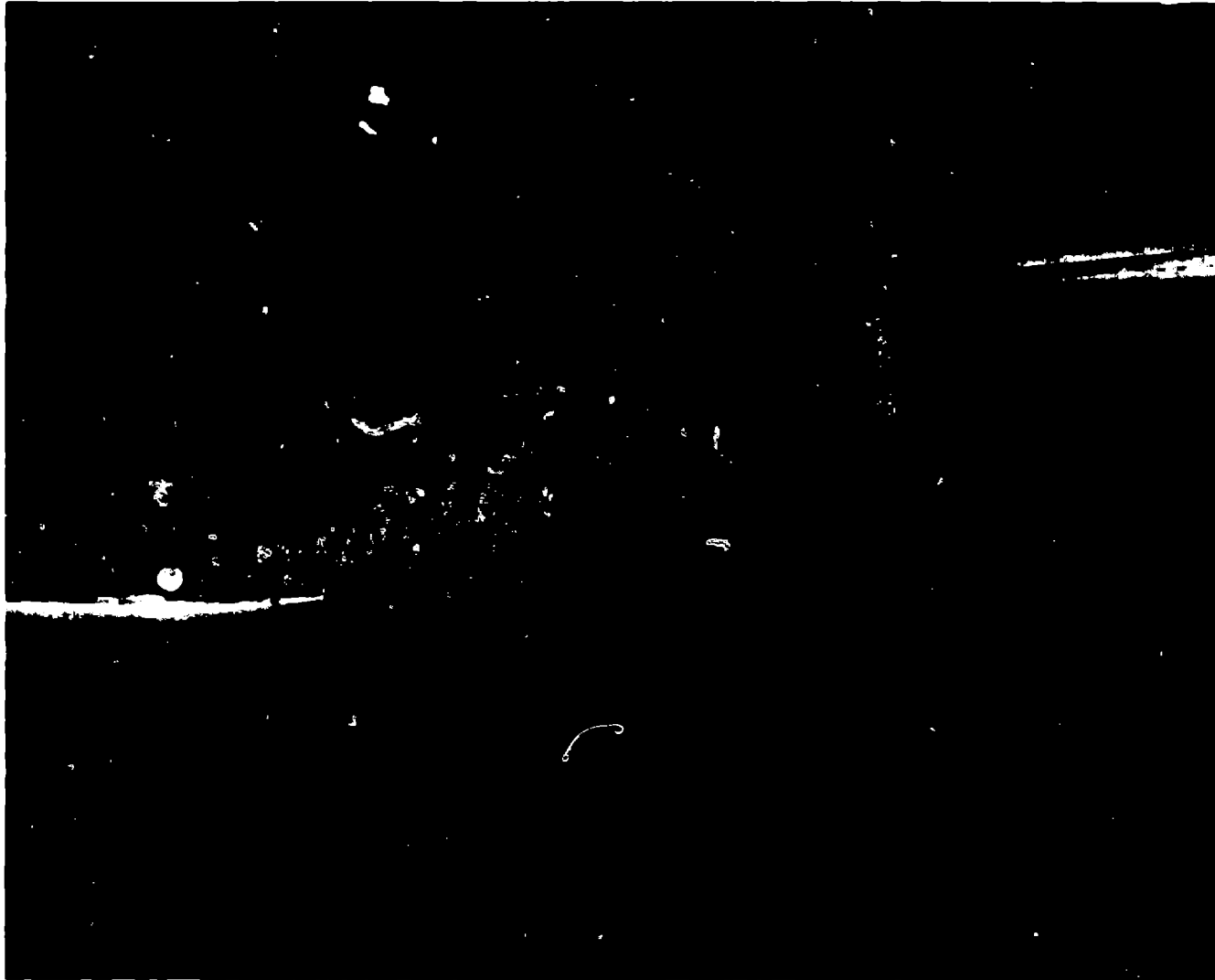


Figure 17: Photograph of oxygen supply and pressurization subsystem

Booster operation results in a rapid increase in accumulator pressure from 4350 psia to 4500 psia followed by a slow decay in pressure back to 4350 psia. Since this rapid increase in oxygen pressure would make oxygen flow control difficult, a Tescom pressure regulator is provided downstream of the accumulator to even out the oxygen pressure. Ideally, the regulator could keep the pressure at a steady 4350 psia. Experience has shown that we must keep the regulator outlet pressure at or below about 4100 psi to avoid excessive pressure pulses at the flow control valve when the booster operates. At this setting the pressure pulses are 40 psi or less. The regulator is provided with an automatic controller that uses the output from a pressure transducer just downstream of the regulator. This signal is compared to an outlet pressure setpoint signal sent by the DA&C system. Following the regulator are a Linde mass flow meter and a Research Control pneumatically-actuated flow control valve with a Moore Products I/P transducer. Oxygen flow control is accomplished by a 4-20 mA signal sent from the DA&C system, which is converted to a proportional 3-15 psi pneumatic signal to the valve by the I/P transducer. The signal from the DA&C system can either be set "manually" at the control panel or (more usually) will be determined "automatically" using the difference between the flow rate measured by the mass flow meter and a setpoint value set on the control panel. Downstream of the control valve the oxygen is fed through a check valve into the waste/water stream. Oxygen flow control is therefore affected by the system pressure as well as the oxygen feed pressure. For this reason it is desirable to keep a reasonable pressure drop across the oxygen flow control valve - about 400 psi in this case. All lines and fittings in the oxygen feed subsystem are high-pressure-rated 316 stainless steel.

Maximum system operating pressure is generally limited by the maximum *allowable* oxygen pressure, which is 5000 psi. Haskel (for one) recommends against the use of pure oxygen at pressures above 5000 psi even with an "oxygen clean" system such as this one. This means that the maximum *operating* pressure should be no higher than 4500 psi. The required pressure drops through the pressure regulator and the flow control valve dictate a maximum system pressure of about 3700 psia.

The primary feature of the preheater/reactor subsystem is a straight Inconel 625 tube, 19 ft long by 0.308 in. od by 0.188 in. id. This tube serves as both the preheater and reactor sections of the subsystem. In the preheater section (the first 8 ft of the tube) the tube is spiral-wrapped with 9 Watlow cable heaters, each 95 in. long by 0.125 in. od, and each capable of producing 1000 W of heating at 220 V. This is actually a tighter wrapping (0.308 in. id) than is recommended for these heaters, but this has so far caused no problems. The heater power is controlled by a 220 Vac, three-phase SCR power controller wired in a delta configuration with 3 heaters, wired in parallel with each other, on each of the three legs. Proportional power control is provided by a 0-10 V

signal from the DA&C system. This signal can be set either manually at the DA&C system control panel, or automatically using the difference between a measured maximum preheater temperature and a setpoint temperature set on the control panel. The purpose of the preheater is to bring the mixture of water, waste and oxygen to operating temperature. The maximum operating temperature for this system is 650 °C (1200 °F). Of course, since all of the reactants are premixed, some, if not most, of the reaction will occur in the preheater. The "reactor" section (the last 11 ft of tube) is wrapped with low-power strip heaters to offset heat loss through the insulation. This is an attempt to keep the reactor section as near to isothermal as possible and to obtain a residence time at temperature. These heaters are controlled by another SCR power controller in a manner similar to the preheater, but use much less power. Roughly 30 thermocouples are attached to the outside of the preheater/reactor tube with glass tape. These thermocouples are used for power control and for display. A real-time plot of temperature vs. distance along the preheater/reactor is displayed on the control panel. The preheater/reactor tube and heaters are placed inside a concentric 10 in. od by 0.250 in. wall aluminum tube and Saffil® alumina-fiber insulation is lightly packed into the intervening space. The aluminum tube has been split longitudinally for installation of the tube, heaters and insulation, and is held together with steel bands.

Cooldown of the process fluid is accomplished by putting a concentric 316 stainless steel cooling jacket around a 6-ft. extension of the Inconel 625 preheater/reactor tube. The total preheater/reactor/cooler length is 25 ft., all enclosed in the 10 in. aluminum tube. Water, with ethylene glycol added as a rust inhibitor, is circulated through the cooling jacket annulus counter-current to the process flow. The water is then circulated through an industrial water-to-air forced-convection heat exchanger (actually an air heater) and back to the cooling jacket using a low-pressure 5 gpm centrifugal water pump.

After going through the cooler the process fluid passes through a Research Control valve to drop and control the system pressure. A photograph of this subsystem is shown in Figure 18. This valve is similar to the oxygen flow control valve, and has an attached I/P transducer to transform the electronic control signal into a proportional pneumatic signal for valve actuation. The 4-20 mA signal from the DA&C system to the I/P transducer may either be set on the DA&C system control panel manually, or it may be set automatically by the control program using the difference between the system pressure, measured by a transducer just upstream of the control valve, and a setpoint pressure set on the control panel. In the low-pressure, low-temperature line downstream of the control valve are several remotely-actuated three-way ball valves used for



Figure 18: Photograph of pressure control subsystem

sampling. These valves are plumbed in series so that, in normal operation, all of the process effluent passes through all of the valves before going into the catch tank. When a sample of the effluent is desired, one of the ball valves is switched and the entire effluent flow is diverted to an attached sample bottle for a period of time. The effluent contains dissolved gas due to excess oxygen in the feed and gas production during processing, so the period of sampling must be limited. For the standard 300 cc sample containers and a flow rate of 1 gph, the sampling period should be limited to about 2 minutes to prevent significant buildup of pressure in the sampling system.

The heart of the DA&C system is a Mac II fx computer running a LabVIEW®-based DA&C program written specifically for this application. A photograph of the DA&C subsystem is shown in Figure 19. The computer is mated to a Hewlett-Packard HP-3852A DA&C Unit via a GPIB interface bus. The HP-3852A has a voltmeter board; three 20-channel analog-to-digital multiplexer ("scanner") boards for monitoring of temperatures, pressures, flow rates, voltages, etc.; two four-channel digital-to-analog (DAC) boards for sending control signals to the various control devices (I/P transducers, power controllers, etc.). The DAC channels may be configured to send either 4-20 mA or 0-10 Vdc. An eight-channel relay actuator board is also available for computer-controlled on/off functions, although it is not used at present.

The DA&C program is run on a 5-second cycle. In each cycle raw voltage data is read in from the scanners; converted to "engineering" units using predetermined calibration factors (the scanner boards are capable of automatically converting thermocouple mV values to temperature values); and logged in a random access data file. On specified data channels the measured value is checked against specified high and low limits, and if the channel is out of limits the reactor is shut down. Computer-controlled shutdown consists of zeroing the preheater power, fully opening the pressure letdown control valve and fully closing the oxygen flow control valve. Control DAC values are generated for the two power controllers, the pressure letdown and oxygen flow control valves and the oxygen pressure regulator. In case the pump stroke adjustment drive is installed, this will also require a DAC control signal. The values of the DAC signals to be sent can be set on the control program front panel or can be determined in a control subprogram by comparing the value of a control channel measurement with a setpoint value specified on the control program front panel. The latter method is referred to as "automatic" control, and is optionally available for operation of the two power controllers and the two control valves. For the power controllers and the pressure letdown control valve a proportional-derivative control scheme is used at present, and for the oxygen flow control valve proportional-only control is used. These control subprograms

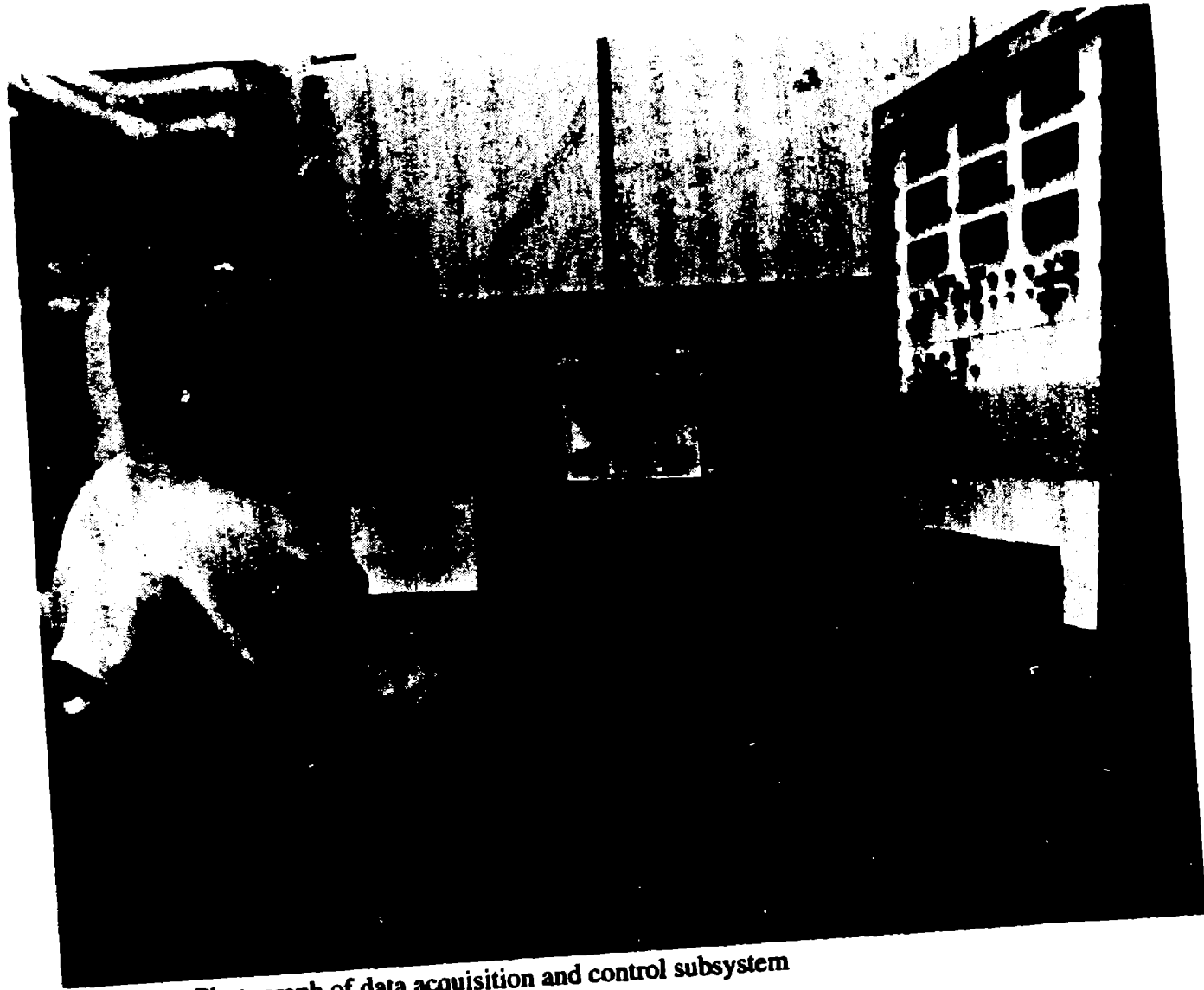


Figure 19: Photograph of data acquisition and control subsystem

were "home-built" and PID control subprograms are now available from National Instruments (makers of LabVIEW).

Besides the control settings and switches, measured and converted data are also displayed for on-line monitoring. These displays include an X-Y plot of reactor tube wall temperature versus distance along the preheater/reactor and strip charts of value-versus time for various data channels, all updated each scanning cycle (i.e., every 5 sec). The channels displayed on the strip charts are varied, but typically include the system pressures, oxygen flow rate, some measure of preheater power, specific (or maximum) reactor temperatures, and/or some DAC signal values.

F. BASE HYDROLYSIS

All chemicals used were of reagent grade. Base solutions were prepared with deionized water. The volume and concentration of base solution were dependent on the material being hydrolyzed. In general, an excess of base was used over that required to match the molar equivalents of nitro groups in the material. Reactions of sodium hydroxide with energetic materials were normally performed in an open beaker or in a flask fitted with a condenser. When open beakers were used, evaporated water was replaced as needed. When analysis of the gaseous hydrolysis products was desired, the reaction was performed in a stainless steel pressure vessel rated to 1000 psi. Hydrolysis reactions with aqueous ammonia were also performed in a sealed pressure vessel. In all cases, an appropriate blast shield was employed during the hydrolysis. Reactions were usually done at the boiling point of the solution, approximately 93°C at Los Alamos elevation. In some cases, a temperature controller was used to obtain a constant temperature below or above (pressure vessel) the solution boiling point. Hydrolysis reactions were considered complete when solid material and gas evolution were no longer visible in the mixture. Runs in the sealed pressure vessel were terminated when the gas pressure leveled off. For some reactions foaming was found to be a problem and was counteracted with an antifoam agent, Hercules Defoamer #4.

G. OPTICAL EXPERIMENTS

1. Raman Spectroscopy

While end product analyses of effluents from our flow reactors allow more comprehensive analysis of products and precise assessment of process efficiency, the use of optical spectroscopic methods allows one to probe reactions *in situ*, and can yield additional insight

into chemical interactions. We report here the use of *in situ* Raman spectroscopy to monitor reactants, products and reaction rates of energetic materials at supercritical and near-critical conditions. Raman spectroscopy is a versatile diagnostic tool that measures the vibrational spectrum of a molecule, and has been applied widely in gas, liquid and solid media. Compared to other optical techniques, Raman spectroscopy is well suited to supercritical fluids because it is immune to quenching at high pressures (or densities) and because it allows easy access to broad spectral ranges. Solvated molecules can usually be identified by their distinct Raman shifts.

A number of experimental setups were used, all similar to the one shown in Figure 20. Raman measurements were made with an argon-ion laser source, tuned to 488 nm. The polarization of the laser output is controlled by a double-rhomb, half-wave retarder, then focused with a 20 cm focal length lens, exciting the sample with about 2 W of cw power. Raman scattering is collected at 90° with a collection lens and sent to a three-stage monochromator (Spex Triplemate), where the light is dispersed by a grating with 600 lines/mm and detected with a cooled charge-coupled device (CCD) camera. The CCD is a 516 X 516 pixel array; vertical columns are summed electronically to generate a one-dimensional array for Raman spectra. Signals are collected typically for 30 seconds.

The sample is passed through an optical cell that can withstand high pressures (>600 atm) and high temperatures (600 °C). One of the optical cell designs used is shown in Figure 21 and a photograph in Figure 22. This cell is constructed from a 316 stainless steel high-pressure "cross" fitting, machined to accept three diamond windows. Diamond (Type II) was chosen as a window material because of its ability to withstand high pressures and its broad spectral transmission, from the ultra-violet to the infrared. We have also built optical cells using sapphire windows. The diamonds shown in the figure are "anvil-type" windows with flat optical faces providing an aperture of 0.6 mm on the inside and 3 mm on the outside. The high pressure seal is aided by an inert gold gasket between the diamond and the cell wall. Two windows are used to pass the laser beam through the cell, with entrance and exit faces 1.6 mm apart. A third window, oriented at 90° with respect to the laser axis, is used to collect Raman scattered light. By positioning the collection window very close to the laser axis, a collection aperture of $f/2$ is achieved. Another cell was used which included two inlet ports allowing separate feed and oxidizer streams.

The reaction mixture is introduced into the optical cell with a standard HPLC solvent pump, which is rated to a pressure of 6000 psi (400 atm) and regulated solvent flow rates of 0-10 mL/min. High pressure fittings rated to 60000 psi at room temperature are used at all of the heated

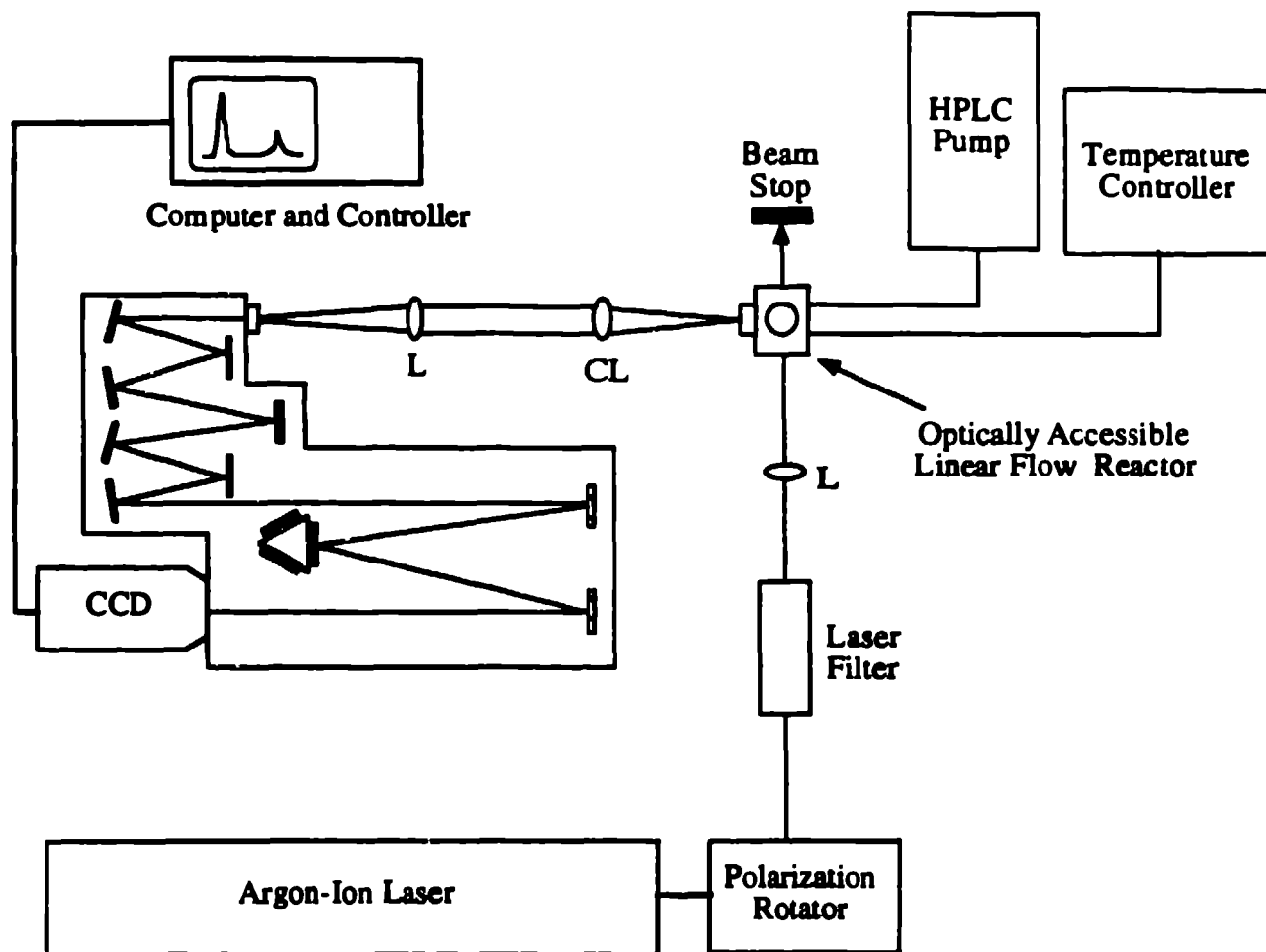


Figure 20. Schematic of Raman apparatus. Polarization rotator: double romb, half-wave retarder; Laser filter: small monochromator; L: lens; Cl: collection lens; CCD: charge coupled device camera for detection. Data collection using Macintosh II computer.

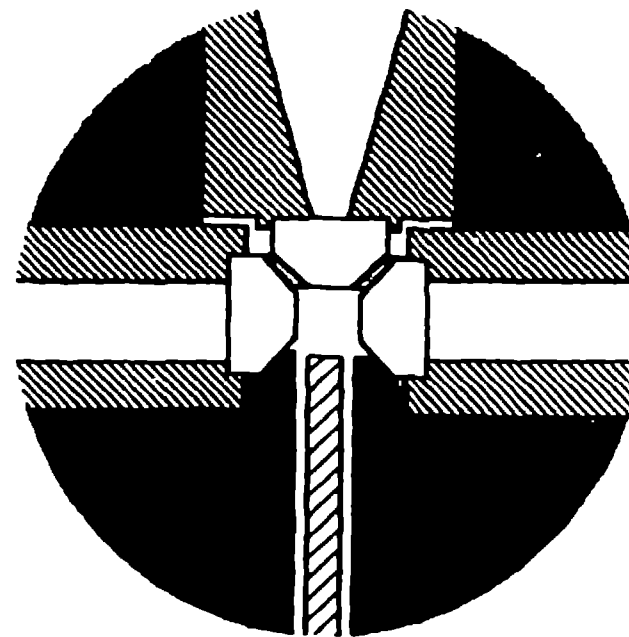
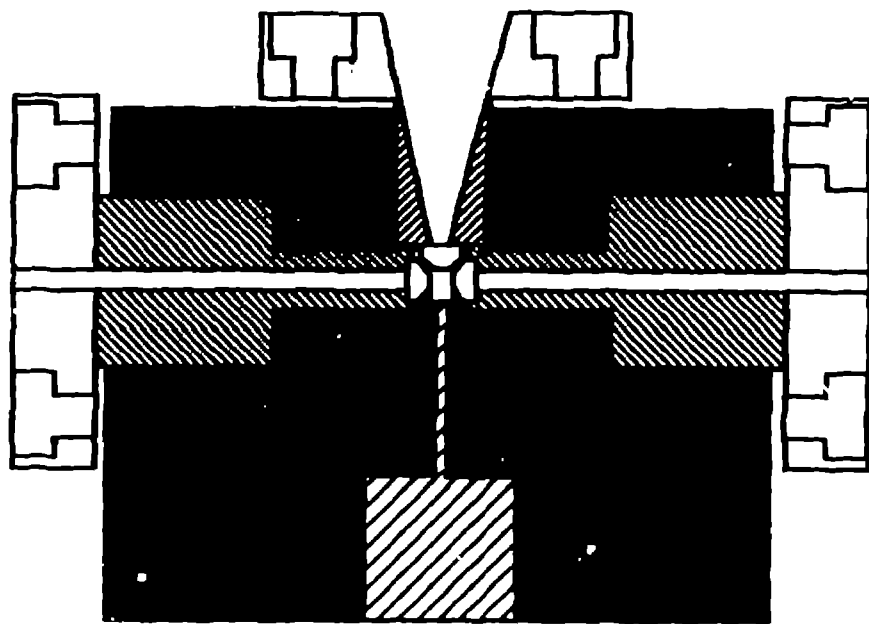


Figure 21: Optical cell with blowup of window region.

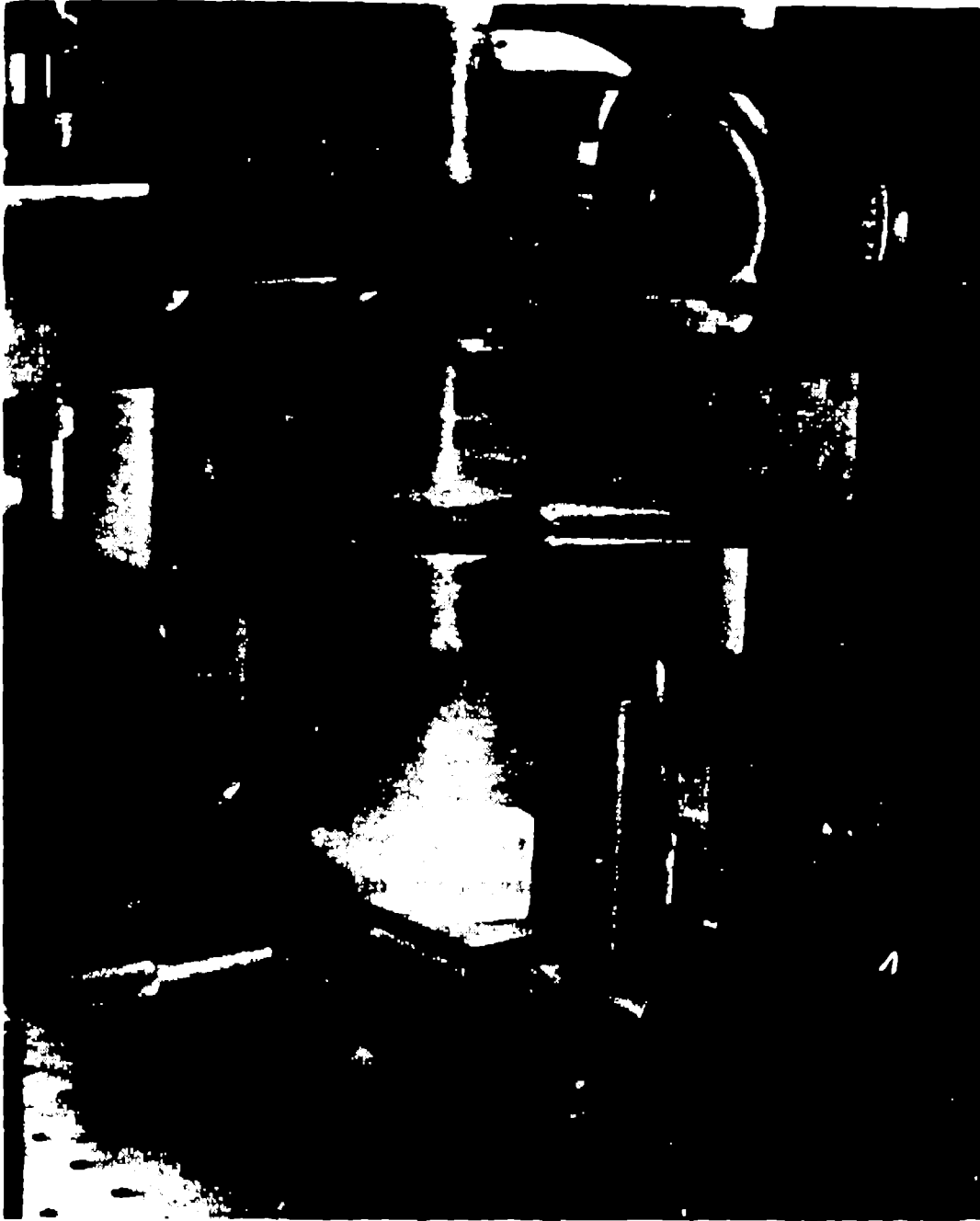


Figure 22: Photograph of the Optical Cell

plumbing ports. Heat is supplied to the cell by four 150 W cartridge heaters imbedded in a brass shell surrounding the stainless steel cell. The fluid temperature is measured with a K-type thermocouple that has an Inconel sheath. The thermocouple is in direct contact with the fluid at a point close to the optically viewed region. Pressure is measured after the optical cell with a standard transducer. The reaction mixture flows through a cylindrical volume in the cell with dimensions of 1.57 mm id and 51 mm length, yielding a volume of 0.10 mL. The optical window is located at the midpoint of this heated length, and the central portion (about one-third) of the flow is imaged optically. Experiments were performed with fluid flow rates in the range 0.05 - 3 g/min, yielding corresponding residence times of 0.5 - 30 seconds. A second reactor, shown in Figure 23, is much like the linear reactors described previously. It measures 10 inches (25 centimeters) by 0.0625 inch (1.56 millimeters) id, providing a volume of 0.50 mL. This reactor was used both as a flow reactor with HPLC pumps and as a batch reactor with a pressure intensifier.

2. Coherent Anti-Stokes-Raman Spectroscopy (CARS)

Coherent anti-Stokes-Raman spectroscopy (CARS) is a technique that is also well suited to noninvasive, *in situ* optical diagnostics. In CARS two tunable lasers operating at frequencies ω_1 and ω_2 are used to excite a Raman-active vibrational mode of a molecule at the frequency $\omega_1 - \omega_2$. A coherent output beam with laser-like characteristics is produced at the frequency $2\omega_1 - \omega_2$. By sweeping ω_2 and monitoring the signal intensity, the shape of the CARS spectrum is mapped out. In addition to the CARS signal generated by the molecular transition (the "resonant" signal), there is a weaker signal generated by the sample at every value of ω_2 , the "nonresonant" signal. Because of the nonlinear nature of the CARS process, the resonant and nonresonant signals combine in a complex way to produce a spectrum having a shape different from that of an ordinary Raman spectrum.

In our experiments, picosecond lasers (pulses of ~20 psec duration) are used to generate the CARS spectrum. A schematic of the CARS setup is shown in Figure 24. A Nd:YAG laser is used to pump two dye lasers at $\lambda_1 = 577$ nm and $\lambda_2 = 609$ nm. These are directed to the larger optical cell described previously. Instead of sweeping the frequency of one of the lasers, we operate the laser at 609 nm in a broad-band mode, so that the resulting CARS beam is broad-band. The beam is sent to a monochromator, which disperses the CARS beam and sends it to a CCD camera that is operated as a linear array detector, registering a broad portion of the spectrum on each laser shot. The lasers are fired at a repetition rate of 500 pulses/second, and the CARS signal is averaged (typically for a few minutes) until satisfactory signal-to-noise ratios are obtained.

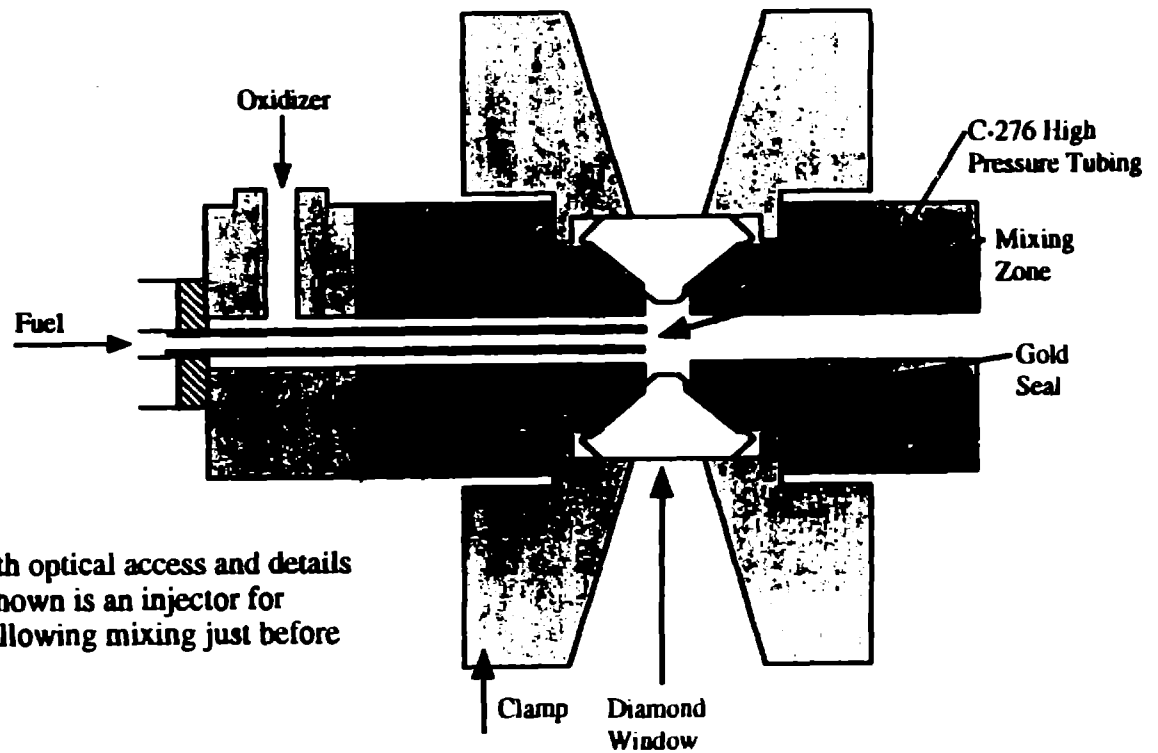
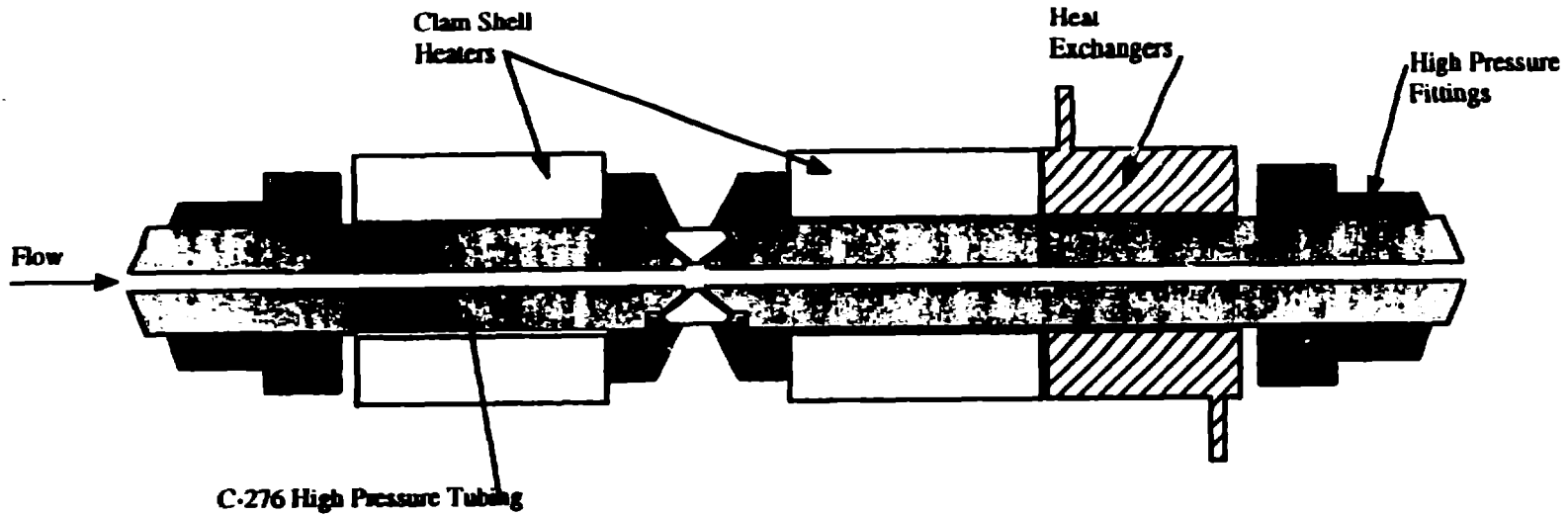


Figure 23. Diagram of linear flow reactor with optical access and details of diamond window seals. Also shown is an injector for introduction of oxidizer and fuel allowing mixing just before the diamond windows.

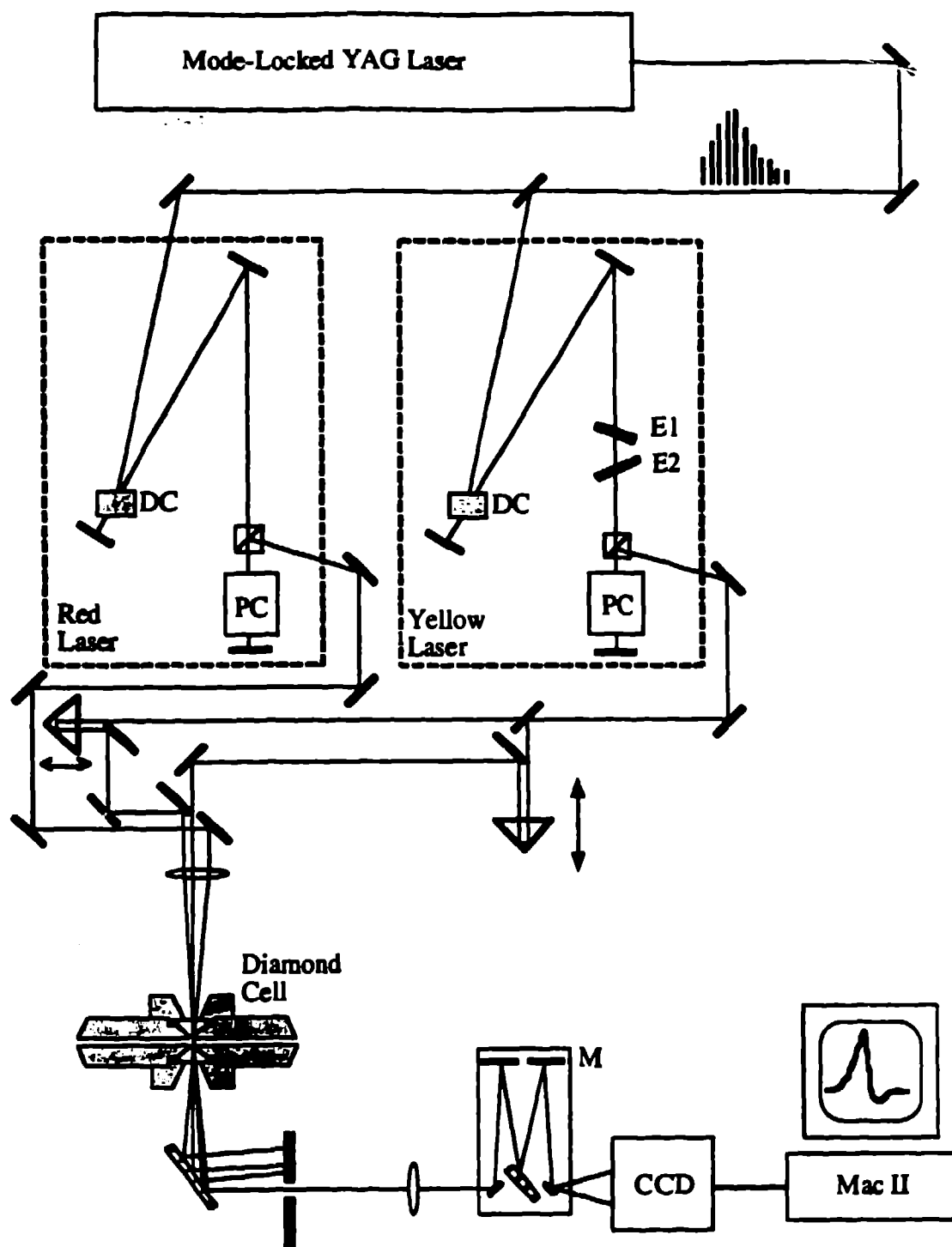


Figure 24. CARS apparatus. DC: dye cell, containing Sulforhodamine 640 for the red laser and Rhodamine 610 for the yellow laser. E1, E2: etalon tuning elements for the yellow laser; these are absent in the broad-band red laser. PC: Pockel's Cell used to fire the dye laser pulse. M: monochromator used to disperse the broad-band CARS beam. CCD: charge-coupled device camera to detect CARS beam. Mac II computer for data acquisition, display, and analysis.

3. Transient Grating Spectroscopy

The transient grating technique is a non-invasive optical method that can be used to measure thermal diffusion constants and the speed of sound of a fluid. Both thermal diffusion constants and speed of sound measurements can be used as sensitive tests for potential equations of state of hydrothermal solutions. Figure 25 shows a schematic of the transient grating experiment. In this experiment, two laser pulses of the same wavelength λ_1 are crossed at an angle θ in the hydrothermal solution, thereby creating a sinusoidal interference pattern of fringe spacing $\Lambda = \lambda_1/[2 \sin(\theta/2)]$ in the overlap region. When the sample absorbs the pump light, the excited molecules quickly relax and deposit their energy to the bath molecules, which produces a spatial modulation in the temperature of the sample. This temperature modulation results in a spatial modulation of the index of refraction and is a volume diffraction grating. This type of grating is called a thermal grating. The grating is probed by Bragg diffraction of a third laser pulse at λ_2 which produces a coherent signal beam also with wavelength λ_2 . Thermal diffusion causes the temperature grating to smear out and the diffracted signal intensity as a function of the pump-probe delay time is described by the equation $S(t) = C \exp[-8\pi^2 D_t t / \Lambda^2]$, where $S(t)$ is the time dependent diffracted signal and D_t is the thermal diffusion constant. In addition, if the pump pulses are short enough, they can produce counterpropagating acoustic waves which appear as large undulations in the transient grating decay spectrum. The speed of sound in the sample is simply the fringe spacing divided by the undulation period.

The sample cell used in the transient grating experiments has two diamond windows for optical access and is very similar to the cell used for the phase behavior (see Section III.C) and Raman optical studies of hydrothermal solutions. The pump light (532 nm, 10 ns pulse width, ~200 μ J/pulse, 10 Hz) is produced from the second harmonic of a Nd:YAG laser. A beamsplitter splits the light into two beams of equal energy, which are focused and overlapped in the sample with a small crossing angle ($< 3^\circ$). The probe beam (585 nm, 10 ns pulse width, ~10 μ J/pulse, 10 Hz) is produced by a Nd:YAG pumped dye laser and is focused into the interaction volume of the sample at the Bragg angle. The time delay between the pump and probe pulses is controlled by a digital delay generator. The diffracted signal beam is spatially and spectrally filtered to reduce scattered pump and probe beam light. The signal is detected with a photomultiplier tube, amplified, integrated with a gated integrator, and sent to a computer where data averaging and acquisition take place.

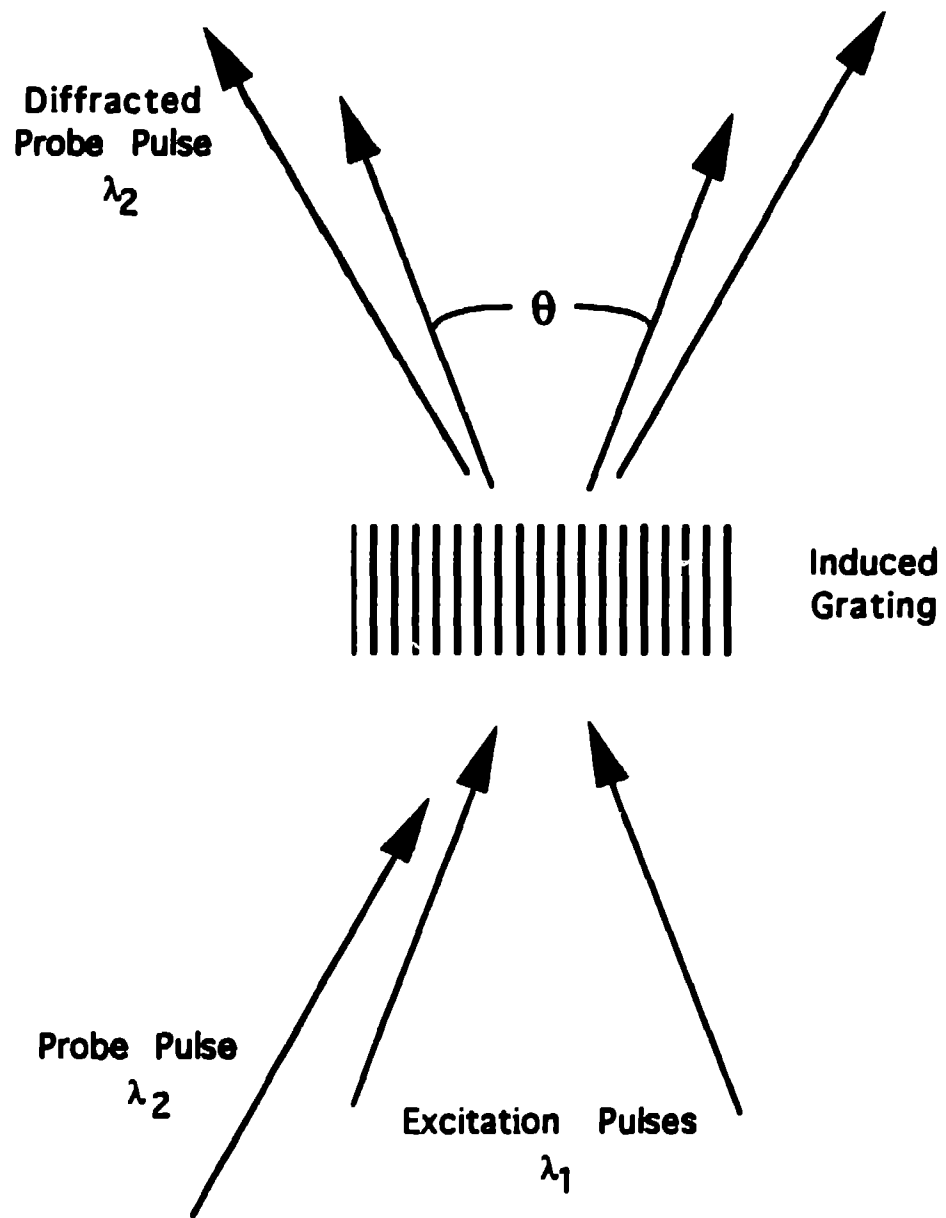


Figure 25. Schematic of a transient grating experiment.

H. ANALYTICAL TECHNIQUES

Many analytical and spectroscopic techniques are needed to identify and quantify the effluent products and reactants resulting from the SCWO process. Our goal is to achieve a mass balance between waste reactant and product species. For purposes of this discussion, these techniques are divided into gas-phase analyses and liquid analyses. Brief descriptions are given of each.

1. Gas-Phase Analysis

a. Fourier-Transform Infrared Spectroscopy (FTIR)

A procedure was developed to quantify the concentration (and thus number of moles) of CO₂ and N₂O (the primary gas-phase products) produced using FTIR. Calibration curves for CO₂ and N₂O were obtained by measuring the fraction of infrared light absorbed by a series of known concentrations of CO₂ or N₂O in the range expected to be produced in SCWO reactions. The unknown concentration is then determined by measuring the fraction of infrared light absorbed by the unknown sample (i.e., the volatile components of the reactor effluent). The dependence on concentration of the integrated absorbance of each of the two major CO₂ IR absorptions (asymmetric OCO stretch, 2350 cm⁻¹, and OCO bend, 630 cm⁻¹) was nonlinear, exhibiting distinctive saturation behavior over the range of pressures (concentrations) from 0.1 to 10 torr. Another observation was that, for a given pressure of CO₂, the observed absorption intensity increased with increasing total pressure. Pressure broadening of absorption lines is a well-understood phenomenon. As total pressure is increased, some molecules will absorb light further from the center of each rotational line, causing a decrease in the center intensity and a concomitant broadening of the peak. The integrated absorbance should remain constant. The reason for the apparently anomalous behavior of our initial results is that the rotational linewidths of most small molecules (including CO₂) are much narrower than the resolution limit of FTIR (maximum resolution = 0.5 cm⁻¹). The observed lines are a convolution of the instrument resolution function and the actual line shape and thus appear to be optically thick to the FTIR, meaning that essentially all the radiation at center frequency appears to be absorbed, resulting in a "saturated" absorbance. As the pressure is increased, more light is absorbed away from the center frequency while the center continues to absorb essentially all the incident radiation. Since the lines are not fully resolved by the spectrometer, absorption of additional light in the wings of the narrow line, but still within the instrument resolution, results in a higher apparent absorbance. This effect can be eliminated by decreasing the concentration of the absorbing species or the pathlength until the line centers are no longer saturated or by increasing the total pressure until the linewidths are

comparable to the instrument resolution. The White cell we used did not have the capability to operate at pressures higher than atmospheric, so the nonlinearity of our calibration curves was not completely corrected for. The calibrations and unknown pressure determinations were made at a total pressure of 600 torr, using N₂ or He as a buffer gas. The resulting calibration data were fit to a saturation function, $y=a(1-e^{-bP})+cP$ where P is the partial pressure of the absorbing gas. A typical calibration curve is shown in Figure 26. This technique enabled us to measure the gas pressure with a relative standard deviation of 3 percent.

b. GC-Mass Spectroscopy

The GC technique is complementary to FTIR, since it is capable of detecting H₂, O₂, and N₂, in addition to all other gases. Three gas chromatographs (GC) have been set up for analysis of the gaseous effluent from the reactor: an HP 5890A Series II with capillary injection ports operated with HP ChemStation software control from a 386-based IBM-compatible computer, and two Perkin-Elmer Model 8410 units. A 10-port gas sampling valve is used to inject gas samples of ~0.1 mL into the capillary column. The carrier gas is He except for one of the gas chromatographs, in which Ar is used for the detection of H₂. Thermal conductivity detectors are installed for quantitative detection of the eluting gases. The column (30 meters x 0.53 millimeter id) used for separating O₂, N₂, H₂, CO, CO₂, CH₄ and CH₃OH is a Chrompack CarboPLOT with carbon molecular sieve adsorbent. A molecular sieve 5A column run in the isothermal mode at -40 °C is used for H₂ and an Alltech CTR-1 column with a temperature ramp program from -10 °C to 180 °C is used for the other gases. A mass spectrometer (HP 5971 MSD) is also available for detection of gases and liquids that elute from the column. In addition, a GC-FTIR interface is installed to a Mattson 500 series FTIR spectrometer, which can be used for characterizing the separated compounds.

c. Quadrupole Mass Spectrometry (QMS)

A UTI quadrupole mass spectrometer is also used to detect H₂, N₂, and O₂. Gaseous products are sampled online through a leak valve. To obtain a steady leak rate, a constant backing pressure of sample plus He buffer gas (600 torr total) was maintained. The pressure in the quadrupole region was typically in the 10⁻⁵ torr range. Calibration of this technique has so far proved difficult due to constantly changing backgrounds.

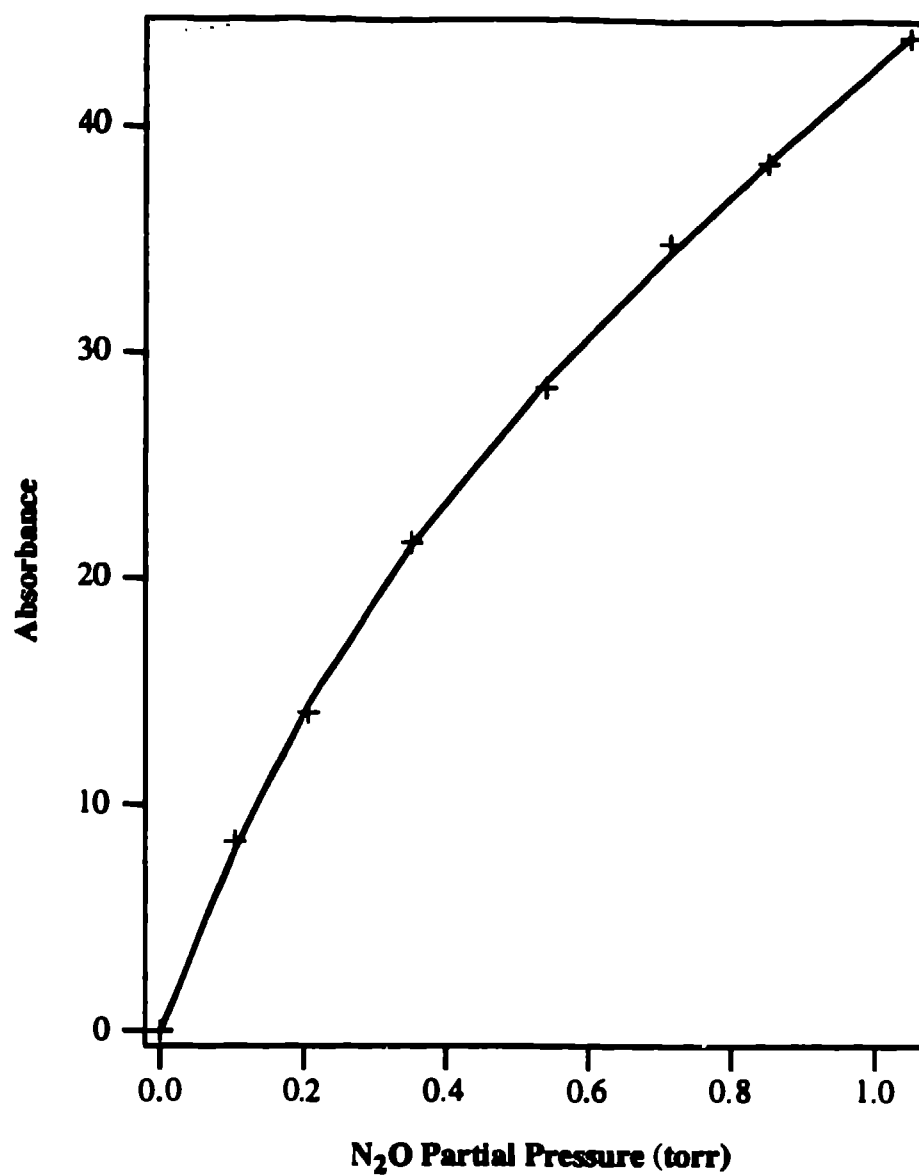


Figure 26. Typical FTIR calibration curve for N₂O, quantity measured in the integrated absorbance for the symmetric N-O stretch versus pressure of N₂O.

2. Liquid-Phase Techniques

a. Metals

The metals analyzed for include sodium, chromium, nickel, iron, molybdenum and gold. In most cases these are done on a Perkin Elmer inductively coupled plasma spectrophotometer (ICP) using indium as an internal standard for all the metals except sodium, for which a lanthanum internal standard is used. If very low detection limits are required, the samples are analyzed using a graphite furnace or flame atomic absorption.

b. Total Organic Carbon (TOC) and Total Inorganic Carbon (TIC)

Total organic carbon (TOC) and total inorganic carbon (TIC) are analyzed using a Rosemount Dohrmann Model DC-190 Carbon Analyzer. Calibrations are done with each set of samples using different concentrations of standardized potassium acid phthalate solution.

c. Inorganic Anions

Inorganic anions, particularly nitrate, nitrite and chloride, are analyzed with a Dionex 4500i Series ion chromatograph using a Dionex IonPac AS4A column with an eluent consisting of 1.5 mM NaHCO_3 and 2.2 mM Na_2CO_3 . In most cases conductivity detection is used, but a UV/visible detector set at 215 nm is used for low levels of nitrate and nitrite.

d. Ammonium Ion

Ammonium ion concentration is determined by an Orion Model 95-12 ammonia electrode using an ionic strength adjuster (ISA) containing 5 M NaOH, 0.05 M ethylenediaminetetraacetic acid (EDTA), and 10 percent methanol. The ISA converts the ammonium ion into dissolved ammonia gas, which is detected by the electrode.

e. TNT, PETN, HMX, NQ, RDX, Hydrazine, and UDMH.

Trace amounts of these explosives are analyzed by reverse-phase liquid chromatography on the Dionex 4500i. The liquid chromatograph uses a Waters 490E Programmable Multiwavelength Detector that allows for simultaneous detection at several wavelengths. This feature is particularly useful if interferences are present, since interferences

usually give different signals at different wavelengths. All these compounds are analyzed using a 150 millimeter x 2.1 millimeter id C8 narrow-bore column that is slightly heated for temperature stability. Trinitrotoluene is measured at wavelengths of 240 and 260 nm using an eluent of 35 percent methanol (MeOH) and 4.5 percent tetrahydrofuran (THF) in water at 0.3 mL/minute in a 6.7- μ L sampling loop; PETN is measured using 48 percent MeOH at 0.3 mL/minute in a 27- μ L loop at 215 and 230 nm; RDX and HMX are both measured using 32 percent MeOH and 4.8 percent THF at 0.3 mL/minute in a 15- μ L loop at 235 and 245 nm; and NQ is analyzed using 4 percent MeOH at 0.3 mL/minute in a 9.5- μ L loop at 263 and 275 nm. UDMH is measured at a wavelength of 294 nm using 65 percent MeOH and sodium phosphate monobasic (NaH_2PO_4) as a buffer at a pH of 2.5. Before analysis, nitrosalicylaldehyde is added to the sample to concentrations of 50 ppm and the sample is heated in a water bath for 5 minutes to form a color complex. Hydrazine is measured at 458 nm using 90 percent MeOH and 10 percent NaH_2PO_4 . One mL of dimethylaminobenzaldehyde (DAMB) reagent is added to 5 mL of sample to form a color complex. Both UDMH and hydrazine use a 15 μ L sampling loop.

f. Methanol

Methanol is analyzed using an SRI Model 8610 gas chromatograph by direct injection on a 30-meter x 0.53-millimeter J&W Scientific DB-Wax column at 60 °C.

3. Base Hydrolysis Product Analysis

Products from the hydrolysis reactions were analyzed by a number of different methods. Nuclear magnetic resonance (NMR) spectrometry was used to identify the major hydrolysis products. A JEOL GSX-270 multi-nuclear spectrometer was used to obtain proton, carbon, nitrogen, and phosphorus NMR spectra. Analyses were performed on the hydrolysis solution with a small amount of deuterated water added to provide a lock signal. Mass spectrometry was used to analyze gaseous hydrolysis products (DuPont model 104) and, in some cases, for solid residue analysis (Finnigan-Mat model 8200). Quantitative analysis for inorganic and organic anions was performed with a Dionex model 2000i ion chromatograph using a conductivity detector. Solid residues from dried hydrolysis solutions were tested for energetic material by observing their burning characteristics in a flame and by differential thermal analysis (DTA) using a Dupont model 910 thermal analyzer.

SECTION III

REACTIONS OF ENERGETIC MATERIALS BELOW WATER SOLUBILITY LIMITS

A. INTRODUCTION

Much of our effort has focused on reactions of solutions having concentrations less than half of their solubilities at room temperature. We have obtained destruction efficiencies and product analyses for the SCWO of AP, NM, PETN, HMX, RDX, TNT, NG, N₂H₄, UDMH and NQ. In some cases, Cl, N, and C mass balances have been obtained. In addition, for the AP and NM reactions we have obtained kinetic data for limited ranges of temperature and concentration.

B. DESTRUCTION EFFICIENCIES AND REACTION PRODUCTS UNDER HIGHLY OXIDIZING CONDITIONS

The destruction efficiencies for the SCWO of five explosive compounds, PETN, HMX, RDX, TNT, and NQ are given in Table 5. These reactions were run at high temperatures (near 600 °C) and with a large excess of oxidant. Numerous reactions have been run at lower temperatures and with varying amounts of oxidant, and are discussed in subsequent sections. In addition, N₂H₄, UDMH, AP and NM, which are unique in their high solubilities and their chemistry, will be discussed in separate sections.

TABLE 5. DESTRUCTION EFFICIENCIES FOR ENERGETIC MATERIALS BELOW WATER SOLUBILITY LIMITS^a

Substrate	PETN	HMX	RDX	TNT	NQ
Initial conc. (ppm)	3.8	2.6	35.2	65.5	1700.
Destruction efficiency	>0.9825	>0.9900	>0.9992	>0.9998	>0.9999

^aConditions: 600 °C, 5500 psi; excess H₂O₂; 11-s residence time; gold-lined reactor.

The initial concentrations of the explosives were kept at less than half their room temperature solubilities to prevent precipitation and accumulation of explosive material in the feed lines leading

to the reactor. Hydrogen peroxide was used as the oxidizer and was mixed with the feedstock containing explosives before the fluids were heated. In all cases the oxidizer was in thirtyfold excess of the stoichiometry required to convert the explosive into CO₂, H₂O, and N₂. The experimental conditions for each of these explosives were nearly identical: pressure, 340 atm; reactor temperature, 600 °C; and residence time, 11 seconds. The reactions were run primarily in the gold-lined reactor to minimize the heterogeneous chemistry that might occur at the reactor walls. The only compound for which any reactor-dependent chemistry has been observed is AP. No significant difference in DREs or products chemistry was observed for reactions of TNT, HMX, and RDX in the C-276 and the gold-lined reactors. We conclude from these observations that reactions with the C-276 and 316 stainless walls must not be significant for these energetic materials.

For these "extreme" conditions, the aqueous effluent contained no detectable amounts of explosives. The detection limit of the HPLC/UV-vis analysis ranges from 20 to 50 parts per billion (ppb) depending on the compound. Consequently, the measured destruction efficiencies represent lower limits defined by the low starting concentrations and the detection limits.

Gaseous and liquid effluents from these reactions have been analyzed to determine the products of reaction. Typical FTIR spectra of the gaseous effluent from the reactions of NQ, TNT, and RDX with excess oxidant are shown in Figure 27. These spectra show IR absorbances corresponding to CO₂, N₂O, and H₂O. Qualitative FTIR analyses of gas phase products of SCWO of energetic materials with and without oxidant are summarized in Table 6. It is clear from these analyses that the extreme conditions of high temperature and excess oxidant produce only CO₂ and N₂O in the gaseous effluent. Other possible products such as CO, CH₄, NO, and NO₂ are not detected and are, therefore, below parts per million (ppm) levels (generally below 0.1 percent of the starting C and N). Additional products that are likely to be produced in these reactions, but which cannot be quantified by FTIR, include N₂, O₂ (no infrared-active vibrations), and H₂O (swamped by large water background absorption). In addition, quantitative measurements of the CO₂ and N₂O produced are summarized in Tables 7 and 8.

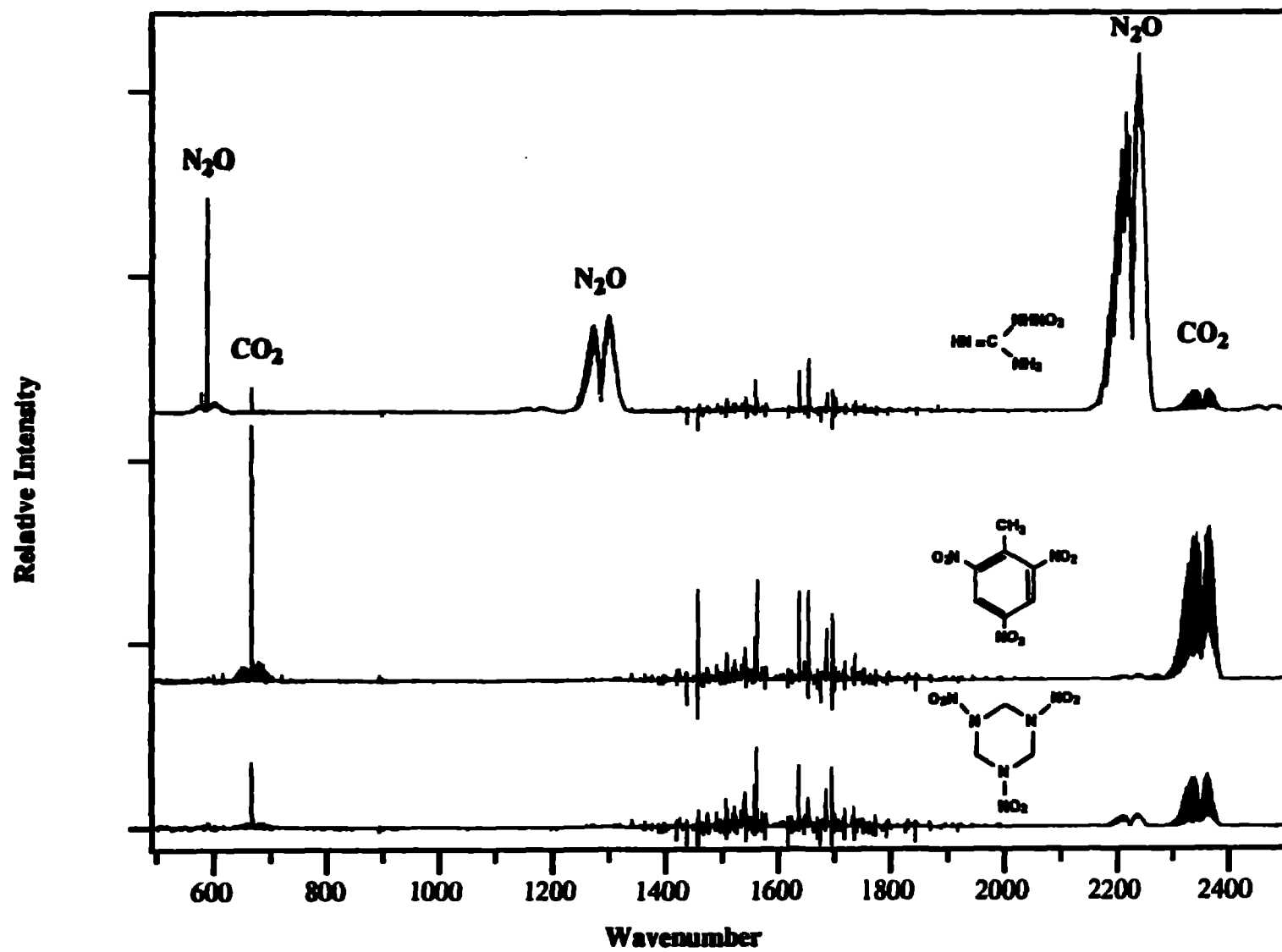


Figure 27. FTIR spectra of the reaction products of SCWO of NQ, TNT, and RDX.

TABLE 6. FTIR ANALYSIS OF GAS-PHASE PRODUCTS OF SCWO OF ENERGETIC MATERIALS^a

Substrate	Without oxidant	With oxidant
PETN	CO ₂ , CO	CO ₂
HMX	CO ₂ , N ₂ O	CO ₂ , N ₂ O
RDX	CO ₂ , CO, N ₂ O	CO ₂ , N ₂ O
TNT	CO ₂ , CO, CH ₄ , NO	CO ₂ , N ₂ O
NQ	CO ₂ , N ₂ O	CO ₂ , N ₂ O

^aConditions: 600 °C, 5500 psi; 11-s residence time; gold-lined reactor.

The reactor effluents have been analyzed for carbon content and the results are summarized in Table 7. The final two columns list the percentage of the starting C that is observed in the aqueous effluent (as organic and inorganic C) and as CO₂ in the gaseous effluent. For PETN and HMX, both the TIC and TOC quantities are below detection limits (0.1 ppm). Detectable quantities of organic carbon were found for RDX, TNT, and NQ. Since in all of these cases the substrate is destroyed to levels well below the detection limits of the HPLC analysis (10 ppb) and since no volatile organics were observed in the FTIR analyses, the observed organics must be nonvolatile reaction products such as formate or acetate. For the TNT reactions, greater than 94 percent of the C was detected as CO₂, with the remainder detected as nonvolatile organics in solution. The only substrate to give significant TIC (carbonate or bicarbonate) quantities is NQ. In this case, 83 percent of the C is detected as CO₃²⁻ or HCO₃⁻ while 21 percent is detected as gaseous CO₂, accounting for most of the C.

TABLE 7. ANALYSIS OF CARBON PRODUCTS IN EFFLUENT STREAMS FOR SCWO OF ENERGETIC MATERIALS^a

Substrate	[C] _i ^b (ppm)	TIC (ppm) ^c	TOC (ppm) ^c	% C _{aqueous}	% C _{CO2}
PETN	2	d	d	d	81
HMX	2	d	d	d	87
TNT	24	0.2	1.7	8	98
RDX	5.7	<0.1	<0.1	<4	98
NQ	195	152	10	83	21

^aConditions: 600 °C, 5500 psi; excess H₂O₂; 11-s residence time; gold-lined reactor; ^bInitial carbon concentration.; ^cTIC, Total inorganic carbon, TOC, Total organic carbon; ^dSince starting concentrations of PETN and HMX are ~2-3ppm, the analyses for TOC and TIC are below detectable limits.

Reactor effluents have also been analyzed for nitrogen content and the results are summarized in Table 8. For PETN, HMX, and RDX, some N₂O was observed in the FTIR spectra, but quantitative analysis showed the amounts to be less than 0.5 percent of the initial N. With excess oxidant, significant amounts of nitrite and nitrate were observed for all substrates except NQ. Most of the detected N from NQ was determined to be N₂O. Trinitrotoluene (TNT) produced the greatest fraction (65 percent) of NO_x⁻. Since NO_x⁻ is an undesirable product, some effort has been made to determine conditions for which its production can be minimized in the case of TNT. These results are summarized in Section III.D. In all cases examined so far, a large fraction of the initial nitrogen remains undetected by our analytical techniques. We have interfaced a mass spectrometer to the gas-liquid separator on the gold-lined reactor which enables us to obtain on-line analyses of the effluent gases. We have observed formation of N₂ in the SCWO oxidation of TNT. In addition, we have a gas chromatograph interfaced to the gas-liquid separator of the sand bath reactor, with the appropriate column and detector for separation and detection of N₂. Preliminary experiments on SCWO of nitromethane with this setup indicate the formation of N₂; however, we have not obtained quantitative analysis for N₂ for any of the very low concentration experiments.

TABLE 8. ANALYSIS OF NITROGEN PRODUCTS IN EFFLUENT STREAMS FOR SCWO OF ENERGETIC MATERIALS^a

Substrate	PETN	HMX	RDX	TNT	NQ
% NO ₃ ⁻	18.7	12.4	10.1	36.6	0.03
% NO ₂ ⁻	6.0	5.3	14.1	28.5	0.04
% N ₂ O	b	b	b	4.0	35

^aConditions: 600 °C, 5500 psi; excess H₂O₂; 11-s residence time; gold-lined reactor. ^bLess than 0.5%.

C. REACTIONS OF AMMONIUM PERCHLORATE (AP)

This section summarizes the data for the SCWO reactions of AP. Because of corrosion problems, most of these reactions were performed in the gold-lined reactor. Some results in the C-276 reactor are included for comparison. Sodium hydroxide was always added to the AP solutions in a 1:1 stoichiometry to ensure a net pH balance. This is particularly important for the gold-lined reactor, where the presence of a high Cl⁻ ion concentration together with a low pH and highly oxidizing conditions may result in the oxidation of the gold liner to AuCl₄⁻ (see Section VII.B.1).

Data for the dependence of destruction efficiencies and reaction products on temperature and concentration are summarized in Tables 9 and 10, respectively. The products containing Cl and N are given as a percentage of the initial Cl and N concentration, respectively. At temperatures lower than 400 °C, no decomposition of the ammonium perchlorate is observed. Most of the ammonia and all of the perchlorate are recovered. The small ammonia loss is likely due to the evolution of ammonia gas from the feed solution and effluent. The AP begins to react at 450 °C and is nearly completely destroyed (99.6 percent) after 11 seconds at 600 °C. The effect of concentration on destruction efficiency appears to be less straightforward, since results at the intermediate concentration (0.01 M) indicate a lower destruction efficiency of 87.5 percent. These results appear to be inconsistent with the results at higher and lower concentrations and we suspect there was a problem with the analyses of these data.

Almost all the chlorine from the perchlorate appears in the effluent as sodium chloride (NaCl). Although salt solubility decreases in supercritical water, the sodium chloride product remains in solution at low concentrations or temperatures. However, when the concentration and/or temperature are raised, the Cl mass balance is degraded, probably due to precipitation of Cl⁻

salts in the reactor. We have found that our mass balances improve when the reactor is cooled and flushed between runs and the flushing solutions are included in the analysis. With this procedure a burst of Cl^- is generally observed in the first or second flush sample as the reactor is cooled.

The liquid effluent also contains a small amount (< 2 percent) of nitrogen as nitrite (NO_2^-) and nitrate (NO_3^-). The mass spectra indicated that both nitrous oxide (N_2O) and oxygen (O_2) are produced. The amount of N_2O produced was quantified using the FTIR/White cell and appears to increase with increasing temperature and AP concentration. Most of the N was not detected (for the best case, 600 °C, only 25 percent is detected) and likely occurs as N_2 . The FTIR and mass-spectrometric analyses of the gaseous effluent did not detect the presence of chlorine (Cl_2), nitrosyl chloride (NOCl), or nitrogen dioxide (NO_2).

TABLE 9. AP SCWO PRODUCTS AS A FUNCTION OF TEMPERATURE^a

T (°C)	% ClO_4^-	% Cl^-	% NO_2^-	% NO_3^-	% N_2O	% NH_4^+
400	100	0.0	0.3	0.0	0.0	95.0
450	95.5	6.9	0.8	0.3	1.3	85
500	46.0	16.0	0.0	2.0	13.6	40.0
550	3.5	17.0	0.0	2.0	23.1	0.0
600	0.4	5.0	0.2	0.2	23.3	0.0

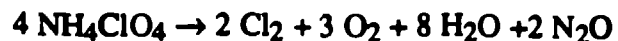
^aConditions: 0.1 M AP; equimolar NaOH; residence time varied from 11 - 52 s (600 - 400 °C); flush between runs not analyzed; gold-lined reactor.

TABLE 10. AP SCWO PRODUCTS AS A FUNCTION OF CONCENTRATION^a

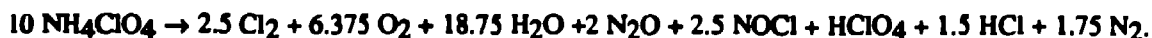
[AP] (M)	% ClO_4^-	% Cl^-	% NO_2^-	% NO_3^-	% N_2O
0.001	0.3	108.1	7.1	1.9	0.0
0.01	12.5	95.0	1.1	1.0	13.7
0.1	0.4	69.1	0.0	3.8	23.0

^aConditions: 600 °C; equimolar NaOH; 11-s residence time; flush between runs included in analyses; gold-lined reactor.

Previous studies of the thermal decomposition of solid ammonium perchlorate show that a variety of products is possible (Reference 10). Below 300 °C, the equation



represents the majority of the products. At higher temperatures more nitric oxide (NO) is produced. Between 350 °C and 450 °C gas analysis of the products of thermal decomposition gives



Thus the decomposition of AP in supercritical water avoids the formation of the hazardous products (Cl₂, NOCl) formed in thermal decomposition.

Above 450 °C, ammonium perchlorate detonates. The possibility of explosive energy release was investigated. Concentrated solutions of ammonium perchlorate (1.0 M, 117.5 g/L) were rapidly heated to temperatures over 600 °C at pressures near 340 atm in a small batch reactor. Neither pressure nor temperature transients indicative of rapid energy release were observed. These results indicate SCWO is, therefore, more controlled (i.e., safer) than thermal decomposition.

One interesting consequence of the gold-lined reactor is a lower destruction efficiency for AP compared to that found for the C-276 reactor. Comparisons of the destruction efficiencies in the two reactors at various temperatures are summarized in Table 11. The conditions for these reactions are roughly equivalent except that the residence time in the C-276 is approximately 80 percent that in the gold-lined reactor. Despite the longer residence times in the latter reactor, the destruction efficiencies are always poorer at a given temperature. The AP is 99.95 percent destroyed at 500 °C in the C-276 reactor while the best destruction efficiency achieved in the gold-lined reactor is 99.6 percent at a higher temperature, 600 °C. We attribute this difference to the absence of reactions with the reactor walls in the case of the gold-lined reactor. The extensive corrosion of the C-276 reactor by AP reactions supports this conclusion (see Section VII.B.1).

TABLE 11. COMPARISON OF AP SCWO REACTIONS IN C-276 AND GOLD-LINED REACTORS^a

Destruction Efficiency(%)	400 °C	450 °C	475 °C	500 °C	550 °C	600 °C
C-276 Reactor	0	40	86	99.95	-	-
Gold-Lined Reactor	0	4.5	-	54.0	96.5	99.6

^aConditions: 0.1 M AP; equimolar NaOH; residence time varied from 11 - 52 s (600 - 400 °C); flush between runs not analyzed.

A series of experiments was run on mixtures of AP and RDX in an attempt to model the complex mixtures actually found in a rocket motor. Ammonium perchlorate, NaOH and RDX were mixed in a 1:1:2 molar ratio. This ratio yields a slight oxygen deficiency if the reaction goes to completion, according to



Experiments were performed with and without additional oxidant (H₂O₂) and at temperatures ranging from 500 to 600 °C (Table 12). The oxidant was added in a 2:1 molar ratio with RDX, to yield an oxygen balance as defined by the equation above. The best possible comparison to the chemistry of pure RDX is with SCWO reactions at the same concentration, at 600 °C and with a large excess of oxidant (Tables 5, 7, 8, pages 54, 58, and 59). The destruction efficiency of RDX is the same in both cases (99.92 percent). Only one-third of the C is recovered as CO₂ for the mix, compared to nearly 100 percent for the pure RDX under these conditions. The nitrogen chemistry is also significantly different. While the percent N converted into nitrite is similar for both the pure and mix cases, no formation of nitrate is observed in the case of the mix whereas 10 percent of the N in pure RDX was converted to nitrate. Another puzzling observation is that the percent N converted to nitrite drop a factor of two to three with the addition of oxidant. It is likely that the differences in both the C and N chemistry are due to the difference in the oxygen balance in these reactions. The large excess (30 equivalents) of oxidant used in the reactions of the pure RDX solutions probably results in better conversion of all the C to CO₂ with the negative side effect of causing the formation of nitrate.

The best possible comparison with the chemistry of pure AP is to reactions run at slightly higher concentration (1.00 x 10⁻³ M or 118 ppm) and at 600 °C (Table 10, page 60). The chemistry yields a slightly smaller destruction efficiency of the ClO₄⁻. The addition of oxidant (H₂O₂) causes the destruction efficiency of ClO₄⁻ to decrease from greater than 97 percent to less

than 91 percent. This observation suggests that better destruction of ClO_4^- may be achieved by adding more reducing agents (fuels). This is consistent with the higher destruction efficiencies observed in the C-276 reactor, where the reactor itself was acting as a source of reductant.

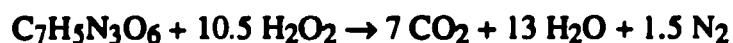
TABLE 12. SCWO OF AP AND RDX MIXTURES^a

T (°C)	[H ₂ O ₂] added (ppm)	% Cl ⁻	% ClO ₄ ⁻	% NO ₂ ⁻	% NO ₃ ⁻	% N ₂ O	% CO ₂
500	0	100.0	5.0	44.0	1.0	0.3	23
500	11	89.0	20.0	15.0	1.0	0.4	27
550	0	96.0	3.0	45.0	1.0	0.4	28
550	11	86.0	10.0	18.0	0.0	10.1	28
600	0	98.0	3.0	30.0	0.0	10.5	34
600	11	86.0	9.0	18.0	0.0	15.2	33

^aConditions: 18.3 ppm AP; equimolar NaOH; 34.6 ppm RDX; residence time varied from 11 - 16 s (600-500 °C); flush between runs included in analysis; gold-lined reactor.

D. REACTIONS OF TRINITROTOLUENE (TNT)

This section discusses the SCWO reactions of TNT in greater detail, particularly the effects of temperature and oxidant concentration on observed destruction efficiencies and reaction products. Data for CO₂ production from the SCWO of TNT in the linear reactor at 600 °C, 5400 psi, 4 grams/minute flow rate and a large excess (~thirtyfold) of H₂O₂ are summarized in Table 13. Expected pressures of CO₂ are calculated from initial concentrations of TNT and the volume of effluent collected, using the ideal gas law and assuming complete conversion of the TNT to CO₂ according to the following equation:



The average percent C detected as CO₂ in these experiments is 98 percent. The residual C could be tied up in the nonvolatile product observed in the HPLC analysis shown in Figure 28 (identity and concentration unknown). It is possible that this product is a small nonvolatile organic acid such as formic acid. Nitrogen balances for these reactions are not complete. Detected products, including

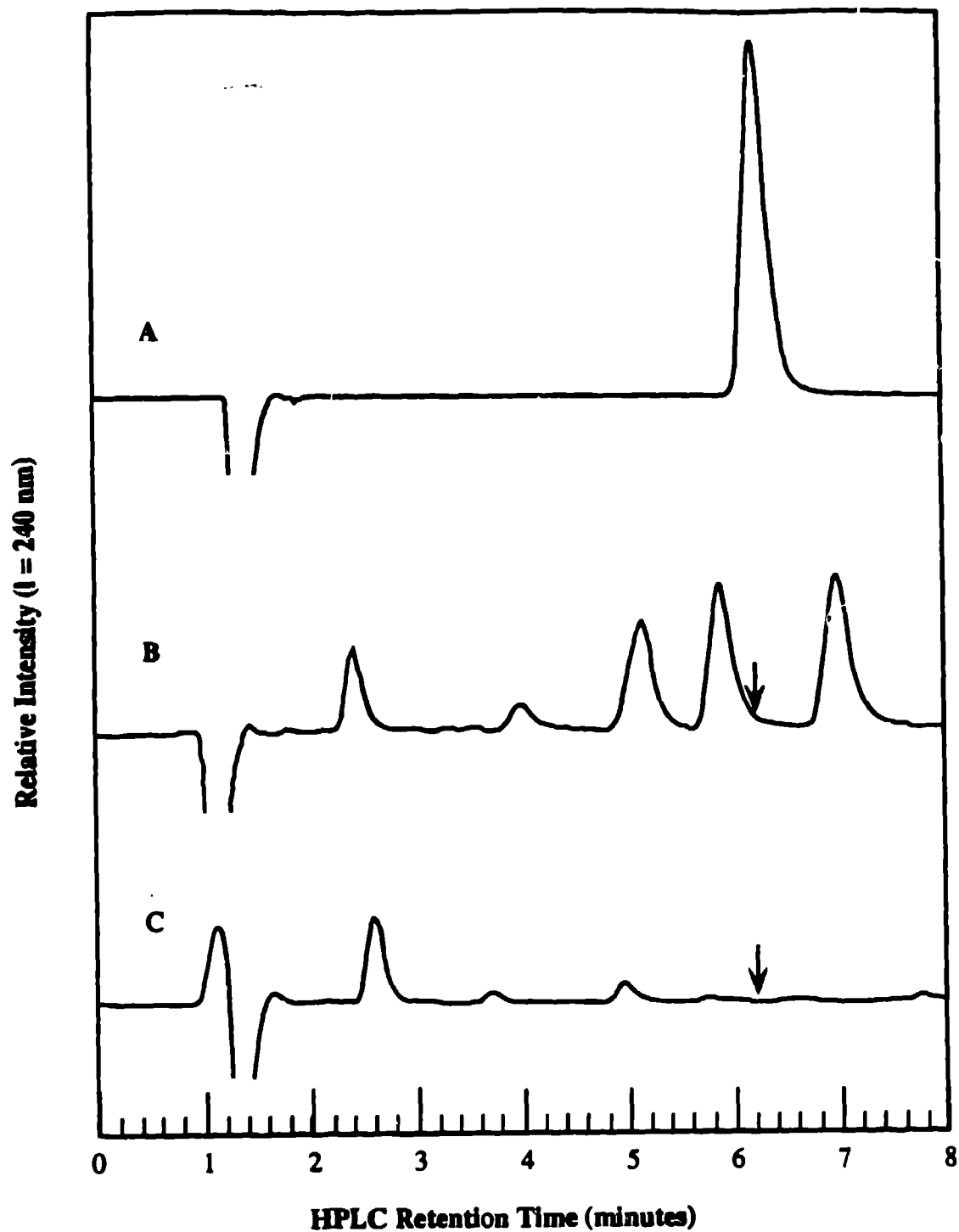


Figure 28. HPLC analysis of aqueous TNT solutions: (A) TNT standard, 32.4 ppm; (B) SCWO reaction (550°C) without added oxidant; (C) SCWO reaction (550°C) with excess H₂O₂. The arrows indicate where the TNT peak should occur.

N_2O , NO_3^- and NO_2^- accounted for about 69 percent of the starting N, (Table 8, page 59). The remaining N must occur as N_2 or ammonia.

TABLE 13. CO_2 PRODUCTION IN THE SCWO OF TNT

Exp.	$P_{\text{meas}}^{\text{a}}$ (mtorr)	$P_{\text{calc}}^{\text{b}}$ (mtorr)	%C detected
1	260	259	100
2	245	272	90
3	314	303	104
4	232	244	95
5	258	261	99

^aDetermined from integrated FTIR band intensities and CO_2 calibration curves.

^bCalculated from the ideal gas law assuming complete oxidation.

A large number of experiments have been conducted on TNT to determine the SCWO chemistry as a function of reaction temperature and oxidant concentration. All of these experiments were performed using TNT solutions near one-half the solubility limit in water (65 ppm). In all cases, the TNT was destroyed to below detectable limits of ~10 ppb, yielding a destruction efficiency of greater than 99.98 percent. The product analyses are summarized in Tables 14 and 15. The values listed in these tables represent averages of at least 10 runs each. The NO_2^- and NO_3^- values are listed as a percentage of the starting nitrogen concentration. Similarly, the total inorganic carbon (TIC) and total organic carbon (TOC) values are listed as a percentage of the starting carbon concentration. The ratio of H_2O_2 to TNT represents a stoichiometric ratio based on complete reaction of TNT with H_2O_2 to form CO_2 , H_2O , and N_2 .

TABLE 14. TNT SCWO PRODUCTS AS A FUNCTION OF H₂O₂ CONCENTRATION

Exp.	Temp (°C)	H ₂ O ₂ :TNT ^a	%NO ₂ ⁻	%NO ₃ ⁻	Total %NO _x ⁻	%TIC	%TOC	%Total C
1	600	0:1	18	0	18	12	34	46
2	600	1:1	11	6	17	15	0	15
3	600	2:1	6	6	12	14	0	14
4	600	5:1	33	38	71	9	0	9
5	600	20:1	25	49	74	4	0	4

^aStoichiometric ratio based on equation on page 49.

TABLE 15. TNT SCWO PRODUCTS AS A FUNCTION OF TEMPERATURE

Exp.	Temp (°C)	H ₂ O ₂ :TNT ^a	%NO ₂ ⁻	%NO ₃ ⁻	Total %NO _x ⁻	%TIC	%TOC	%Total C
1	500	0:1	18	0	18	14	28	42
2	600	0:1	18	0	18	12	34	46
3	400	20:1	11	30	41	4	18	22
4	500	20:1	26	51	77	4	11	15
5	600	20:1	25	49	74	4	0	4

^aStoichiometric ratio based on equation on page 65.

The most efficient conversion of TNT to CO₂, as determined by FTIR analysis of the gas production and by the TIC and TOC analyses of the aqueous effluents, occurs at the highest temperature (600 °C) and the highest H₂O₂ concentration. These conditions also yielded the highest concentrations of NO₂⁻ and NO₃⁻. In general, at lower temperatures and lower ratios of H₂O₂:TNT, less NO₂⁻ and NO₃⁻ are observed. While these conditions do not compromise the destruction efficiency of TNT, they tend to leave more carbon in the aqueous effluent. Much of this carbon appears as carbonate, however, which can be removed by lowering the pH. The best conditions for the destruction of TNT and any organic byproducts with minimum NO₂⁻ and NO₃⁻ formation appear to be 600 °C and a 1:1 stoichiometric (as defined on page 65) ratio of H₂O₂:TNT.

E. REACTIONS OF NITROMETHANE (NM)

This section summarizes experiments on the SCWO of nitromethane. These experiments were conducted primarily in either the C-276 linear flow reactor or in the shorter optical cell configured as a linear flow reactor. The destruction of nitromethane was monitored using the FTIR/White cell, by the intensity of the N–O stretching band at 1590 cm^{-1} . The integrated intensity of this band indicates that the nitromethane is greater than 98 percent destroyed at $550\text{ }^{\circ}\text{C}$ and in the short residence time (< 1 second) of the optically accessible reactor (Figure 23, page 45). The FTIR spectrum of the $550\text{ }^{\circ}\text{C}$ run is compared to the spectrum at $300\text{ }^{\circ}\text{C}$ in Figure 29. It is clear from these data that little of the NM has reacted at $300\text{ }^{\circ}\text{C}$, but most is destroyed at $550\text{ }^{\circ}\text{C}$. All the peaks in the $550\text{ }^{\circ}\text{C}$ spectrum have been assigned to vibrations of the residual CH_3NO_2 and volatile reaction products, including CO_2 , CO , CH_4 , N_2O , NO , and HCN . These are indicated in Figure 29. Expected reaction products that were not detected include N_2 and O_2 (no infrared absorptions), NO_3^- and NO_2^- (not volatile species) and H_2O (obscured by large H_2O background). Other possible products that are detectable under these conditions at levels above 1 ppm but were not observed include NH_3 and NO_2 .

Quantitative analyses of the reaction products were obtained from these spectra. The infrared assignments and number densities (molecules per cm^3 in the White cell) calculated from literature values of the absorption cross sections are summarized in Table 16. The starting number density of the CH_3NO_2 was measured to be 5.7×10^{16} molecules/ cm^3 . The number density for HCN could not be calculated because the absorption cross section is not available, but a reasonable estimate yields a number density of less than 2.0×10^{14} molecules/ cm^3 . The mass balance for the reaction was calculated from these measured number densities and is summarized in Table 17. The carbon is completely accounted for. It is almost evenly distributed between CO and CH_4 , with a small amount occurring as CO_2 . Only 41 percent of the nitrogen was detected, mostly as N_2O . Nitrogen dioxide (NO_2) and NH_3 were not detected and if present are below our 1 ppm detection limit. Based on previous experiments, we expect a small amount (~ 4 percent) of the nitrogen to occur as NO_3^- and NO_2^- . The remaining 55 percent likely occurs as N_2 , which is not detectable by FTIR analysis. The undetected hydrogen (36 percent) most likely occurs as H_2O . Given this reasonable assumption and the ~ 4 percent of the oxygen that occurs as NO_3^- and NO_2^- , 27 percent of the oxygen remains unaccounted for. It is possible that the decomposition produces O_2 , which would not be detected in the FTIR analysis.

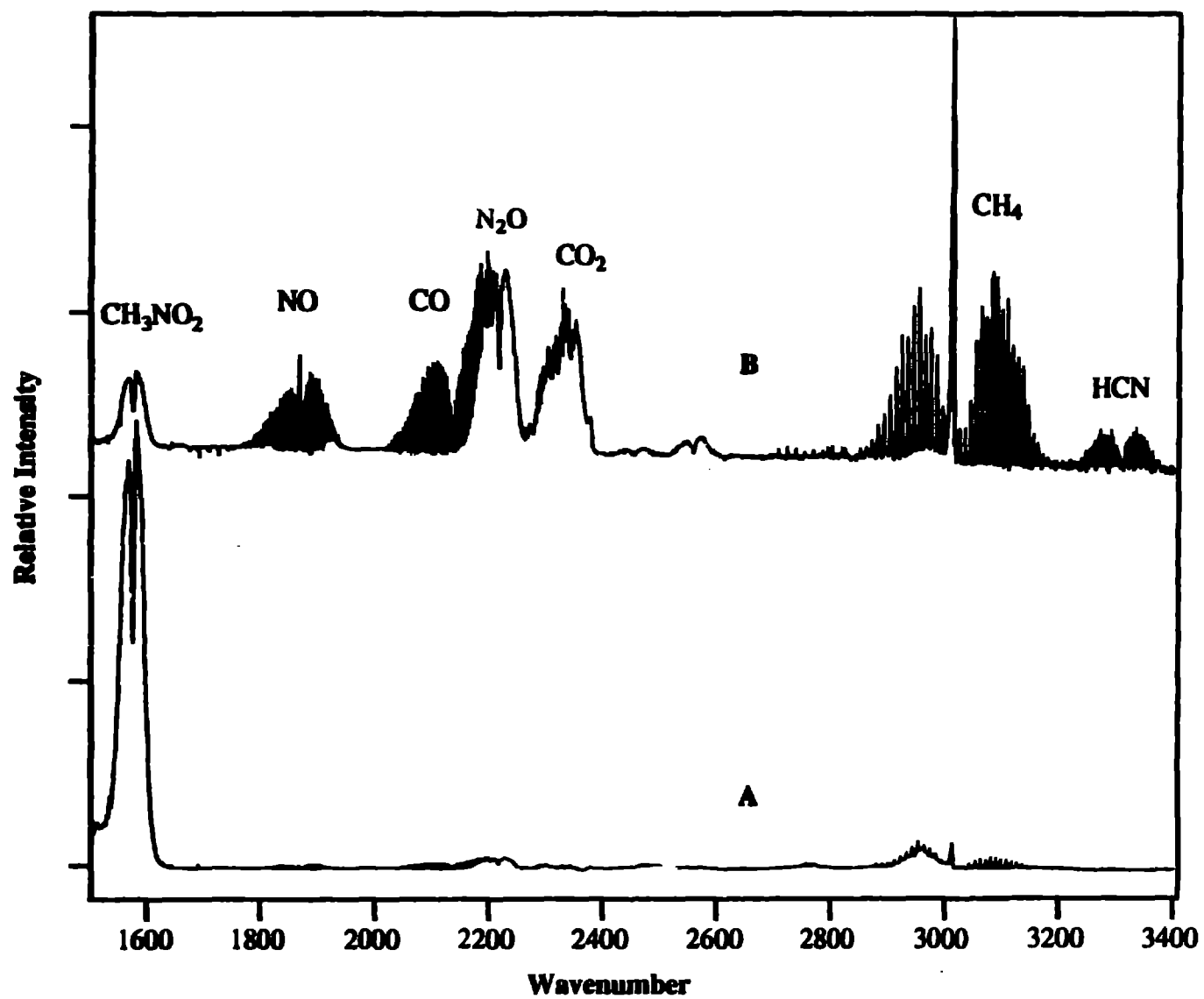


Figure 29. FTIR product analysis of SCWO of nitromethane. (A) CH₃NO₂ in H₂O, 300 °C, 5000 psi; (B) CH₃NO₂ in H₂O, 550 °C, 5000 psi.

TABLE 16. FTIR ANALYSIS OF NITROMETHANE DECOMPOSITION PRODUCTS^a

Product	ν (cm ⁻¹)	Absorbance	$\sigma \times 10^{19}$ (cm ² /molecule) ^b	$N \times 10^{-15}$ (molecules/cm ³) ^c
CH ₃ NO ₂	1590	0.022	2.82	0.8
CO ₂	2360	0.039	1.05	3.7
CO	2120	0.025	0.08	27.0
CH ₄	3020	0.126	0.46	27.0
N ₂ O	2235	0.052	0.48	11.0
NO	1875	0.028	3.16	0.9
HCN	3312	0.009	?	?

^aReaction conditions: 550 °C, 4800 psi, 2-s residence time.

^bAbsorption cross section, estimated from Sadtler Commercial Spectra of Gases and Vapors, 1972.

^cCalculated number density, $N = (A/\sigma)$.

TABLE 17. MASS BALANCE FOR NITROMETHANE DECOMPOSITION IN SCW AT 550 °C

PRODUCT ^a	%C (±1%)	%N (±1%)	%O (±1%)	%H (±1%)
CH ₃ NO ₂	1	1	1	1
CO ₂	6	-	6	-
CO	47	-	24	-
CH ₄	47	-	-	63
N ₂ O	-	38	10	-
NO	-	2	1	-
H ₂ O ^b	-	-	27	36
TOTAL	101	41	69	100

^aBased on number densities of products detected by FTIR. Number density of CH₃NO₂ before reaction, $N_0 = 5.7 \times 10^{16}$ molecules/cm³. Products not detected include NO₃[•] and NO₂[•]. N₂ and O₂ not detectable.

^bCalculated from undetected H.

Measurements can be made as a function of residence time and temperature, yielding kinetic information for reactant destruction and product formation. Additional analysis using the GC-mass spectrometer would enable the determination of N₂ and O₂ as well as the validation of other volatiles detected by the FTIR. While this would allow more complete mass balances, the

impossibility of detecting the small quantities of H₂O produced in these reactions remains as an intrinsic barrier to a complete mass balance.

The addition of H₂O₂ as an oxidant in the SCWO of nitromethane radically changed the product composition and the destruction efficiency. The reaction of NM with a thirtyfold excess of oxidant under similar conditions (600 °C, 5400 psi) resulted in > 99.9 percent destruction of the NM and produced only CO₂ and small amounts of N₂O. These results are dramatically illustrated in the FTIR spectrum shown in Figure 30. Quantitative data for CO₂ production are summarized in Table 18. The measured and expected CO₂ values were determined as described for TNT, assuming complete conversion of the NM to CO₂ according to the following equation:



The first two experiments were performed with a 3-day old solution of NM in water whereas a freshly prepared solution was used for the latter two. Evaporation is the likely cause for the difference in the two sets of experiments. No other volatile products (i.e., CH₄ or CO) were detected. If such components are present they comprise less than 0.1 percent of the total carbon. The percentage of the nitrogen detected as N₂O is 4.5 percent. The remaining N likely occurs as N₂.

TABLE 18. CO₂ PRODUCTION IN THE SCWO OF NITROMETHANE

Exp.	P _{meas} ^a (torr)	P _{calc} ^b (torr)	%C detected
1	0.69	1.09	63
2	0.70	1.08	65
3	0.82	1.06	77
4	0.80	1.06	75

^aDetermined from integrated FTIR band intensities and CO₂ calibration curves.

^bCalculated from the ideal gas law assuming complete oxidation.

The carbon remaining in the aqueous effluent was analyzed and these results are summarized in Table 19. Under these conditions, very little of the initial carbon remains in the aqueous effluent. For NM reactions with oxidant, greater than 80 percent of the C was detected as CO₂, while only one percent was detected in solution. Without oxidant, 64 percent of the C was detected in the gas phase as CO₂, CO, and CH₄ and four percent of the C was detected in solution.

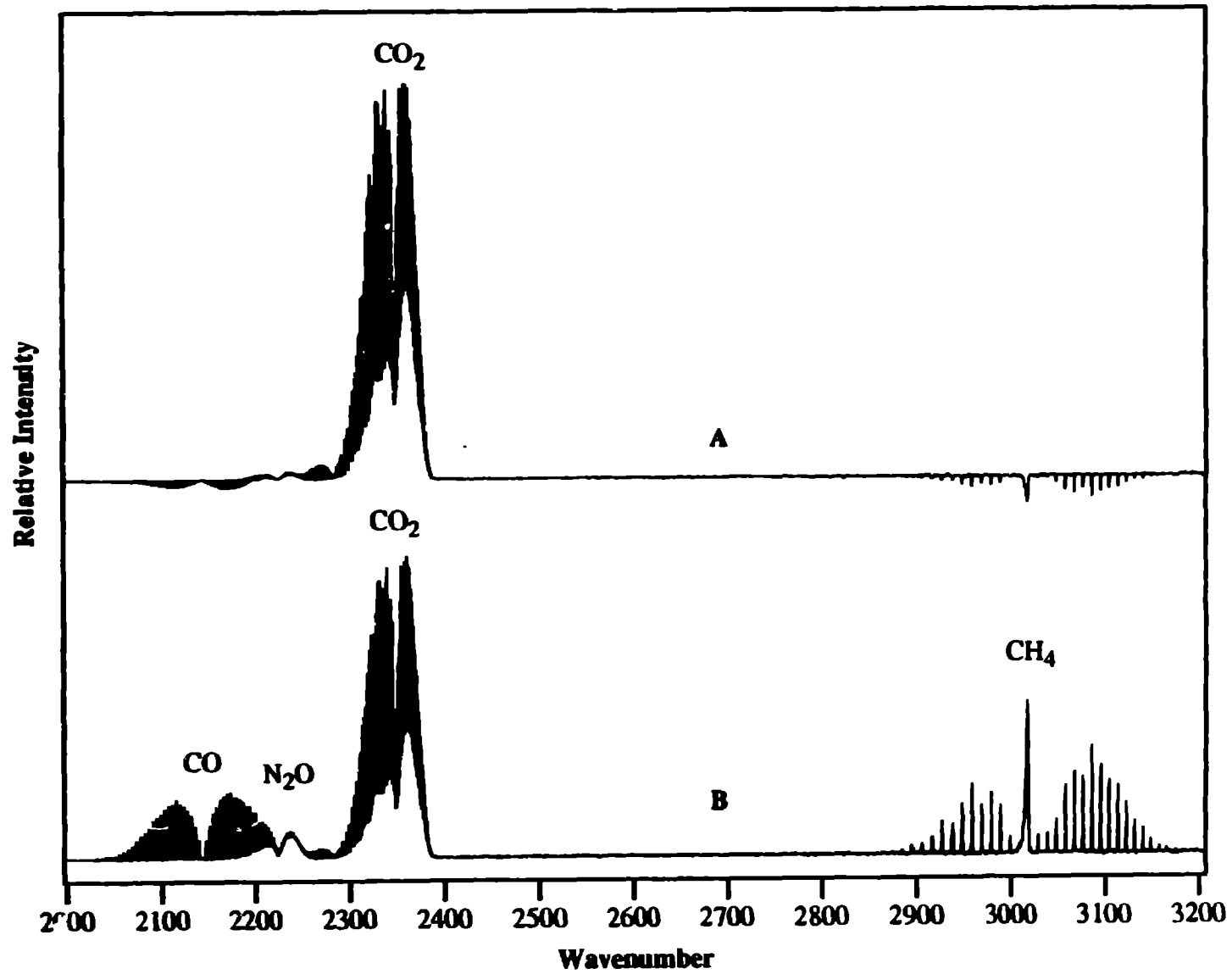


Figure 30. FTIR product analysis for the SCWO of NM at 600 C. (A) NM plus oxidant (H_2O_2); (B) NM without oxidant.

We cannot account for the "missing" C at present, but we suspect volatilization of the NM from the stock solution causing less than anticipated starting concentrations.

TABLE 19. ANALYSIS OF RESIDUAL CARBON IN AQUEOUS EFFLUENT FOR SCWO OF NM AT 600 °C

Solution	No. of Runs	[C] _i (ppm)	TIC (ppm) [‡]	TOC (ppm) [†]	%C
NM + H ₂ O ₂	4	85	0.2	0.8	1.2
NM + H ₂ O ₂	10	75	<0.1	0.5	0.8
NM	4	79	0.2	2.9	4

F. REACTIONS OF NITRATE

Nitrates are formed when explosives are oxidized in supercritical water. As discussed in previous sections, the amount of nitrogen converted to nitrate and nitrite depends upon the substrate and the reaction conditions. The chemistry of nitrogen appears to be more complicated than that of carbon in supercritical water. To produce an effluent which is free of NO_x⁻, the nitrogen chemistry needs to be understood. To gain a better understanding, we are studying the reactions of nitrates with simple organics in supercritical water. This work is partly sponsored by the Department of Energy's Office of Technology Development and has applications for the treatment of nitrate-containing radioactive wastes stored in underground tanks at the Hanford Reservation in Washington. In this section we discuss the reactions of nitrate with methanol in supercritical water.

Experiments were conducted in which nitrate was reacted with methanol. A 1:1 stoichiometry was assumed for the reaction. Experiments have been conducted at 25 degree intervals from 450 °C to 525 °C, and at 30.9 MPa (4500 psi). Residence times have ranged from 5 to 18 seconds. Figures 31 and 32 display nitrate and methanol decomposition as a function of temperature and residence time. Reaction conditions resulted in observed methanol destruction efficiencies ranging from 31% at 450 °C to 85% at 525 °C. Corresponding nitrate removals ranged from 15% to >99%. At 500 °C and above, ammonia appeared to be the predominate nitrogen species. Below 500 °C, nitrite was the predominant nitrogen species. Gas phase analysis (by GC) indicated the production of N₂, N₂O, and O₂. Gas phase analysis by FTIR showed that some samples contained trace amounts of NO. Carbon was recovered as an inorganic species, as determined by TIC analysis. This species was either carbonate or bicarbonate, depending on the pH of the effluent stream. Effluent pH values were neutral to basic (7 - 10). No carbon products

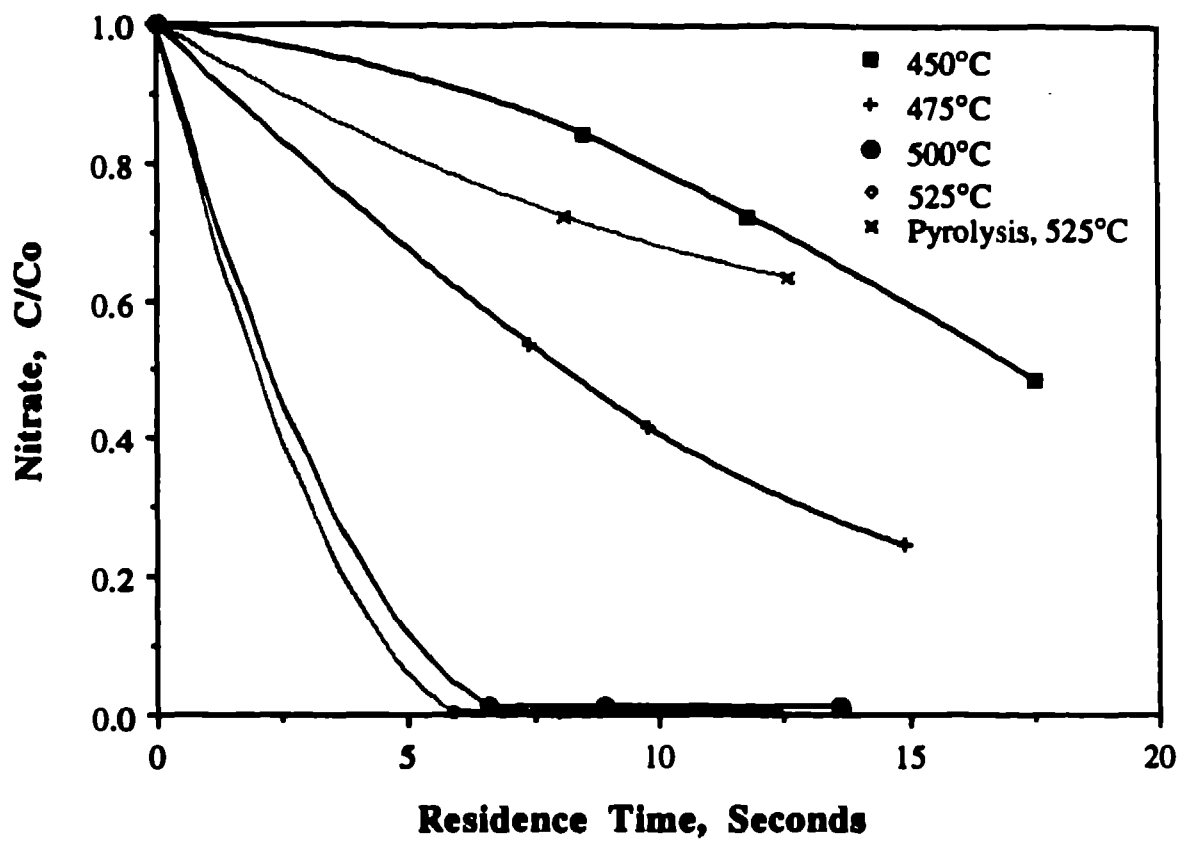


Figure 31. Nitrate removal as a function of temperature and residence time.
Lines drawn to aid in viewing.

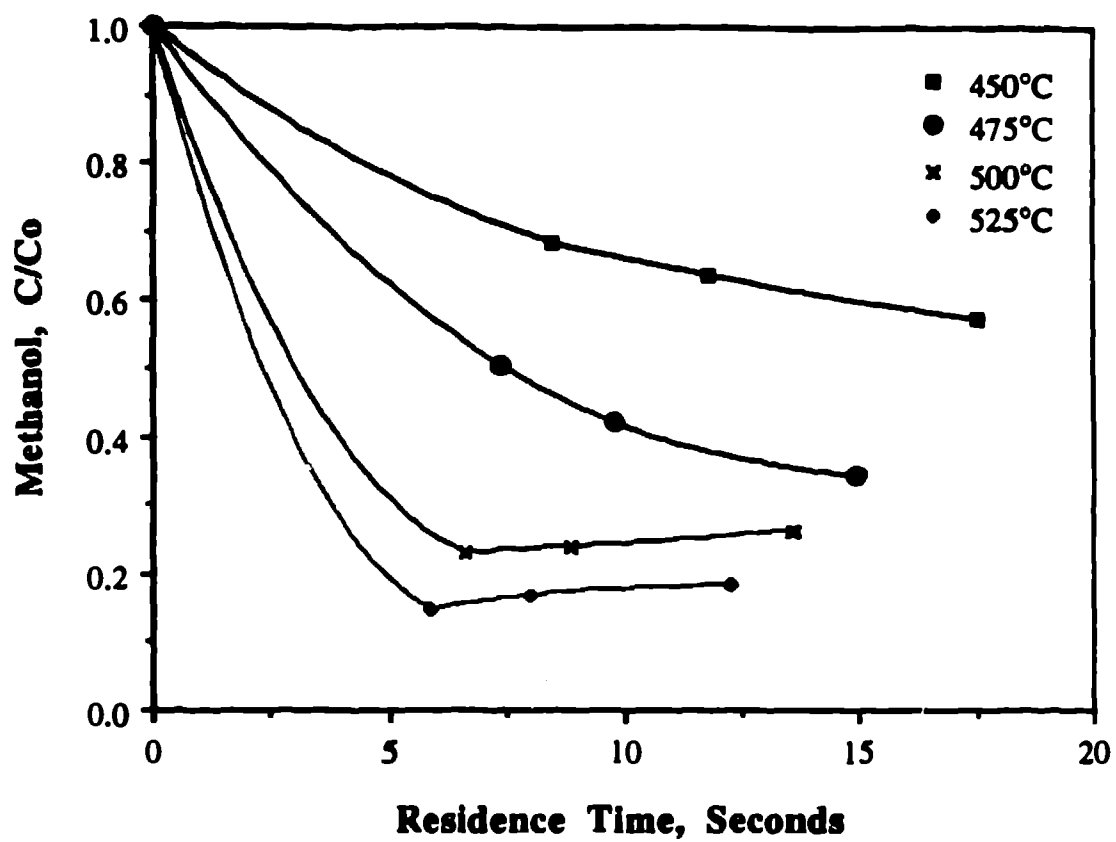


Figure 32. Methanol removal as a function of temperature and residence time.
Lines drawn to aid in viewing.

of incomplete combustion (CO , CH_4) were detected in the gas phase. Trace amounts of CO_2 were detected by FTIR in several gas samples.

A nitrate pyrolysis run was also conducted. At $525\text{ }^\circ\text{C}$ and a 12.6 second residence time, a maximum nitrate conversion (to nitrite) of 36% was observed. No ammonia was detected in nitrate pyrolysis at $525\text{ }^\circ\text{C}$. For all experiments, mass recoveries for nitrogen and carbon have been $100\% \pm 10\%$.

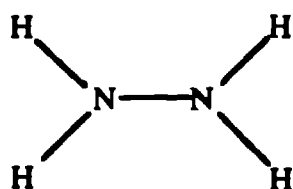
In addition to carbon and nitrogen species, aqueous effluent and reactor rinse samples were also analyzed for sodium (present in the sodium nitrate feed) and corrosion products (Fe, Cr, Mo, and Ni). Trace amounts of corrosion products were recovered in all experiments. While iron and nickel have appeared only at sub-ppm levels in all experiments, chromium and molybdenum have been present in both effluent and rinse water samples. At temperatures above $500\text{ }^\circ\text{C}$, these species have been recovered primarily in reactor rinse water samples. These samples, which were yellow tinted, are believed to contain the hexavalent forms of chromium (CrO_4^{2-}) and molybdenum (MoO_4^{2-}). These species likely deposited on the reactor walls as sodium precipitates. Sodium also precipitated substantially with carbonate species. These precipitation reactions are supported by ion balances performed on reactor rinse samples. Such balances have been successful in predicting measured pH values to within one pH unit. Effluent concentrations of sodium, bicarbonate, chromium, and molybdenum decreased with increasing temperatures, which indicated decreasing solubilities with increasing temperatures. The absence of iron and nickel indicated that these metals formed a passivating oxide film on the reactor surface, which was insoluble in water rinses.

Future studies funded by the DOE will investigate the kinetics of the $\text{MeOH} / \text{NO}_3^-$ reaction in more detail. These will include additional experiments at different residence times and temperatures. Different stoichiometries will be investigated. Also, further studies of nitrate and methanol pyrolysis will be conducted. Other experiments, such as reactions of sodium nitrite with methanol, and reactions of nitrate with a different organic compound are being considered for the understanding of kinetic mechanisms.

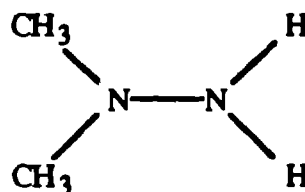
G. REACTIONS OF HYDRAZINE

1. Introduction

This section summarizes the experiments on the supercritical water reactions of hydrazine and unsymmetrical dimethylhydrazine (UDMH). Hydrazine and UDMH are important rocket propellants, the structures of which are given below. In particular they find use as flight control thrusters which are actuated for short periods of time. With special catalysts they can decompose in milliseconds providing very precise attitude control. Both these propellants present special hazards in handling and disposal. Neat solutions may spontaneously ignite in air and both are suspect carcinogens. The break down products of UDMH using conventional destruction techniques are undesirable (Reference 11). In particular, dimethyl nitrosoamine which is a carcinogen, is produced by incineration of UDMH.



Hydrazine



Unsymmetrical dimethylhydrazine

Hydrazine and UDMH are both clear liquids and completely miscible in water at all temperatures. In water, the auto-ignition problem is abated and the resultant mixture is very suitable for destruction using the hydrothermal processing techniques described in this report. Because of the solubility characteristics, though, problems associated with solid explosives such as HMX, RDX and TNT are not an issue. Thus, even with our bench-scale reactors we have demonstrated large processing capabilities using up to one weight percent solutions.

We have studied the pyrolysis and oxidation reactions of hydrazine and UDMH in supercritical water using both hydrogen peroxide and nitrate from nitric acid or sodium nitrate as oxidants. Table 20 summarizes the product formation for these reactions.

TABLE 20. SUMMARY OF HYDRAZINE AND UDMH SCWO REACTIONS

Reaction	Major Products	Minor Products
N_2H_4 + no oxidizer	N_2, H_2, NH_3, NH_4^+	
N_2H_4 + H_2O_2	N_2	$N_2O, NH_4^+, NO_3^-, NO_2^-$
N_2H_4 + HNO_3	N_2, N_2O	NH_4^+, NO_3^-, NO_2^-
N_2H_4 + $NaNO_3$	$N_2, N_2O, NaOH$	NH_4^+, NO_3^-, NO_2^-
$(CH_3)_2N_2H_2$ (fuel rich)	CO_2, N_2	$N_2O, CO, CH_4, NH_4^+,$ amines
$(CH_3)_2N_2H_2$ (fuel lean)	CO_2, N_2	$N_2O, NO_3^-, NO_2^-, CO_3^{2-}$

Under oxidizing conditions the primary products are relatively innocuous, consisting of various amounts of nitrogen, nitrous oxide and also CO_2 in the case of UDMH (see following discussions). Under fuel rich conditions, incomplete combustion products resulted.

The destruction of the parent compound was essentially complete. In every experiment the destruction efficiency was better than 99.999%, with or without oxidizer. Table 21 shows the measured destruction efficiency for hydrazine and UDMH. These numbers are for the destruction of a 0.5 wt% solution, and represent lower limits due to our limits of detection (0.01 ppm).

TABLE 21. DESTRUCTION EFFICIENCIES FOR THE SCWO OF HYDRAZINE AND UDMH

Species	Destruction (%)
N_2H_4	>99.9998
$(CH_3)_2N_2H_2$	>99.9998

2. Experimental

All the results reported in this section were from experiments conducted in the gold-lined reactor described in Section II.A. Some experiments were conducted in a similar reactor constructed of C-276, but severe corrosion was observed when HNO_3 or $NaNO_3$ was used as the oxidizer. (See section VII.B.4.) For our purposes, the gold liner minimizes chemistry due to wall reactions. For these experiments the reactor was kept at a constant temperature of $600^\circ C$, 340 atm,

and a total flow rate of 4 ml/min. This provides a reaction residence time of approximately 11 seconds. The fuel and oxidizer were mixed cold using two HPLC pumps running at 2 ml/min. For mass balance calculations and to ensure desired fuel:oxidizer ratios the weight loss of the fuel and oxidizer mixtures was monitored continuously using Percisa 3000D top-loading balances.

Both hydrazine and UDMH solutions were prepared at concentrations of 1 weight-percent (wt%) for all runs except the isotopic comparisons with $H^{14}NO_3$ and $H^{15}NO_3$, which were prepared at 0.25 wt%. When mixed with the oxidizer stream in the reactor, the effective concentration was halved. This relatively high loading caused high rates of gas production, necessitating the redesign of the gas/liquid separator to accommodate larger volumes.

The gas phase effluent was analyzed using the combination of gas chromatography set up to quantify N_2 , N_2O , O_2 , CO_2 , CO , H_2 , and CH_4 , FTIR spectroscopy with 0.5 cm^{-1} resolution, and mass spectroscopy. The liquid effluent was routinely analyzed for nitrates, nitrites, ammonium, and TIC and TOC in the case of UDMH. Metals analysis was performed, but very few corrosion products observed.

3. Hydrazine Reactions

Several experiments investigating the destruction of hydrazine were conducted. These experiments included hydrazine pyrolysis (no oxidizer), and reaction with an oxidizer, either hydrogen peroxide or nitric acid. Based on our previous results with explosives, a large excess of oxidizer leads to a high concentration of nitrate and nitrite in solution. Therefore, the oxidizer in these experiments did not exceed twice stoichiometric as defined by the reaction equations to follow. Tables 22 and 23 show the product analysis of these experiments. The equivalence ratio (ϕ) is given by the ratio of the stoichiometric oxidizer concentration to the actual concentration as defined by the equation corresponding to the specified reaction.

TABLE 22. HYDRAZINE NITROGEN MASS-BALANCE (AS A % OF THE STARTING NITROGEN CONCENTRATION)

Species	Pyrolysis	H ₂ O ₂ Ø=1	H ₂ O ₂ Ø=0.5	HNO ₃ Ø=1
N ₂	60	98	94	78
N ₂ O	0	0.1	0	21
NH ₃	not quantified	0	0	0
NH ₄ ⁺	29	1.0	0	0.2
NO ₃ ⁻	0	0.1	0.1	0.0
NO ₂ ⁻	0	0.1	0	0.2
Total	89	99.3	94.1	99.4

TABLE 23. HYDRAZINE HYDROGEN MASS-BALANCE, PYROLYSIS (AS A % OF THE STARTING HYDROGEN CONCENTRATION)

Species	pyrolysis	pyrolysis
H ₂	19	19
NH ₃	not quantified	16 (estimated)
NH ₄ ⁺	44	44
Total	63	79

a. Hydrazine Pyrolysis

Hydrazine is effectively destroyed (Table 21, page 77) in hot, high pressure water in less than 11 seconds. However, without oxidizer present, large amounts of NH₃/NH₄⁺ and H₂ are observed. Ammonia is probably the major product of the pyrolysis of hydrazine and is in equilibrium with NH₄⁺ through the reaction H₂O + NH₃ → NH₄⁺ + OH⁻. Nitrogen and NH₄⁺ are detected in nearly equal molar ratios. Ammonia is observed in the FTIR spectrum shown in Figure 33. A small background of CH₄, which is due to reduction of char left over from previous experiments, has been subtracted from this spectrum. Because NH₃ appears to be sticking to the wet walls of our manifold we are unable to quantify this species, thus unable to achieve a nitrogen or hydrogen mass balance. If we assume that all undetected nitrogen is NH₃, then the hydrogen mass balance becomes 79%.

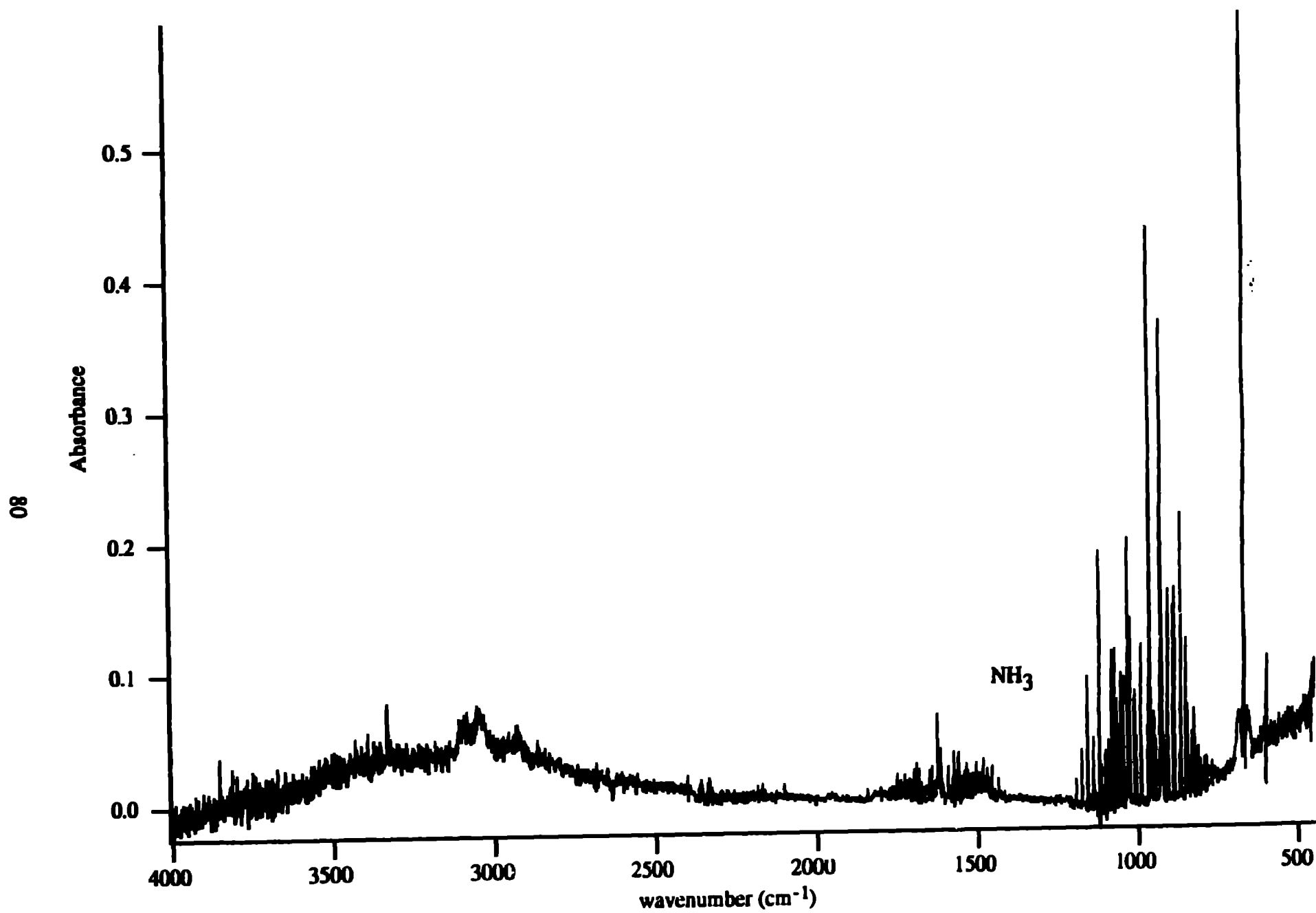
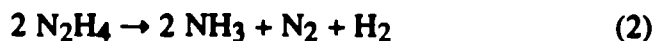


Figure 33. FTIR spectrum of gas effluent from Hydrazine pyrolysis, primarily ammonia (NH₃).

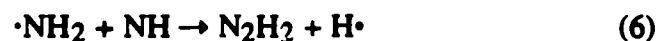
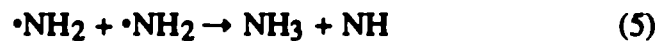
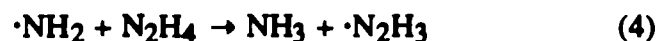
Typical global models for hydrazine pyrolysis are represented by reaction 1 and 2 (References 13-19).



Since we have not obtained a mass balance for the hydrazine pyrolysis a global reaction stoichiometry can not be determined, but probably is a combination of reactions 1 and 2. The N-N bond of hydrazine is weaker than the N-H bond (70.8 Kcal/mole and >100 Kcal/mole, respectively) (Reference 12), thus the first elementary step in the pyrolysis of hydrazine is most likely to be (References 13-19)



followed by elementary steps such as:



These and related radical reactions are likely to dominate the chemistry under the low density conditions employed. At 600°C and 340 atm the water density is approximately 0.15 g/cc. Higher densities may support ionic chemistry leading to different products. The nitrogen chemistry is quite complex. Many of the postulated intermediates have not been observed nor have the reaction rates been measured in previous gas phase studies (References 13-20). Based on current understanding of gas phase reaction mechanisms (Reference 20), we postulate a simplified mechanism as shown in Figure 34.

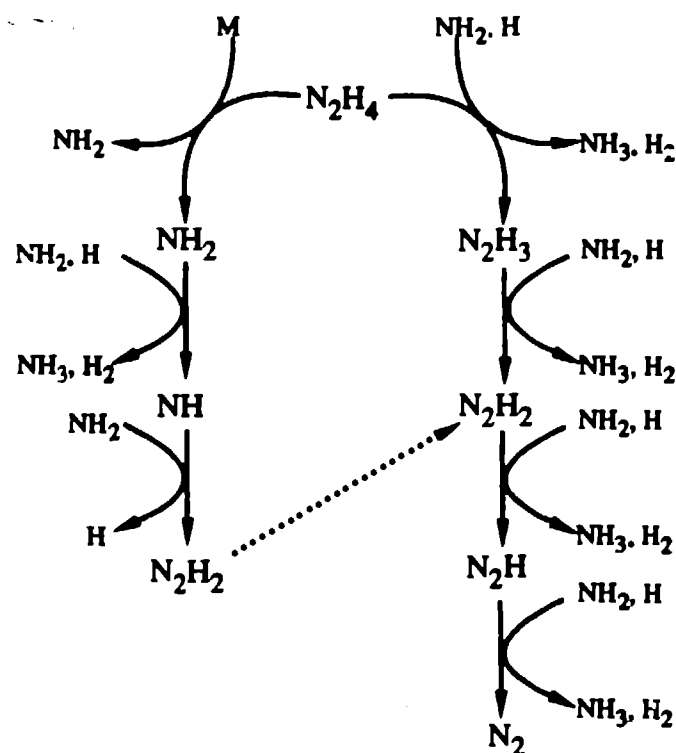


Figure 34. Proposed hydrazine decomposition mechanism in supercritical water.

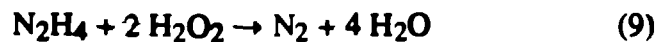
Each step is a hydrogen abstraction accomplished by reactions such as 7 and 8 leading to observed final products NH_3 , H_2 and N_2 .



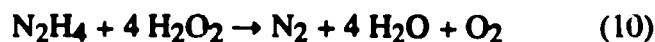
We observed virtually no oxygenated products of nitrogen leading us to believe that water plays little role in the decomposition of hydrazine under these conditions.

b. Hydrazine Reaction with Hydrogen Peroxide

With the addition of an oxidizer in the form of hydrogen peroxide no incomplete combustion products are observed. The only major product is nitrogen (Table 22, page 79). The amount of nitrate and nitrite in the liquid effluent and of N_2O in the gas produced were more than two orders of magnitude smaller than the amount of N_2 produced. Two ratios of fuel-to-oxidizer were run based on a stoichiometric case given in reaction equation 9.



Reaction equation 10 is an equivalence ratio of 0.5 and represents a fuel lean case.



By normalizing the moles of product obtained to the number of moles of hydrazine reactant we can show that these global reactions (9 and 10) reflect reality (see Tables 24 and 25).

TABLE 24. HYDRAZINE + H₂O₂ PRODUCT RATIOS, $\phi = 1$

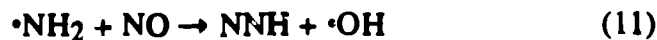
	N ₂ H ₄	N ₂	O ₂
expected	1	1	0
actual	1	0.98	0.03

TABLE 25 HYDRAZINE + H₂O₂ PRODUCT RATIOS, $\phi = 0.5$

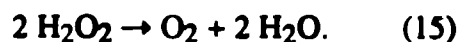
	N ₂ H ₄	N ₂	O ₂
expected	1	1	1
actual	1	0.94	1.05

Other than releasing excess oxygen, the addition of excess oxidizer to hydrazine has essentially no effect or benefit. The FTIR spectrum had only trace amounts of N₂O in the $\phi=1$ case and no infrared active products in the $\phi=0.5$ case. In both cases the nitrogen mass balance obtained (Table 22, page 79) was quite reasonable.

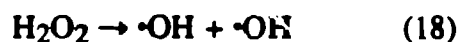
Miller, in his paper on the oxidation of ammonia in flames (Reference 20), shows NO as an important intermediate (and product) leading to the formation of N₂. For example, reactions such as



all play a major role in the formation of the nitrogen final product. In our study we have never observed NO as an end product in the oxidation of N₂H₄. The lower temperatures in the SCWO reactor vs. that of a flame do not promote the formation of NO. We therefore postulate that N₂H₄ oxidizes primarily by OH radical abstraction of hydrogen atoms. The oxidizer, hydrogen peroxide, supplies O₂ to the reaction by quickly reacting in warm water by reaction 15



The initiation step is probably reaction 2, the cleavage of the weak N-N bond of hydrazine. The following three elementary steps are responsible for the formation of a large hydroxyl radical pool:



These hydroxyl radicals proceed to abstract hydrogen atoms from nitrogen containing intermediates eventually forming nitrogen. The abstraction reaction is:



where R is N₂H₃, N₂H₂, N₂H etc. as seen in Figure 34, page 82. Since neither H₂ nor NH₃/NH₄⁺ were observed in this reaction, the OH radical abstraction of hydrogen atoms from all radicals is probably the dominate pathway. The formation of H₂ and NH₃ is suppressed by reaction of $\cdot\text{NH}_2$ and $\text{H}\cdot$ with $\cdot\text{OH}$. Hydroxyl radical abstraction of hydrogen atoms may also be faster than H₂N-NH₂ bond cleavage, suppressing NH₂ radical formation. The oxidation of hydrazine with hydrogen peroxide in SCW reactors appears to be an excellent method for its destruction, producing only the benign products N₂ and H₂O.

c. Hydrazine Reactions with Nitric Acid

Nitrogen tetroxide (N₂O₄) is an oxidizer typically used with hydrazine and dimethylhydrazine in liquid fueled rockets. It would be convenient to use N₂O₄ as the oxidizer in the SCWO process since it is stored close proximity to the fuel. Nitrogen tetroxide disproportionates into nitric and nitrous acid (HNO₃ and HNO₂) when placed in water. Therefore, the use of nitric and nitrous acid as oxidizers in reactions with hydrazine is essentially equivalent to

the use of N_2O_4 as the oxidizer in aqueous solution. This section will describe our results using nitric acid (HNO_3) and isotopically labeled nitric acid ($H^{15}NO_3$) to oxidize hydrazine in SCW.

Table 22, (page 79) shows the mass balance results when using normal HNO_3 as the oxidizer for the destruction of hydrazine in SCW. All the conditions were identical with the previous experiments discussed ($600^\circ C$, 340 atm, 11 sec residence times) except that in this case we only used a 0.25 wt% hydrazine feed solution. A major difference in the HNO_3 combustion chemistry was immediately noticed. Nitrous oxide gas was produced in large quantities (approximately 20% of the gas phase effluent) in stark contrast to oxidation with hydrogen peroxide, where the only product was nitrogen. The nitrogen mass balance obtained was good (Table 22, page 79) and hydrazine was destroyed with >99.9992% efficiency. Virtually no NO_3^- remained in the liquid effluent and only 0.2% of the starting nitrogen ended up as NO_2^- . Equimolar mixtures of N_2H_4 and HNO_3 were used in this experiment. The results show that this case is slightly fuel lean. We might expect much higher liquid effluent concentrations for fuel:oxidizer ratios less than one. However, since hydrazine was destroyed to relatively benign products, excess oxidizer is unnecessary.

A global reaction equation that comes close to predicting the product distribution is given in equation 20. Table 26 shows the actual product distributions normalized to the starting hydrazine concentration.



TABLE 26. HYDRAZINE + HNO_3 PRODUCT RATIOS

	N_2H_4	N_2	N_2O	O_2
expected	1	1.2	0.3	.1
actual	1	1.17	0.31	0.03

To investigate further this new chemistry with the NO_3^- oxidizer, an identical experiment was run using the ^{15}N isotopically substituted HNO_3 . This compound was obtained from Aldrich at a concentration of 40 wt% in water and 98% isotopic purity. Since the objective of this experiment was to follow the nitrogen, we did not attempt to measure mass balance. Mass spectroscopy and FTIR spectroscopy provided the definitive diagnostics for comparison between the $H^{14}NO_3$ and $H^{15}NO_3$ experiments.

Figure 35 is the mass spectrum between 0 and 50 amu of the gas effluent from the $H^{14}NO_3$ experiment. This spectrum can easily be simulated using known cracking patterns for N_2 and N_2O (which are instrument dependent) and the measured $N_2:N_2O$ gas ratio. Table 27 presents a qualitative analysis of the mass spectra.

TABLE 27. MASS SPECTRUM ASSIGNMENTS OF FIGURES 35 AND 36

Mass Number	Assignment N = ^{14}N	Comments
14	N	Cracking from N_2 and N_2O
15	^{15}N	Isotopic N cracking from N_2 and N_2O
16	O	Cracking from O_2
17	OH	Cracking from water
18	H_2O	Residual reactor water
28	N_2	N_2 parent peak and cracking from N_2O
29	$N^{15}N$	Isotopic N_2 and cracking from N_2O
30	NO, $^{15}N_2$	Cracking from N_2O or isotopic N_2
31	^{15}NO	Isotopic NO cracking from N_2O
32	O_2	Excess oxygen from reactor
44	N_2O	N_2O parent peak
45	$N^{15}NO$ / ^{15}NNO	Isotopic N_2O
46	$^{15}N_2O$	Isotopic N_2O

Figure 36 is the mass spectrum for the $H^{15}NO_3$ experiment. Table 27 also assigns these peaks. First note that the $^{14}N:^{15}N$ ratio in this experiment is 2:1, given the equimolar starting ratio of hydrazine and isotopic nitric acid. As expected, this 2:1 ratio is preserved in the mass spectrum of the products as seen from the ratios of mass numbers 14 and 15 ($^{14}N:^{15}N$) or the mass numbers 28 and 29 ($^{14}N^{14}N:^{14}N^{15}N$). Second, almost all of the nitrous oxide formed was labeled with one ^{15}N (mass number 45), i.e. 99% of the nitrogens came from nitric acid. Third, mass peaks 28 and 29 are nearly the same integrated area when the small contribution from $^{14}N^{15}NO$ cracking is subtracted. This implies two reaction pathways of comparable magnitude leading to the formation of nitrogen.

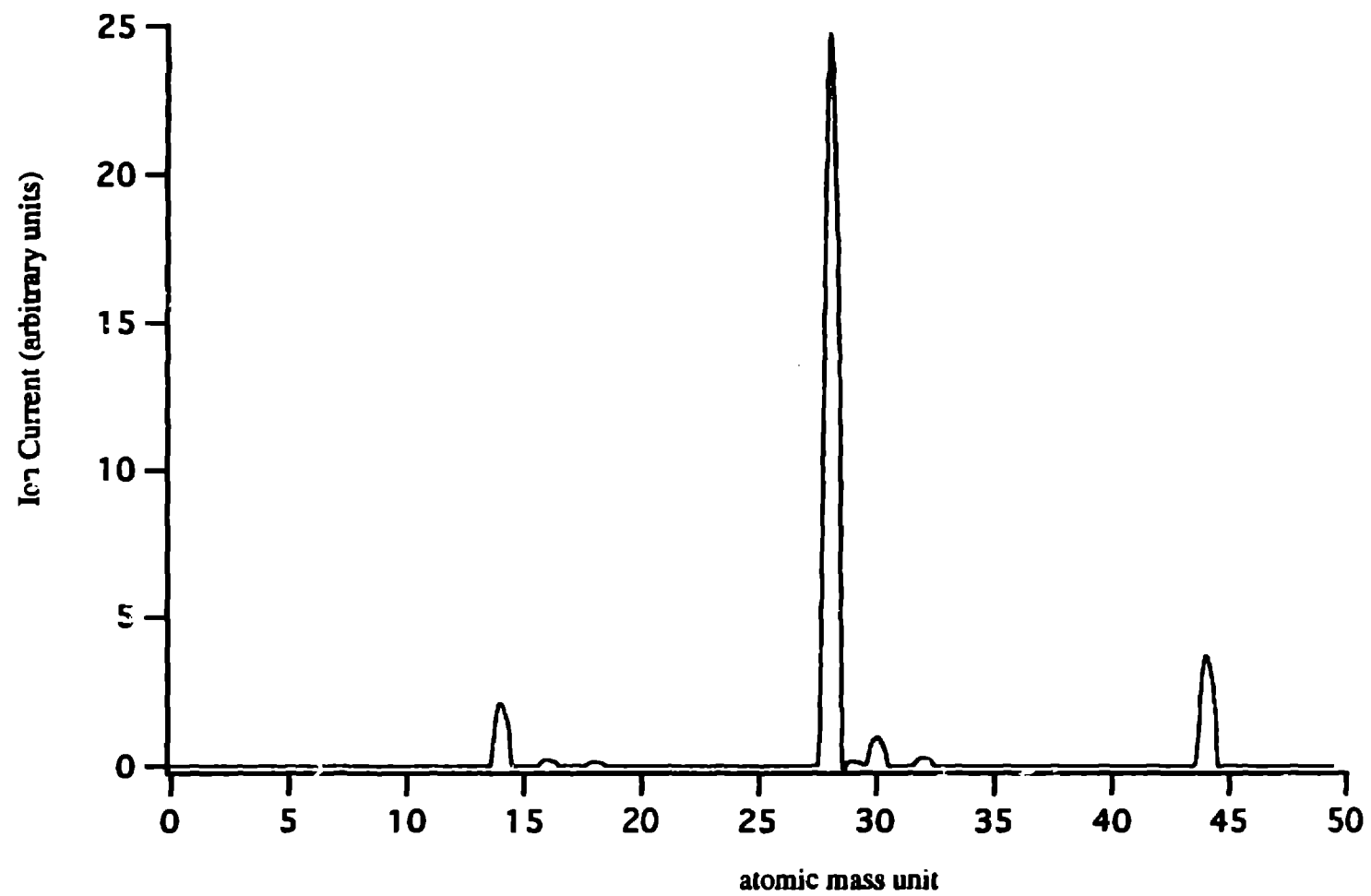


Figure 35. Mass spectrum of the gas effluent resulting from the SCWO of hydrazine with $H^{14}NO_3$.

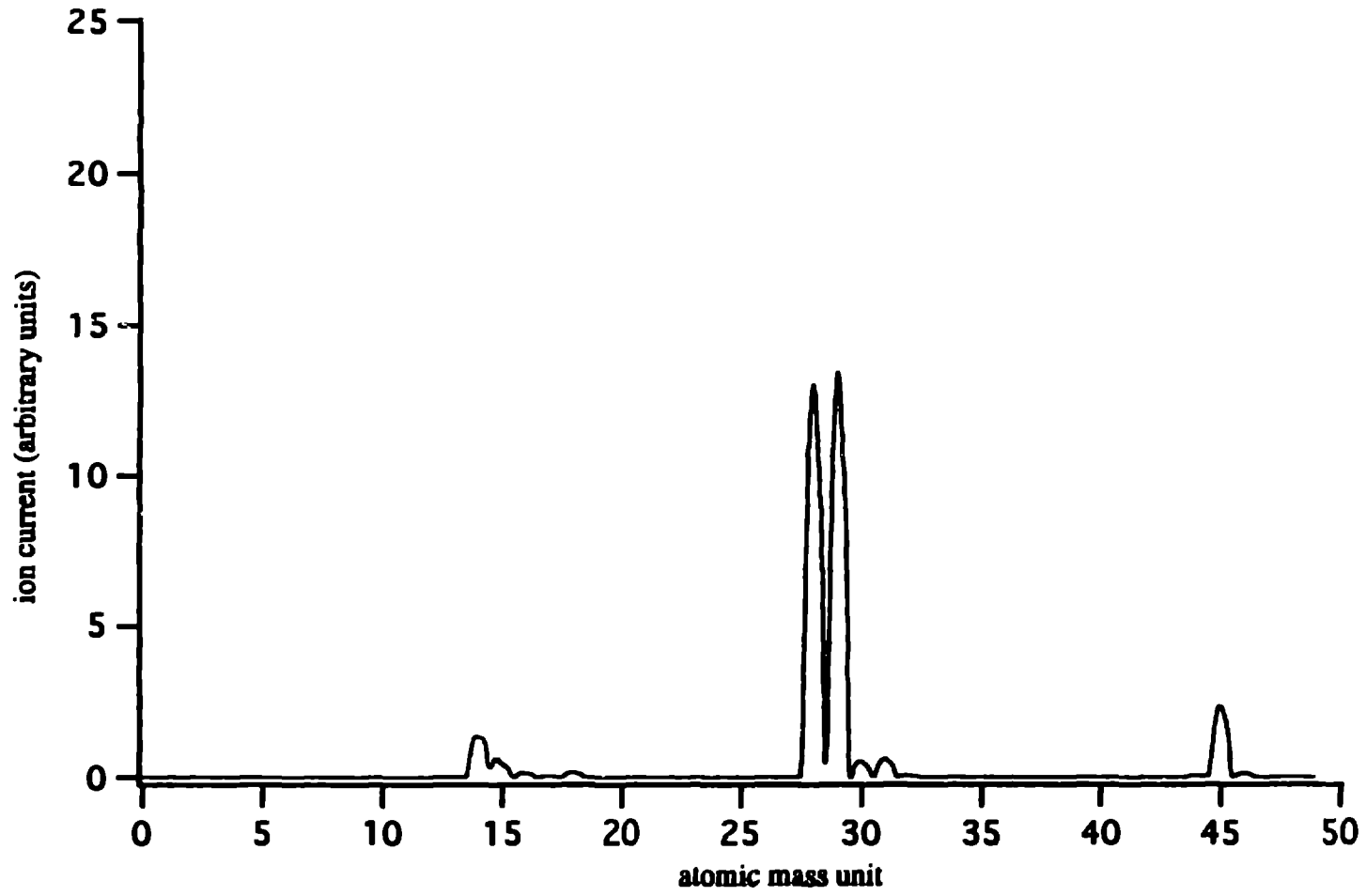


Figure 36. Mass spectrum of the gas effluent resulting from the SCWO of hydrazine with H^{15}NO_3 .

We can determine explicitly that we have $^{14}\text{N}^{15}\text{N}^{16}\text{O}$ and not $^{15}\text{N}^{14}\text{N}^{16}\text{O}$ from the FTIR spectra, Figures 37 and 38. Figure 37 covers the entire infrared spectrum of the gas effluent and compares the SCWO of hydrazine with H^{14}NO_3 (a) and H^{15}NO_3 (b). The only infrared active gas was N_2O after subtraction of trace quantities of CO_2 due to the combustion of char from previous experiments. Each vibrational mode in Figure 37 b exhibits an isotopic shift consistent with a $^{14}\text{N}^{15}\text{N}^{16}\text{O}$ molecule (Reference 21). Figure 38 a is the spectrum expanded around the $0110-0000$ Q-branch region of N_2O . If any $^{15}\text{N}^{14}\text{N}^{16}\text{O}$ existed it would appear near the arrow drawn in the bottom trace. This implies that the N-O bond in nitric acid stays intact during the formation of nitrous oxide. There are small amounts of $^{14}\text{N}^{14}\text{N}^{16}\text{O}$ and $^{15}\text{N}^{15}\text{N}^{16}\text{O}$ in the mass and FTIR spectra, indicating that other minor reaction channels do exist.

The oxidation of hydrazine with nitric acid seems to be very complex. One possible explanation for the observed reaction products may be a reaction scheme such as:



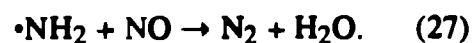
where the sequence would start with HNO_3 producing hydroxyl radicals and NO_2 . The hydroxyl radicals would feed into the N_2H_4 oxidation mechanism as discussed previously, again inhibiting the $\text{H}_2\text{N-NH}_2$ bond cleavage favoring hydrogen abstraction leading to the formation of N_2 , or in this case $^{14}\text{N}^{14}\text{N}$. The NO_2 could either react as in reaction 23, or go into a different reaction loop which also acts to abstract the hydrogen



atoms from hydrazine (reaction 25). Summing reactions 21 and 22 gives the general reaction 24. The chemical cycle represented by reactions 24 and 25 would ultimately



produce ^{15}NO and again $^{14}\text{N}^{14}\text{N}$. The labeled NO would form the $^{14}\text{N}^{15}\text{N}$ and $^{14}\text{N}^{15}\text{NO}$ products observed in the mass spectrum by reactions such as:



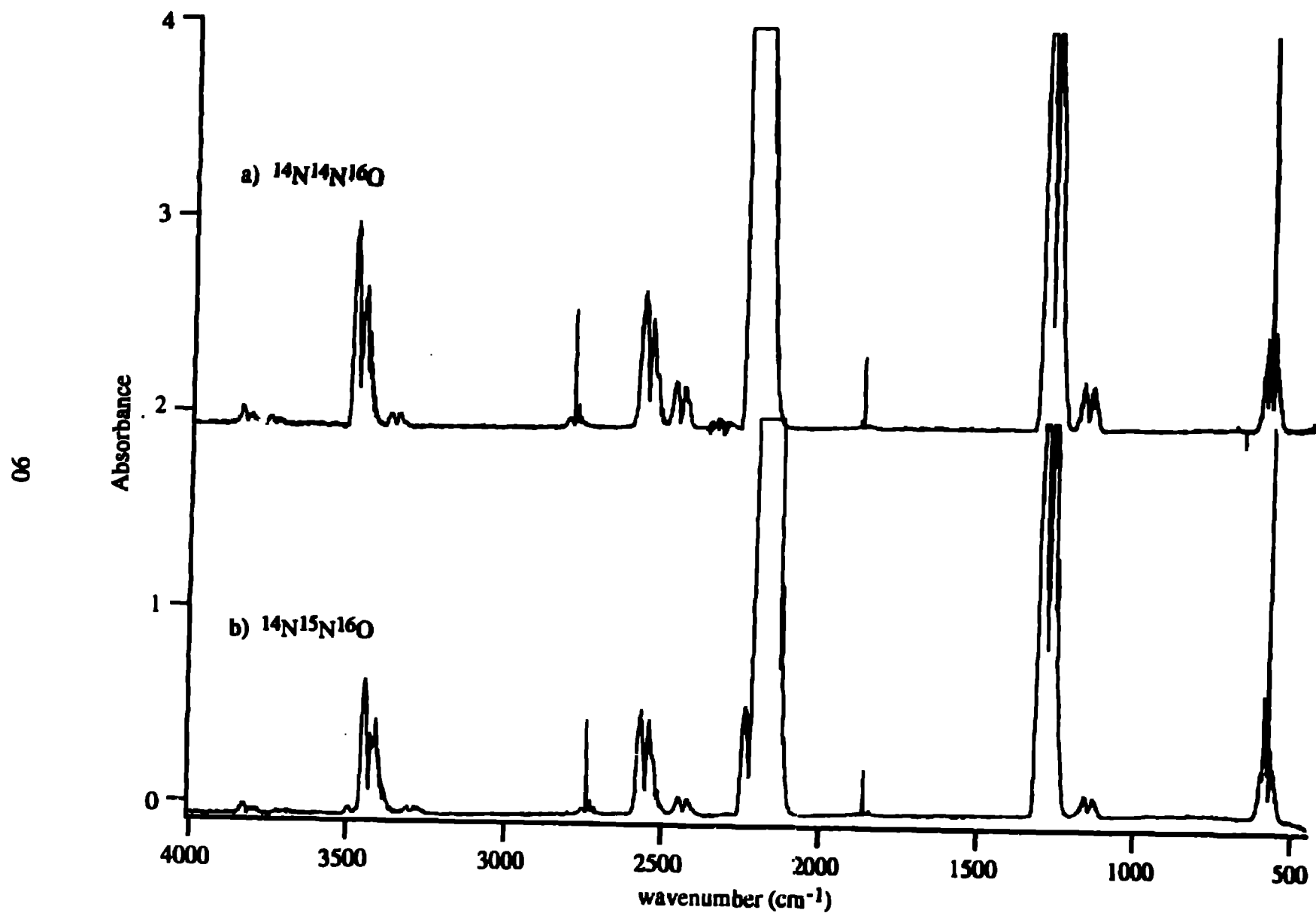


Figure 37. FTIR spectrum of gas effluent from a) SCWO of hydrazine with H¹⁴NO₃ and b) SCWO of hydrazine with H¹⁵NO₃. These spectra show only nitrous oxide (N₂O).

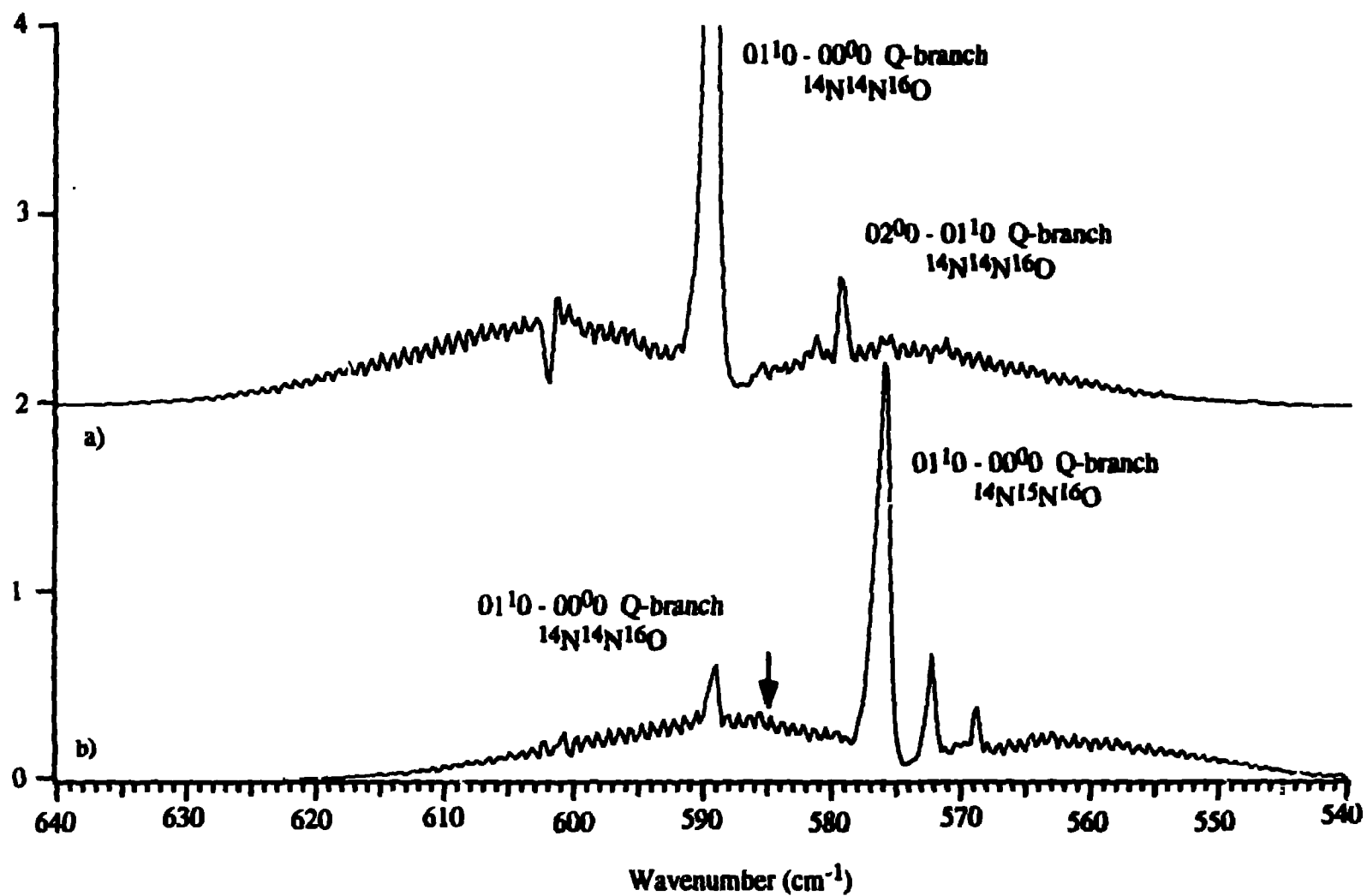
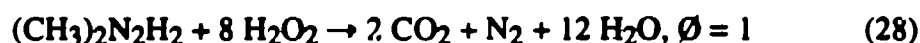


Figure 38. Expansion of $01^{10}-00^{00}$ Q-branch region around 600 cm^{-1} of Figure 37. The arrow indicates where $^{15}\text{N}^{14}\text{N}^{16}\text{O}$ species would appear if it were present in the sample.

Nitrous oxide may also react by numerous pathways to form the $^{14}\text{N}^{15}\text{N}$. If this reaction had been carried out for longer times it is possible that all the N_2O would have been converted to N_2 . This oxidizer (and therefore N_2O_4) may also be an excellent choice for the conversion of hydrazine to benign products. Experiments reacting hydrazine with nitrous acid (HNO_2) have yet to be explored.

4. Unsymmetrical Dimethylhydrazine Reactions

The destruction of unsymmetrical dimethylhydrazine in SCW was investigated. These experiments included UDMH added to hydrogen peroxide at different stoichiometric ratios. One pyrolysis experiment (no oxidizer) was done, but unidentified, and perhaps undesirable products resulted, so these experiments were discontinued. As with hydrazine, these experiments did not exceed twice stoichiometric as defined by the following reaction equations.



Tables 28 and 29 summarize the product analyses of these experiments.

TABLE 28. UNSYMMETRICAL DIMETHYLHYDRAZINE NITROGEN MASS BALANCE (AS A % OF STARTING NITROGEN CONCENTRATION)

Species	$\text{H}_2\text{O}_2, \phi=1$	$\text{H}_2\text{O}_2, \phi=0.5$
N_2	60.8	100.3
N_2O	0.3	1.1
NH_3	not quantified	0
NO	detected (FTIR)	0
NH_4^+	0.8	0
NO_3^-	0.7	1.8
NO_2^-	0.2	0.5
Total	62.8	103.7

TABLE 29. UNSYMMETRICAL DIMETHYLHYDRAZINE CARBON MASS-BALANCE (AS A % OF STARTING CARBON CONCENTRATION)

Species	H ₂ O ₂ , $\phi=1$	H ₂ O ₂ , $\phi=0.5$
CO ₂	96.1	91.7
CO	0.2	0
CH ₄	0.5	0
TIC	1.7	1.2
TOC	<0.03	<0.03
Total	98.5	92.9

Figure 39 compares the FTIR spectra of these two experiments. Apparently the reaction as written in equation 28 is not sufficient to cause complete combustion. Although the carbon was oxidized to CO₂ with good efficiency (Table 29), the nitrogen balance was very low. We suspect, based on the cation HPLC analysis, that there may also be mono or dimethyl amines remaining in the liquid effluent, in addition to unquantified ammonia gas. With the addition of excess oxidizer the reaction is driven to completion, the major products being N₂ and CO₂. Tables 30 and 31 show the exact product ratios.

TABLE 30. PRODUCT RATIO NORMALIZED TO THE STARTING (CH₃)₂N₂H₂ CONCENTRATION, $\phi=1$

	(CH ₃) ₂ N ₂ H ₂	CO ₂	N ₂
expected	1	2	1
actual	1	1.92	0.61

TABLE 31. PRODUCT RATIO NORMALIZED TO THE STARTING (CH₃)₂N₂H₂ CONCENTRATION, $\phi=0.5$

	(CH ₃) ₂ N ₂ H ₂	CO ₂	N ₂	O ₂
expected	1	2	1	4
actual	1	1.83	1.01	4.06

An important point is that dimethyl nitrosoamine ((CH₃)₂NO₂) was not observed in any oxidation runs of UDMH. Destruction efficiencies were 99.9998% or better (Table 21, page 77).

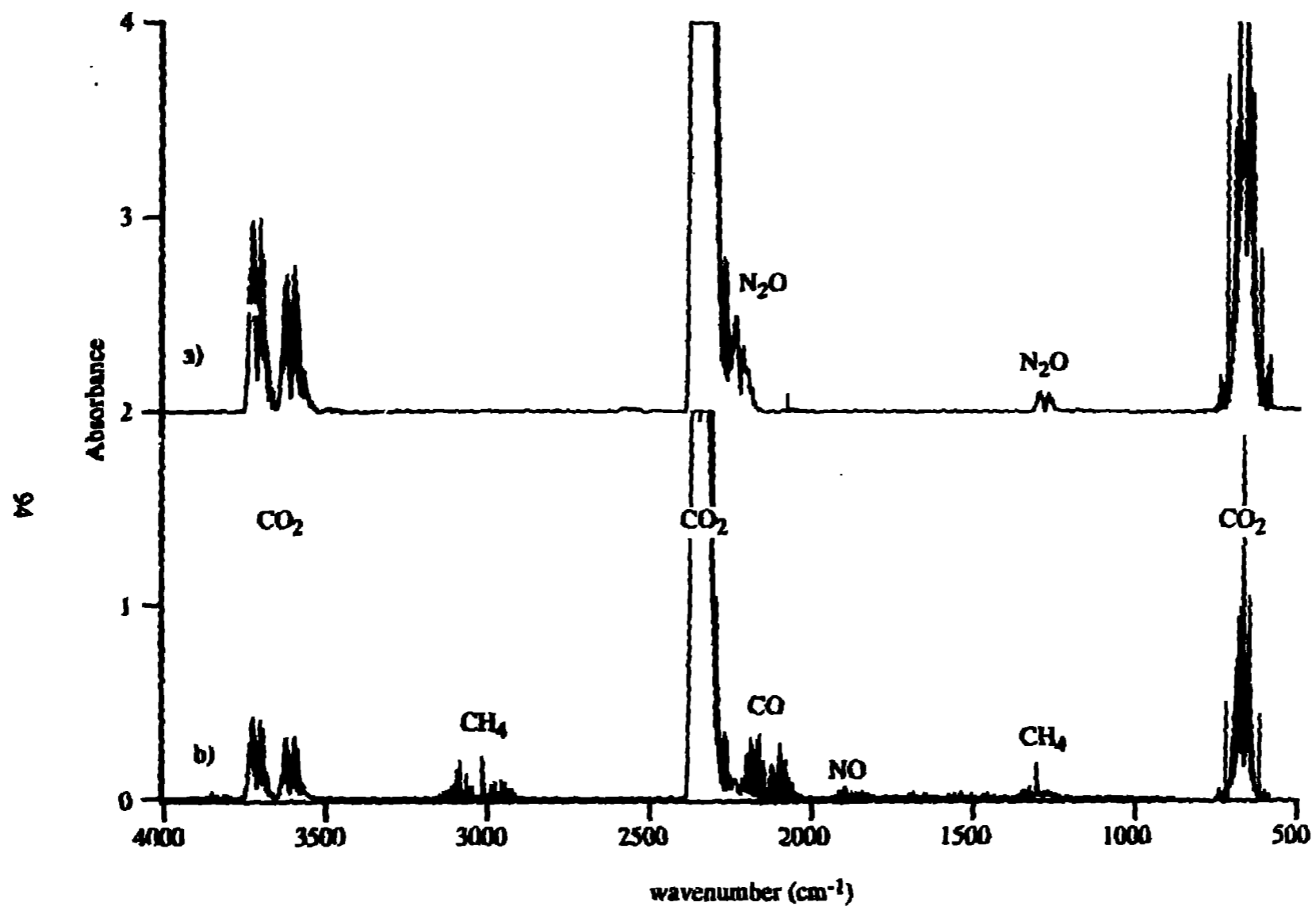


Figure 39. FTIR spectrum of gas effluent from a) SCWO of UDMH with H_2O_2 based on reaction equation 29 (fuel lean), and b) SCWO of UDMH with H_2O_2 based on reaction equation 28.

5. Conclusion

Supercritical water oxidation techniques are ideally suited for destroying hydrazine and UDMH hazardous wastes. Destruction efficiencies better than 99.999% were routinely observed, and with the addition of suitable oxidizers the major products were environmentally benign, (N_2 , CO_2 and water). No hazardous or carcinogenic products were produced. Because of their miscibility with water in all proportions, large throughput may easily be obtained, making scaleup easier. Plugging and corrosion were not a problem in the gold lined reactor.

H. REACTIONS OF NITROGLYCERIN (NG)

1. Introduction

Safety regulations at LANL forbid the handling of neat nitroglycerine (NG). Consequently, we have studied the reactions of NG in supercritical water by means of an extraction process that did not require the direct handling of pure NG. Our approach was to use supercritical CO_2 ($SCCO_2$) as an inert solvent to extract NG from a triple base propellant, M31A1E1. This propellant is 18% (by weight) NG, 22% nitrocellulose (NC) and 55% nitroguanidine (NQ). We have shown that NG can be preferentially extracted from M31A1E1 in $SCCO_2$, leaving the insoluble NC and NQ behind. After extraction into supercritical CO_2 , the NG was directly injected into a SCW reactor for processing.

2. Supercritical CO_2 Extraction/Injection Apparatus

The apparatus used for supercritical CO_2 extraction and subsequent injection into the supercritical water reactor is shown in Figure 40. A cylinder of CO_2 equipped with a liquid delivery tube supplies the CO_2 . The high pressure liquid (1000 psi) is first cooled in a heat exchanger to approximately 0 °C. The pressure is then boosted to operating levels (4000-6000 psi, well above the critical pressure of 1073 psi) in a constant flow, high performance liquid chromatography pump (LDC Analytical, Constametric 3200) with cooled heads. The high pressure CO_2 is pumped through a heat exchanger submerged in a constant temperature bath held above the critical temperature of CO_2 (31°C), typically at 44 °C. The supercritical CO_2 is passed through a filter assembly containing the material to be extracted, approximately 200 mg of the propellant. This solution is then injected into the SCW reactor. A check valve between the extractor and SCW reactor prevents backflow of water. The water and oxidizer are pumped

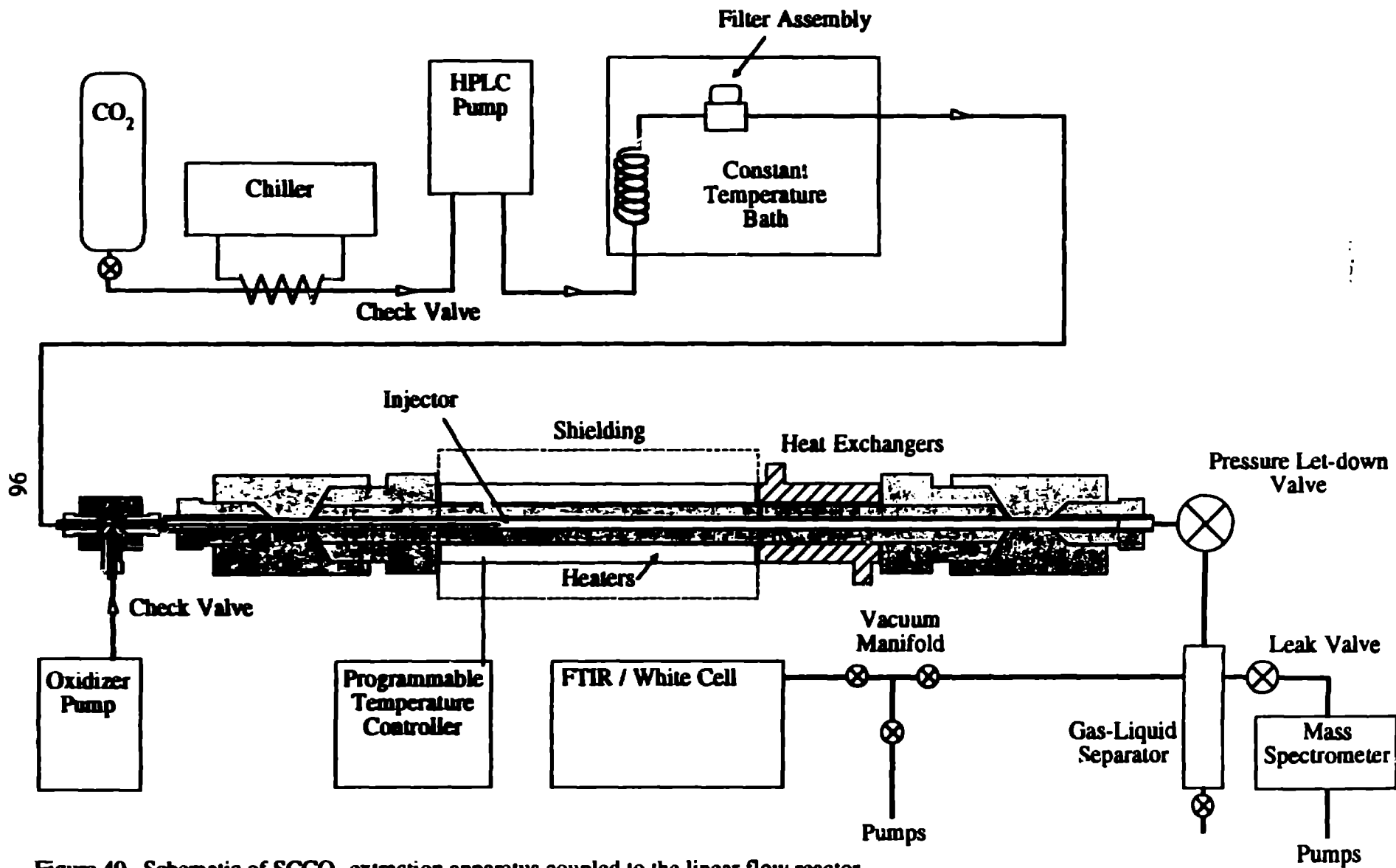


Figure 40. Schematic of SCCO₂ extraction apparatus coupled to the linear flow reactor.

separately so that the relative concentrations of all components can be varied independently.

Solubility experiments are performed with an apparatus having essentially the same front end, but with a pressure letdown valve and a trap instead of a SCWO reactor on the back end. Liquid CO₂ is pumped with a HPLC pump through a heat exchanger that heats it above the critical temperature. The pressure from the pump to the pressure letdown valve is held above the critical pressure (1073 psi). The SCCO₂ is pumped through the extraction cell, a metal thimble with 7 micron frit, that contains approximately 200 mg of the propellant. The pressure is reduced to less than 100 psi at the valve, and dissolved material precipitates in the trap. Gaseous CO₂ flow rate is monitored with a steel ball float flowmeter as it exits the system.

3. Supercritical CO₂ Extraction of Nitroglycerine

The solubility of nitroglycerin in supercritical CO₂ was examined by extraction of M31A1E1 and subsequent analysis of the soluble and insoluble components. A 207 mg sample of propellant flakes was extracted for about 6 hours with SCCO₂ at a temperature of 40 °C and a pressure of approximately 3700 psi. The liquid CO₂ was pumped at a rate of 0.45 ml per minute. When the experiment was terminated, the propellant residue left in the extraction cell was found to weigh 164 mg, indicating that twenty-one percent by weight had been extracted. The yellow liquid extract was found to have collected mostly in the tubing between the pressure letdown valve and the trap.

The identities of the extracted and unextracted components were determined by proton nuclear magnetic resonance (¹H NMR). Each hydrocarbon component of M31A1E1 is clearly identifiable in the spectrum of M31A1E1 shown in Figure 41: δ (chemical shift) = 7.66, NQ (singlet); δ = 7.0 (two triplets), EC; δ = 5.77 (septet), NG; δ = 4.9 (quartet), NG; δ = 4.20 (triplet), DBP; δ = 4.0 (broad singlet), NC; δ = 1.6, 1.35 (two multiplets), DBP; δ = 0.89 (multiplet), EC, DBP. The ¹H NMR spectrum of the extracted material is shown in Figure 42. It is clear from this spectrum that nitroglycerine and the two binder materials DBP and EC are preferentially extracted by supercritical CO₂. These components comprise 22.5% by weight of M31A1E1, consistent with the weight fraction extracted. The ¹H NMR spectrum of the undissolved residue is shown in Figure 43. This spectrum accounts for all of the hydrocarbon components which remain unextracted, including nitrocellulose and nitroguanidine.

These data show that nitroglycerine and the EC and DBP binders are quantitatively extracted in SCCO₂. The actual solubilities of the extracted components in SCCO₂ could not be determined from these experiments because the rate of extraction was not measured. Experiments

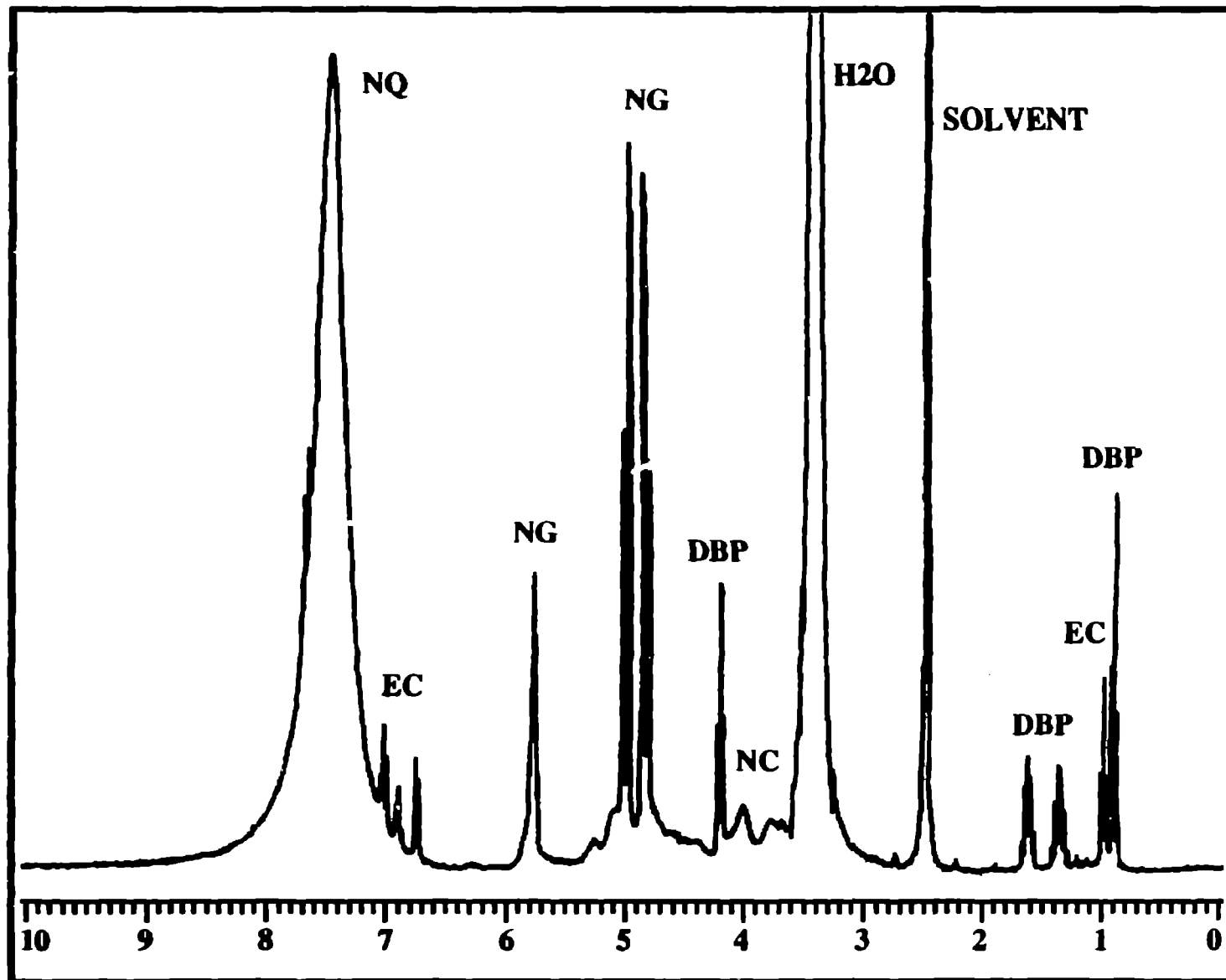


Figure 41. ^1H NMR of M31A1E1 in DMSO

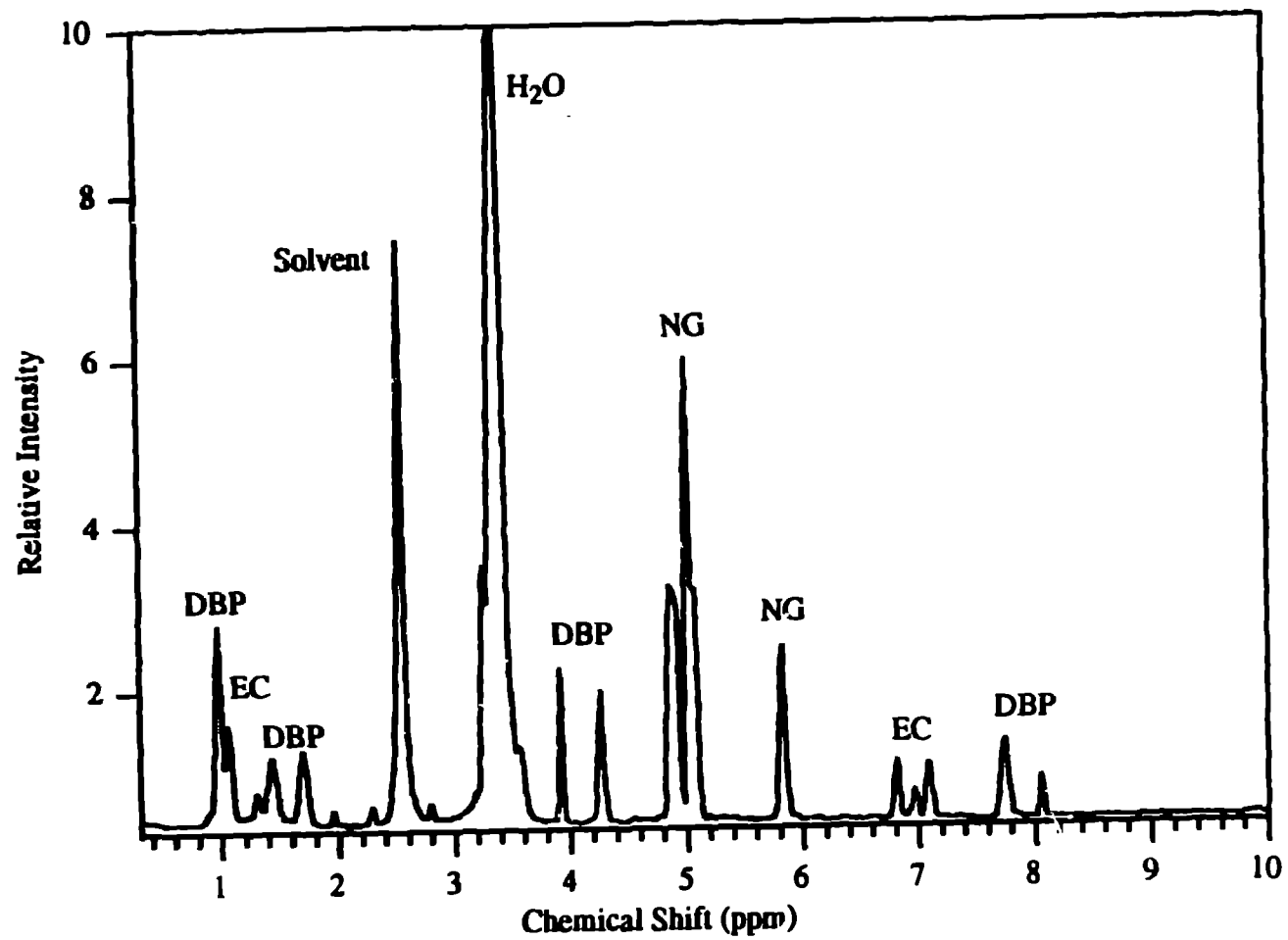


Figure 42. ^1H NMR of extracted material from supercritical CO_2 extraction of M31A1E1.

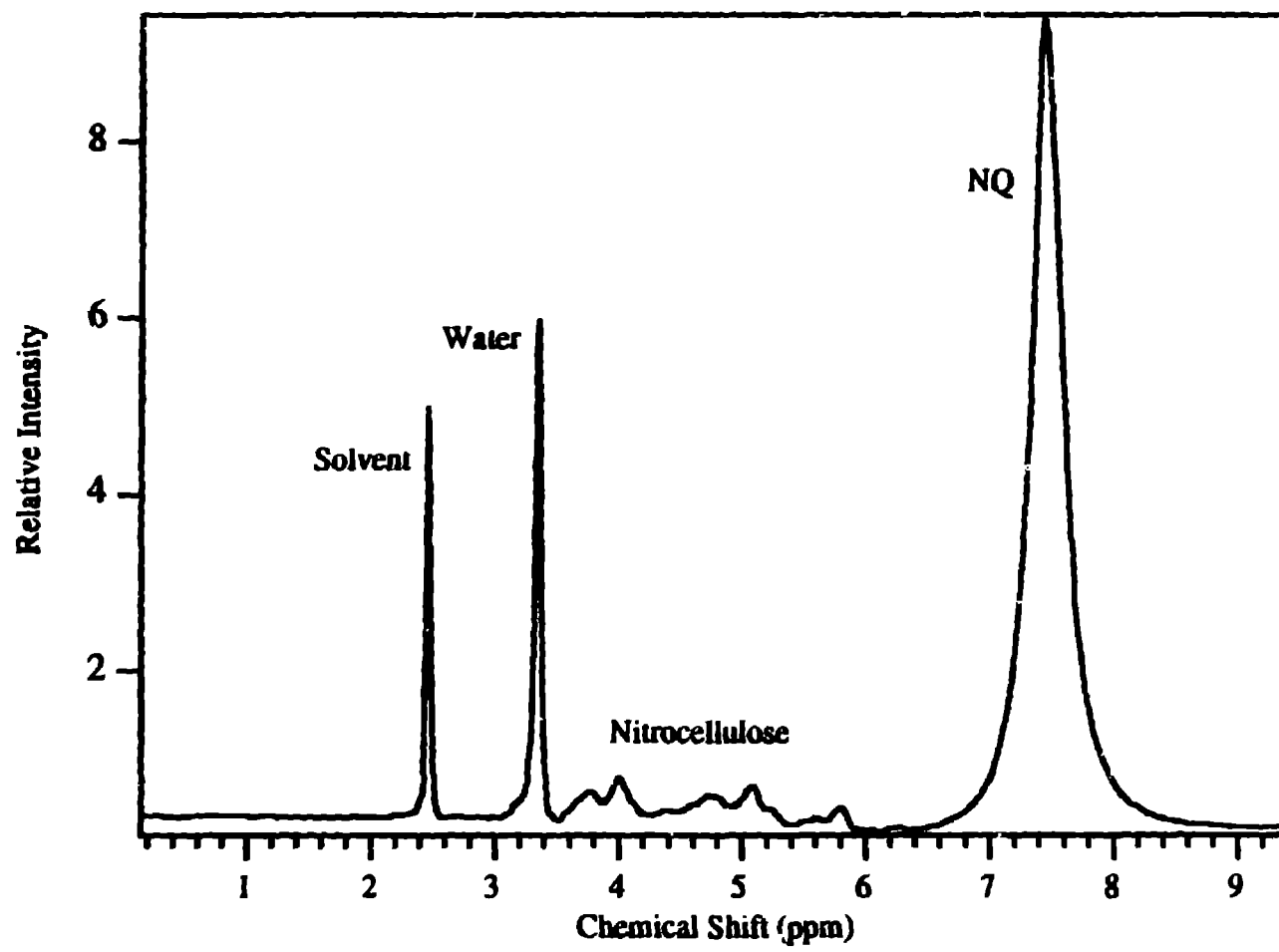


Figure 43. ^1H NMR of residual (unextracted) material from supercritical CO_2 extraction of M31A1E1.

on the combined SCCO₂ extraction/SCWO of nitroglycerine, however, indicate that these components are very soluble and are extracted very rapidly (less than 10 minutes under the conditions employed). It is not surprising that the major components of M31A1E1 are not soluble in SCCO₂. Nitroguanidine is highly polar and not likely to be soluble in the relatively nonpolar solvent SCCO₂. Nitrocellulose is a medium molecular weight polymer that also requires a more polar solvent such as DMSO to solubilize it.

A potential safety hazard was observed in these extraction experiments. The extracted nitroglycerin tends to drop out of solution and accumulate in the tubing between the pressure letdown valve and the trap. This is the region of the extractor where the pressure is reduced to below the critical pressure. The CO₂ expands rapidly in this region, probably resulting in substantial cooling. As a result, NG tends to accumulate in this tube near the letdown valve. This tube is attached at both ends with threaded high pressure fittings. Accumulation of NG in this tube could lead to contamination of the threads or sealing cones and possible detonation during assembly/disassembly. Because of the unpredictable nature and sensitivity of NG, it was determined that this extractor was unsafe and no further extraction experiments were performed with this apparatus.

4. SCW Processing of SCCO₂ Extracted Nitroglycerine

Nitroglycerine extracted from M31A1E1 in SCCO₂ was processed in supercritical water using the apparatus shown in Figure 40, page 96. The nitroglycerine was extracted as described previously, then injected directly into the heated region of a linear flow SCW reactor. All reactions were conducted in a gold-lined reactor to prevent interferences from corrosion reactions. Reactions were conducted at 550 °C, 5000 psi and 4mL/min flow rate (11 s residence time), conditions which were known from previous results in our laboratories to result in complete oxidation of all carbon present. Hydrogen peroxide was used as the oxidant; a dilute solution was pumped independently and mixed in the cold region prior to injection into the reactor. A thirty-fold excess of oxidant was used based on the following chemical reaction:



The carbon concentration was calculated from the composition of the extracted material determined from previous extraction experiments.

Data obtained for runs with two different flow rates of the SCCO₂ extract-solution are presented in Table 32. The analytical results are presented for carbon and nitrogen products: they were obtained from TOC/TIC, ion chromatography and FTIR analyses. The gaseous products of

the SCW reaction were analyzed by FTIR. One of the major nitrogen products, N₂ is not observed because it does not have an infrared active vibration. It was qualitatively observed by gas chromatography. The major C product, CO₂ was also unobservable due the large excess of CO₂ present from the extraction step. Species not detected (below detection limits, typically <100 ppb) include NO, NO₂ and CO. Another observation not reflected in the data in Table 32 is the rate of appearance of these products in the reactor effluents. Approximately 90% of each of the products in the aqueous effluent was observed in the first 40 ml sample taken subsequent to initiation of the extraction/SCWO process. This indicates that the extraction occurs very rapidly, primarily within the first 10 minutes (10 to 30 ml of CO₂ flowed through the extractor). This corresponds to a concentration of NG of up to 4 mg/ml in SCCO₂.

TABLE 32. COMBINED SCCO₂ EXTRACTION/SCWO TREATMENT OF M31A1E1

Product	3mL/min ^a	1mL/min ^a
	mg (%) ^b	mg (%) ^b
TOC	0.7 (9)	0.02 (0.2)
TIC	4.4 (59)	0.7 (9)
NO ₃ ⁻	24.4 (36)	15.2 (21)
NO ₂ ⁻	2.3 (4)	1.5 (3)
N ₂ O	10.6 (43)	na

^aCO₂ flow rate; other reaction conditions: gold-lined reactor, 550 °C, 5000 psi, 4 mL/min H₂O flow, 30-fold excess H₂O₂.

^bPercent of initial carbon or nitrogen occurring as specified product; starting weight of M31A1E1 ~200 mg; extracted N ~ 16 mg; extracted C ~ 8 mg.

It is clear from the results presented in Table 32 that the extracted nitroglycerine has been destroyed in the SC²V reactor. The organic carbon content of the reactor effluent is reduced to 9 and 0.2% of the starting C concentration for the two flow rates respectively. In other words, 91 and 99.8% of the starting C present as NG is converted to CO₂ or CO₃⁻, depending on the flow rate. It is interesting that at the faster CO₂ flow rate (*i.e.* shorter reaction time), the reaction does not go to completion, leaving about 9% of the organic carbon incompletely oxidized. In addition, more of the C is left in solution as inorganic carbon (carbonate or bicarbonate) at faster flow rates. The major nitrogen products are N₂O and NO₃⁻.

These results are consistent with previous results for the supercritical water oxidation of energetic materials such as HMX, RDX and TNT. The NG is completely destroyed and converted

to CO₂ or inorganic carbon. The nitrogen is primarily converted to N₂O and NO₃⁻. The high nitrate content of the products is a consequence of the strongly oxidizing nature of these reactions, given the large (thirty-fold) excess of oxidant. We have shown with other energetic materials that the nitrate produced can be reduced by using a 1:1 stoichiometry of oxidant to carbon.

SECTION IV

INCREASING THROUGHPUT OF EXPLOSIVES

Three approaches have been explored for increasing the throughput of bulk explosives in a SCWO reactor. These include the introduction of the explosive as a slurry, the use of a cosolvent, and the pretreatment of explosives by hydrolysis.

A. REACTIONS OF SLURRIES

One of the simplest methods to continuously feed high concentrations of explosives into a supercritical water reactor is as a slurry of small particles ($< 100 \mu\text{m}$) in water. This method presents potential safety hazards because it requires mechanical pumping and heating of comparatively large amounts of solid explosive entrained in water. An explosion could occur if sufficient material collects or settles in the reactor feed tubes. In addition, the operation of the SCWO reactor could be difficult to control if the rate of reaction of the explosive depends strongly on particle size or morphology. In this section, we report on experiments and calculations designed to characterize the behavior of small particles in high-temperature water and to help evaluate the hazards associated with processing slurries of explosives.

1. Small Bomb Calorimeter Experiments

Initial experiments with the optically accessible reactor studied slurries of 1,3,5-triamino-2,4,6-trinitrobenzene (TATB), chosen for its inertness and high deflagration temperature, $T_d = 384 \text{ }^\circ\text{C}$, which is above the critical temperature of water. Slurries of TATB, 5 to 20 percent by weight, were loaded by syringe into the reactor, which was then sealed and pressurized to about 200 atmospheres. The temperature was then slowly ramped ($\sim 200 \text{ }^\circ\text{C}/\text{hour}$) up to a maximum of $600 \text{ }^\circ\text{C}$. A total of five such experiments were conducted with no sudden temperature or pressure surges (our sampling rate is 10 per second) that would characterize deflagration. Calculations based on the known volume of gases produced in a TATB detonation suggest that the expected magnitude of the pressure rise for a deflagration would have been observable in these experiments. In general, the images obtained during these runs were somewhat obscured by the high light scattering of the slurry. In all of the runs, however, the TATB was observed to disappear gradually as the temperature approached $300 \text{ }^\circ\text{C}$, well below the deflagration and critical temperatures. It is possible that the TATB is dissolving at this temperature. At higher

temperatures, the TATB appears to decompose, leaving only a slight (insoluble) tar and other organics dissolved in the aqueous effluent upon cooling.

Quantitative measurements of the temperature and pressure changes resulting from reactions of slurries as they were heated were made in the batch reactor (Figure 11, page 23). The reactor volume was adjusted to 200 μL to permit the use of small quantities of material. Milligrams of explosive were added to 100 μL of water to make a slurry of 5 to 20 percent explosive by weight. The balance of the reactor volume was air. The pressure and temperature of the reactor were recorded at one-second intervals on a computer as the reactor temperature was increased in a controlled ramp. The pressure rise due to reaction of the explosive was determined by obtaining a baseline pressure rise using an equal quantity of water with no explosive. This pressure difference gives a measure of both the extent and rate of reaction of the explosive. Figure 44 shows results for the behavior of TATB as it is heated. It is interesting to note that while the deflagration temperature of TATB is 384 $^{\circ}\text{C}$, it begins to react at significantly lower temperatures (300-330 $^{\circ}\text{C}$). These measurements are in agreement with the qualitative observations made in the optically accessible reactor. For quantities of TATB less than 10 mg (10 percent by weight), the reaction is generally slow, requiring more than 30 seconds to reach a constant pressure (complete reaction). Quantities greater than 13 mg always yielded a sudden pressure rise, which occurred in less than our one second time resolution. One exception was a run with 8 mg of TATB that also showed a sudden pressure rise. This behavior may depend on the degree of dispersion of the solid in the water. The slurry was not stirred, and some settling or clumping of the "wet" TATB could have occurred. These results indicate that the behavior of slurries may be unpredictable and that above certain concentrations the slurry can react very rapidly. Such uncertainties raise concerns about using slurries in supercritical water reactors.

In contrast, similar experiments performed with a double-base propellant (DBP, nitroglycerin/nitrocellulose), shown in Figure 45, show no unpredictable behavior. Reactions were performed with slurries composed of up to 16 percent by weight of the DBP. Slow pressure releases (reactions) were observed in every case; however, further studies are required to insure that this is generally true. A run made without the addition of water is also shown to demonstrate the rapid reaction (deflagration) that occurs under these conditions.

A series of experiments was also carried out on HMX slurries in a 1 ml constant volume reactor. The cell pressure was monitored as the temperature was gradually increased. The results of these experiments with HMX are shown in Figure 46. For a 1% HMX slurry in water, the pressure started to increase as the temperature approached 200 $^{\circ}\text{C}$ and then stabilized

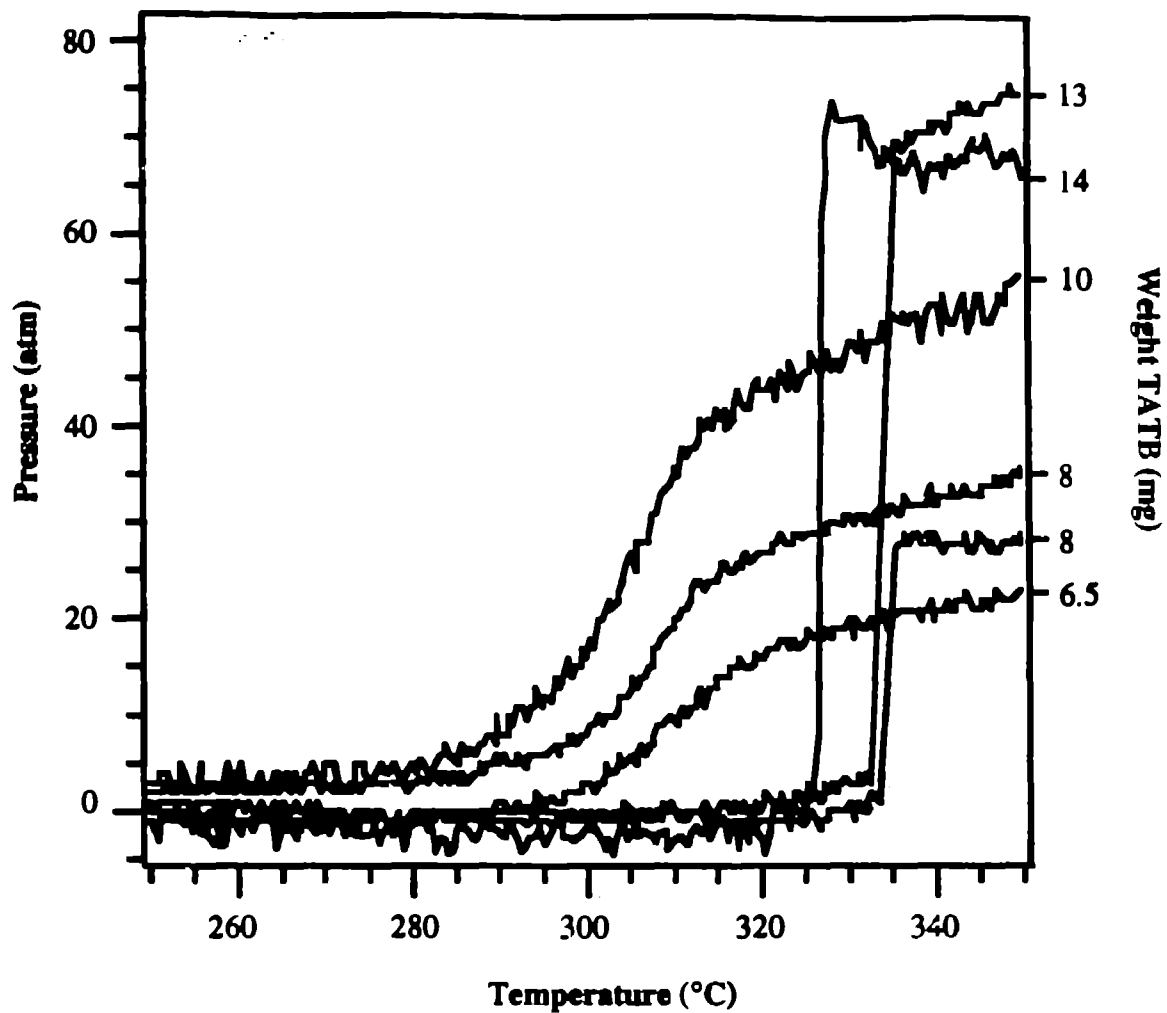


Figure 44. Pressure rises observed due to reactions of TATB slurries in water as a function of temperature and starting concentration. Background pressure rises have been subtracted.

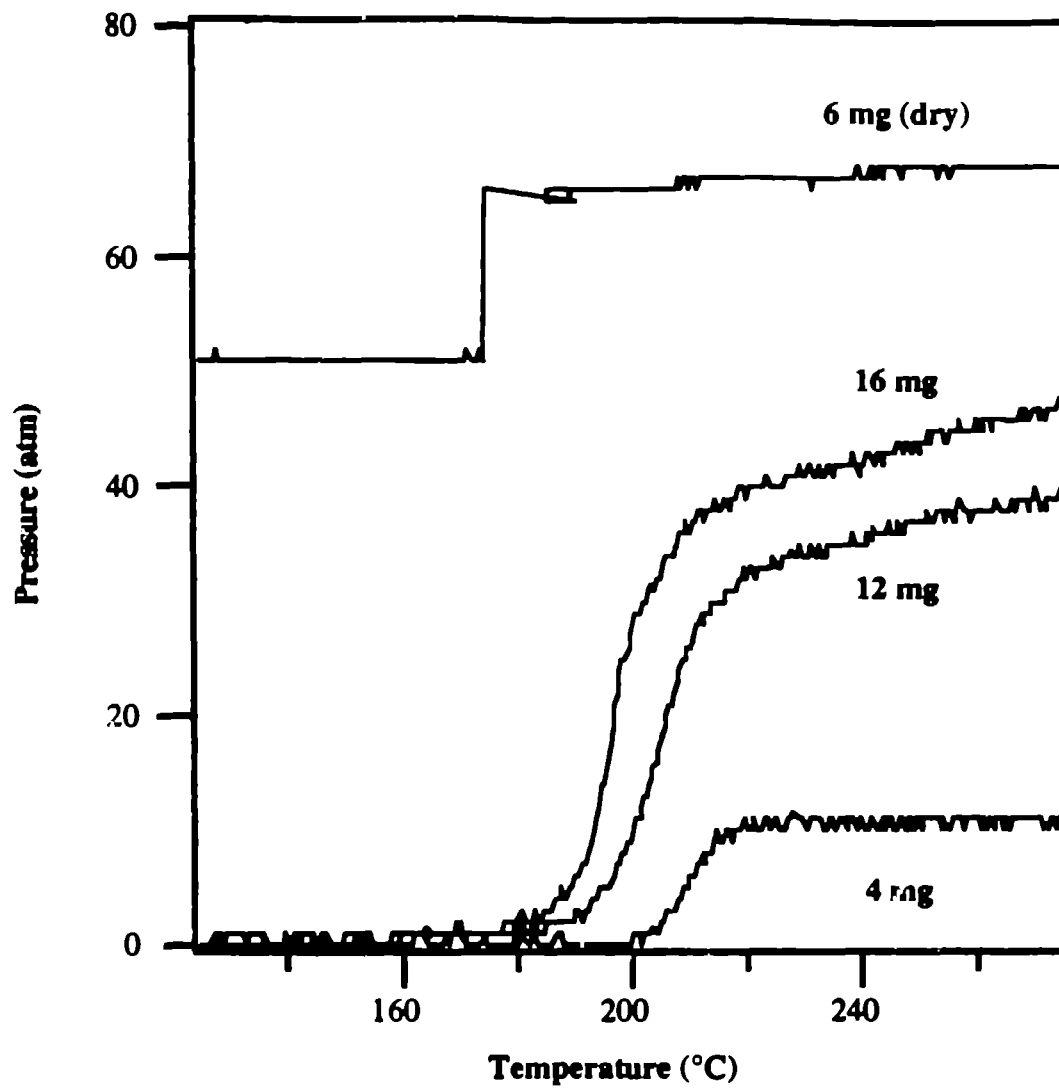


Figure 45. Pressure rises observed due to reactions of DBP slurries in water as a function of temperature and starting concentration. Background pressure rises have been subtracted.

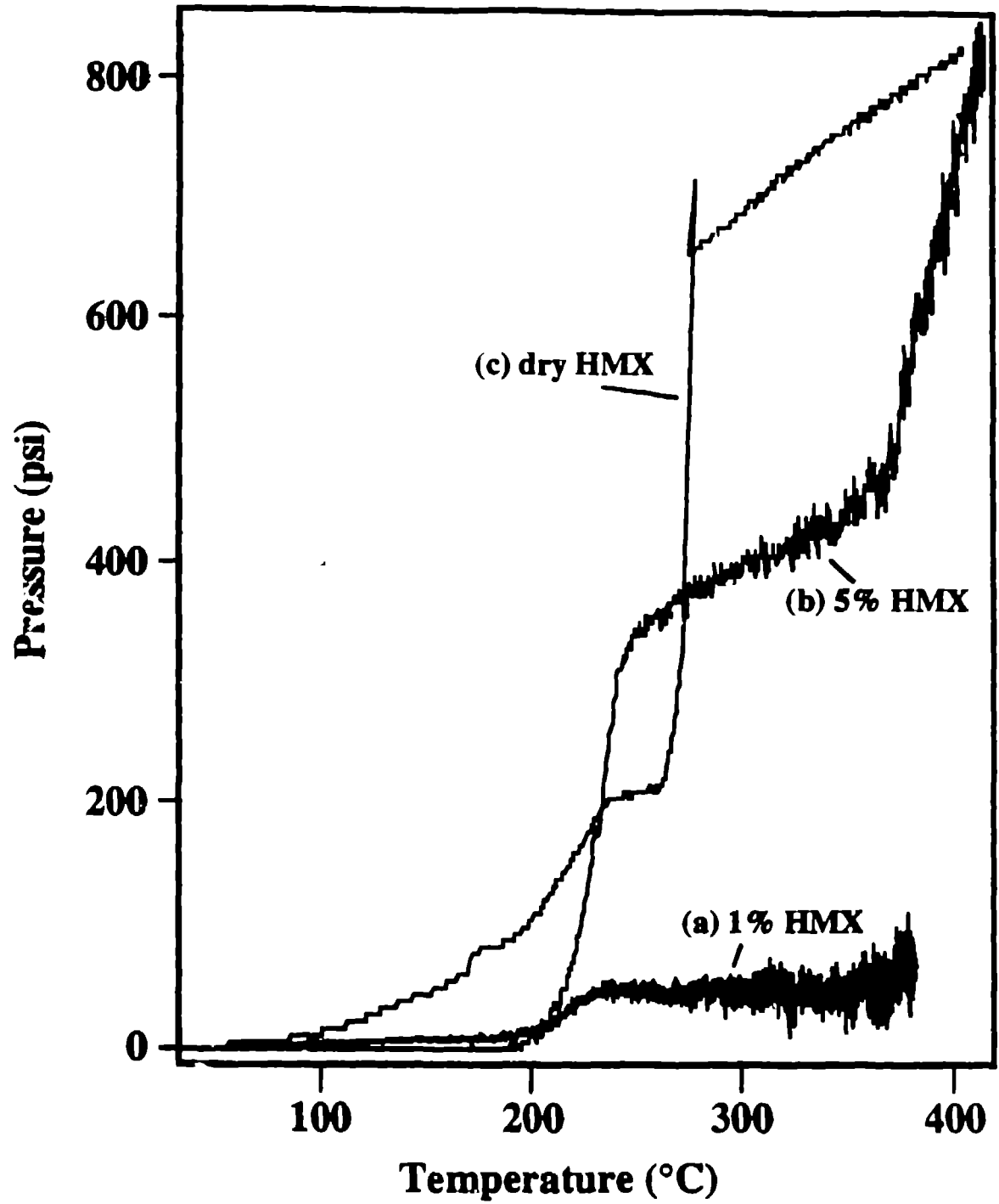


Figure 46. HMX decomposition pressure as a function of temperature. (a) 1% HMX in water, (b) 5% HMX (80 mg) in water, and (c) 80 mg HMX dry.

near 240°C. For 5% HMX in water, the pressure also sharply increased as temperature was increased above 200°C, followed by a similar plateau region. However, near the critical temperature, the pressure exhibited a second sharp increase, as shown in Fig. 46. For both these runs, the pressure contribution due to water was subtracted to reflect the effect of HMX decomposition and subsequent heat up of product gases in the supercritical water environment. For comparison, the decomposition of dry HMX in air in the same cell is also shown in this figure. Near 260°C, the HMX undergoes an extreme pressure increase from 200 to 650 psi. This reflects the spontaneous decomposition of HMX. Clearly the HMX decomposition reaction is moderated by the presence of water as reflected in the more moderate pressure increases from 200 to 400°C. Reaction products are also different for the two reactions as shown in Table 33.

TABLE 33. MASS SPECTROMETRIC ANALYSIS OF HMX DECOMPOSITION
PRODUCT GASES

Dry HMX (wt/wt %)		5% HMX in H ₂ O (wt/wt %)	
N ₂	73%	N ₂	62%
O ₂	18%	CO ₂	27%
CO ₂	3.8%	N ₂ O	7.6%
H ₂	2.8%	O ₂	2.3%
CO	1.4%	H ₂	1.0%

As seen in Table 33, the dry decomposition of HMX produces primarily nitrogen and oxygen in the gas phase, with a trace of CO₂, H₂, and CO. In contrast, the wet decomposition yields a significant amount CO₂ and N₂O in place of much of the oxygen, and virtually no CO forms.

2. Slurry Flow Experiments in One Gallon per Hour Reactor

A series of tests were initiated to evaluate the effectiveness of the one gallon per hour reactor system, described in Section II.E, for pumping explosive slurries. For safety reasons, initial tests were done with melamine in place of the explosive. The melamine simulates many of the physical properties of the granular explosive, but without the high chemical reactivity. Like HMX, melamine is relatively insoluble in water and has a density of 1.6 g/cm³, which is similar to that of HMX, 1.8 g/cm³.

Water slurries containing 1 to 10 percent by weight melamine have been pumped through this reactor, both under ambient conditions and at nominal process conditions (550°C, 3700 psi, and an oxygen flow of 4 slm) that are more typical for chemical destruction. The reactor tube remained free flowing throughout all the runs. However, using the initial pump and reactor inlet configuration shown in Figure 47 (a), significant plugging was observed at both the pump inlet and the pressure letdown valve. The settling of particles in the pump clogs the check valves (both inlet and outlet). With these check valves inoperative, the slurry pumping rate dropped to virtually zero. To alleviate plugging at the pump inlet, a second small recirculating pump was added to the system, as shown in Figure 47 (b). The Little Giant pump recirculated the feed at a flow rate of approximately 3 gal/min. Even with the recirculating pump, slurries of 100 μm melamine still plugged the pump inlet. However, decreasing the particle size to 50 μm alleviated this problem. Decreasing the particle size decreases their overall settling rate. However, even with the decreased particle size, plugging at the pressure letdown valve was still observed. Because the melamine is far less reactive than typical explosive compounds, the required reactor residence time is probably longer than our present design allows. Consequently, we do not believe that plugging of the letdown valve will be a problem when HMX or other explosive slurries are used, since the explosive particles should all be destroyed before reaching this valve.

The use of viscosity enhancers to slow the settling rate of particles in the slurries has also been explored. Sodium carboxymethylcellulose (CMC) was chosen as a suitable viscosity enhancer for these experiments. The first questions to be addressed involved whether the CMC could be pumped through the system, and whether it would be destroyed by the SCWO process. A 1 percent solution of CMC was successfully pumped through our reactor system under cold conditions, indicating that the increased viscosity would not limit the overall system flow rate. Under SCWO conditions at approximately 400°C, the CMC gum was not completely mineralized as the effluent stream had a brown color and a bad odor. Higher temperatures of 580 °C appeared to destroy all of the CMC additive, but a comprehensive product analysis has not yet been completed. We attempted to pump 10 percent melamine in a 1 percent CMC/water mixture under cold conditions. The letdown valve closed up very fast (within 4 minutes). Significant settling occurred at the inlet. The effective settling rate is difficult to accurately quantify. Nevertheless, based on our observations, the settling rate for 10 percent melamine in 1 percent CMC gum/99 percent water appeared to be approximately half as bad as the 3 percent melamine mixture in water.

Experiments were also conducted to determine if an actual HMX slurry could be safely and effectively pumped using our present apparatus. A 3 percent weight slurry of fine HMX

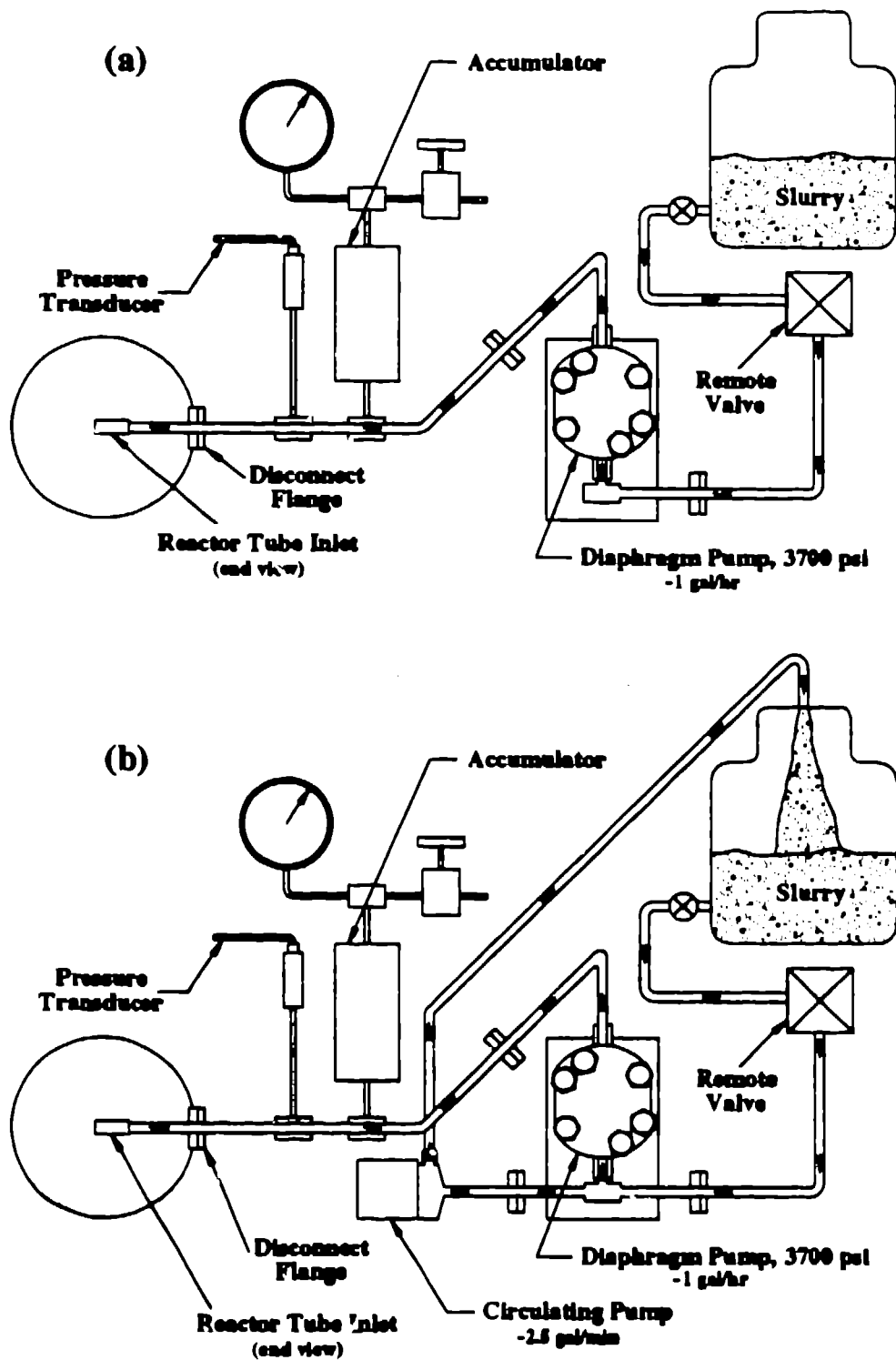


Figure 47. Pumping unit and Reactor inlet. (a) original configuration, (b) with circulating pump added.

(98 % of the particles are less than 44 microns) was employed in these experiments. The apparatus was the same as used for the melamine experiments discussed above, except that the heated reactor tube was replaced with a filter manifold, since the purpose of these experiments was to evaluate the pumping system rather than to measure the destruction efficiency. This filter manifold, which consisted of six filters, each 5 microns in size, was placed directly upstream of the letdown valve to prevent contamination of the letdown valve. The previous studies with melamine had shown that the letdown valve would plug if any solids were to reach this valve. In addition, a system vent valve was placed upstream of both the filter manifold and letdown valve. This valve allowed remote venting of the system from high to ambient pressure if either the letdown valve or the filter manifold was plugged. Special flanges were also designed and added to allow the disconnection of the system in a potentially HE contaminated environment. These flanges were of conflat-type design, except that two concentric viton o-rings were used as the sealing surface instead of a copper gasket and a knife edge on the flange.

In the actual test, deionized water was pumped for approximately 30 minutes to establish steady state conditions. The Lewa diaphragm pump was pressurized to 3700 psi and the flow was set at 1 gal/hour. The flow was then switched from deionized water to a two gallon slurry reservoir of 3 percent HMX in deionized water. A small Giant pump recirculated the slurry at the pump inlet, as was done with the melamine slurry, to prevent plugging at the inlet. When flow was switched to the 3 percent HMX slurry, the pressure remained steady, indicating smooth flow of the slurry. Approximately seven minutes after switching to the HMX slurry, however, pressure began to build up. The letdown valve was opened up to compensate for the increased pressure, but this proved to be ineffective, indicating that the filter manifold or the letdown valve was fully plugged. To further demonstrate that indeed either the letdown valve or the filter manifold (or both) had plugged, flow was then switched through the system vent. The HMX slurry flowed freely through the system vent, but was not under pressure since the letdown valve was bypassed.

In previous experiments, the melamine slurry, used to create HMX, took approximately 18 minutes to plug the filter manifold. Two possible scenarios exist to explain why HMX plugged sooner than melamine. First, since the same filter manifold was used in the HMX experiment and the previous melamine experiment, some residual melamine may have remained. The second explanation is that the particle size of HMX was smaller than the melamine, and a small amount of HMX of less than 5 microns in size may have passed through the filters to plug the letdown valve. However, in either case, this experiment demonstrated that an HMX slurry can be effectively and safely pumped using our present Lewa pump system.

3. Particle Settling Calculations.

For a suspension of solids of large enough size to settle under gravity in a static fluid, horizontal transport in a pipe may involve any one of three flow regimes. These may be identified as: (1) saltation flow in which the solid particles form dunes at the bottom of the conduit. At low fluid velocities, only the particles on the surface may be swept along in a bouncing motion called "saltation". This regime can result in unsteady or periodic behavior and plugging in worst the cases. The dunes can move along the bottom if the fluid shear forces are large enough; (2) "heterogeneous" flow in which settling occurs to some degree so that particles are not uniformly distributed over the flow field. Thus a solid density gradient may exist from top to bottom within the pipe. The minimum flow velocity required to sustain heterogeneous flow is designated as V_m ; (3) "homogenous" flow in which fluid turbulence is high enough so that solids are uniformly distributed. The mixture can then often be treated as a single phase non-Newtonian fluid. The fluid velocity required for homogenous flow is referred to as the critical velocity, V_c . Variables influencing the hydrodynamics of the suspension include particle shape, volume fraction of solids, particle size, and particle size distribution. In addition, solids wettability, surface charge, the ionic nature of the fluid, and the degree of turbulence will all play a role. While rigorous treatment of solids transport in the hydrothermal system is not feasible, empirical correlations can be employed to estimate V_m .

Most empirical correlations for V_m have a basis in dimensional analysis and give the Froude number (ratio of inertial to gravitational forces) as a function of the Reynolds number (ratio of inertial to viscous forces), ratio of particle to tube diameter, solid to fluid density ratio, and volume fraction of solids. Correlations may or may not include corrections to account for particle shape and size distributions. Of the many correlations available in the literature, only a few were selected for the present calculations. Emphasis was placed on widely used correlations and those which were regressed to data taken in relatively small diameter pipes and involving particle sizes in the range expected for slurried propellants. Perhaps the most widely used correlation for V_m is due to Durand (Reference 22) and is of the form

$$V_m = F [2 g D (s - 1)]^{0.5} \quad (1)$$

where g is the acceleration due to gravity, D is the nominal pipe diameter and s is the ratio of solid to fluid density. The parameter F is given graphically as a function of particle size and volume fraction solids. Spells' correlation (Reference 23) is of the form

$$\frac{V_m^2}{gd_{85}} = K \left(\frac{\rho_m V_m D}{\mu} \right)^{0.775} (s - 1) \quad (2)$$

with $K = 0.0251$ and $\rho_m = \rho[1 + V_s(s-1)]$. Here ρ is the density of the carrier fluid, μ the fluid viscosity, and V_s is the volume fraction solids. The quantity d_{85} is the particle diameter such that 85% by weight of the solid is smaller than d_{85} . Spells found that V_c was approximately 2.4 times greater than V_m and both could be estimated using the functional form of eq. (2), provided the constant K was suitably adjusted. Cairns et al. (Reference 24) focused on particle diameters in the 240-380 μm range, in pipes of 1.9 to 5 cm diameter. Their correlation is of the form

$$\frac{V_m^2}{gd_{50}} = 9.8 \left(\frac{V_s D V_m \rho}{\mu} \right)^{0.3} (s - 1)^{0.6} \quad (3)$$

Here d_{50} is defined analogously to d_{85} above. When compared to other correlations, Durand's predictions were generally conservative, i.e. they estimated a higher V_m . In virtually all cases examined, the data used in the regressions showed significant amounts of scatter. Thus as a caveat, the correlations should not be regarded as highly accurate. Errors of plus or minus 25-30% can routinely be expected. Use of the correlations for gas-like carrier fluid densities may also be suspect, as the correlations were developed for liquid suspensions. Correlations for pneumatic transport of solids may be more accurate in such cases. Also, pipe diameters for the cases examined here are at the low end of those used in data correlation.

Calculations were performed using eqs. (1-3) for several particle sizes and loadings. For a selected particle size, the same value was used for d_{50} and d_{85} in the above correlations. This gives some indication of the effects of particle size distribution. Physical properties of the carrier fluid were assumed to be those of water at 450 °C and 3700 psia. Thus, the values $\rho = 0.113 \text{ g/cm}^3$ and $\mu = 3 \times 10^{-4} \text{ g/cm-sec}$ were used. Furthermore, the solid density was assumed to be $\rho_s = 1.8 \text{ g/cm}^3$, which is reasonable for HMX. For a fixed particle size of 50 μm (i.e. d_{50} or d_{85}), calculations were performed for solids loadings of $V_s = 0.03, 0.01, \text{ and } 0.10$. The predicted V_m values for these cases are shown in Figures 48 to 50 as a function of pipe diameter. Also

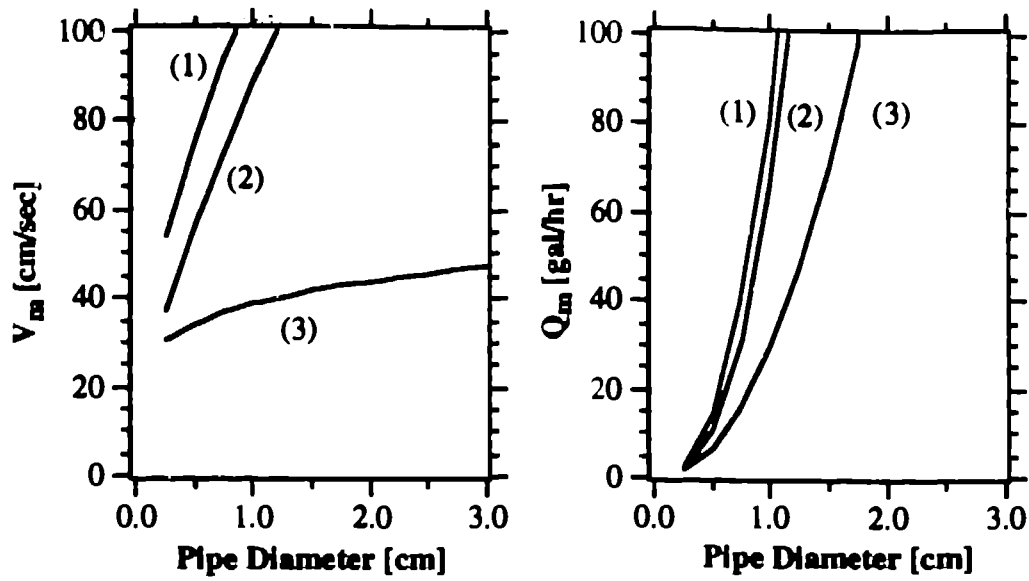


Figure 48. Predicted V_m and Q_m for $V_s = 0.03$ and $d = 50$ mm. The labels (1-3) correspond to eqs. (1-3).

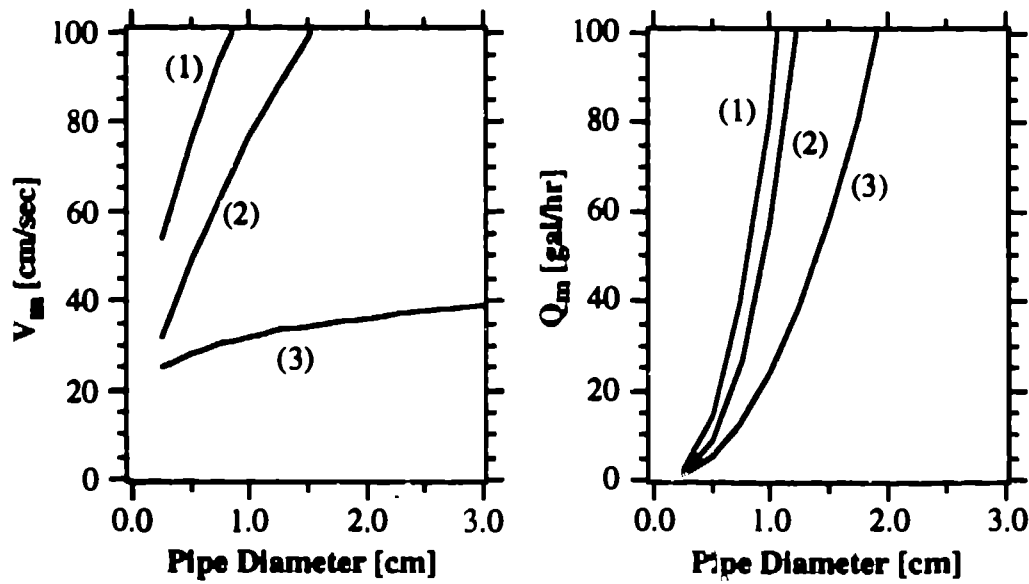


Figure 49. Predicted V_m and Q_m for a solids volume fraction of 0.01 and particle size of 50 mm. The labels (1-3) correspond to eqs. (1-3).

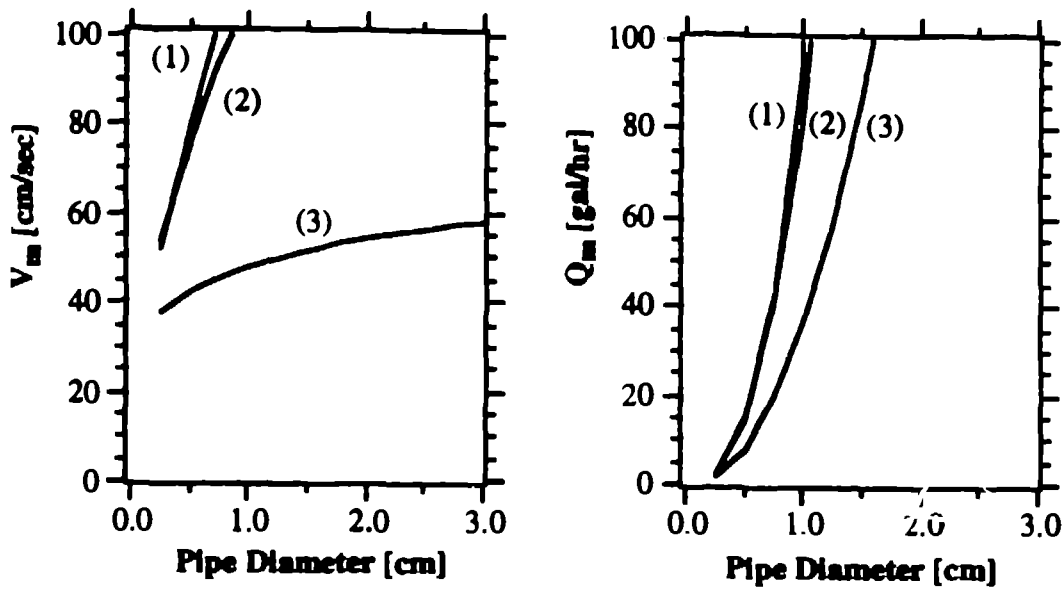


Figure 50. Predicted V_m and Q_m for $V_s = 0.10$ and $d = 50$ mm. The labels (1-3) correspond to eqs. (1-3).

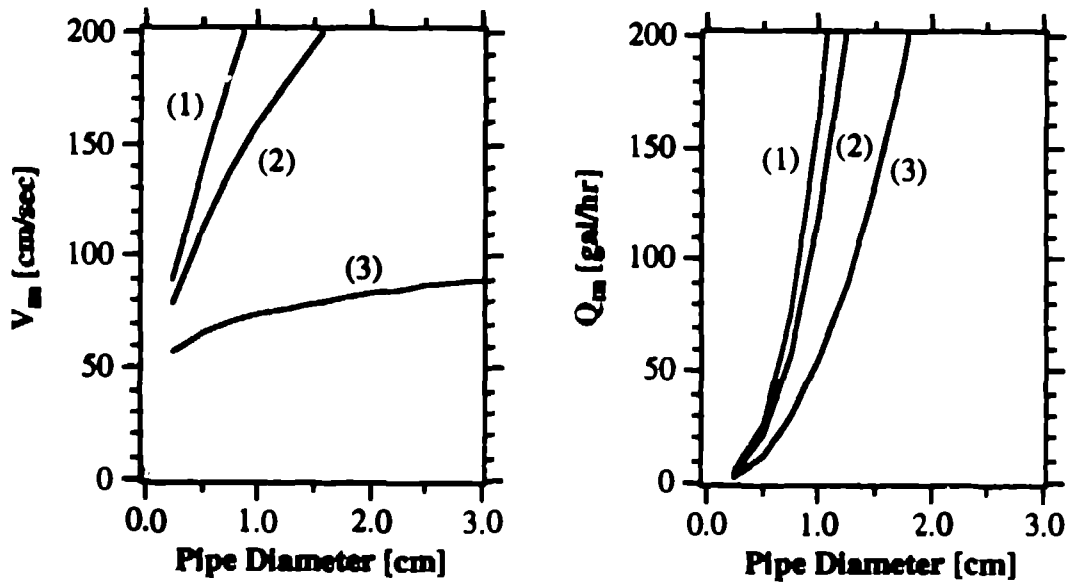


Figure 51. Predicted V_m and Q_m for $V_s = 0.03$ and $d = 150$ mm. The labels (1-3) correspond to eqs. (1-3).

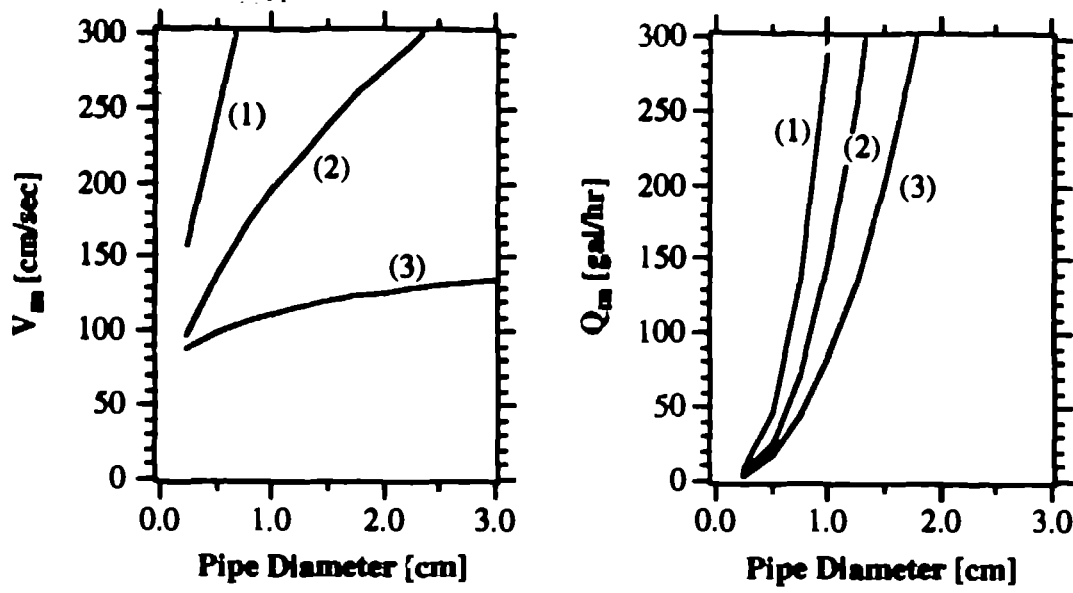


Figure 52. Predicted V_m and Q_m for $V_s = 0.03$ and $d = 300$ mm. The labels (1-3) correspond to eqs. (1-3).

shown is the corresponding volumetric flow rate, Q_m , in gallons per hour (gph). From these figures, we see that the required minimum flow velocity increases less than a factor of two for an order of magnitude increase in solids loading. Figures 51 and 52 show results obtained using a solids volume fraction of 0.03 and particle sizes of 150 and 300 μm . A comparison of Figures 48, 51, and 52 shows that particle size is a more important parameter than solids loading. For a constant solids loading, a factor of six increase in particle size increases the required minimum flow velocity roughly a factor of three. For the slurry pumping experiments discussed above, the particle size was 100 μm and solids loading up to 0.10 were employed. For the reactor pipe id of 0.188 in. (0.5 cm), we estimate from the figures that a flow velocity of 40 - 90 cm/sec would be required to insure that the particles will not settle out of the flow in the reactor region. The actual flow velocity employed in these experiments was roughly 50 - 55 cm/sec in the reactor.

B. INTRODUCTION OF EXPLOSIVES IN A CO-SOLVENT

The feasibility of dissolving explosives in a cosolvent for introduction at higher concentrations into the reactor was investigated. The linear reactor (Figure 15, page 30) permits injection of reactants that are insoluble in water, but that can be dissolved in a cosolvent and injected directly into the supercritical region of the reactor. Separate pumps are employed to flow the water (reaction medium) through the main (outer) reactor tube and the reactants through the inner injector tube. The flow rate of each pump can be adjusted to give the desired concentration of reactant in the water. The mixing region is observable through optical (diamond) windows. The modified reactor was tested in a series of experiments in which a one-percent solution of HMX in methyl ethyl ketone (MEK) was injected into water in varying ratios under supercritical conditions. No oxidant was added in these experiments. Temperatures at the injector were varied from 100 °C to 400 °C while the pressure was maintained between 290 and 375 atm. For most experiments the water flow rate, 3 mL/minute, was kept about 7.5 times greater than the HMX/MEK flow rate, 0.4 mL/minute. For a few experiments the flow rates of the two solutions were set equal at 3.0 mL/minute. These injection rates yield very high concentrations of HMX, ranging from 0.1 percent to 0.5 percent. The injection and subsequent mixing were observed through the optical window using a TV camera and magnifying optics, and recorded with a VCR. Under these conditions we did not observe a solid phase of HMX (due to precipitation of insoluble material) forming near the opening of the injector.

When the reactor was operated under the conditions described, less than 10 percent of the MEK was destroyed. A large number of organic products were observed in the HPLC analyses, most likely from the thermal decomposition of the MEK. The identity of these products has not

been determined. The HMX was completely destroyed for all concentrations employed. The highest HMX concentration employed was 5000 ppm, yielding a detection-limited destruction efficiency of 99.9996 percent. The effluent contained low concentrations of nitrite (0.3 to 6 ppm) and nitrate (0.1 to 0.6 ppm). Less than 0.5 percent of the nitrogen in the HMX is converted into NO_x^- . This result differs from experiments in which HMX is the only organic present in solution. The high concentration of MEK and low level of oxidizer produces a smaller percentage of nitrogen as NO_x^- .

Dissolving HMX in MEK is convenient for introducing high concentrations of HMX into the reactor. However, this approach produces significant quantities of MEK decomposition products. Although thermal decomposition of the MEK is relatively low at temperatures at which most of the HMX decomposes, these products not only interfere significantly with the analysis of the HMX reaction products, but are themselves likely to be undesirable waste. It would be possible to separate the remaining MEK for reuse and to destroy the MEK decomposition products in a second SCWO step. The extra energy and oxidant required for these steps are likely to be significant.

C. BASE HYDROLYSIS OF EXPLOSIVES

1. Introduction

The instability of energetic materials to strong bases is well known. The three classes of explosive compounds, namely nitroaromatics, nitrate esters and nitramines, can all be decomposed under alkaline conditions (References 25-29). Our experiments indicate that the hydrolysis of certain explosives in basic solutions produces water soluble products that can be processed by SCWO. Our experiments show that NQ, RDX, HMX, TNT, NC, and NG can be hydrolyzed at low temperatures ($< 150\text{ }^\circ\text{C}$) and low pressures ($< 60\text{ psi}$) to produce water-soluble, nonexplosive products. In addition, the following formulations were subjected to base hydrolysis: PBX 9404, tritonal, triple-based gun propellant M31A1E1, and CYH class 1.1 rocket propellant. Compositions of the formulations that were studied are listed in Table 34.

TABLE 34. COMPOSITIONS OF FORMULATIONS USED IN BASE HYDROLYSIS EXPERIMENTS

Component / Weight Percent	9404	Tritonal	M31A1E1	CYH
HMX	94.0			10.8
Nitrocellulose (NC)	3.0		21.5	21.6
Tris(2-chloroethyl) phosphate	3.0			
TNT		80.0		
Aluminum		20.0		19.8
Nitroguanidine (NQ)			54.7	
Nitroglycerine (NG)			18.0	29.6
Dibutylphthalate (DBP)			3.0	
Ethyl Centralite (Diethyldiphenylurea)			1.5	
Potassium sulfate			1.25	
Carbon black			0.05	
Ammonium perchlorate				10.8
Glycerol triacetate (triacetin)				5.3
3-Hydroxyphenol (resorcinol)				1.1
2-Nitrodiphenylamine				1.0

Although experiments have been performed on all of the materials mentioned above, the work has focused on HMX, PBX 9404, and the propellant formulations. With the exception of PETN, all of the energetic materials studied decomposed completely to non-energetic products. PETN only partially decomposed due to its higher resistance to base hydrolysis and problems with its watability in aqueous solution. In this section we discuss hydrolysis experiments for NQ, TNT, HMX, PBX 9404, RDX, M31A1E1, and CYH. These materials were hydrolyzed under basic conditions. Experiments were conducted using both open and sealed containers, and using both small and large pieces of explosives. The products of hydrolysis were analyzed by the following techniques: Fourier-transform nuclear magnetic resonance spectrometry (FTNMR); Fourier-transform infrared spectroscopy (FTIR); gas chromatography (GC); mass spectrometry (MS); and ultraviolet spectroscopy (UV). The hydrolysis of the energetic materials NC and NG was not studied directly. However, the results of their hydrolysis can be inferred from our study of the triple base propellant, M31A1E1, which contains these components. We complete this section with a discussion of the SCWO of the hydrolysis products.

2. Hydrolysis of Nitroguanidine

Hydrolysis of nitroguanidine (NQ) was studied under a variety of experimental conditions in an open container. In several experiments, flaked NQ samples weighing approximately 200 mg each were placed in beakers and mixed with sodium hydroxide solution at a 1:1 molar ratio of Base:NQ. Although some of the NQ dissolved in the aqueous solution, no reaction was evident upon mixing at room temperature. The mixtures were heated on a steam table to approximately 74 °C over a period of 5 minutes, maintained at 74 °C for 30 minutes, and then cooled. During heating, the vigorous evolution of gaseous products was observed. At the solution boiling point, some foaming occurred but did not require the addition of a defoaming agent. The resulting solutions were analyzed for starting material and products. In this case, gaseous effluents were not captured or analyzed, although the odor of ammonia could be detected in several experiments. After the reaction was complete, a golden yellow homogeneous solution remained. In one experiment, the aqueous solution resulting from the hydrolysis was diluted from 2.0 ml to 1.0 liter, and the diluted solution was analyzed for unreacted NQ by UV spectroscopy. A standard solution of NQ in water was prepared and found to have an absorbance maximum at 263 nm, with a molar absorptivity of $14,500 \text{ cm}^{-1}\text{M}^{-1}$. Analysis of the diluted hydrolysis solution from experiment 1 showed that 99.97 percent of the NQ had reacted. The destruction of NQ may be even greater since no attempt was made to separate reaction products that could contribute to the UV absorbance at 263 nm and thereby cause a greater apparent NQ concentration. Similar experiments were conducted in which distilled water alone was used without any sodium hydroxide. After heating for 30 minutes, it was observed that most of the NQ remained undissolved, indicating that the heating in water alone is not sufficient for the hydrolysis to occur.

Larger scale open-container tests were also conducted. These large-scale hydrolysis experiments involved 500-gram pressed charges and were performed at a firing site. The explosive charge, a 2.5-inch by 2.5-inch diameter cylinder of pressed NQ, was placed in an open container with 4 liters of sodium hydroxide solution. The mixture was heated to a final temperature of 74 °C. Total heating time averaged about 3 hours, including the time required to reach the final temperature. The progress of the reaction was monitored remotely using a video camera and recorder. During heating, gas evolution was visible from the sides and top of the cylinder. The color of the solution gradually changed from clear to dark yellow. Flakes of NQ could be observed peeling from the charge. The resulting mixture was filtered to remove unreacted explosive, and the aqueous phase was analyzed and processed in an SCWO reactor. In the first large-scale experiment, the sodium hydroxide to NQ mole ratio used was relatively low, i.e., NQ was in excess. When the test was terminated, a 16-gram piece of NQ remained.

Analysis of the hydrolysis solution by UV spectroscopy showed it to be saturated with NQ. The solution was also analyzed for hydrolysis products by ^{13}C NMR and found to contain four different carbon species (Figure 53). The peaks between 0 and 60 ppm in Figure 53 are due to an NMR reference compound. An aliquot of the solution was evaporated to dryness and the solid residue was analyzed by GC/MS. By matching the mass spectra obtained to a spectral library, the following products were identified: ammonium carbamate; sodium carbonate; urea; and guanidine carbonate. The products were verified by collecting additional NMR spectra of the sample spiked with the suspected materials.

A second large-scale NQ hydrolysis experiment was performed with a higher sodium hydroxide-to-NQ mole ratio of 1.25. Ultraviolet spectroscopic analysis of the hydrolysis solution showed no detectable amount of NQ. The ^{13}C NMR spectrum of the solution in this case showed three carbon species (Figure 54). Spiking the sample identified two of the products as carbonate and urea, but the ^{13}C chemical shift of the third product did not match that of guanidine, carbamate, or nitroguanidine. The splitting of the peak indicates that the carbon is bonded to nitrogen. Splitting of ^{13}C peaks by ^{14}N is uncommon but can occur if the molecule is highly symmetric. Examination of ^{13}C NMR correlation charts shows that the chemical shift of the unknown is close to that of nitriles and isocyanates. Further evidence for the presence of a nitrile or isocyanate is shown by the infrared spectrum of the sample (Figure 55). Although the spectrum in Figure 55 is of the carbonate/urea/unknown mixture, the absorbance near 2200 wavenumbers is consistent with a nitrile or isocyanate. Based on the starting material, NQ, possible candidates for the unknown were cyanamide and the cyanate anion. By comparison with known samples of cyanamide and cyanate, the unknown was identified as cyanate. Additional small scale experiments were conducted to determine if the NQ hydrolysis could be driven to completion (i.e., all the NQ converted to carbonate). In these experiments, the sodium hydroxide-to-NQ mole ratio was increased to 2.6 and the mixture was maintained at the final temperature for 3 hours. NMR analysis of the hydrolysis solution showed the same three products as before, with the major product being cyanate.

A closed-container NQ hydrolysis was done to identify the gaseous reaction products. In this experiment, 3.0 g. of NQ was mixed with sodium hydroxide solution with a base:NQ ratio of 1.25:1, sealed in a 50 ml pressure vessel, and heated to approximately 80 °C. After the pressure leveled off, heating was terminated and the vessel cooled to room temperature. The pressure of the cooled vessel was found to be 110 psi. Analysis by MS showed the major gaseous product to be nitrous oxide, with a small amount of ammonia. NMR analysis of the liquid phase gave the same three products as described above.

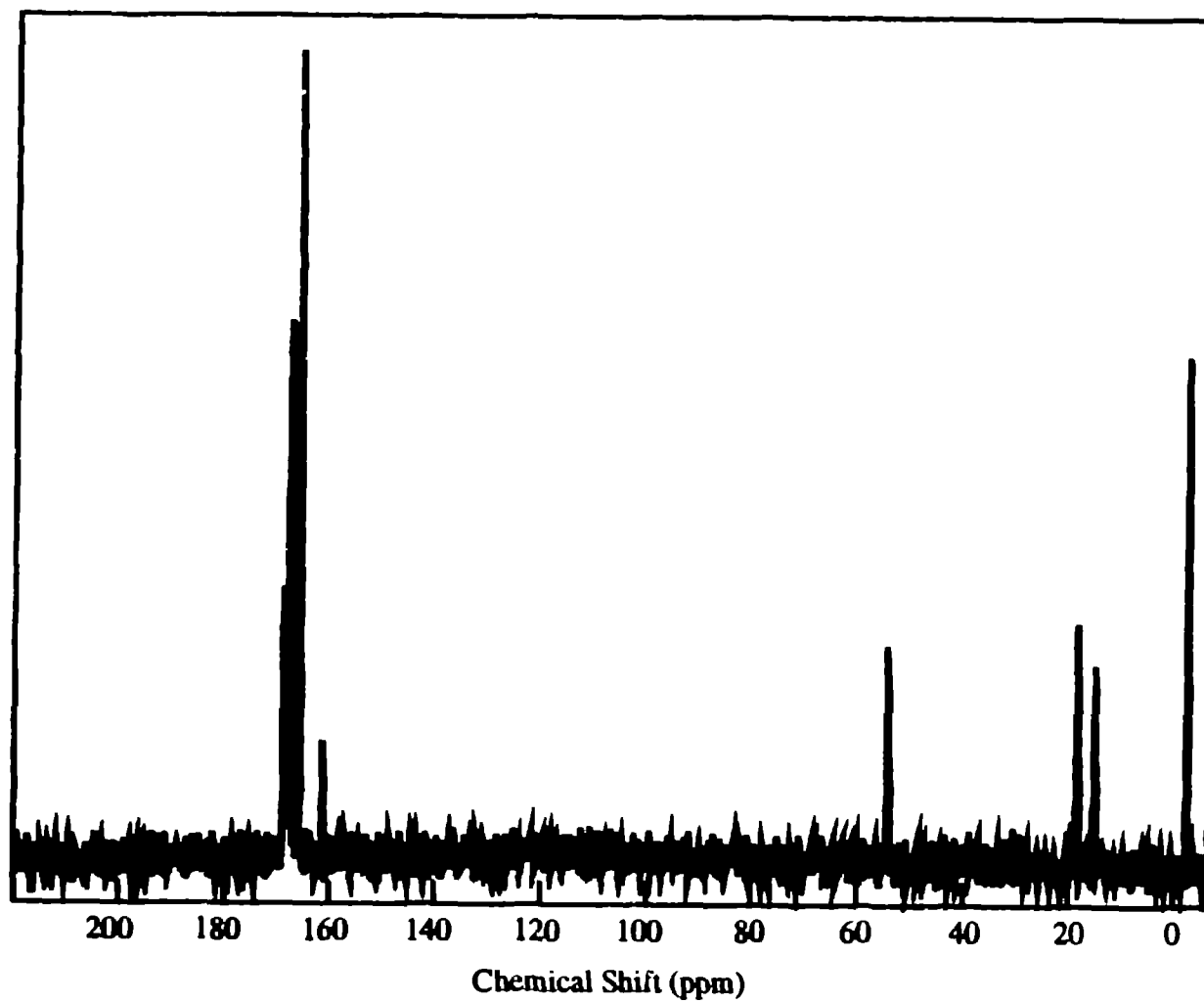


Figure 53. ^{13}C NMR of NQ hydrolysis residue. Peak assignments are as follows: 167.51, carbamate; 166.38, carbonate; 164.69, urea; and 160.31 guanidine.

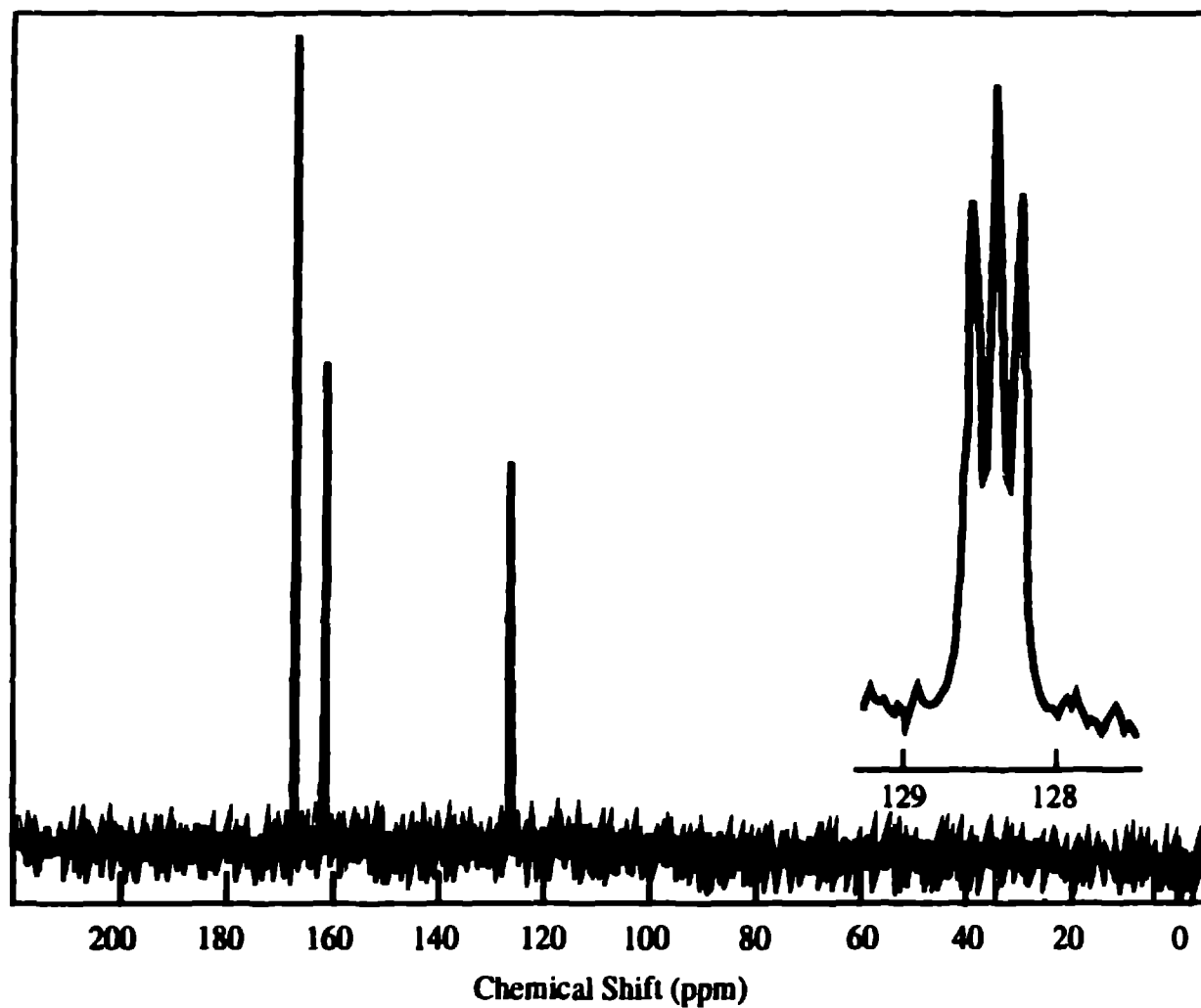


Figure 54. ^{13}C NMR of NQ hydrolysis residue with excess NaOH. Peak assignments are as follows: 168.16, carbonate; 162.65, urea; and 128.44, cyanate or cyanamide.

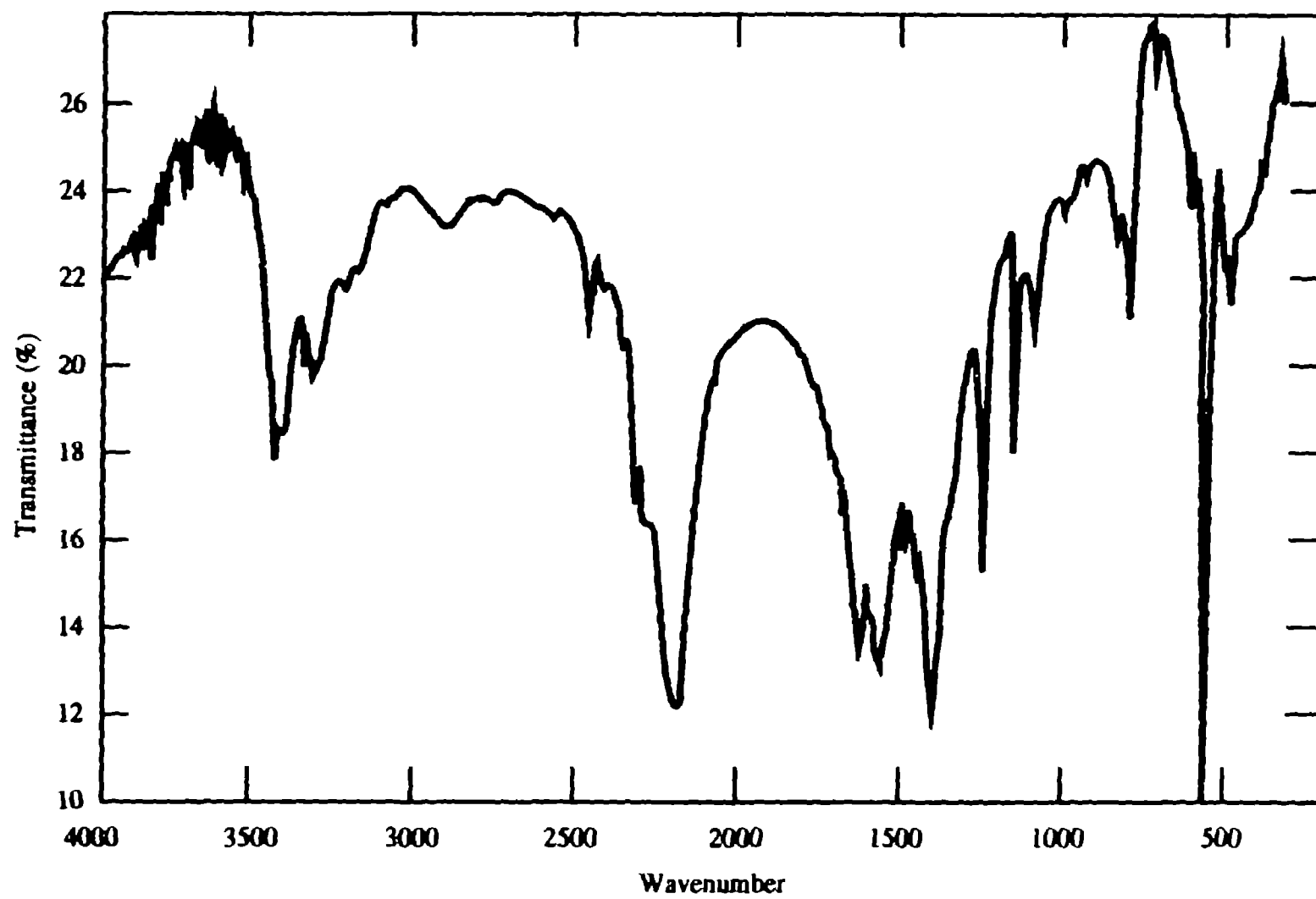
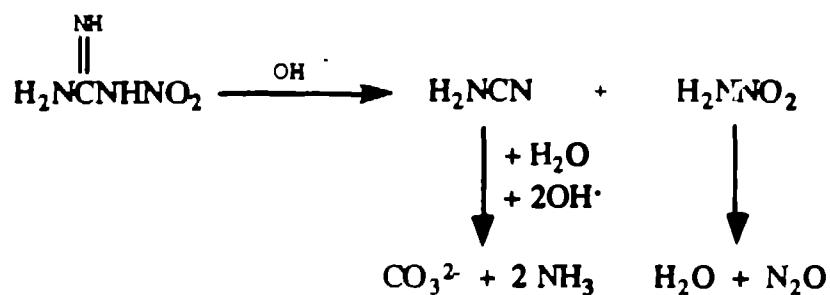
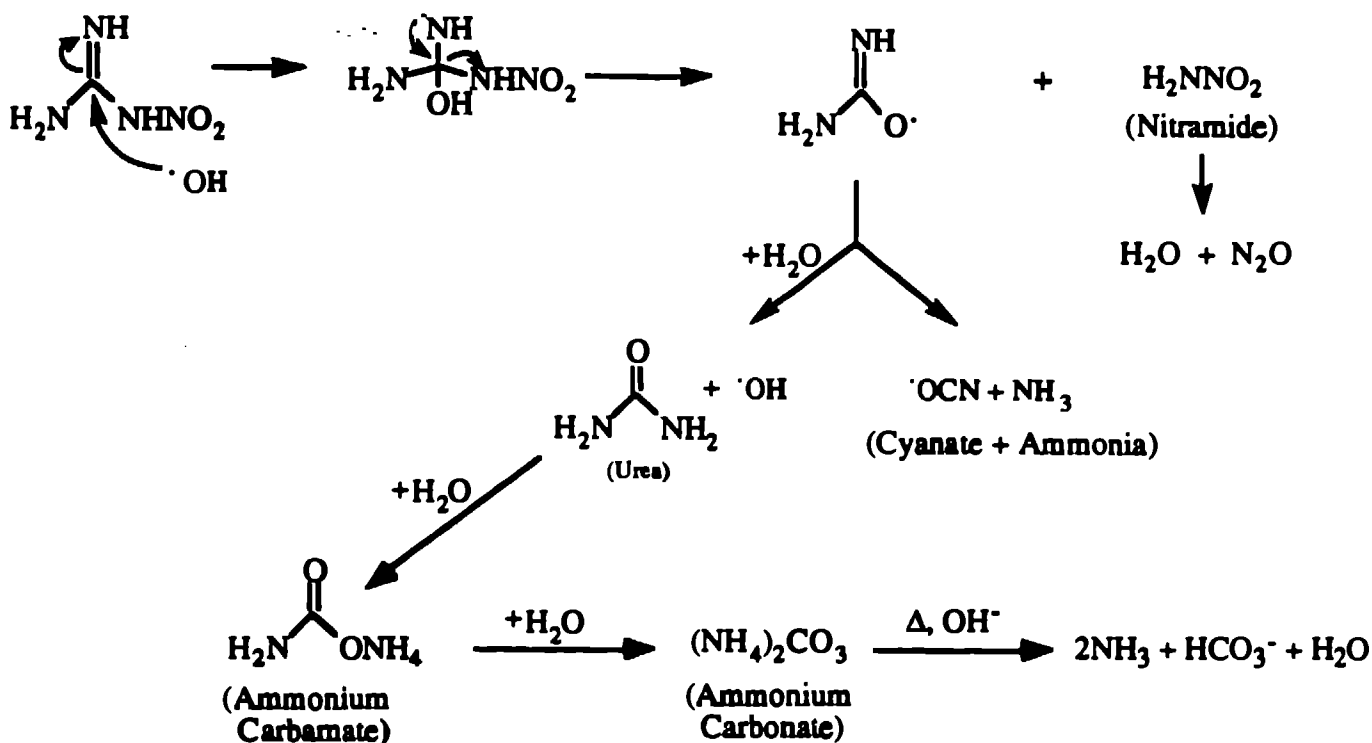


Figure 55. FTIR of solid NQ hydrolysis residue.

The mechanism of NQ hydrolysis is thought to proceed by decomposition of the material to give cyanamide and nitramide (Reference 27). According to Reference 27, cyanamide further decomposes to ammonia and carbon dioxide (carbonate in basic media) and nitramide to water and nitrous oxide.



However, in addition to nitrous oxide, ammonia, and sodium carbonate, we have detected urea, ammonium carbamate, and sodium cyanate as major products, and this simple mechanism does not account for this product distribution. We have also found that when urea and ammonium carbamate are hydrolyzed under the same conditions as used for NQ, the only product is carbonate. When cyanamide is subjected to base hydrolysis, urea and sodium carbonate are produced. From this information we propose the following more comprehensive mechanism for NQ hydrolysis.



In the above mechanism, one equivalent of base is consumed per mole of starting C to convert that C to a mixture of cyanate and carbonate (sodium salts). It was generally observed, however, that an excess of base (1.25:1 molar ratio) was required to complete the hydrolysis reaction.

3. Hydrolysis of Trinitrotoluene

Trinitrotoluene (TNT) experiments were performed only on a small scale in a closed container. When the TNT was mixed with sodium hydroxide solution at a Base:TNT molar ratio of 1.25:1, the solution turned a clear, pale red. The mixture was heated to 150 °C and the pressure leveled off at 64 psi after 109 minutes of heating. A control was run that did not contain TNT and was found to develop a pressure of 61 psi, indicating that minimal gaseous products were produced by the TNT hydrolysis. The gases were analyzed by MS and the major gaseous product was CO₂. The liquid phase was dark black with a suspension of tar-like material. Attempted analysis of the products was unsuccessful due to clogging of filters and insolubility of the material. Because the pH of the aqueous solution was no longer basic after the hydrolysis, it was evident that more base should be employed.

In a subsequent experiment, the sodium hydroxide-to-TNT mole ratio was six. The mixture was sealed in a 100-ml vessel and heated to 150 °C, under which conditions the pressure leveled off at 54 psi after 73 minutes. Upon cooling, the residual pressure was too low to measure. The liquid phase appeared dark black and homogeneous, consistent with the earlier literature (Reference 25). Analysis by ¹³C NMR gave a single carbon species having a chemical shift that corresponds to a carbonyl group, and no ¹³C peaks matching those of TNT. It appears that TNT is completely hydrolyzed to a nonexplosive, water-soluble product that we have not identified.

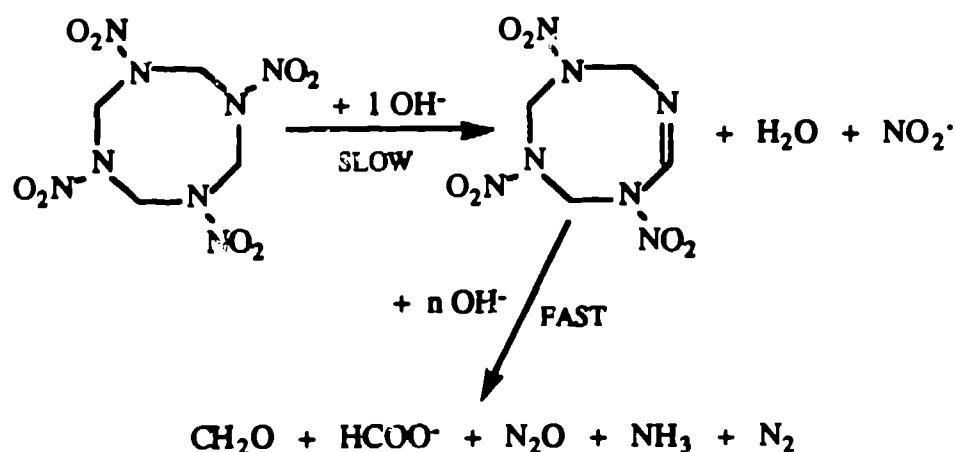
4. Hydrolysis of HMX and PBX 9404

Because HMX is a major component in both DOE and DoD formulations, we have performed a large number of hydrolysis experiments on it. We have also done many experiments with PBX 9404, which is 94.0 weight percent in HMX. The experiments on PBX 9404 were conducted in conjunction with our DOE program, but the results will be included here because of the obvious relevance to this project. The complete composition of PBX 9404 is shown in Table 34, page 120. Base hydrolysis has been done on the PBX in the form of molding powder, 1 inch by 1 inch pressed pellets (23 g), 5 and 1/8 inch diameter hemispheres (1.1 kg), and 1 and 5/8 inch by 1 inch pieces (63 g) encased in 1/8 inch steel. The amount of sodium hydroxide used in the reactions was 6 moles per mole of HMX contained in the PBX. Four moles are required for complete reaction with HMX and a two mole excess was added for reaction with the binder and plasticizer. Upon mixing PBX 9404 and sodium hydroxide solution at ambient temperature, there was no visible reaction. When the mixture was heated to temperatures above 60 °C, the NC binder decomposed quickly, leaving behind HMX powder. In the 70 to 80° range, vigorous gas evolution was observable and the mixture began to foam. When the solution boiling point was reached, 93 °C, the foaming was severe enough that a defoaming agent had to be added. During the reaction, the odor of ammonia was detected. Upon completion of the reaction, the resulting homogeneous solution was clear brown and had a pH of approximately 15. Titration of the solution to determine the amount of hydroxide consumed showed that 4.4 moles was used per mole of HMX in the PBX 9404.

We have observed that the time required for complete destruction of the HMX depends on temperature, stirring efficiency, particle size of the material, and volume of the hydrolysis solution. Reactions in which the solution volume was 4 milliliters per gram of PBX did not react completely after many hours of heating. When the volume was increased (keeping the total amount of NaOH reactant the same) to 15 ml/g PBX 9404, reaction was complete after several

hours of boiling. Subsequent experiments were carried out with volumes of 7 and 10 ml/g of PBX. In most cases, a solution volume of 10 ml/g was used to effect complete decomposition of PBX 9404 in a reasonable amount of time. Typically, the reaction is finished after 2 hours of boiling with constant stirring. The rate of HMX hydrolysis appears to become progressively slower as the reaction proceeds. This may be due to "salting-out" of the HMX from the hydrolyzing solution as the concentration of the product salts increases. The solubility of HMX in water is very low, 5 ppm at 20 °C, and is likely to be lower in concentrated salt solution. To compensate for this problem, experiments were performed with dimethylsulfoxide (DMSO), a good solvent for HMX, added to the hydrolysis solution. The time required for hydrolysis of HMX in 100 % aqueous solution was compared to that in 10 % by volume DMSO solution. The reaction time was found to decrease by a factor of three. Presumably, the rate enhancement is due to a solubility effect but the reactivity of DMSO in base may also contribute.

The rate-limiting step of the alkaline hydrolysis of HMX is postulated (Reference 12) to be a bimolecular elimination reaction producing nitrous acid. The intermediate produced in the slow step of the reaction is very unstable to base, and quickly decomposes to the products shown.



Of the gaseous products shown above, we have found that nitrous oxide is produced in much larger quantity than is ammonia or nitrogen. A trace of hydrogen was also detected. Although formaldehyde is shown as one of the products, we have not detected it under the reaction conditions we have used. Formaldehyde itself is unstable in strong bases, producing the formate ion by the Cannizzaro reaction (Reference 30).

Quantitative analysis was performed on the product solution from the hydrolysis of 5.05 grams of PBX 9404 in 50 ml of 2 molar sodium hydroxide. The hydrolysis solution was

analyzed by ^{13}C NMR (Figure 56). None of the peaks corresponds to PBX 9404 components, and the major peak at 171.01 ppm has a chemical shift typical of a carbonyl group. Subsequent NMR analyses identified the major product as the formate anion. However, the carbon NMR spectrum shows at least fifteen minor carbon species in addition to the formate. The hydrolysis solution was also analyzed by ion chromatography for formate, nitrite, nitrate, and chloride. The results of the analysis are listed in Table 35. The weight percentages of carbon, nitrogen, and chlorine in PBX 9404 are 16 %, 36 %, and 1.1 %, respectively. As shown in Table 35, 35 % of the total carbon was converted to formate. The balance of the carbon remains in solution as unidentified, water-soluble products. Nineteen percent of the starting nitrogen has been converted to nitrite, and 0.4 % ends up as nitrate. Most of the remaining nitrogen is in the form of nitrous oxide (N_2O) gas, but the exact fraction has not yet been determined. The chlorine from the PBX 9404 plasticizer, tris(2-chloroethyl) phosphate (CEF) is almost completely converted to chloride ion; 80 % is accounted for. Phosphorus NMR analysis of the hydrolysis products indicates that the CEF phosphorus is not converted to inorganic phosphate, but remains an organic species, possibly a hydroxyethyl phosphate. Also shown in Table 35 are the mole ratios of the products to the starting moles of HMX or CEF.

TABLE 35. ANIONIC PRODUCTS FROM THE HYDROLYSIS OF PBX 9404

Anion	Conc. (g/liter)	Total Moles	Wt. % of Total	Mole Ratio
Formate	22.5	0.024	35 % of C	1.5 / HMX
Nitrite	22.5	0.024	19 % of N	1.5 / HMX
Nitrate	0.633	0.52 e-3	0.4 % of N	0.032 / HMX
Chloride	0.891	1.3 e-3	80 % of Cl	2.4 / CEF

Several experiments were conducted which examine the use of ammonium hydroxide in place of sodium hydroxide. In one experiment, sodium hydroxide and HMX were mixed in a mole ratio of 5 to 1 and sealed in a 100-ml pressure vessel. After heating for 59 minutes at 160 °C, the pressure leveled off at 87 psi. A control was run without HMX and the maximum pressure was 76 psi. When the vessel was cooled, the residual pressure was 12 psi. The major gaseous product was nitrous oxide. The NMR analysis of the clear, yellow liquid phase gave a spectrum almost identical to that of the PBX 9404 hydrolysis products discussed above. The major nonvolatile product was found to be formate. For comparison, a similar HMX hydrolysis was done using ammonium hydroxide instead of sodium hydroxide. The 5-to-1

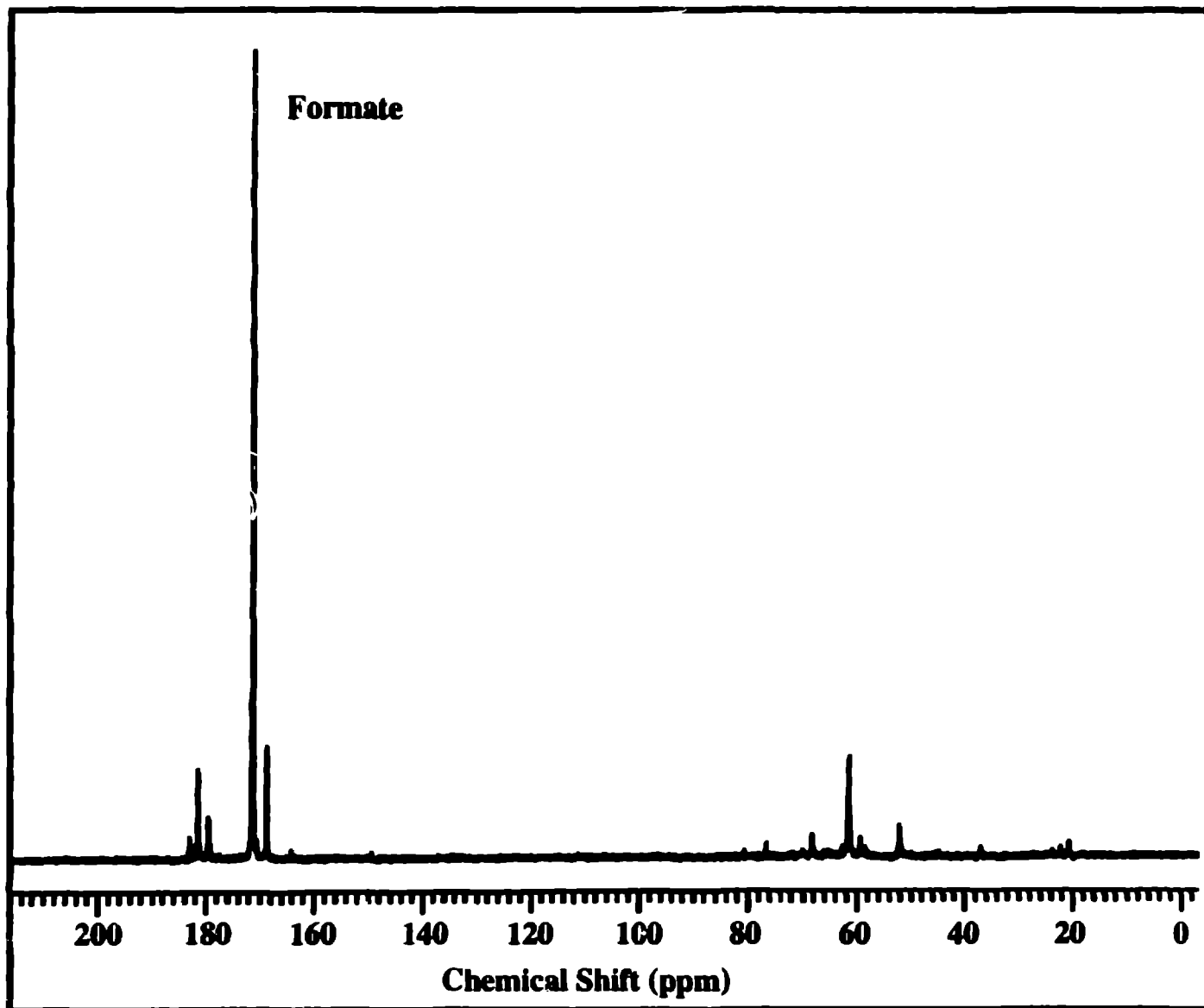
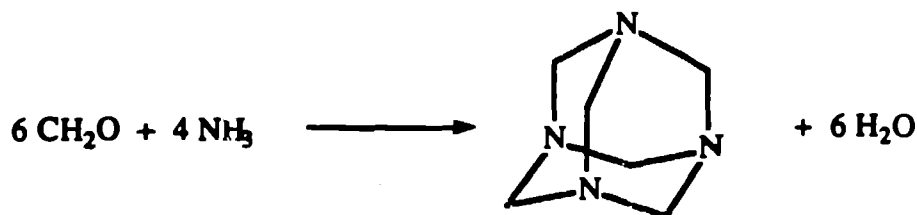


Figure S6. ^{13}C NMR spectrum of HMX hydrolysis residue.

ammonium hydroxide/HMX mixt was heated to 150 °C, reaching a final pressure of 104 psi after 60 minutes (compared to the control, which gave a final pressure of only 56 psi). When the vessel was cooled to room temperature, the residual pressure was 34 psi. Analysis of the gaseous products again gave nitrous oxide as the major product and significantly more nitrogen than produced in the sodium hydroxide experiment. The nitrogen formation may be due to decomposition of ammonium nitrite. The NMR and MS analyses of the liquid phase showed the major product to be hexamethylenetetramine instead of formate.

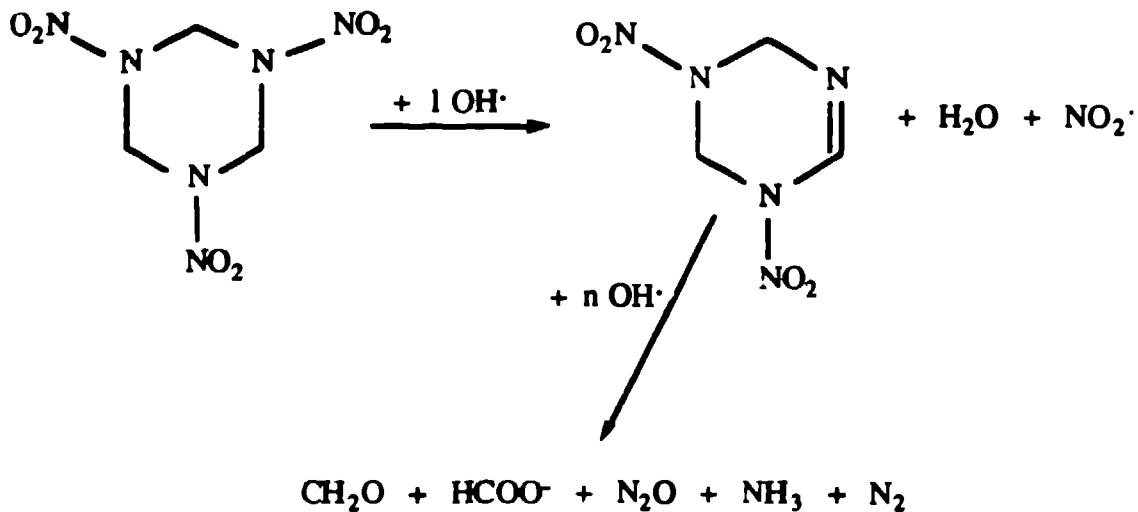
When the HMX hydrolysis reaction is carried out with aqueous ammonia as the base, much less formate ion is produced and a significant amount of hexamethylenetetramine is formed. Interestingly, hexamethylenetetramine can be used as a starting material for HMX and RDX syntheses. Its production can be explained by the reaction of ammonia and formaldehyde as follows:



5. Hydrolysis of RDX

RDX was hydrolyzed using ammonium hydroxide as the base in a 1-liter pressure vessel. The pressure vessel was heated to 150 °C. After 49 minutes the pressure of the system had leveled off at 70 psi. Upon cooling, the residual pressure was found to be 15 psi; however, the gaseous products were not analyzed. The liquid phase was analyzed by ¹³C NMR, which showed two carbon species. The major product is identified as hexamethylenetetramine and the other product is probably formate.

From References 25 and 26, the mechanism of base hydrolysis of RDX is the following:



Hydrolysis of the product formed by the first step proceeds very rapidly, making isolation of the first product difficult. The kinetics of this process have been previously investigated (References 31-33). When ammonium hydroxide is used for the base hydrolysis, the major product is hexamethylenetetramine. Its production can be explained by the reaction of ammonia and formaldehyde, as was discussed in the section on HMX.

6. Hydrolysis of M31A1E1 Propellant

M31A1E1 is a gun propellant manufactured at the Radford Army Ammunition Plant in Radford, VA. The hydrolysis and SCWO of this propellant were conducted in conjunction with our project sponsored by the U. S. Army Corps Of Engineers Construction Engineering Research Laboratory. We received the M31A1E1 propellant in the form of tubular sticks of dimensions 29 by 0.275 inches with a 0.098 inch diameter perforation. For small scale hydrolysis reactions of less than a gram, the propellant was ground to a powder. Larger scale reactions of up to a quarter pound were performed on the propellant stick as received. Normally, ten to fifteen milliliters of 2 molar sodium hydroxide were used per gram of M31A1E1. This translates to a two to three fold molar excess over the moles of nitro groups in the propellant, assuming the nitrocellulose is 13% nitrated. No reaction was visible upon mixing at ambient temperature. When the mixture was heated above 60 °C, gas evolution was observed, and at boiling a small amount of foaming occurred. Completion of the reaction occurred on the same general time scale as described for

NQ. The resulting solution was dark brown with a suspension of carbon black, which is a minor component (0.05%) of the propellant.

Analysis of the M31A1E1 hydrolysis products was performed by mass spectrometry, ^1H and ^{13}C nuclear magnetic resonance (NMR), and by ion chromatography. Figure 57 shows the ^1H and ^{13}C NMR spectra of a solution of the propellant in deuterated dimethylsulfoxide. Absorbances due to nitroguanidine (NQ), nitroglycerine (NG), nitrocellulose (NC), ethyl centralite (EC), and dibutylphthalate (DBP) can be seen in the proton NMR. Because NC is polymeric, the peaks due to it are very broad. The largest absorbances seen in the ^{13}C NMR are due to NQ and NG. The small peaks are EC and DBP, and the carbons of NC do not show up at all. Figure 58 is the ^{13}C NMR spectrum of the water-soluble hydrolysis products. The major peaks from the spectrum have been identified as sodium carbonate, urea, and sodium cyanate (NaOCN), which are the same products as for the NQ hydrolysis. In addition, sodium formate was detected and at least ten minor products that contain carbon. One of the minor products was identified as sodium oxalate. Previous studies (Reference 26) of nitroglycerine hydrolysis have identified nitrate, nitrite, acetate, and formate as the primary products. These products have also been detected from nitrocellulose hydrolysis, along with many others such as ammonia, cyanides, and modified cellulose. The ^1H and ^{13}C NMR spectra of the hydrolysis products showed no detectable amount of any of the propellant components.

A small scale experiment was performed to obtain quantitative analysis of some of the M31A1E1 hydrolysis products. A 120 milligram piece of propellant was hydrolyzed in excess sodium hydroxide solution for 30 minutes at 93 °C. The gases evolved were collected and analyzed by mass spectrometry. The mass spectrographic data identify the major gaseous product as nitrous oxide (N_2O). The amount of nitrous oxide gas evolved was found to be approximately 200 cc per gram of propellant hydrolyzed. The aqueous solution of hydrolysis products was analyzed by ion chromatography. Anions detected and quantified by ion chromatography include nitrite, nitrate, carbonate, cyanate, and oxalate. In addition, at least ten minor products, including formate, were detected but could not be quantified. The carbon was also quantified by TOC and TIC analyses. The concentration of urea was estimated from the integrated ^{13}C NMR. Although ^{13}C peak intensities are very dependent on relaxation times, this approach was found to be self-consistent by comparing the concentrations of carbonate and cyanate estimated from ^{13}C peaks to the concentrations determined by independent analytical techniques. These results are summarized in Tables 36, 37, and 38.

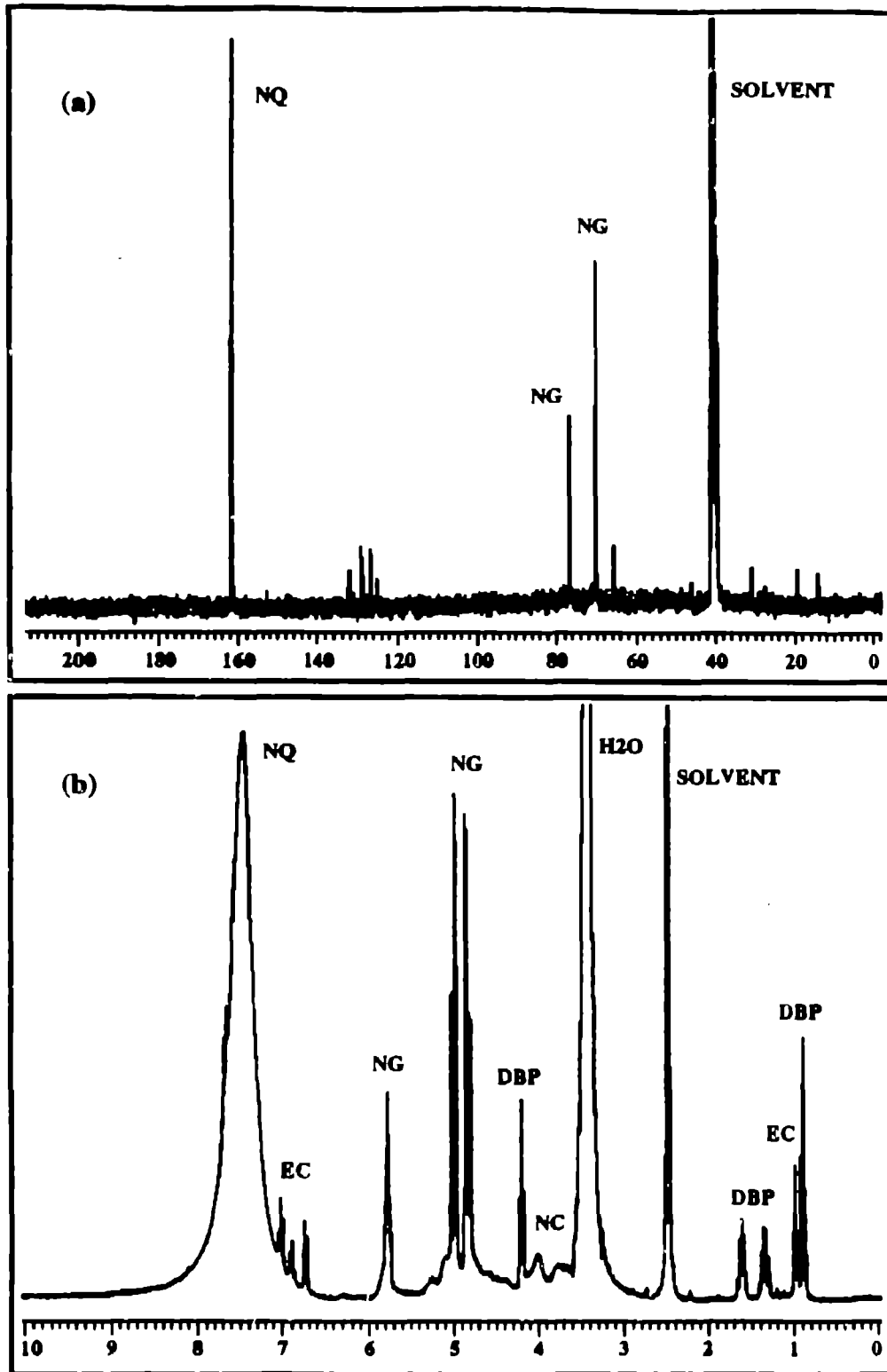


Figure 57. Spectra of M31A1E1 in deuterated DMSO. (a) ^{13}C NMR and (b) ^1H NMR.

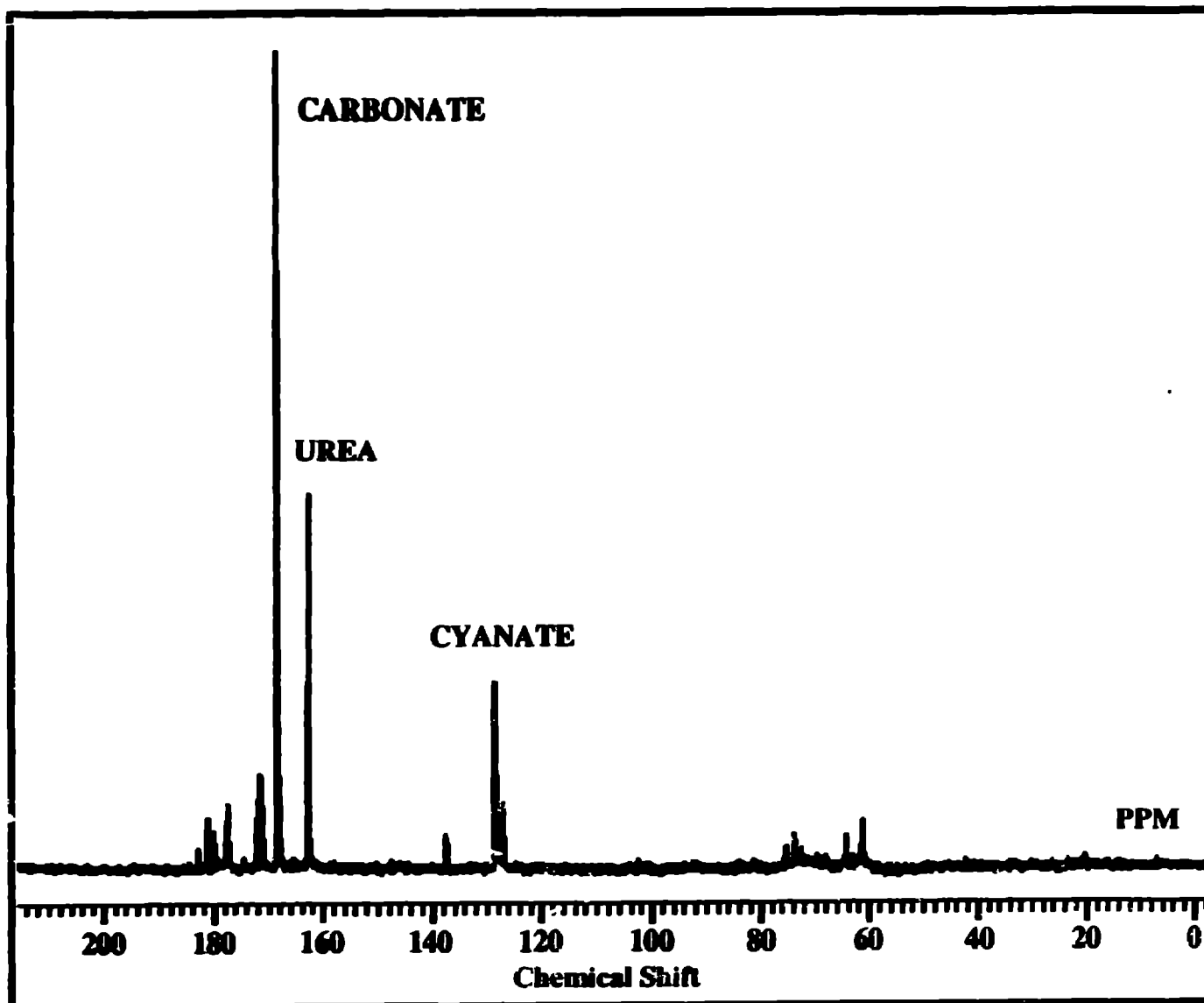


Figure 58. ^{13}C NMR spectrum of the water-soluble hydrolysis products of M31A1E1.

TABLE 36. CARBON PRODUCTS FROM M31A1E1 HYDROLYSIS

Product	[Product] ppm ^a	[C] ppm (%) ^b
Cyanate (OCN ⁻)	3565	1019 (12)
Oxalate (O ₂ CCO ₂ ²⁻)	1145	312 (3)
Urea (OC(NH ₂) ₂)	5729	1146 (13)
TIC (CO ₃ ²⁻ , HCO ₃ ⁻)	2504	2504 (29)
Total C		4981 (57)

^aDetermined by Ion Chromatography except for urea, which is estimated from ¹³C NMR peak intensities

^b% is the percent C occurring as specified product; the initial concentration of C was 8750 ppm

TABLE 37. TOC/TIC ANALYSIS OF M31A1E1 HYDROLYSIS PRODUCTS

	ppm	% carbon ^a
TOC	5853	67
TIC	2504	29
Total C	8357	96

^a% is the percent C occurring as the specified product

Calculated mass balances for carbon are shown in Tables 36 and 37. A comparison of these tables shows that a considerable fraction of the organic carbon is contained in molecular forms that could not be quantified with the analytical techniques employed. The calculated mass balance for nitrogen is shown in Table 38. In contrast to the carbon analysis, all of the nitrogen is accounted for, within the experimental error of the analytical procedures. The bulk of the nitrogen is converted to N₂O and lost from solution. The nitrogen remaining in solution is primarily urea and nitrite.

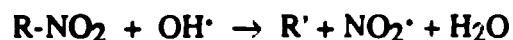
TABLE 38. . . NITROGEN PRODUCTS FROM M31A1E1 HYDROLYSIS

Product	[Product] ppm	[N] ppm (%) ^a
Ammonium (NH ₄ ⁺)	309	240 (1)
Nitrate (NO ₃ ⁻)	4225	954 (5)
Nitrite (NO ₂ ⁻)	5940	1808 (10)
Cyanate (OCN ⁻)	3565	1188 (7)
Urea (OC(NH ₂) ₂)	5729	2674 (15)
Nitrous Oxide (N ₂ O)	(gas)	(gas) (64)
Total N		(102)

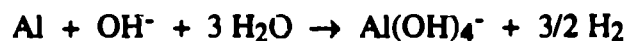
^aPercent N occurring as specified product

7. Hydrolysis of CYH Propellant

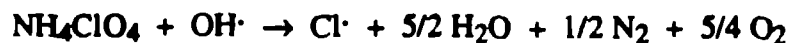
CYH is a double-base rocket propellant that is class 1.1 and contains 19.8 wt % aluminum. The material was received in the form of large chunks, approximately 50 g in weight, and was processed to smaller particles for the hydrolysis experiments. Reactions with sodium hydroxide were first performed on a very small scale, 100 mg, and later scaled up to as much as five grams. The amount of sodium hydroxide used was at least a factor of 2 greater than that required for complete reaction with all components of the propellant, according to the following analysis. The components of the propellant which react with base are the organic explosives, the aluminum and the ammonium perchlorate. Our work on the hydrolysis of pure explosives has revealed that generally one unit of base is consumed per nitro group in the explosive:



The reaction of aluminum metal with base consumes one mole of base per mole of aluminum:



Finally, the reaction of ammonium perchlorate with base consumes one mole of base per mole of AP:



The concentration of N, Al and AP in CYH (1.1) propellant is 0.011, 0.0074 and 0.001 moles per gram of propellant, respectively. According to the above analysis, the sum of the number of moles of N, Al and AP per gram of propellant yields the number of moles of OH⁻ required (0.0194 moles or 0.8 g NaOH) per gram of propellant. Typically, 20 milliliters of 2 molar sodium hydroxide solution (1.6 g NaOH) per gram of propellant were used. Upon mixing the propellant with the sodium hydroxide solution at ambient temperature, reaction was observed as gas evolution from the particles. Presumably, the gas was hydrogen from the reaction of aluminum metal with base.

During the reaction of 5 grams of CYH with 100 ml of base solution, the temperature of the solution rose slightly from the aluminum reaction and, after approximately ten minutes, leveled off at 3 ° above ambient. Heat was applied to the mixture causing more vigorous gas evolution as the temperature increased. As the boiling point of the solution was reached, foaming became a problem and was counteracted with a defoaming agent. After boiling for approximately 30 minutes, no solids or gas evolution were visible and the reaction was considered complete.

The hydrolysis products were analyzed by NMR spectrometry. The ¹³C and ¹H NMR spectra of a DMSO extract of CYH is shown in Figure 59, while the corresponding spectra for the hydrolyzed solution is shown in Figure 60. No CYH was observed in the hydrolysis solution and the major carbon-containing products were identified as acetate and formate anions. A small amount of carbonate was detected along with at least ten minor unidentified products. In another experiment, ion chromatographic analysis was performed on a product solution in which 520 mg of CYH was reacted with 20 ml of 2 molar sodium hydroxide. The results are presented in Table 39. From the composition of CYH listed in Table 34, page 120, the total carbon and nitrogen contents of the propellant can be calculated as 16 and 14 percent, respectively. The ion chromatography accounts for 44 % of the total carbon and 45 % of the total nitrogen. The gaseous products from CYH hydrolysis were analyzed and found to contain hydrogen, nitrous oxide, and a small amount of nitrogen.

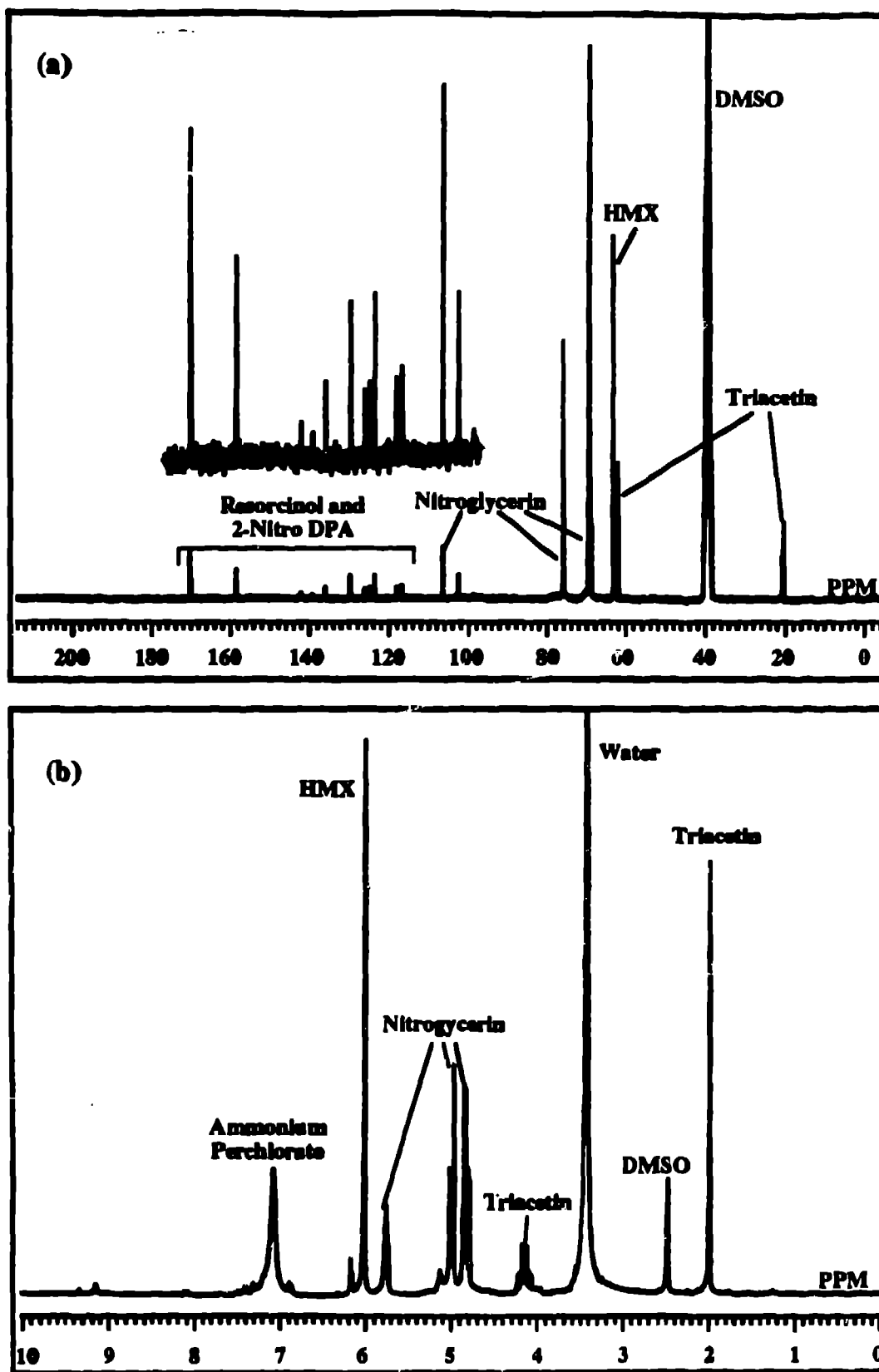


Figure 59. Spectra of CYH in DMSO and water solution. (a) ^{13}C NMR and (b) ^1H NMR.

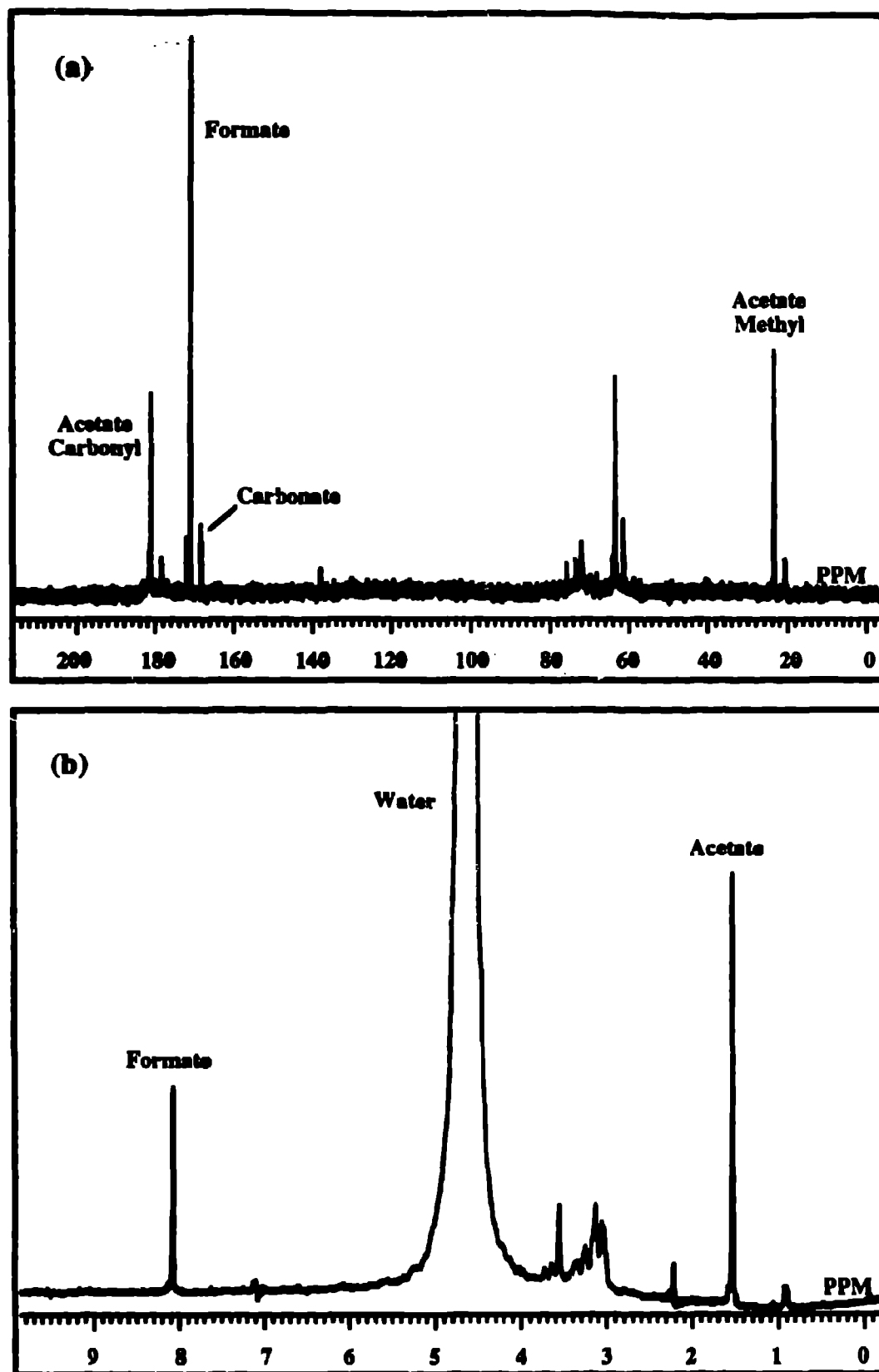


Figure 60. Spectra of CYH hydrolysis products. (a) ^{13}C NMR and (b) ^1H NMR.

TABLE 39. ANIONIC PRODUCTS FROM THE HYDROLYSIS OF CYH PROPELLANT

Anion	Conc. (g/liter)	Total Moles	Wt. % of Total
Acetate	3.40	1.2 e-3	34 % of C
Formate	1.55	0.69 e-3	10 % of C
Nitrite	3.69	1.6 e-3	32 % of N
Nitrate	2.10	0.68 e-3	13 % of N

8. SCWO of Hydrolysis Products

Several solutions resulting from the hydrolysis experiments were processed in the gold-lined supercritical water reactor. These included TNT, RDX, NQ, HMX, and the triple-based propellant M31A1E1. The chemical composition of these effluents has been discussed; they contain essentially organic decomposition products from the explosives. These effluents were analyzed for nitrites, nitrates, ammonia, TIC and TOC. The results are presented in Table 40.

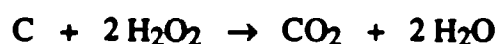
TABLE 40. ANALYTICAL ASSAY OF HYDROLYSIS EFFLUENT

Substrate	NO ₂ ⁻ (ppm)	NO ₃ ⁻ (ppm)	NH ₄ ⁺ (ppm)	TIC (ppm)	TOC (ppm)	Substrate (ppm)
TNT	2577	5.06	185	1080	3380	<2
RDX	1476	111	2325	34.7	1777	2.6
NQ	5.1	57.1	a	a	a	1886
HMX	605	355	a	<0.5	10255	22.5
M31A1E1	5940	4225	309	2504	5853	a

a: not analyzed

Except for NQ, the hydrolysis effluent typically contained more NO₂⁻ than NO₃⁻. This is not surprising since hydrolysis is not an oxidative process. The unusually large NH₄⁺ concentration found in RDX resulted from the ammonium hydroxide (NH₄OH) that was used to initiate hydrolysis. Sodium hydroxide was the base used in the other cases. Although the NQ hydrolysis effluent was not analyzed for NH₄⁺, the odor of NH₃ was apparent. The total carbon analysis exhibited high organic concentrations indicative of the breakdown products. The effluents were also analyzed for any remaining explosive and we see fairly efficient destruction as a result of the hydrolysis (better than 98 percent in all cases, and for TNT and RDX better than 99.9 percent).

These effluents were processed through an SCWO reactor at 600 °C at a residence time of 11 seconds. The hydrolysis solutions were processed directly, except for the M31A1E1 solution, which was diluted a factor of ten prior to injection into the SCWO reactor, to yield an initial carbon concentration of 836 ppm. Attempts to run the undiluted M31A1E1 hydrolysis mixture resulted in clogging of the reactor, probably due to precipitation of sodium carbonate. In each case, the amount of oxidant, H₂O₂, was in excess of the stoichiometric ratio. In addition, for the M31A1E1 mixture, two different oxidant concentrations were examined. In this case, the concentration of the oxidant was varied from a stoichiometric ratio to a ten-fold excess based on the following chemical reaction



The results are presented in Tables 41, 42, and 43. We demonstrate extremely high destruction efficiencies for the combined hydrolysis / SCWO processes, ranging from > 99.99 percent to > 99.9999 percent. The residual explosive concentrations were all below detectable limits after processing through the SCWO reactor.

TABLE 41. INITIAL CONCENTRATIONS AND DESTRUCTION EFFICIENCIES FOR HYDROLYSIS / SCWO PROCESSES

Substrate	Oxidant concentration	Initial concentration (ppm)	Destruction Efficiency (%)
TNT	excess	11350	>99.9971
RDX	excess	11200	>99.9996
NQ	excess	125000	>99.99992
HMX	excess	15000	>99.9995
M31A1E1	stoichiometric (1:1)	836	>99.9909
M31A1E1	10:1	836	>99.9989

The major gas-phase products as determined by FTIR spectra taken during the SCWO process were N₂O and CO₂. A typical FTIR spectrum is shown in Figure 61, which was obtained during the SCWO of the M31A1E1 hydrolysis mixture. It was not possible to obtain a mass balance on the hydrolysis / SCWO procedure because the gas effluent was not completely accounted for during the hydrolysis step.

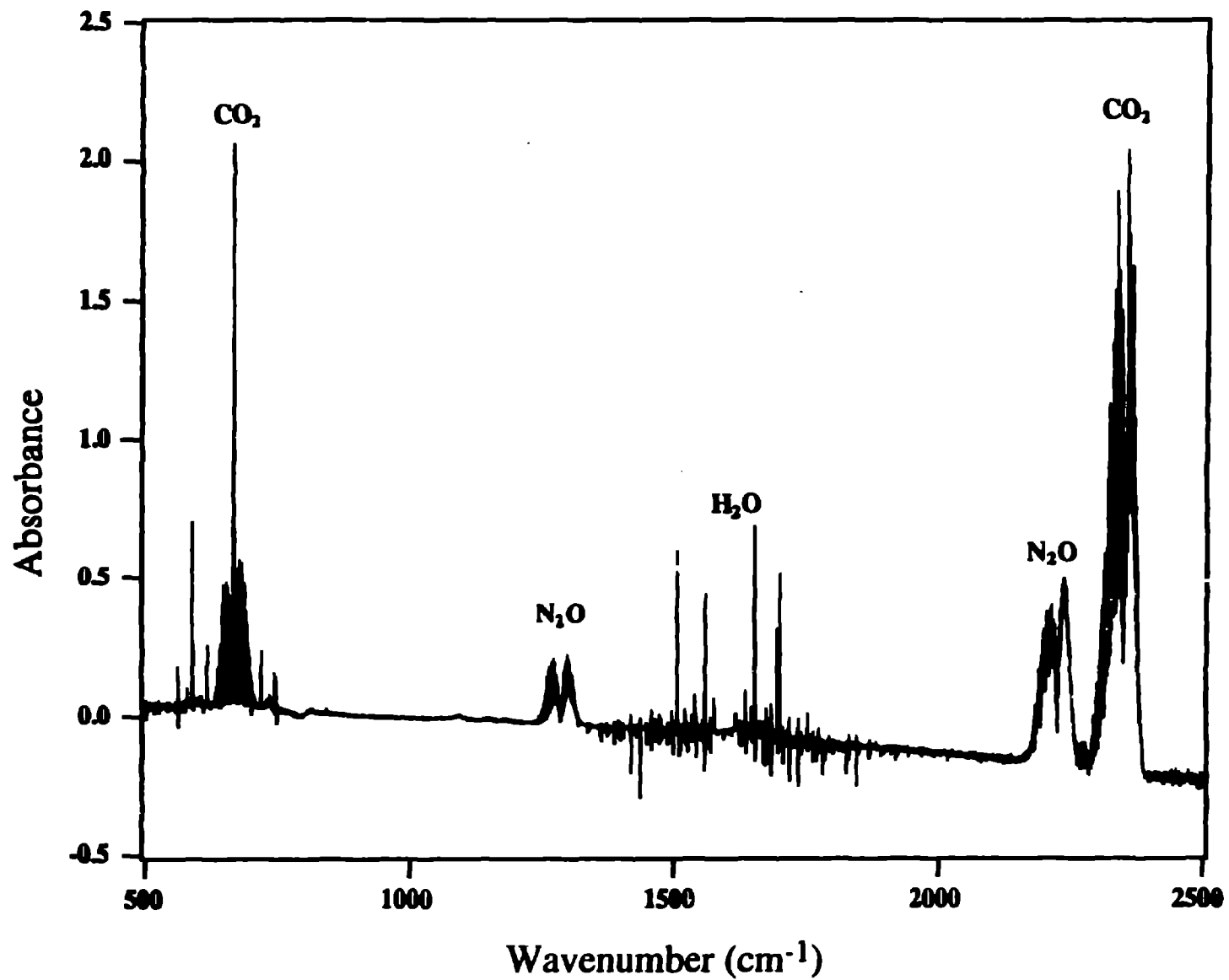


Figure 61. FTIR spectrum of gas-phase products from SCWO of M31A1E1 hydrolysis solution.

The analysis for the carbon content of the aqueous reactor effluent is shown in Table 42. The data are presented in both parts per million and as a percent of the total initial carbon content. Appreciable quantities of TIC remained in solution for all explosives except HMX. The inorganic carbon was probably present as HCO_3^- or CO_3^{2-} . The TOCs were very low and, for TNT, below detection limits. In the solubility-limited studies of NQ (i.e., those with no hydrolysis pretreatment), the aqueous carbon accounted for 83 percent of the total. With hydrolysis the aqueous carbon is less than one-half of one percent. This result may be due to the different chemical pathways of the oxidation of the hydrolysis products rather than for NQ itself. The remaining carbon product for all cases (at least through the SCWO reactor) was present in the form of CO_2 .

TABLE 42. ANALYSIS OF AQUEOUS CARBON PRODUCTS IN EFFLUENT STREAMS AFTER SCWO

Substrate	TIC		TOC	
	(ppm)	(% of Initial C)	(ppm)	(% of Initial C)
TNT	9.63	9.51	<0.2	<0.01
RDX	37.89	3.72	0.46	0.07
NQ	22.42	0.31	0.49	0.01
HMX	0.20	0.06	0.70	0.09
M31A1E1 (1:1)	33.3	3.98	0.08	0.009
M31A1E1 (10:1)	30.6	3.66	0.01	0.001

The nitrogen content of the SCWO reactor effluent was analyzed and is presented in Table 43. Again, the data are presented as ppm and as a percent of total initial nitrogen. The trends are similar to the straight SCWO of these explosives. The total concentration of nitrites and nitrates in the aqueous effluent was much higher, but the starting explosive concentrations were two orders of magnitude higher than in the solubility-limited experiments. The actual percent of starting nitrogen converted to NO_2^- and NO_3^- was lower for TNT, RDX and HMX and about the same for NQ. Trinitrotoluene (TNT) continues to show the highest NO_x^- production rates. Nitrous oxide (N_2O) and nitrogen (N_2) are found in the FTIR and the mass spectra as the only detectable gas-phase nitrogen species.

TABLE 43. ANALYSIS OF AQUEOUS NITROGEN PRODUCTS IN EFFLUENT STREAMS AFTER SCWO

Substrate	NO ₂ ⁻		NO ₃ ⁻	
	(ppm)	(% of Initial N)	(ppm)	(% of Initial N)
TNT	28.22	7.56	89.95	17.05
RDX	18.11	0.23	2.32	0.022
NQ	8.54	0.01	166.59	0.11
HMX	2.93	0.09	133.99	2.88
M31A1E1 (1:1)	2.77	0.05	0.95	0.01
M31A1E1 (10:1)	13.2	0.23	97.2	1.28

SECTION V

SPECTROSCOPIC MEASUREMENTS IN SUPERCRITICAL WATER

A number of optical diagnostics were developed as part of the effort to better understand the hydrothermal destruction processes. These *in-situ*, non-invasive diagnostics are useful in the investigation of fundamental properties of supercritical fluids, including phase equilibria and chemical kinetics. The Raman and Coherent Anti-Stokes Raman Spectroscopy (CARS) diagnostics were utilized to identify intermediate and product species, yield information on their state, such as solvation, and measure reaction rates. Transient grating spectroscopy was applied to the measurement of diffusivity and fluid sound speed, which yield state information. Further, the real-time nature of the diagnostics may be exploited for the development of process monitoring and control.

A. RAMAN MEASUREMENTS OF HYDRAZINE

The Raman spectrum of a mixture of 2 wt% hydrazine (N_2H_4) in water at 270 atm is shown in Figure 62. Spectra are shown over a range of temperatures from room temperature to just above the critical temperature of water ($T_c=374$ °C). The broadest feature in these spectra is the O-H stretching band of water. One of the N-H stretching bands of hydrazine is indicated at 3300 cm^{-1} . (There are also two smaller bands at 3220 cm^{-1} and 3361 cm^{-1} .) (Reference 34) As the temperature increases, this band disappears and a new band grows in at 3314 cm^{-1} , which we assign (Reference 35) to NH_3 . The intensity of this band suggests that ammonia is a major product of hydrazine decomposition.

The integrated area of the Raman peak at 3300 cm^{-1} serves as a measure of the hydrazine concentration. By using the optical cell as a steady-state flow reactor, the kinetics of the decomposition may be determined. This was done by setting the flow rate to some constant value and allowing the system to equilibrate. From the known water density and heated volume, we calculate the residence time of the fluid from the entrance of the cell to the optical window, with the fluid flow in a steady-state condition. The Raman intensity then gives the fraction of hydrazine remaining at this residence time. By repeating this for various flow rates, the decay of the concentration is measured as a function of residence time. Figure 63 shows the decay of the hydrazine Raman signal as a function of residence time at 400 °C. At times longer than those shown, the intensity decays to zero, as expected. For each data point, the Raman intensity of

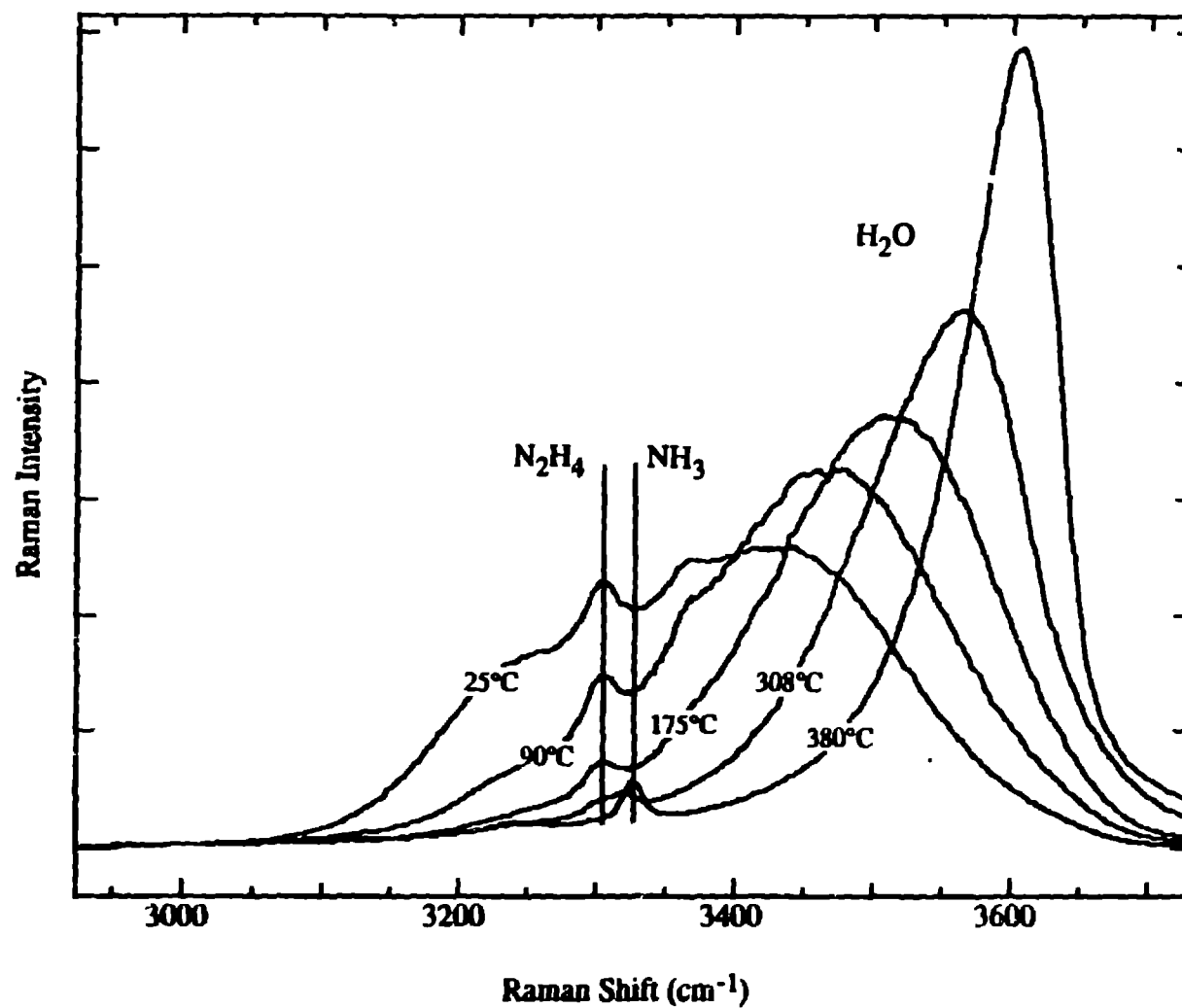


Figure 62. Raman spectra of hydrazine in water at 270 atm, in the region of the N-H stretching vibrations. Spectra are shown from 25°C to 380°C. Curves were scaled to the same total area.

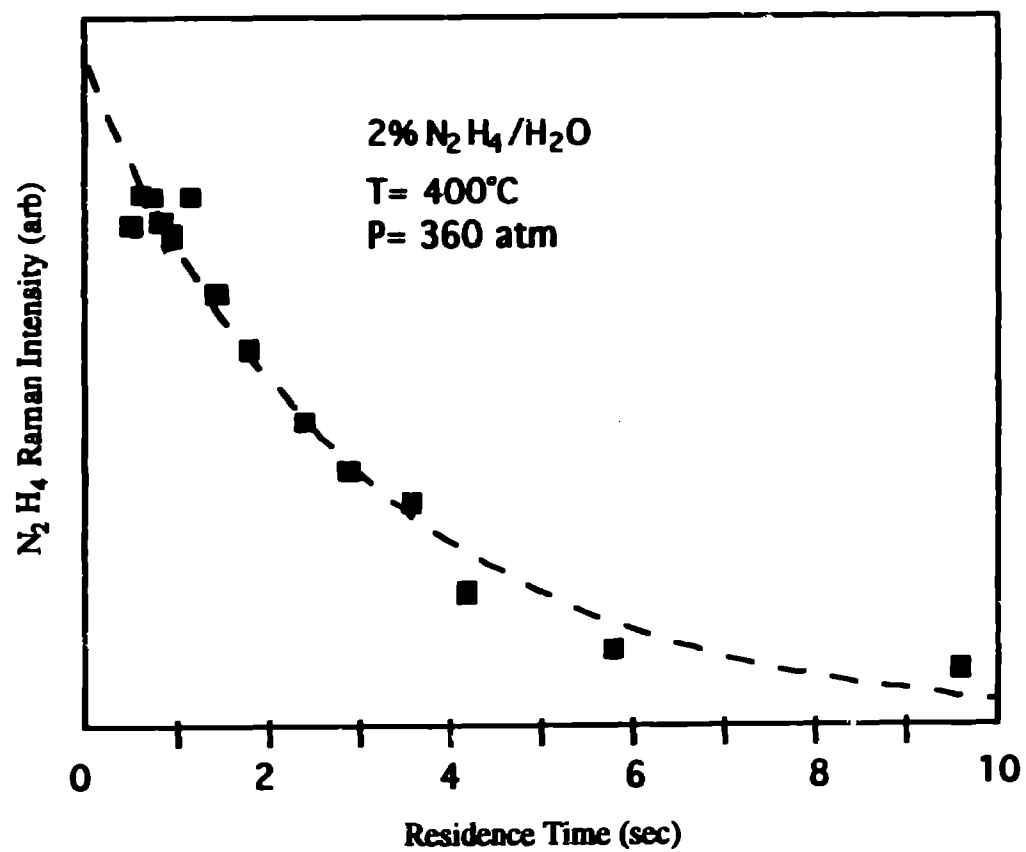


Figure 63. Decay of hydrazine Raman intensity as a function of average residence time in the optical cell. The dashed line is an exponential fit to the data.

hydrazine was normalized to the peak area of the water band to correct for signal fluctuations. Although the limited signal-to-noise ratio does not permit us to rule out non-exponential decay of the concentration, we can at least assign an effective first-order rate constant for decomposition, $k(400\text{ }^\circ\text{C}) = 0.32\text{ sec}^{-1}$.

An alternative analysis is made by following the hydrazine concentration while heating the optical cell. At each temperature, we calculate the residence time in the reactor, measure the extent of decomposition from the Raman intensity and deduce the effective first-order rate constant. At several temperatures throughout the range depicted, the decay was followed as a function of residence time to verify that it was approximately exponential. Agreement between the two methods was excellent. In this way, an Arrhenius plot for the rate is generated, as shown in Figure 64. We derive the rate expression $k(\text{sec}^{-1}) = 5.2 \times 10^8 \exp(-14220/T)$. It is interesting to note that the critical temperature of water (647 K, or $10^4/T_c = 1.55$) is situated in the middle of the range of our measurements shown in Figure 64. There does not appear to be any anomalous or discontinuous behavior of the rate as one passes through the critical temperature.

Tsang (Reference 38) has analyzed the available data on the elementary hydrazine decomposition reaction and used RRKM theory to derive the high-pressure limit, k_∞ . Pressure-dependent measurements suggest that this reaction should be at the high-pressure limit under our conditions. Tsang gives a rate of $k_\infty(\text{sec}^{-1}) = 10^{16.25} \exp(-32300/T)$ in the temperature range 840-1150 °C. It is probably not appropriate to extrapolate this rate down to 400 °C, but it is interesting to note that the extrapolation gives a rate in our temperature range that is much smaller than what we observe, by a factor of 10^4 . There are several possibilities for this difference: (1) our disappearance rate could be influenced by chain-reaction processes; (2) the decomposition in our optical cell might be surface catalyzed at the reactor walls; (Reference 15) (3) the reaction mechanism in near-critical and supercritical water may be different from that in gases. Melius (Reference 39) has presented calculations relevant to the last possibility, which indicate that solvation can reduce activation barriers to reaction. In addition, uncertainties in reactor residence time and temperature may be important, as discussed below.

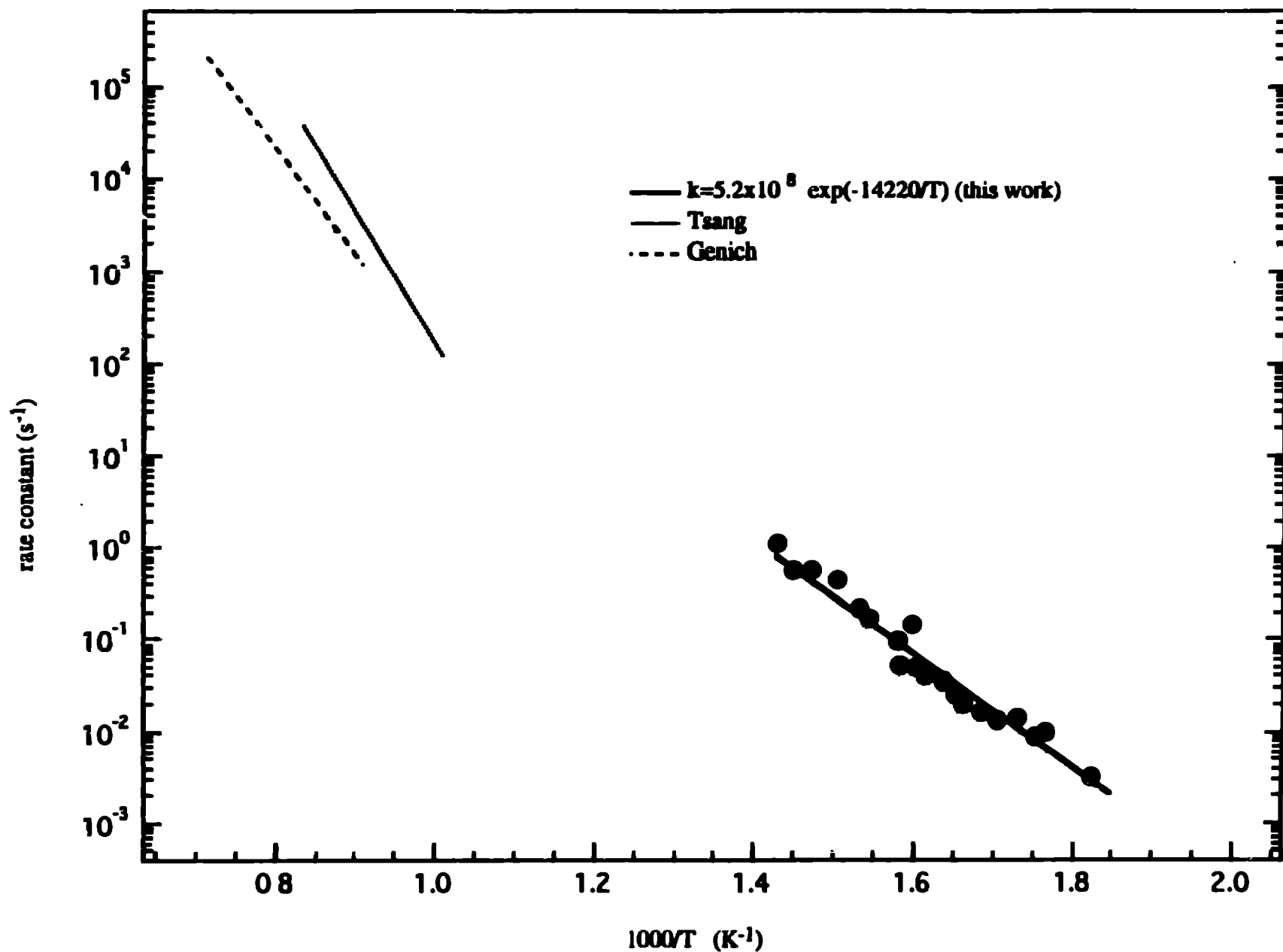


Figure 64. Arrhenius plot of effective first-order decay rate for 2% $\text{N}_2\text{H}_4/\text{H}_2\text{O}$ at 350 atm. Rates were determined by monitoring Raman intensity as a function of temperature, shown as circles. Also shown are rates for reaction (1) in the gas phase reported by Genich¹⁵ and Tsang¹⁹.

We measured the relative Raman cross sections of N_2H_4 and NH_3 in water for the bands near 3300 cm^{-1} to quantify the amount of ammonia produced. We found that the N_2H_4 cross section is greater by a factor of 1.3 ± 0.1 . Comparison of the intensity of the unreacted N_2H_4 peak to the NH_3 peak after reaction gives the conclusion that 1.5 ± 0.2 moles of NH_3 are produced per mole of N_2H_4 consumed. This is greater than the 0.9-1 mole of NH_3 produced in the gas phase (References 13-14) and close to the 1.3 moles of NH_3 observed for heterogeneous decomposition. (Reference 15) We also expect to produce N_2 and H_2 in this reaction. (References 13-19) These products were not observed, probably due to their smaller Raman cross sections and the limited sensitivity of our measurements.

These experiments were carried out at low flow rates, where the Reynolds number for the fluid flow is fairly small (in the range 10-1000). In the absence of disturbances, this would give rise to laminar flow, in which the reactor has a distribution of residence times rather than a single, well-defined residence time. Also, it is possible that a radial temperature gradient could exist in the fluid. These uncertainties make it difficult to derive reliable decomposition rate constants from the data. Although the plug-flow approximation can be used at low Reynold's numbers if certain criteria are satisfied, (Reference 37) those conditions were not always met in these experiments. In addition, the heat-up time of the fluid in the reactor was not measured and was a function of flow rate. However, preliminary fluid dynamics calculations that we have carried out using the code FLUENT (Fluent, Inc., Lebanon, NH), suggest that the heat-up time is much shorter than the 3 seconds reaction time shown in Figure 63, page 149. The calculated radial temperature distributions in the fluid are fairly narrow. In addition, natural (gravity-induced) convective heating effects and obstructions in the flow tube may disrupt the flow patterns and impart some degree of turbulence to the fluid, which is desirable for use of the plug-flow approximation. Therefore, one must exercise care in interpreting the results in a more quantitative fashion.

B. RAMAN MEASUREMENTS OF NITROMETHANE (NM)

The Raman spectrum of 0.15-10% nitromethane/water mixtures were collected at temperatures from 500-560 °C at pressures near 5500 psi. The flow rates of the solutions through the reactor were varied from 0.1 to 2 g/minute, corresponding to reactor residence times of 0.2 to 3 seconds. The evolving concentration of the nitromethane was determined by integration of the Raman scattering intensity of the methyl stretching peak near 2980 cm^{-1} . The C-N stretching peak at 900 cm^{-1} was also monitored. Decomposition of NM and formation of product CH_4 (2914 cm^{-1}) was observed at temperatures above 520 °C. An example at 554° is shown in Figure 65.

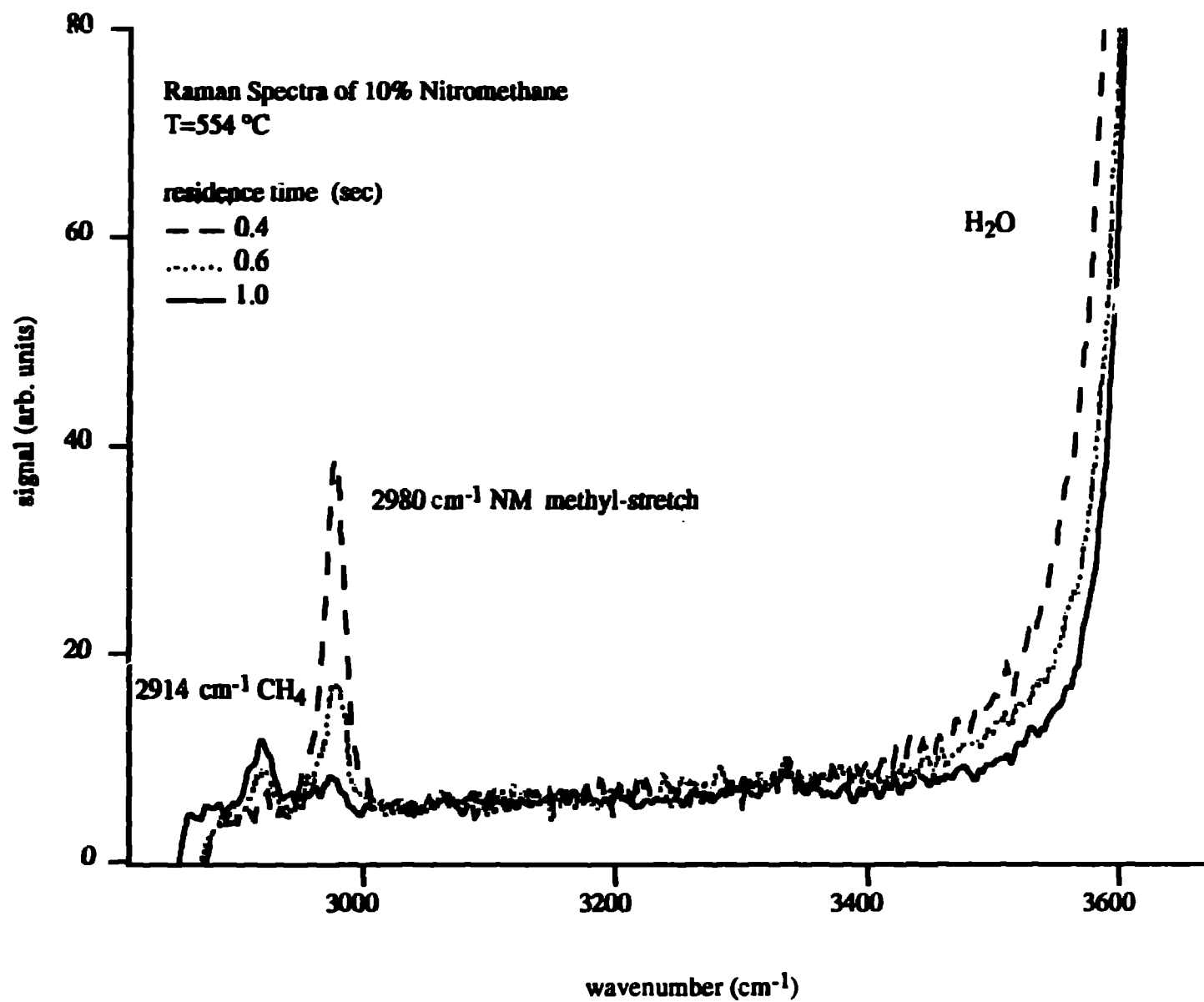


Figure 65: Raman spectra of 10% nitromethane in water at 554 °C and 370 atm in the region of the methyl-stretching vibrations.

Figure 66 shows the time history of a 10% solution at two temperatures. At longer times, full destruction of the nitromethane, within experimental uncertainties, was observed.

Although the limited signal-to-noise ratio does not permit us to rule out non-exponential decay of the concentration, we can assign effective first-order rate constants for decomposition in four experiments. The rate constant for nitromethane decomposition determined from these optical measurements is combined with determinations from end product analysis of total organic carbon (TOC) from our flow reactor and results of sub-critical temperature experiments at SRI (Reference 40) (Figure 67). It is encouraging to note the good agreement, and fit to an Arrhenius expression, over a wide temperature range with diverse experimental setups.

Addition of hydrogen peroxide accelerated the nitromethane reaction rate. Three seconds residence time was sufficient for the destruction in mixtures of 10% nitromethane and twice stoichiometric H_2O_2 at 280 °C and 3000 psi. In this case, methane was not an observed product.

C. RAMAN MEASUREMENTS OF AMMONIUM PERCHLORATE (AP)

Raman spectroscopy was used to follow the decomposition of AP in supercritical water. The optically accessible reactor (Figure 23, page 45) was configured as a batch reactor and coupled to a pressure intensifier with water used as a pressure-transfer fluid. Ammonium perchlorate solutions were prepared at a concentration of 100 g/L, which is about one-half the solubility limit at room temperature. Small samples (0.1 mL) were loaded into the reactor and heated to 550 °C. Temperature, pressure and Raman spectra were recorded once every 10 seconds. At temperatures below the critical point of water, the perchlorate ion produced a strong Raman signal (the symmetric Cl-O stretch at 974 cm^{-1}). The Raman peak of the ammonium ion near 3100 cm^{-1} could not be observed because it lies near the strong and broad O-H stretching peak of liquid water. Near the critical temperature (374 °C), the Raman scattering from the perchlorate ion disappears and a feature at lower energy appears for about 10 seconds, after which it disappears. When the solution is cooled, the perchlorate signal does not reappear indicating that it has reacted. A fine black powder remains as a suspension in solution after the reaction. Analysis of this powder using inductively-coupled plasma atomic emission (ICP-AE) indicated that it contained large amounts of iron with trace amounts of other metals. These suggest that the perchlorate ion reacts with the 316 stainless-steel reactor walls to form metal oxides.

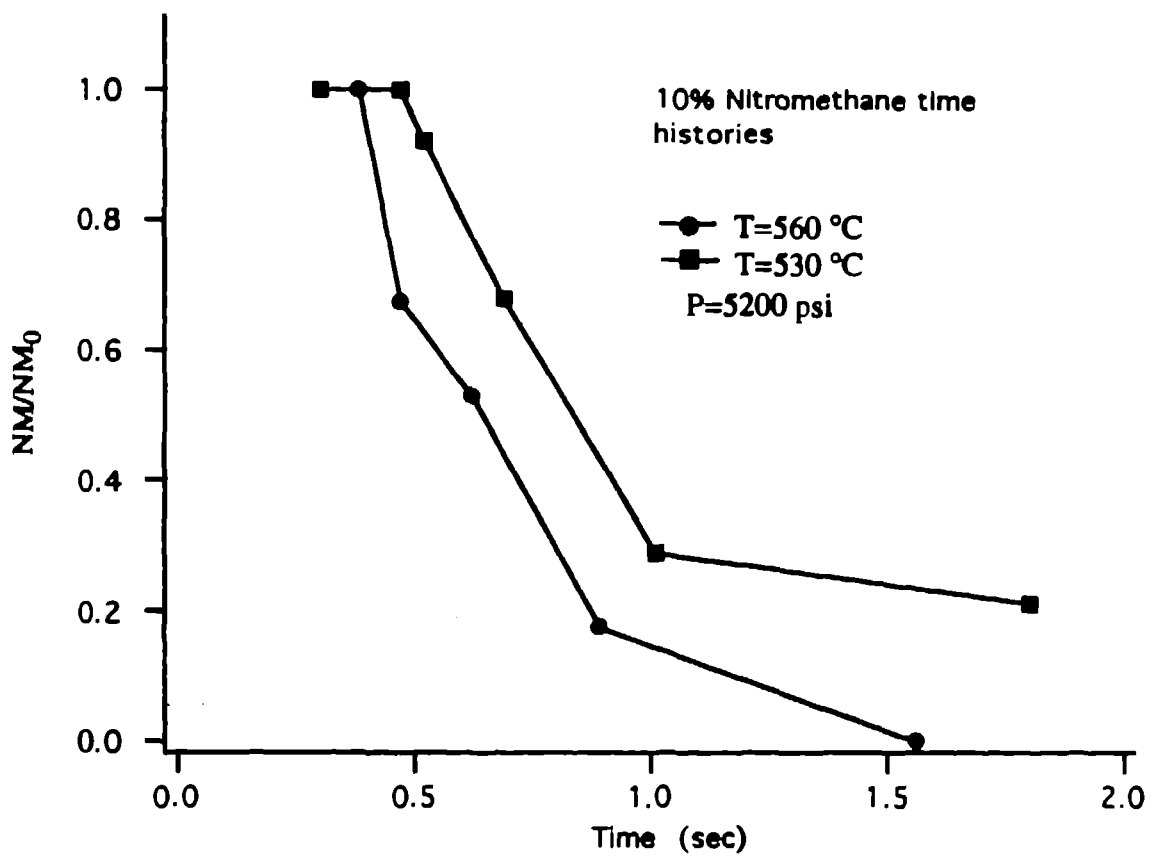


Figure 66. Decay of nitromethane Raman intensity as a function of residence time in the optical cell.

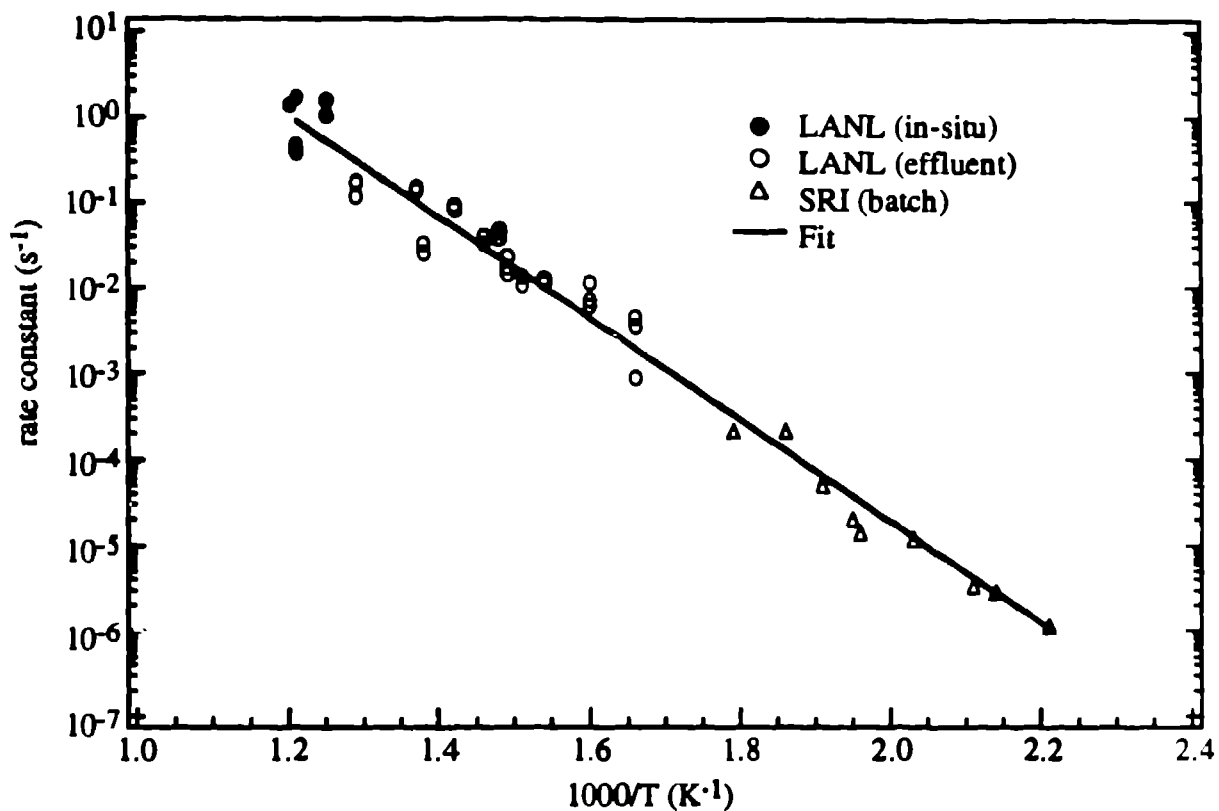


Figure 67. Arrhenius plot of effective first order decay rate for nitromethane/water mixtures. Solid circles were determined by monitoring Raman intensity, open circles were determined from effluent analysis. Also shown are the determinations of Jayaweera (Reference 40).

D. MEASUREMENTS OF NITROMETHANE USING CARS

The CARS spectra of 5 percent nitromethane in water are shown in Figure 68. Shown in the figure are (a) the spectrum of pure water at 410 °C and 340 atm, the spectrum of the MN/water mixture at (b) 410 °C and 340 atm, and (c) room temperature and 340 atm. Spectrum (a) shows the contribution made by the nonresonant CARS generated by the water and by the diamond windows of the cell. This produces a large background "hump" in all of the spectra. The shape of the hump reflects the spectral profile of the broad-band laser. The sharp feature in the center of the spectra (b) and (c) is due to the Raman band of nitromethane at 917 cm^{-1} , which corresponds to the C-N stretching motion of the molecule.

The most salient difference between the CARS spectra at room temperature and supercritical temperatures is the width of the spectrum, which increases from 2 cm^{-1} at 20 °C to 8 cm^{-1} at 410 °C. In the room-temperature liquid, the Raman spectrum of the molecule consists of a single, sharp vibrational transition. As the temperature increases, the density decreases, and nitromethane becomes more of a gas-phase-like molecule that can rotate freely. The rotation gives rise to additional structure within the vibrational band. Although this additional structure cannot be resolved under these conditions, it appears as a broadening of the Raman spectrum. Hence, optical diagnostics of solute molecules in supercritical water can give information on the solvation environment.

Analysis of the observed CARS line shapes would be simplified considerably if the nonresonant contribution from the water solvent and the diamond windows were absent. It is possible to eliminate this contribution with a modification of the technique that involves rotating the polarizations of the input laser beams and using polarization filtering of the signal beam.

E. TRANSIENT GRATING EXPERIMENTS

Experiments were performed to demonstrate the feasibility of measuring thermal diffusion constants and the speed of sound on hydrothermal solutions using the transient grating technique. Thermal grating decay rates were measured for I_2 dissolved in aqueous KI solutions. Figure 69 shows a typical thermal grating decay for a solution at 5040 psi and 400 °C, and a fringe spacing of $13.5\text{ }\mu\text{m}$. The line is the least squares fit to an exponential function and has a lifetime of $42.1 \pm 2.3\text{ }\mu\text{s}$, which corresponds to a thermal diffusivity $(0.56 \pm 0.03) \times 10^{-3}\text{ cm}^2\text{ s}^{-1}$. The thermal

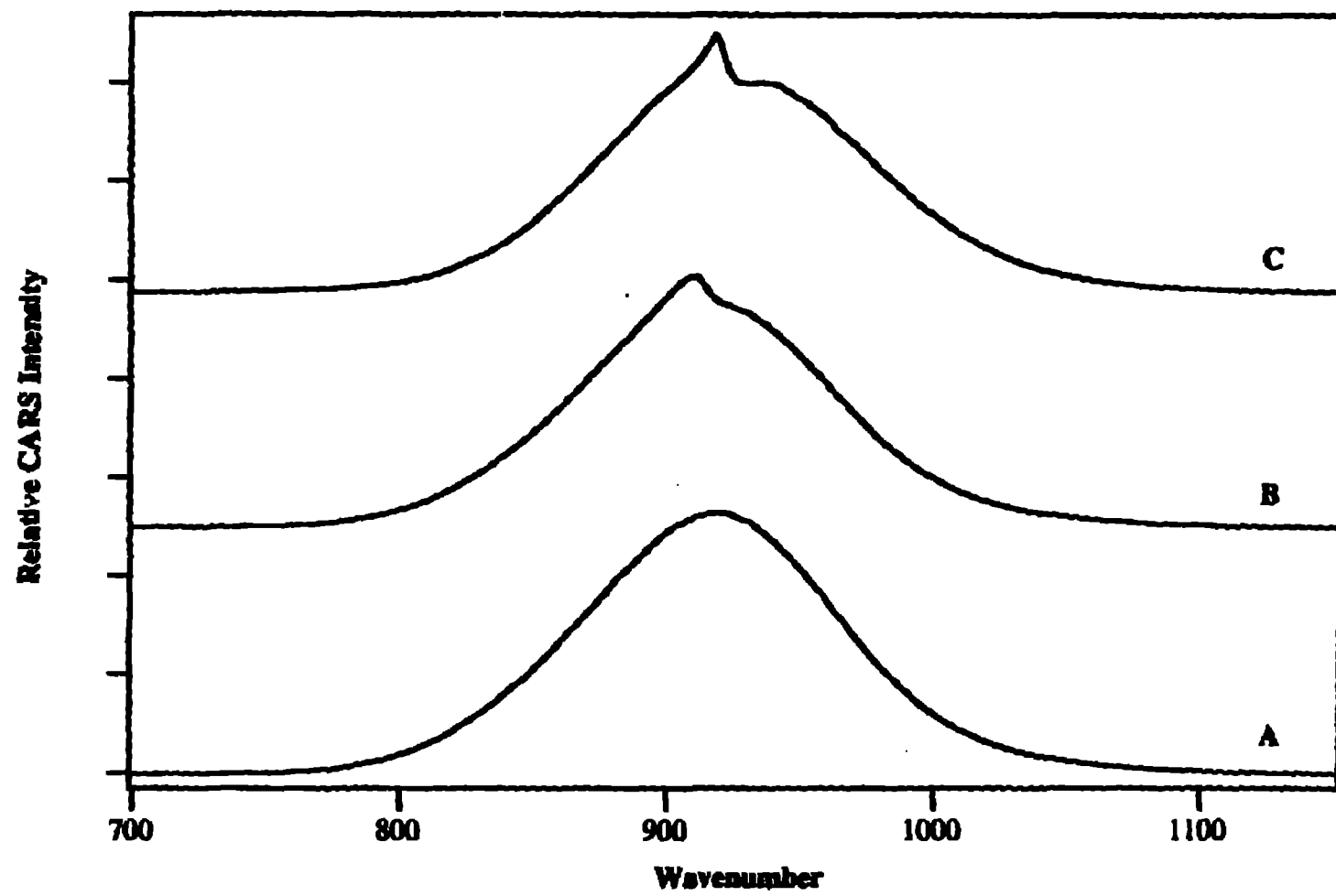


Figure 68. CARS spectra of NM in water at high pressure (348 atm). (A) Non-resonant water background; (B) Supercritical water (410 °C); (C) Subcritical water (20 °C).

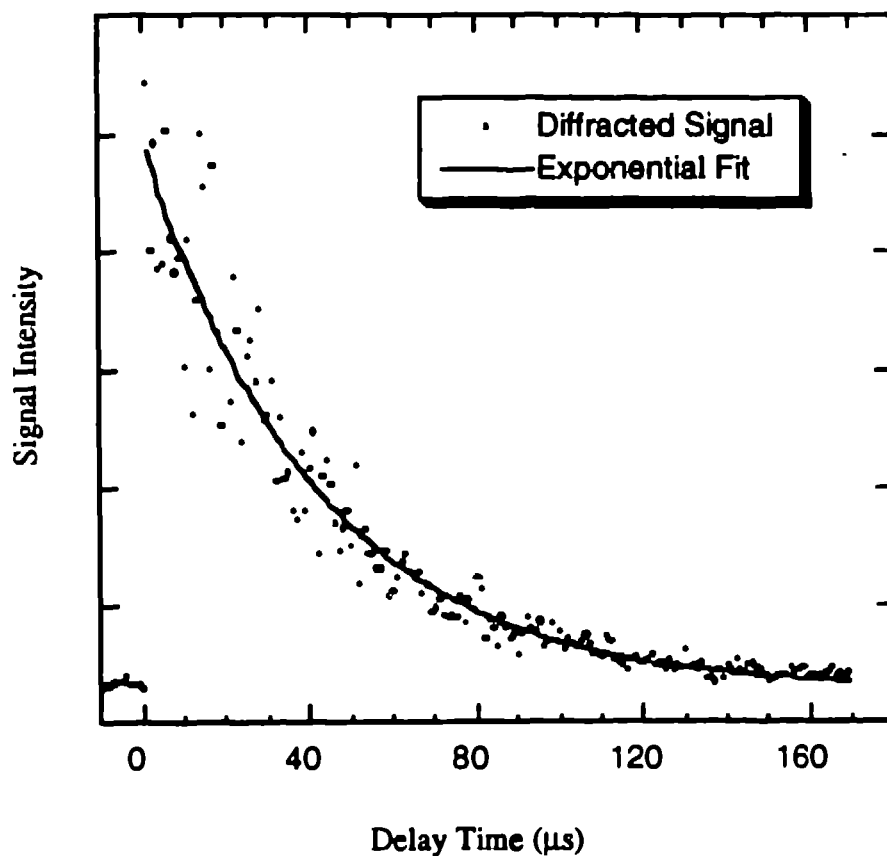


Figure 69. The thermal grating decay for an $I_2 + KI + \text{water}$ solution at 400°C and 5040 psi . The line is the exponential least-squares fit of the data. The grating fringe spacing is $16.1 \mu\text{m}$.

diffusivity of pure water under these conditions is $0.69 \times 10^{-3} \text{ cm}^2 \text{ s}^{-1}$. Ultraviolet transmitting diamond windows (Type I) would allow the technique to be applied to virtually any UV or visible light absorbing hydrothermal solution.

Figure 70 shows the grating signal resulting from acoustic waves generated in the same $\text{I}_2 + \text{KI} + \text{water}$ solution, at 450°C and 5060 psi. The fringe spacing is $13.5 \mu\text{m}$ and the acoustic signal period is 28.3 ns. The measured speed of sound is 477 m s^{-1} . This measured speed is reasonable as the speed of sound of pure water under these conditions is 505 m s^{-1} . The fastest speed of sound that can be measured with the current 10 ns pulse width lasers is approximately 1000 m s^{-1} . Measurements of faster speeds requires larger fringe spacings, but a grating needs greater than about 20 fringes for efficient probe scattering, and the current diamond window aperture of $600 \mu\text{m}$ limits the feasible fringe spacing to less than about $30 \mu\text{m}$.

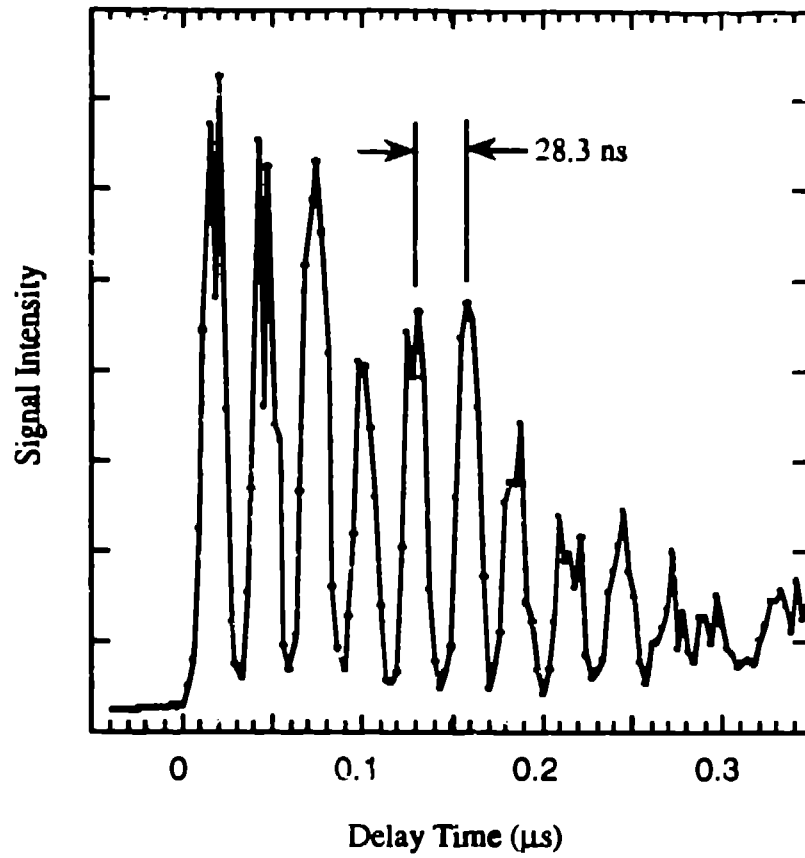


Figure 70. Transient grating signal from acoustic waves generated in a 450° C and 5060 psi methanol/dye solution. The grating fringe spacing is 13.5 μm and the acoustic signal period is 28.3 ns.

SECTION VI

THERMOCHEMISTRY OF ENERGETIC MATERIALS IN SUPERCRITICAL WATER

While supercritical water oxidation appears to have great potential as a way to dispose of energetic materials cleanly and safely, because of the nature of these materials, it is imperative to determine the heat released during the process. We have a commercial (Setaram 121) differential scanning calorimeter (DSC) to measure heats of reaction under supercritical conditions. We have measured heats of decomposition for ammonium perchlorate (AP), neat and in aqueous solutions, using cells supplied with the DSC at supercritical conditions. Results are given in Table 44.

TABLE 44. HEAT OF DECOMPOSITION OF AP IN STAINLESS STEEL CELLS

Weight of AP (mg)	Melting Point (°C)	Temp. of Decomp. (°C)	Heat of Decomp. (cal/g)
Neat AP			
3.90	243	357	440
3.32	244	356	406
2.79	242	366	374
2.31	242	367	393
1.85	241	357	335
5.1M AP in aqueous solution			
0.6	--	251	2165
0.6	--	263	2448
0.6	--	253	2210
0.1M AP in aqueous solution			
0.176	--	333	2542
0.176	--	329	2547
0.176	--	334	2346
0.265	--	336	2130
0.352	--	343	2590

Neat AP melts at 242 °C and decomposes at 349 - 373 °C with heats of 334 - 440 calories per gram AP. The decomposition in aqueous solution exhibits different behavior. Solutions 0.1 M in AP decompose at 329 - 343 °C with heats of 2130 - 2590 calories per gram AP. With 5.1 M solutions of AP, a decrease in the temperature of decomposition to 251 - 263 °C is observed. However the measured heats of decomposition, 2164 - 2447 calories per gram AP, are similar to those for the 0.1 M solutions. These results may indicate a strong influence of water on the energetics of decomposition of AP.

SECTION VII

REACTOR CORROSION

A. REACTOR METALLURGY AND CORROSION

One of the most critical issues affecting the practical implementation of SCWO processing to the treatment of energetic materials is reactor wear caused by corrosion. Corrosion of the Hastelloy C-276 reactor does not, at this time, appear to be a major problem with most of the energetic materials under investigation. The exception is ammonium perchlorate (AP), which causes severe corrosion of C-276 and, under certain conditions, 316ss gold-lined reactor. However, corrosion by AP has been reduced to acceptable levels in the gold-lined reactor by maintaining a basic pH with the addition of caustic.

B. CORROSION CAUSED BY SCWO REACTIONS OF ENERGETIC MATERIALS

On occasion, we have experienced mild to severe corrosion of experimental test apparatus. Corrosion reactions at the reactor wall may affect the reaction process under investigation, and in the extreme has resulted in failure of pressure containing components. Our experiences with corrosion caused by SCWO reactions of energetic materials are described in this section.

1. Corrosion by SCWO of Ammonium Perchlorate (AP)

The only compound for which any reactor-dependent chemistry has been observed is AP. The destruction chemistry of AP in SCWO is unique among the energetic materials since AP has no carbon, and is a strong oxidant. The chemistry is best described by the following equation:



The Cl is converted into Cl^- , formally reduced from 7^+ to 1^- , and excess oxygen is produced in the reaction. The highly oxidizing nature of this reaction is evident by the strong oxidative corrosion of the Hastelloy C-276 reactor. The addition of reducing equivalents, in the form of a fuel such as a hydrocarbon, may improve the destruction of AP as well as reduce the reactor corrosion.

Because of corrosion problems with the Hastelloy C-276 reactor, most of these reactions were performed in the gold-lined reactor. Sodium hydroxide is added to the AP solutions in a 1:1 stoichiometry to ensure a net pH balance. However, we have run AP in the gold-lined reactor in both alkaline and acidic solutions. Significant corrosion is observed in acidic solutions of AP. At low pH, the oxidation of gold, $Au^0 \rightarrow Au^{+3} + 3e^-$ is activated. The oxidant could be NO_3^- produced in the decomposition of AP or the perchlorate itself. The gold complexes with chloride ion and is dissolved into solution as $AuCl_4^-$. These reactions are analogous to the well-known dissolution of gold in aqua regia. By raising the pH, this corrosion pathway is blocked as shown in Table 45.

An interesting observation with the gold-lined reactor is a lower destruction efficiency for AP compared to that found for the Hastelloy C-276 reactor. We attribute this difference to the absence of reactions with the reactor walls in the case of the gold-lined reactor. The extensive corrosion of the Hastelloy C-276 reactor by AP reactions supports this conclusion.

TABLE 45. CORROSION PRODUCTS FOR SCWO OF AMMONIUM PERCHLORATE

Reactor Material	Au (ppm)	Cr (ppm)	Fe (ppm)	Mo (ppm)	Ni (ppm)
Hastelloy C-276	---	130.00	---	54.00	39.00
Gold-lined 316ss (acidic)	1622.00	3.36	65.38	---	55.04
Gold-lined 316ss (alkaline)	0	0.99	0.99	---	3.73

2. Corrosion by TNT, HMX, PETN and RDX

No significant difference in DREs and products chemistry was observed for reactions of TNT, HMX, PETN and RDX in the Hastelloy C-276 and the gold-lined reactors. We conclude from these observations that reactions with the Hastelloy C-276 and 316 stainless walls must not be significant for these energetic materials. The metals concentrations in the reactor effluent are just above background levels, corroborating the above conclusion. Corrosion products from the Hastelloy C-276 reactor are given in Table 46.

TABLE 46. CORROSION PRODUCTS FOR SCWO OF EXPLOSIVES IN HASTELLOY C-276 ALLOY LINEAR REACTOR

Substrate	Cr (ppm)	Fe (ppm)	Mo (ppm)	Ni (ppm)
TNT	0.246	<0.02	0.095	<0.02
RDX	0.085	<0.01	<0.01	0.075
HMX	0.097	0.013	0.07	0.0375
PETN	<0.01	0.032	0.62	0.0572

3. Corrosion by Nitrate

Nitrates are formed when explosives are oxidized in supercritical water. As discussed in previous sections, the amount of nitrogen converted to nitrate and nitrite depends upon the substrate and the reaction conditions. A nitrate pyrolysis run was also conducted. At 525 °C and a 12.6-second residence time, a maximum nitrate conversion (to nitrite) of 36 percent was observed. No ammonia was detected from nitrate pyrolysis at 525 °C. In addition to analysis for carbon and nitrogen species, aqueous effluent and reactor rinse samples were also analyzed for sodium (present in the sodium nitrate feed) and corrosion products (Fe, Cr, Mo, and Ni). Trace amounts of corrosion products were recovered in all experiments. While iron and nickel have appeared only at sub-ppm levels in all experiments, chromium and molybdenum have been present at higher concentrations in both effluent and rinse water samples. At temperatures above 500 °C, these species have been recovered primarily in reactor rinse water samples. These samples, which were yellow tinted, we believe contain the hexavalent forms of chromium (CrO_4^{2-}) and molybdenum (MoO_4^{2-}). These species likely deposited on the reactor walls as sodium salts. Sodium also precipitated substantially with carbonate species. These precipitation reactions are supported by ion balances performed on reactor rinse samples. Such balances have been successful in predicting measured pH values to within one pH unit. Effluent concentrations of sodium, bicarbonate, chromium and molybdenum decreased with increasing temperatures, which indicated decreasing solubilities with increasing temperatures. The absence of iron and nickel in the rinse effluent indirectly suggests formation of an insoluble passive oxide film on the reactor surface. However, no metallographic examination has been conducted to verify this.

4. Corrosion by Hydrazine

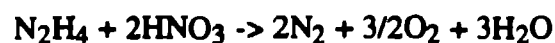
We have also investigated the reactions of hydrazine with an oxidizer in SCW. We chose the nitrate anion as the oxidizer to simulate reactions of nitrogen tetroxide, since we expect to

produce nitric and nitrous acid upon dissolution of N_2O_4 in water. We expected the following reaction of hydrazine with nitrate:



A new Hastelloy C-276 reactor was used for this reaction, having the unique feature of a vertical orientation, with the flow against gravity. This feature caused problems since one of the products of this reactions is NaOH as shown in the above equations. NaOH is molten above 300 °C and apparently forms a separate, molten alkaline salt phase at the concentrations employed (1000 ppm NaOH). This molten alkaline phase settled out in the bottom of the reactor, aided by gravity and produced severe corrosion in this part of the reactor, requiring rebuilding.

A reaction was also run using nitric acid as the source of nitrate oxidizer using the following assumed reaction stoichiometry:



With higher acid concentrations (pH=1) we again experienced sever reactor corrosion leading to plugging. In this case the corrosion was confined to the preheater section of the reaction tube.

C. CORROSION TESTING OF REACTOR MATERIALS

1. Introduction

Predicting corrosion rates for structural materials in high-temperature hydrothermal processing environments is not yet possible due to: (1) a general lack of corrosion data at elevated temperatures and pressures, and (2) poor understanding of basic corrosion mechanisms in high-temperature supercritical dense phase systems. The situation is further complicated by the sheer complexity of the substances proposed for treatment, the variety of possible corrosion mechanisms, and the wide range of operating pressures and temperatures and oxidizing/reducing environments under consideration.

Nevertheless, in view of the need to identify corrosion resistant materials for the construction of process equipment, we have initiated a corrosion testing and evaluation program. We plan to investigate the corrosion resistance provided by several alloys, and hope to gain an

improved understanding of the corrosion processes that are active in hydrothermal processing systems.

Corrosive attack may occur via a number of mechanisms which may act individually or in combination to render a particular material unsuitable for a particular process application. Nine of the more common corrosion attack mechanisms include:

- 1) Uniform corrosion
 - a) electrochemical
 - b) direct attack (chemical reaction)
- 2) Pitting corrosion
- 3) Crevice corrosion
- 4) Galvanic corrosion of dissimilar metals
- 5) Stress corrosion cracking
- 6) Intergranular corrosion
- 7) Dealloying
- 8) Embrittlement
- 9) Corrosive wear.

The type of corrosion mechanism active in a particular location is strongly affected by the fluid phase or phases present. For hydrothermal processing systems, it is necessary to investigate corrosion mechanisms that might occur in the preheater and cooldown heat exchangers, as well as in the main process reactor. The preheater and cooldown heat exchangers will be exposed to phases ranging from a cool liquid/slurry at one end, to hot supercritical dense phase with the possible presence of molten salts at the other end. The cooler liquid regions perhaps favor ionic electrochemical attack, and the hotter regions perhaps favor gas-phase oxidation/direct attack.

2. Discussion of Corrosion Testing Methods

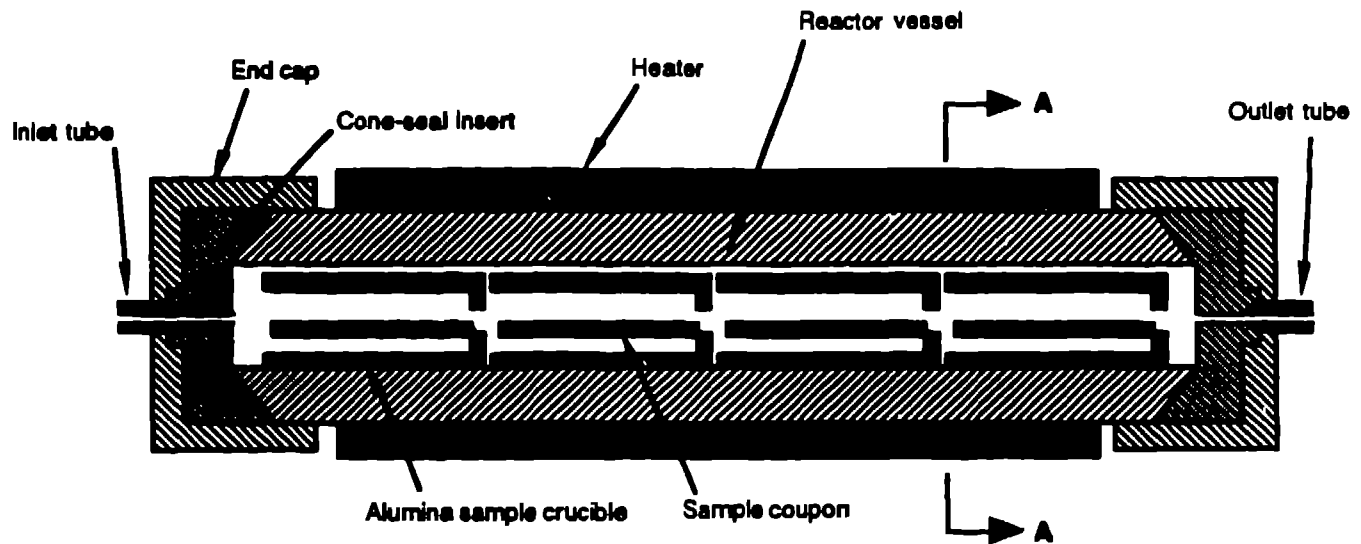
a. Coupon Testing

In view of the variety of available alloys and pure metals, the number of known corrosion mechanisms, and the many environmental factors affecting corrosion, our initial approach was to try to reduce the number of variables for study. We carried out a two-tiered investigation: First, the weight change caused by exposure to supercritical conditions was measured for a variety of sample coupons to investigate resistance to uniform corrosion and pitting

corrosion. For these tests we exposed sample coupons to basic (NaOH) or acidic (HCl) solutions of increasing concentration. Second those materials exhibiting resistance in these tests were short-listed, for future, more rigorous investigation into resistance to other corrosion mechanisms. In subsequent testing, the test coupons could be so arranged as to simulate tensile/residual stresses, welds, crevices, and contact between dissimilar metals.

An extended coupon testing program is difficult to perform for the following two reasons. (1) It is necessary to construct an experimental apparatus that can contain high-temperature, high-pressure, and a variety of potentially highly-corrosive substances in a safe and predictable manner for an extended period, and (2) poor reliability of delicate HPLC pumps and precision high-pressure pressure regulators due to the corrosive, non-homogeneous nature of the fluid media.

In the interim, while we considered ways to build a safe and reliable test apparatus, we assembled a temporary corrosion test apparatus as depicted in Figure 71 and Figure 72, and obtained sample coupons of a wide variety of alloys and pure metals. Our temporary apparatus included a 1/2 in. id x 20 in. long 316ss tubular reactor vessel and 6,000 psi-rated Tescom regulator. Sample coupons are approximately 0.25 in. wide x 1.375 in. long x 0.0625 in. to 0.125 in. thick. As a safety precaution the high-temperature components were located behind a Lexan barrier in a limited access area.



(NOTE: Actual reactor holds 12 sample crucibles)

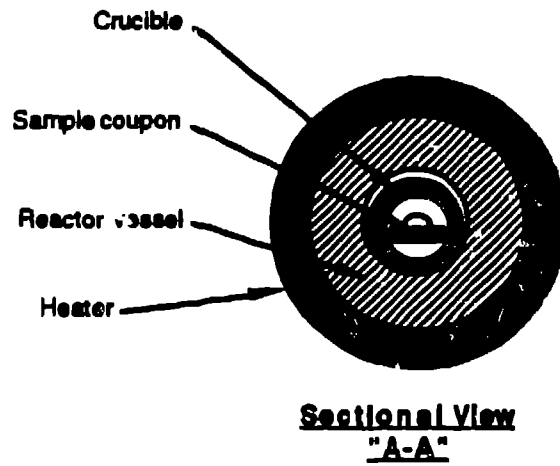


Figure 71. General arrangement of a SFWO corrosion test reactor.

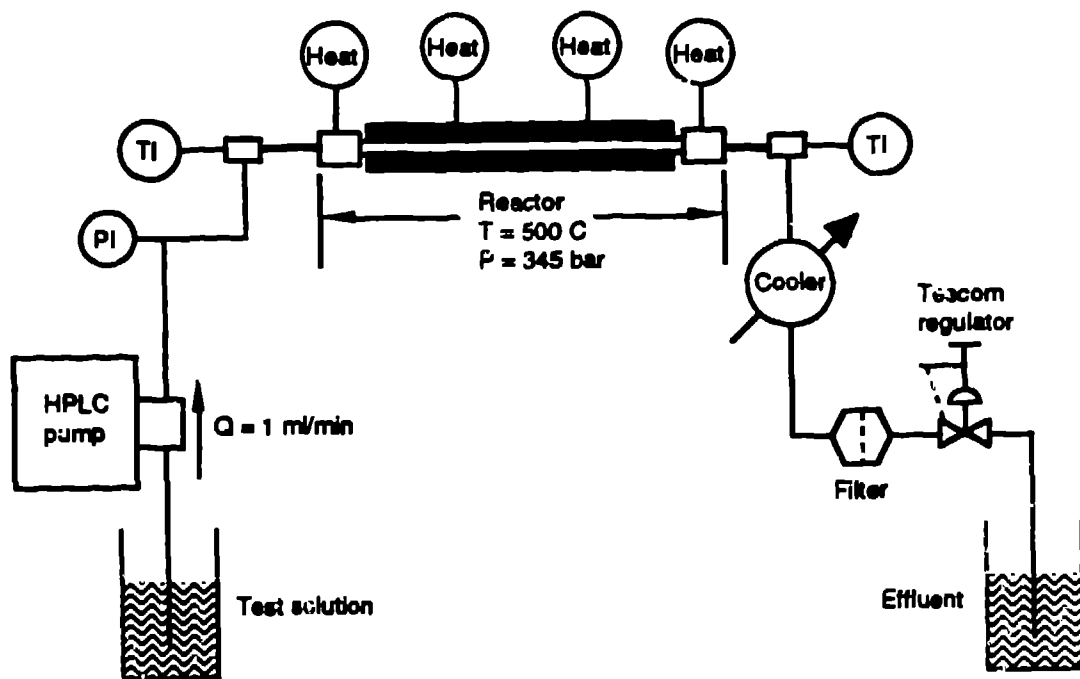


Figure 72. Flow schematic of SCWO corrosion test loop.

The nominal composition of alloys tested to date can be found in Table 47.

TABLE 47. NOMINAL COMPOSITION OF TEST ALLOYS

Alloy	Cr %	Ni %	Mo %	Co %	W %	Fe %	Other	Test Status
Haynes alloy HR-160	28	37	0	29	0	2		NaOH test
Haynes alloy N	6	71	15	0.2	0.5	5	1.0% Si	NaOH test
Haynes alloy 230	22	57	2	5	14	3		NaOH test
Inconel 625	21	62	9	1	0	5	3.7% Cb	NaOH test
Hastelloy C-276	16	57	16	2.5	4	5	1.0% Mn	NaOH test
Al ₂ O ₃ -coated Ultimet	26	9	5	54	2	3		NaOH test
Haynes alloy 214	16	75	0	0	0	3	4.5% Al	
Haynes alloy 556	22	20	3	18	2.5	31		
Haynes alloy G-30	28	43	4	5	1.5	13	1.5% Mn	
Hastelloy C-22	22	56	13	2.5	3	3		
Haynes alloy HR-120	25	37	2.5	3	2.5	33		

b. Corrosion by Basic Solutions

High concentrations of PEP's may be safely introduced into hydrothermal processing reactors by first hydrolyzing the material in a basic solution of NaOH. Base hydrolysis produces water soluble materials that can be pumped to high pressure for hydrothermal processing. Due to the caustic nature of the hydrolysis products, there is a need to identify suitable corrosion-resistant structural materials for the reactor that will hold up in caustic environments. The required concentration of base has been observed to be as high as 1.0 M. We decided to examine corrosion resistance to NaOH solutions of increasing concentration, without the presence of an oxidizer. In view of the low concentrations of corrosion products previously observed with basic solutions, it was felt that the 316ss reactor might allow testing for a reasonable period. Operational limitations imposed a maximum coupon exposure time of 5.0 hours. Based on this exposure time, the sample coupon surface area, and maximum sensitivity of the precision laboratory balance, the corrosion rate resolution could be as low as 1.0 mils/year equivalent weight change. The results of these tests can be found in Table 48, as follows:

TABLE 48. AVERAGE COUPON WEIGHT CHANGE

	[Na+],ppm	2.29	22.9	229	458
	Theoretical pH	10	11	12	12.3
Hastelloy C-276		-0.002%	0.023%	0.028%	0.046%
Haynes Alloy 230		0.005%	0.019%	0.046%	0.092%
Inconel 625		-0.006%	0.004%	0.026%	0.025%
Haynes Alloy HR-160		-0.003%	0.017%	0.000%	0.011%
Haynes Alloy N		0.009%	0.004%	-0.010%	0.050%
Al ₂ O ₃ -coated Haynes Ultimec		0.135%	0.046%	0.374%	0.430%

From the above it appears that the coupons tended to gain weight during the test. All coupons experienced an increasing weight gain with increasing [Na+], except for Haynes Alloy HR-160 and Haynes Alloy N. Comparison against Inconel 625 is considered important, as this alloy is currently prime candidate for pilot-scale plant fabrication yet is expensive and difficult to source in the required structural shapes.

Testing was interrupted twice due to reactor leakage. Disassembly and inspection of the inlet cone-seal insert revealed several fully-penetrating radial cracks. It is important to note that cracks occurred in both 316ss and Hastelloy C-276 inserts. As cracking occurred shortly after switching from deionized water to pH=13 NaOH solution, we believe the cracks to be caused by the concentrated NaOH environment. Out of concern for the integrity of the 316ss reactor, we chose to limit testing to pH<13.

During each test we periodically measured the pH of the test solution and effluent. We noticed that the pH of the effluent during the test never achieved the same value as the test solution pH, and on flushing the system with deionized water prior to cooldown/shutdown, there was a sharp increase in effluent pH. We concluded that the NaOH was largely insoluble in water at test conditions, and was separating out as a molten NaOH at the bottom of the reactor vessel. Consequently, we cannot determine what fluid phase (or phases) the coupons have been exposed to. In view of this, we now believe that the chosen experimental design is not suitable for corrosion testing under (potentially) multi-phase supercritical conditions. However, the test apparatus can and will continue to be used for corrosion testing under single-phase subcritical conditions.

c. Static Corrosion Test Apparatus

We have designed an alternate test apparatus for testing under all conditions, including multi-phase supercritical conditions. This apparatus is depicted in Figure 73. In this design, instead of using sample coupons, we are fabricating replaceable 3/8 in. od x 18 in. long tubular reactors from a variety of candidate alloys. Tube id will be designed to produce a tensile stress at the inner wall near to the maximum ASME allowable tensile stress for the test temperature and pressure. The system is designed to allow testing to 1,000 bar and 550 °C. By making the reactor tube itself out of the candidate material, we avoid the experimental problems associated with multi-phase segregation, and at the same time permit investigation of the materials resistance to a far wider and more realistic range of corrosion mechanisms. The reactor tubes will be charged with the actual waste or waste simulant at design temperatures and pressures, and held at these conditions for extended periods of up to several weeks, or until tube failure. To avoid problems associated with pump reliability and plugging of pressure regulators, we plan to maintain static pressure via an intensifier. If desired, the air pressure to the intensifier and the reactor temperature can be cycled for fatigue testing. We can also conduct extended testing with difficult-to-handle wastes, such as slurries, that would otherwise present pumping and plugging problems which are difficult to address at the small-scale. The design allows the periodic recharging of the system with fresh fluid. We will also be able to insert unstressed witness wires of various advanced materials and noble metal alloys which are being considered for unstressed internal system components, such as liners and sensor elements. Upon completion of the specified test period, the reactor tube will be removed and sectioned for comprehensive metallographic examination.

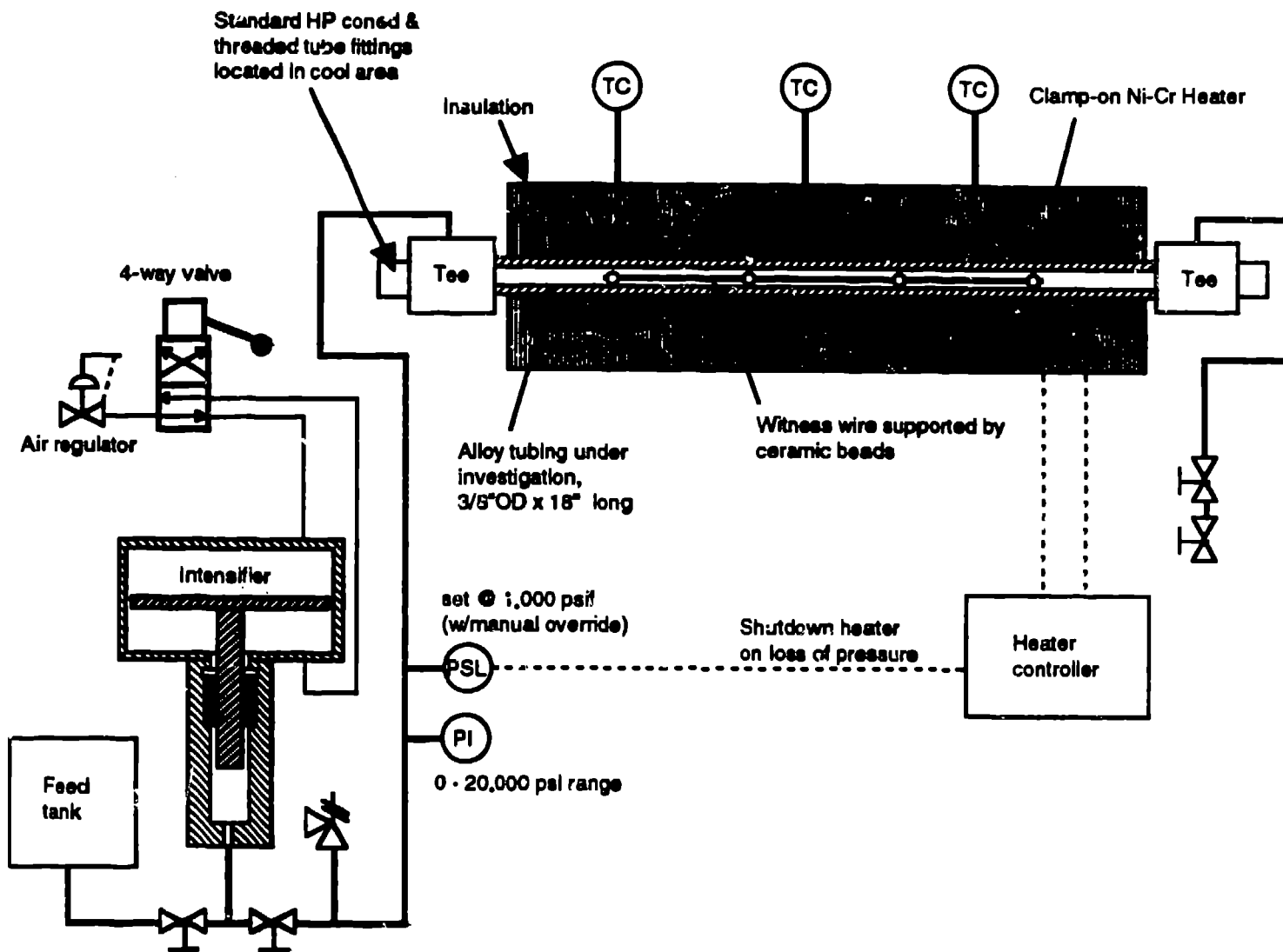


Figure 73. "Static" corrosion test reactor.

SECTION VIII

SALT SOLUBILITY STUDIES

A. INTRODUCTION

The solubility and phase behavior of compounds formed in base hydrolysis of propellants containing metallic aluminum is an important aspect of the treatability of such propellants in a hydrothermal system. Solubility depends in a complex way on the *temperature*, *pressure*, and overall *composition* (number and concentration of species). Salt solubility generally increases with increasing *temperature*; exceptions are salts such as carbonates which exhibit retrograde solubility behavior. The temperature of a hydrothermal processing system is determined by maximizing the destruction efficiency of the hydrolyzed propellant components (which generally occurs at higher temperatures) while minimizing corrosion and other unwanted reactions (nitrate formation). Unfortunately, temperature dependent solubility data from the literature does not generally extend to high enough temperatures to be in the "hydrothermal" range. Another difficulty is that the optimum hydrothermal processing temperature may be less than the liquid-vapor critical temperature (T_C) of the solution, which adds the complexity of multi-phase behavior. Prediction of salt behavior for multi-phase conditions requires solubility data in both aqueous and vapor phases. *Pressure* determines the density of the hydrothermal medium which in turn greatly influences salt solubilities; increasing the pressure increases the density, which in general increases salt solubility. Finally, salt solubility is determined by the solution *composition*. Base hydrolyzed propellants are complex, multicomponent solutions containing a wide variety of ionic species. A reasonable approach to handling this complexity, however, is to focus on the solubility behavior of those components which are highest in concentration in the hydrolyzed propellant and/or are expected to be least soluble, based on knowledge of solubility at lower temperatures. Data for selected two- and three-component systems should prove valuable for predicting the behavior of a multicomponent system. We have therefore chosen to study the phase and solubility behavior of the two major components expected to be the least soluble of the products of base hydrolysis of aluminum-bearing propellants. These are 1) aluminates from the reaction of aluminum with strong base, and 2) carbonates from the base hydrolysis and subsequent hydrothermal oxidation of the organic components of the propellant.

B. PRODUCTS OF BASE HYDROLYSIS OF ALUMINUM-BEARING PROPELLANTS

1. Composition of Aluminum-Bearing Propellants

CYH is a typical aluminum-bearing propellant. The composition on a weight basis is approximately as follows:

ammonium perchlorate (NH ₄ ClO ₄)	- 11%
aluminum	- 21%
energetic materials	- 68%

The energetic materials are HMX, nitrocellulose, and nitroglycerine. We have hydrolyzed a small amount of solid CYH in concentrated sodium hydroxide solution at room temperature, followed by heating to the boiling point for thirty minutes, after which no further reaction was evident (Reference 41). No attempt was made to analyze the gases evolved during the reaction, but the remaining solution was analyzed by ion chromatography. The products relevant to the solubility studies are discussed below. Our studies of the solubilities of these products under hydrothermal conditions assumed that the solution produced in the base hydrolysis step is hydrothermally processed without further treatment, for example to alter the pH or remove the aluminum.

2. Products of Ammonium Perchlorate Hydrolysis

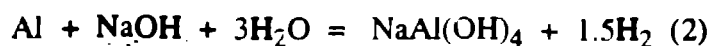
Ammonium ions react with strong base to produce ammonia and water:



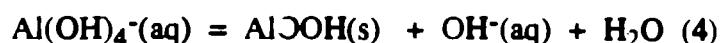
Since the solution is boiled in the last phase of base hydrolysis, most of the ammonia produced leaves the solution as a gas. The perchlorate ion does not react with base under hydrolysis conditions, so the net effect is to convert ammonium perchlorate to sodium perchlorate, which is a highly soluble salt.

3. Products of Aluminum Hydrolysis

Base hydrolysis oxidizes aluminum metal to the 3⁺ oxidation state. The presence of excess hydroxide causes the subsequent formation of "aluminate" ions, sometimes written as AlO₂⁻, but more properly written as Al(OH)₄(H₂O)₂⁻. We will abbreviate aluminate ions as Al(OH)₄⁻.



Sodium aluminate is highly soluble in water at room temperature, particularly in solutions of high pH, since high pH suppresses the formation of the insoluble compounds gibbsite, Al(OH)_3 , and boehmite, AlOOH .



It is important to maintain high pH since Tikhonov (Reference 42) reports that, at low pH, the aluminum hydroxide gradually converts to boehmite at room temperature, and boehmite converts to alumina (Al_2O_3) above 600 °C. [The above discussion is somewhat oversimplified since Al(OH)_3 and AlOOH each have two isomers]. The reaction sequence



would cause severe plugging problems in a flow reactor since the last three species are highly insoluble at low pH. A much more favorable situation exists at high pH. Apps and Neil (Reference 43) measured the equilibrium constants for reactions (3) and (4) between 0 and 350 °C. They found gibbsite and boehmite to be highly soluble in basic solutions, with solubility increasing with temperature along the vapor saturation curve. Extension to temperatures above the critical temperature of water is not straightforward, however. The presence of dissolved salts raises the liquid-vapor critical temperature of the solution, so that multi-phase behavior is possible at temperatures well in excess of 374 °C. Also, the dielectric strength of water decreases dramatically with increasing temperature and decreasing density above T_c . Therefore, salt solubilities are expected to decrease with increasing temperature, regardless of whether the system is a liquid, vapor, or supercritical fluid. Data in the literature are nonexistent for the system of interest above 350 °C. New experimental data are required to ascertain whether aluminum salts will stay in solution during hydrothermal processing.

4. Products of Energetic Materials Hydrolysis

The carbon products of hydrolysis of CYH are mostly acetate and formate ions, with a small amount of carbonate and several less abundant unidentified species. Most of the nitrogen is evolved as gas (NH_3 , N_2O and N_2); the remaining nitrogen is in the form of nitrite and nitrate anions. Slightly less than half of the carbon and nitrogen were accounted for in the solution, the rest presumably having left as gaseous species.

The carbon- and nitrogen-containing species resulting from base hydrolysis are not the most stable products possible; they reflect the fact that base hydrolysis was carried out at relatively low temperature, and equilibrium was not reached due to kinetic considerations. In studies of hydrothermal oxidation of organics at LANL (Reference 44), incomplete oxidation to form species such as acetate, oxalate, and formate ions is often observed at temperatures below 400 °C. At temperatures above 400 °C, however, conversion of these anions to carbonate is virtually complete in a few seconds or less. Under these conditions, nitrite ions are effective oxidizing agents, the nitrogen ending up as either N₂ or N₂O. At slightly higher temperatures, nitrate ions are similarly good oxidizing agents. The conclusion is that base hydrolysis of CYH propellant, followed by hydrothermal oxidation, will convert all of the organic carbon into either neutral species (gases) or carbonate anions, while all of the organic nitrogen will end up as neutral species or possibly as unreacted nitrite and nitrate anions. Nitrites and nitrates are in general highly soluble and are not expected to precipitate under hydrothermal conditions.

C. PHASE BEHAVIOR UNDER HYDROTHERMAL PROCESSING CONDITIONS

1. Basic Aluminate and Carbonate Solutions

Having determined that aluminate and carbonate are the species most likely to produce precipitates in the hydrothermal processing of base-hydrolyzed CYH propellant, we now turn our attention to the phase behavior of basic sodium aluminate and sodium carbonate solutions. It is well known that the liquid-vapor critical temperature of a solution of a nonvolatile salt in water is higher than that of pure water (374 °C). For example, Urusova (Reference 45) found that a 2.9 molar solution of NaOH had a critical temperature of 450 °C. A study by Marshall and Jones (Reference 46) showed that the elevation of the critical temperature for solutions of many common salts is in the range of 25-65 °C for 1.0 molar solutions. Because a base-hydrolyzed propellant solution is expected to have a large excess concentration of sodium hydroxide, together with a large amount of aluminate and other dissolved salts, it is likely that the liquid-vapor critical temperatures will exceed 450 or even 500 °C. Hydrothermal processing will probably take place at a temperature in the 400-500 °C range; that is, processing may take place at subcritical temperatures, unless the feed solution is diluted to avoid this possibility. The number of phases that the system can partition into will be determined by whether the system is above or below its critical temperature.

2. Solutions Below the Liquid-Vapor Critical Temperature

In a hydrothermal process, a solution initially at room temperature would be pumped at high pressure into a heated reactor. As temperature increases at constant pressure, density (hence dielectric constant) decreases and salts may become less soluble. [Some salts exhibit retrograde solubility behavior; that is, their solubility decreases with temperature even at constant density.] If solubility limits are exceeded, solids or molten salts will separate from the aqueous phase. As temperature continues to increase, the vapor pressure of the solution may exceed the applied pressure, and a vapor phase will appear. Since the solubility of the salt in the (less dense) vapor phase will be less than that in the aqueous phase, the aqueous phase will become more and more concentrated in salt (unless it was already saturated, in which case more solid or molten salt will separate out). If the vapor pressure of the remaining solution is higher than the applied pressure when the maximum temperature is reached, the aqueous phase will disappear entirely, leaving a solid or molten salt phase incorporating a small amount of water, and a vapor phase consisting mostly of water with some dissolved salt. The existence of solid or molten salt phases will degrade the performance of the reactor by causing plugging and excessive corrosion. The following conditions should be met in order to avoid these problems: 1) the solubility limits in the aqueous phase should not be exceeded; and 2) the applied pressure must be greater than the vapor pressure of the aqueous phase so that no vapor phase can form.

3. Solutions Above the Liquid-Vapor Critical Temperature

If the conditions outlined in the previous section have been met at the point in the reactor where the solution is just below the critical temperature, the system is a single homogeneous aqueous phase. As the temperature increases beyond T_c , the system changes smoothly and continuously to a supercritical fluid with all salts still in solution. As temperature continues to increase at constant pressure, however, density (hence salt solubility) decreases, and again solids or molten salts may separate out. Thus, even at supercritical temperatures, it is necessary to keep the pressure (density) high enough to keep the salts in solution.

It is clear that several kinds of experimental data are required in order to design a hydrothermal reactor for aqueous salt solutions:

- 1) vapor pressure vs. temperature
- 2) critical temperature
- 3) salt solubility in liquid, vapor, and supercritical fluid as a function of temperature and pressure.

In the following sections we discuss experimental results pertaining to each of the above categories for basic carbonate and aluminate solutions.

D. SOLUBILITY AND PHASE EQUILIBRIA MEASUREMENTS

1. Experimental Techniques for the Study of Solubility and Phase Behavior

Two experimental approaches have been employed to study phase behavior and solubility in hydrothermal systems. One approach uses an optical cell to observe the behavior of static solutions as they are heated under high pressure. By decreasing the applied pressure at constant temperature, phase changes (crystallization of solids, appearance of molten salts, vapor-liquid equilibria) can be observed visually or by their effect on the optical transmission of the cell. The other approach uses a packed-bed flow tube to measure salt solubilities. Solutions initially at room temperature are pumped at high pressure into a heated packed bed, after which they are cooled and passed through a pressure letdown valve. If the salt concentration entering the packed bed exceeds the solubility at the final temperature and pressure, salt will precipitate in the bed and the solution exiting the cell will be saturated with salt. Inductively coupled plasma spectroscopy and acidimetric titration analysis of the effluent stream gives a direct measurement of salt concentration and hence solubility. This method probably works best for salts that separate out as solids rather than molten salts, since molten salts may partially or completely flow out of the packed bed and be redissolved in the cooldown section. Since both sodium aluminate and sodium carbonate have very high melting points, they will separate out as solids. Sodium hydroxide, on the other hand, is molten at the temperatures used in this study. In principle, the packed-bed method works for sub- or supercritical temperatures, and for any pressure, with one possible exception. If the temperature is subcritical and the pressure is in the two-phase liquid-vapor (or liquid-liquid) region, there is no direct method for distinguishing what fraction of the fluid is in each phase, and so the solubility cannot be found unambiguously in either phase.

The optical cell was fabricated from a commercial 4-way cross (Hi-P) made for 1/4 in. high pressure tubing, measuring 1 in. x 2 in. x 2 in., made of Inconel 625 alloy. The optical axis is in the orthogonal direction to both pairs of tube fittings on the cross. Diamond windows are pressed into cone-shaped depressions in the bottom of wells that are machined into the faces of the

cross. Thin (0.003 in.) gold washers between the diamonds and the cell walls allow the faceted diamonds to make a pressure-tight seal. The diamonds are squeezed into place with pusher blocks made from Inconel 718. Spring washers, also made of Inconel 718, are used to compensate for the difference in thermal expansion between diamond and Inconel, keeping nearly constant pressure on the pusher blocks as the cell is heated up. Fluid is conveyed into and out of the cell by Inconel 625 tubing connected to two of the ports of the cross. A third port houses a type K thermocouple, used for temperature control, which is inserted in close proximity to the region of the cell near the windows. The fourth port on the cross is plugged. The cell can operate at temperatures up to 600 °C and pressures up to 1200 atm.

Phase changes in the cell are monitored by two coaxial optical systems. A white-light source enters the cell from the left. On the right, a lens forms a magnified image of one of the diamond windows on a color CCD camera. By means of a beamsplitter, a helium-neon (HeNe) laser is passed through the cell from right-to-left, and another beamsplitter is used to deflect the transmitted HeNe beam to a photodiode. The CCD camera is equipped with a blue filter to block scattered laser light, and the photodiode is equipped with a bandpass filter to discriminate against white light. The CCD camera output allows visual observation of phase changes, which can be seen in several ways. When solid precipitates from solution, crystals may be seen growing on the window or dropping out of the bulk of the solution. A salt which is at a temperature above its melting point will sometimes be observed to separate out as a molten liquid blob. When a vapor-liquid equilibrium is established, density gradients will be seen propagating across the liquid phase, and sometimes bubbles are seen. The laser diagnostic is particularly sensitive to the appearance of a vapor phase. When the pressure above an aqueous phase is lowered until a vapor phase appears, the laser transmission through the cell drops abruptly, allowing the vapor pressure to be determined accurately and reproducibly.

Sodium aluminate and sodium carbonate solubility studies were also performed in a packed-bed flow apparatus shown schematically in Figure 74. Primary features of the apparatus include a preheat section followed by a packed bed, in which salt precipitation occurred, and then a 100 micron high temperature filter to capture precipitates. The packed bed consisted of a microreactor constructed from 6 in. of 1 in. od (0.5 in. id) Inconel 625 tubing with cone closures at each end. The internal volume of the microreactor is 19 mL and was packed with 0.25 in. to 0.5 in. pieces of 0.3125 in. od Inconel 625 high pressure tubing. Similarly, the high temperature filter was constructed of Inconel 625 and housed four 0.75 in. diameter 316 stainless steel sintered filter discs. All tubing in the hot sections of the apparatus was constructed from 0.25 in. od C276 high pressure tubing.

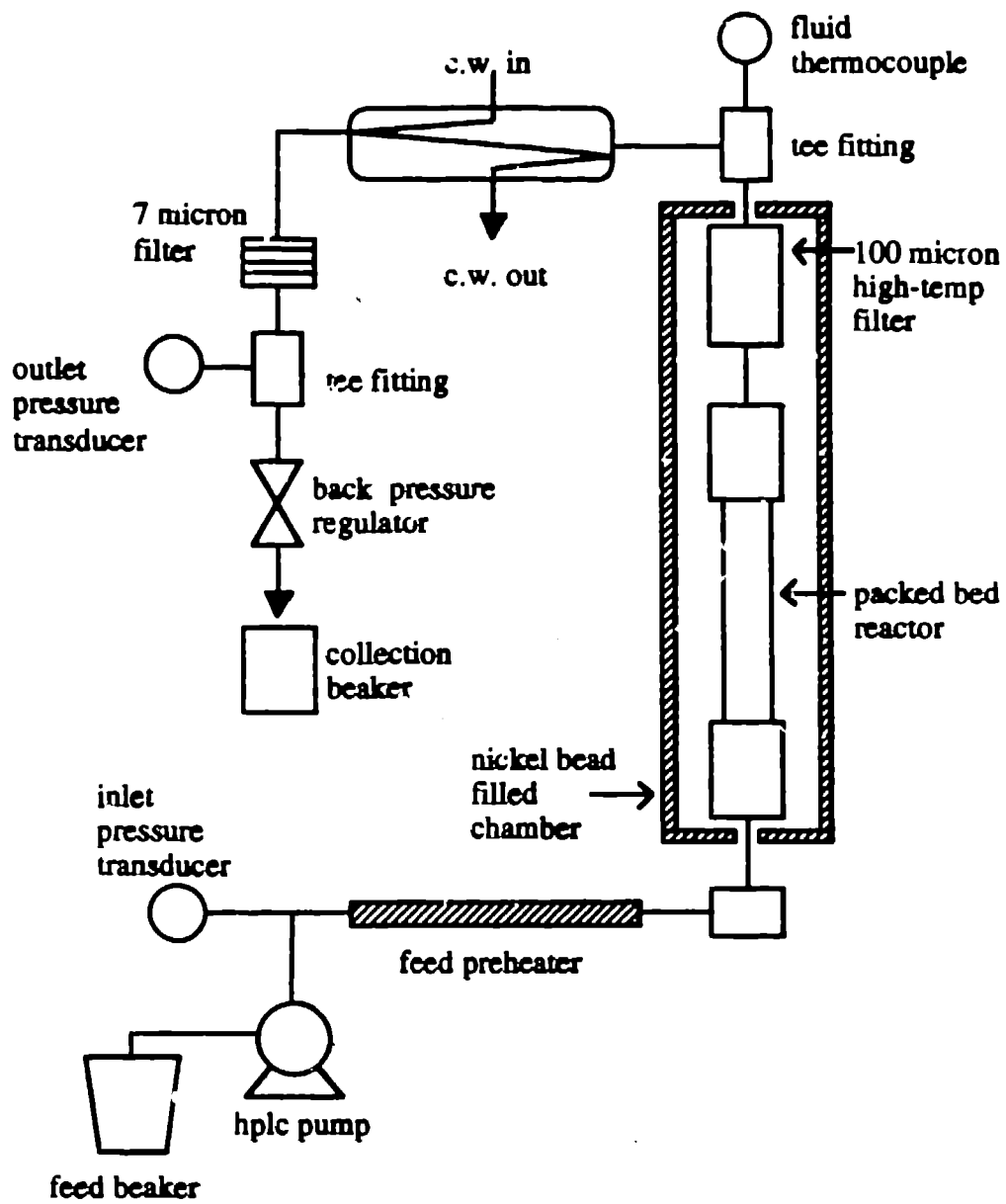


Figure 74. Packed-bed flow apparatus for salt solubility studies.

The preheat section consisted of 0.6 m of C276 high pressure tubing, surrounded by cylindrical brass clamshell heaters. Heating wire was wound on the brass, and current was supplied to the heating wire with variable transformers. Heat was generated by resistive heating of the wire, which was conducted through the brass to the preheater tubing. The packed bed and the high temperature filter were heated to the desired temperature by heating wire wound inside an 18 in. section of 3 in. od stainless steel tubing. The packed bed and filter were positioned inside the 3 in. od stainless tube and the void spaces were filled with 0.1 in. diameter nickel beads. The heat generated in the heating wire was conducted through the nickel beads to the packed bed and filter and the desired temperature was maintained by regulating the current through the heating wire with microprocessor temperature controllers. A chilled water countercurrent heat exchanger following the high temperature filter reduced the temperature of the effluent stream to near ambient. Pressure reduction was accomplished with a spring loaded, backpressure regulating valve.

Nine type K thermocouples monitored the temperature at various positions on the apparatus. A thermocouple in contact with the fluid stream at the exit of the high temperature filter provided the temperature at which solubility measurements were made. This represented the highest temperature achieved by the fluid in the apparatus. Transducers measured pressures immediately following the feed pump and just prior to pressure letdown. Salt solutions were fed to the system using a high performance, liquid chromatography pump.

Solubility experiments were conducted by heating the apparatus with pressurized deionized water. When the fluid temperature at the exit of the filter reached the desired experimental value, the influent was switched to the feed salt solution. After allowing the system to flush with the feed salt solution for 15-20 minutes, the effluent was collected in vials with zero head space for 2 to 3 hours. Generally, 5 to 7 samples were collected during each experiment and temperature and pressure data were recorded every 5 minutes. After the last sample vial was filled, all heaters were turned off and a recirculating water rinse was initiated. This water rinse served to collect electrolytes and corrosion products which precipitated at high temperature, but which again became soluble as the reactor cooled to ambient conditions.

2. Optical Cell Studies of Basic Aluminate and Carbonate Solution Solubilities

A series of solutions with varying aluminate or carbonate concentrations were made in 1.0 molar sodium hydroxide solutions. The choice of unit molarity for sodium hydroxide was somewhat arbitrary but reflects the fact that hydroxide is present in excess in the products of base hydrolysis of propellants, and the fact that hydroxide ion has a large effect on aluminate and carbonate solubility. The solutions that were tested are listed in Table 49.

TABLE 49. SOLUTION COMPOSITION (MOLAR CONCENTRATIONS OF SUBSTITUENTS) FOR SOLUBILITY STUDIES

sodium aluminate	sodium carbonate	sodium hydroxide
0.5		1.0
2.0		1.0
	0.1	1.0
	0.2	1.0
	0.3	1.0
	0.5	1.0
	1.0	1.0

The aluminate solutions were studied at temperatures of 375, 400, 425, 450, and 475 °C. The experiments consisted of heating the solutions up to the desired temperature at high initial pressure, followed by lowering the pressure until a phase change was observed. In all cases except for the most dilute aluminate solution at the highest temperature, the solutions displayed normal vapor-liquid equilibria. No precipitates were observed as long as the systems were in the liquid phase. For the 0.5 molar aluminate solution at 475 °C, no vapor-liquid phase transition was observed; instead, a solid phase was seen to separate out when the pressure dropped to about 7700 psia. The vapor pressure data are summarized in Table 50.

TABLE 50. VAPOR PRESSURES FOR SODIUM ALUMINATE SOLUTIONS IN 1.0 MOLAR SODIUM HYDROXIDE

T (°C)	Pv (psia)	
	0.5 molar aluminate	2.0 molar aluminate
375	2930	2844
400	4011	3826
425	5203	5254
450	6597	7018
475	supercritical	8751

It is concluded that sodium aluminate is highly soluble in basic solutions at sufficiently high pressures, whether or not the solutions are above their critical temperatures. Aluminate is

therefore not expected to contribute to reactor plugging in hydrothermal treatment of base-hydrolyzed aluminium bearing propellants.

Carbonate solutions in 1.0 molar sodium hydroxide behaved differently from aluminate solutions when heated up under high pressure (typically 10,000 psia in these experiments). For the more concentrated solutions, crystals started to grow before the final temperature was reached, making the cell partially opaque. For the more dilute solutions, the experiments could be done in the normal way, but the normal vapor-liquid phase transition was not observed as the pressure was lowered. Instead, a molten salt phase (and sometimes a solid phase) appeared to separate out. The pressure at which this phase change occurred could not be reproducibly observed with our optical diagnostics. In most cases it was not even clear whether the system was above or below the liquid-vapor critical temperature. Therefore, the experiment was done in a different manner. Starting with a dilute (0.1 molar) carbonate solution, the cell was heated up to 475 °C at a pressure of 10,000 psia. Very little precipitate was seen during heatup and no crystals grew on the window under these conditions. Carbonate concentration was then increased in steps and the experiment repeated, until crystal growth was observed during heatup. In this way it was estimated that sodium carbonate solubility in 1.0 molar NaOH at 475 °C and 10,000 psia is between 0.3 and 0.5 molar. Solubility increases with increasing pressure and/or decreasing temperature (retrograde temperature behavior).

Since it is likely that the sodium hydroxide concentration influences sodium carbonate solubility, we next ran a series of tests in which carbonate concentration was kept fixed at 0.7 molar, and sodium hydroxide concentration was increased in steps, starting at 0.7 molar. As in the previous tests, the solutions were heated to 475 °C while held at 10,000 psia pressure. The results were dramatic, and showed that hydroxide has a large positive influence on carbonate solubility. At hydroxide concentrations of 0.7, 1.4, and 2.8 molar, solid sodium carbonate was seen to crystallize out of solution during the heatup phase, much as in the previous tests. At higher hydroxide concentrations, however, the behavior was qualitatively different. The solution remained as a single phase liquid throughout the heatup period, with no precipitation of sodium carbonate evident. When the pressure was lowered, the liquid appeared to boil at a pressure of approximately 7500 psia, but no sodium carbonate precipitate was observed. At the intermediate hydroxide concentration of 4.2 molar, the most interesting behavior occurred. Again, a single phase solution resulted at 475 °C and 10,000 psia. When the pressure was dropped to about 9040 psia, however, the system segregated into two liquid phases with a clear horizontal line separating them. Again, no solid carbonate precipitate was observed. It appeared that the upper of the two liquid phases was mostly aqueous, while the lower behaved as a sodium hydroxide "melt", albeit with a large amount of water in it, since it occupied a significant fraction of the cell volume. A

high solubility of sodium carbonate in the melt phase would account for the observation that sodium carbonate precipitated from the solutions low in hydroxide, but not from those high in hydroxide. [The use of the word "melt" is descriptive only: for example, in a 5.6 molar sodium hydroxide solution, there are still almost ten molecules of water for each molecule of NaOH.]

3. Summary of Solubility and Phase Behavior Studies at High Density

The solubility of sodium carbonate in dense, high pH, subcritical liquids has been shown to vary strongly with temperature, pressure, and composition. Thus, precipitation and reactor plugging due to carbonate may be of concern in a system treating base-hydrolyzed propellant. The addition of excess hydroxide creates a "melt" phase in which carbonate solubility is dramatically enhanced. However, there is a range of pressures over which the melt phase can coexist with an aqueous phase. It would appear to be prudent to operate a reactor at high enough pressure to avoid the coexistence of two liquid phases. At a temperature of 475 °C, a pressure on the order of 10,000 psia would be required.

Sodium aluminate solubility was found to be high in basic solutions at hydrothermal temperatures and pressures; there is no concern that aluminates from base-hydrolyzed propellants will precipitate as long as the pressure of the system exceeds the saturation vapor pressure of the solution.

Hydrothermal processing of concentrated electrolytes has been shown to require that reactors operate at very high pressure to ensure solubility and single phase behavior. High pressure equipment is more costly and more subject to corrosion than equipment operating at moderate pressures. An alternative is to dilute the solutions to be processed, which will allow the salts to remain soluble at lower pressures during hydrothermal processing. To evaluate the tradeoffs between high- and moderate-pressure processing, we have undertaken a study of salt solubilities at hydrothermal temperatures and pressures in the range of 4000-8000 psia. We now turn our attention to solubilities measured in these low density, supercritical fluids.

4. High Temperature, Low Density Salt Solubility Studies in the Packed-Bed Flow Apparatus

Several measurements were made to determine sodium aluminate and sodium carbonate solubility in supercritical sodium hydroxide solutions as a function of temperature and pressure. The feed salt solutions for these experiments were made in 0.1 molar sodium hydroxide with lesser quantities of either sodium aluminate or sodium hydroxide. Once again the choice of 0.1 molar sodium hydroxide was arbitrary but in this case was selected so that supercritical behavior could

be achieved at the temperatures studied (400 - 475 °C). [Recall that as discussed previously, the critical temperature of a 2.9 molar solution of NaOH is elevated to 450 °C. However, based on experimental observation, the critical temperature of a 0.1 molar NaOH solution is less than 400 °C.]

Carbonate and hydroxide concentrations were determined by acidimetric titration and aluminum and sodium concentrations were determined by inductively coupled plasma spectroscopy. With the determined concentrations of all species in effluent samples the solubility of sodium aluminate and sodium carbonate were calculated. Solubility values were derived from effluent concentrations of aluminate and carbonate, rather than sodium, because additional sodium was added (NaOH) to the feed solutions. The calculated solubility values represent the quantity of sodium aluminate or sodium carbonate that was soluble in the supercritical fluid phase after exiting the high temperature filter.

Table 51 shows the results of the packed-bed flow apparatus solubility studies and confirms that, as anticipated, the supercritical phase solubility of these electrolytes is very low (< 3 g/kg) at these relatively moderate pressures. Temperatures and pressures were determined from the averages of 6-30 readings during the course of the experiment. Reported solubilities are the averages from analysis of 5-7 samples collected during each run. The reported uncertainties are given as two times the estimated standard deviations.

TABLE 51. SUPERCRITICAL PHASE SOLUBILITY OF SODIUM ALUMINATE AND SODIUM CARBONATE IN 0.1 MOLAR SODIUM HYDROXIDE

electrolyte	temperature (°C)	pressure (psia)	solubility (mg/kg)
sodium aluminate	399.7 ± 2.6	5045 ± 34	201 ± 34
	424.9 ± 2.6	5112 ± 123	182 ± 38
	450.1 ± 1.8	5025 ± 48	75 ± 12
	475.5 ± 1.8	5026 ± 57	59 ± 6
	450.2 ± 0.5	6800 ± 158	1530 ± 82
	450.3 ± 0.2	7926 ± 312	2284 ± 68

E. CONCLUSIONS AND RECOMMENDATIONS

Presently, the available solubility data for sodium aluminate and sodium carbonate cover a very small part of the range of temperature, pressure and overall composition that are possible. At the highest pressures, the data are semiquantitative; only lower bounds on solubility may be

established. A few general conclusions are obvious, however. First, the pressure (and its effect on the density and phase) has an enormous effect on salt solubility. Typical solubilities at 450 °C and 5000 psia are on the order of grams/kgH₂O or less, while at 450 °C and 10,000 psia, solubilities are on the order of 100 grams/kg H₂O or more. Second, excess sodium hydroxide can have an enormous effect on solubility, presumably by the creation of a "melt" phase. This effect was particularly pronounced for sodium carbonate solubility. The data strongly suggest that hydrothermal processing of base-hydrolyzed propellants should be carried out in concentrated solutions at high pressure, despite the increased cost and increased corrosion rates that might be encountered.

The packed-bed apparatus has been upgraded and is capable of bridging the gap between the low- and high-pressure data now available. It is recommended that quantitative solubility measurements for the various components of base-hydrolyzed propellants be extended into the high-pressure regime. The effect of excess hydroxide on the solubilities should be carefully examined. These studies would provide data for the design of a demonstration unit for the hydrothermal processing of actual base-hydrolyzed propellant solutions.

SECTION IX

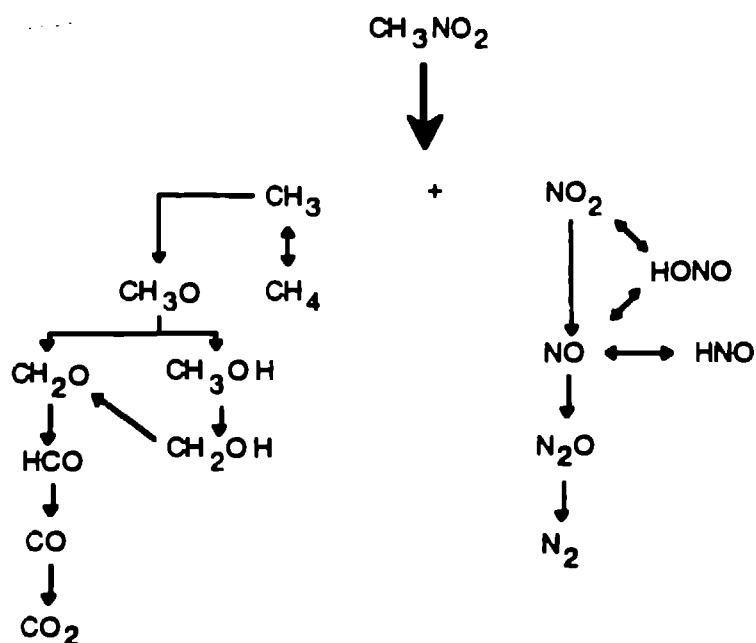
THEORY AND MODELING

A. INTRODUCTION

Design of an actual hydrothermal processing reactor system requires knowledge that includes rates of the pertinent chemical reactions, thermodynamics of the reactant-product-solvent system, and dynamics of fluid flow in the system. Such knowledge provides input to a process model used to optimize design with respect to performance and/or cost, depending on the desired objectives. In this section we report significant progress in the areas of required knowledge, and in preliminary process modeling for optimization of performance/cost.

B. MODELING OF NITROMETHANE REACTION KINETICS

We have had an ongoing interest in kinetic modeling of reactions in supercritical water, as this should provide insight into the chemical mechanisms and how they compare with those of the gas and liquid phases. Constructing a detailed elementary reaction network for nitromethane, however, is not a simple task, due to the size of the molecule and the many possible chemical intermediates formed by the four atoms C, H, N, and O. An attempt to develop such a mechanism has been made by Dr. Carl Melius of Sandia National Laboratories (Livermore, California), who was motivated by a desire to model the detonation of pure nitromethane at ambient conditions (Reference 47). We have adapted this reaction mechanism for use in high-pressure water to simulate the decomposition that occurs under the conditions used in our experiments (550 °C, 330 atm, 0.4 percent nitromethane in water, ~2-s reaction time). Many of the reaction rate values were taken from the combustion literature. Where appropriate, reaction rate constants were set to their high-pressure limits; in some cases, fall-off estimates were used (Reference 48). In a few cases, reactions with water were added because of their importance at high water densities. Apart from these modifications, however, the reaction mechanism is essentially a gas-phase mechanism, with no attempt to account for molecular clustering or other possible "nonideal" effects that may be important in supercritical water. The resulting mechanism includes 44 chemical species and 214 reversible chemical reactions. The overall reaction scheme is depicted below. For several of the chemical species, properties and reactivity are not known, and were estimated by Melius using his quantum chemistry techniques.



Reaction scheme for nitromethane (after Melius)

The results of the model calculations, both with and without additional oxidizer, are shown in Figure 75. At 550 °C in supercritical water without oxidizer, destruction of the nitromethane occurs in about one second, in excellent agreement with the experimental results described in Section III.E of this report. The model predicts that major products will be NO and CO, with smaller amounts of CH_4 , CH_3OH , N_2O , CH_2O , and H_2 . The products N_2 and CO_2 are predicted to form on a longer time scale (seconds to minutes) by further reduction of NO and oxidation of CO. When an excess of hydrogen peroxide is added to the reaction mixture (10 moles of H_2O_2 to 1 mole of nitromethane), the reaction is predicted to proceed about 10 times faster. The carbon is oxidized completely to CO_2 . Nitric oxide (NO) is still the principal nitrogen product, but NO_2 is formed as a secondary product, rather than N_2O . This occurs because the conversion of NO_2 to NO is slowed by the excess oxygen, and production of the intermediate species HONO from NO_2 becomes an important pathway (see the reaction scheme above).

Experimentally, when no oxidizer was added, N_2O was observed in higher amounts than NO, and no methanol or formaldehyde were observed. When oxidizer was added, carbon dioxide was the major carbon product. With some disagreements, then, model predictions and experimental data show qualitative parallels. This agreement is encouraging, considering the preliminary nature of the reaction mechanism used in the calculations. These results demonstrate the valuable predictive capability of this type of calculation, especially in understanding why

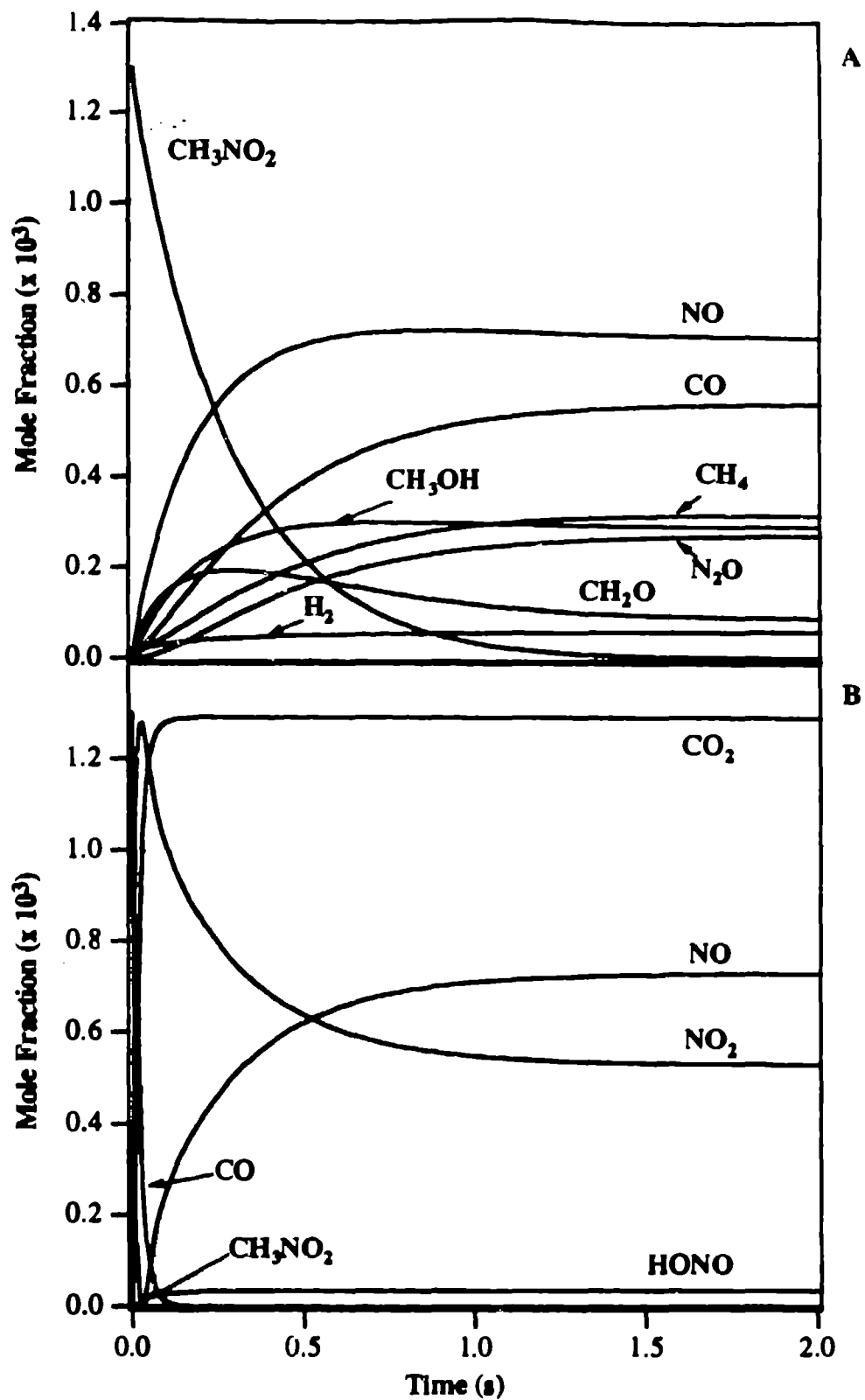


Figure 75. Calculated species profiles for the decomposition of nitromethane in supercritical water (A) at 550 °C, 330 atm and 0.4% v/v nitromethane in water. (B) Same calculation with the addition of H₂O₂ in a 10:1 molar ratio to nitromethane.

different products form under different conditions. Additional work on the reaction mechanism is needed and may produce closer agreement with the observations.

C. STEADY STATE OXIDATION OF H₂ IN SUPERCRITICAL WATER

The combustion of hydrocarbons in supercritical water produces the initial products H₂ and CO, which are further decomposed into H₂O and CO₂ in complete combustion. Since the oxidation of H₂ involves perhaps the simplest kinetics, it is very important to understand this reaction mechanism in supercritical water. Furthermore, there is much experimental data for H₂ oxidation (Reference 49) with which we can compare the steady state kinetic theory.

Oxidation of H₂ in supercritical water is different than normal oxidation at atmospheric pressure. Normal oxidation occurs at high temperature >1000°C where the chain branching reactions $H_2 + O' \rightarrow OH' + H'$ and $H' + O_2 \rightarrow OH' + O'$ dominate (Reference 50). However, in supercritical water the temperature is too low to activate this reaction and instead the three body reaction $H' + O_2 + H_2O \rightarrow HO_2' + H_2O$ occurs.

Experiments show (Reference 49) that the global reaction for oxidation of H₂ in supercritical water $2H_2 + O_2 \rightarrow 2H_2O$ does not depend on O₂ concentration as would normally be expected. This remarkable fact can be explained by a steady state analysis of the detailed reaction kinetics which is described herein.

In Table 52 we show the seven primary reactions for H₂ oxidation in supercritical water and their rates. The first four reactions are the fastest. In steady state (for times of several seconds or longer) the first two reactions occur at twice the rate of the next two reactions. This greatly simplifies the determination of the steady state concentrations because this equality of rates gives the following relations:

$$k_1[H_2][OH'] \sim k_2[H'] [O_2][H_2O] \quad (1)$$

$$k_2[H'] [O_2][H_2O] \sim 2k_3[HO_2']^2 \quad (2)$$

$$k_3[HO_2']^2 \sim k_4[H_2O_2] \quad (3)$$

$$k_1[H_2][OH'] \sim 2k_4[H_2O_2] \quad (4)$$

Because of these relations, the first four reactions in Table 52 produce as many intermediate species (H^{\cdot} , OH^{\cdot} , HO_2^{\cdot} , and H_2O_2) as are consumed, resulting in the net global reaction $2H_2 + O_2 \rightarrow 2H_2O$.

Equations (3) and (4) above give rate relations among the three species OH^{\cdot} , HO_2^{\cdot} , and H_2O_2 which do not depend on O_2 concentration. Also, in Table 52 the remaining three reactions (5-7) only involve these three radicals and do not depend on O_2 . Therefore, in steady state the three species OH^{\cdot} , HO_2^{\cdot} , and H_2O_2 cannot depend on O_2 concentration. This result has been demonstrated in experiments (Reference 49). Furthermore, the first relation above shows that the H^{\cdot} concentration is inversely proportional to O_2 concentration.

TABLE 52. PRIMARY REACTIONS FOR OXIDATION OF H_2 IN SUPERCRITICAL WATER

$$k_i = AT^b e^{-(E/RT)}$$

Reaction	Rate constant	log A	b	E(kJ/mole)
1. $2H_2 + 2OH \rightarrow 2H_2O + 2H$	k_1	8.33	1.51	14.35
2. $2H + 2O_2 + 2M \rightarrow 2HO_2 + 2M$	k_2	16.50	0.00	-4.18
3. $HO_2 + HO_2 \rightarrow H_2O_2 + O_2$	k_3	12.93	0.00	17.62
4. $H_2O_2 \rightarrow OH + OH$	k_4	14.47	0.00	202.55
5. $HO_2 + OH \rightarrow H_2O + O_2$	k_5	16.16	-1.00	0.00
6. $HO_2 + H_2O \rightarrow H_2O_2 + OH$	k_6	12.85	0.0	146.48
7. $H_2O_2 + H_2O \rightarrow HO_2 + H_2O$	k_7	12.85	0.0	5.98

Solving the steady state equations for zero time derivatives of the four intermediate radicals, one derives the global steady state rate for H_2 oxidation

$$d[H_2]/dt = - 9.77 \times 10^{10} [H_2O]^{2/3} [H_2]^{2/3} T \exp(-232,390/RT), \quad (5)$$

where $R=8.31$ J/mole-K, T is the temperature in Kelvin, and the concentrations are in moles/cc. In Figure 76 we compare the steady state rate calculated from Eq. (5) with the experimental data in

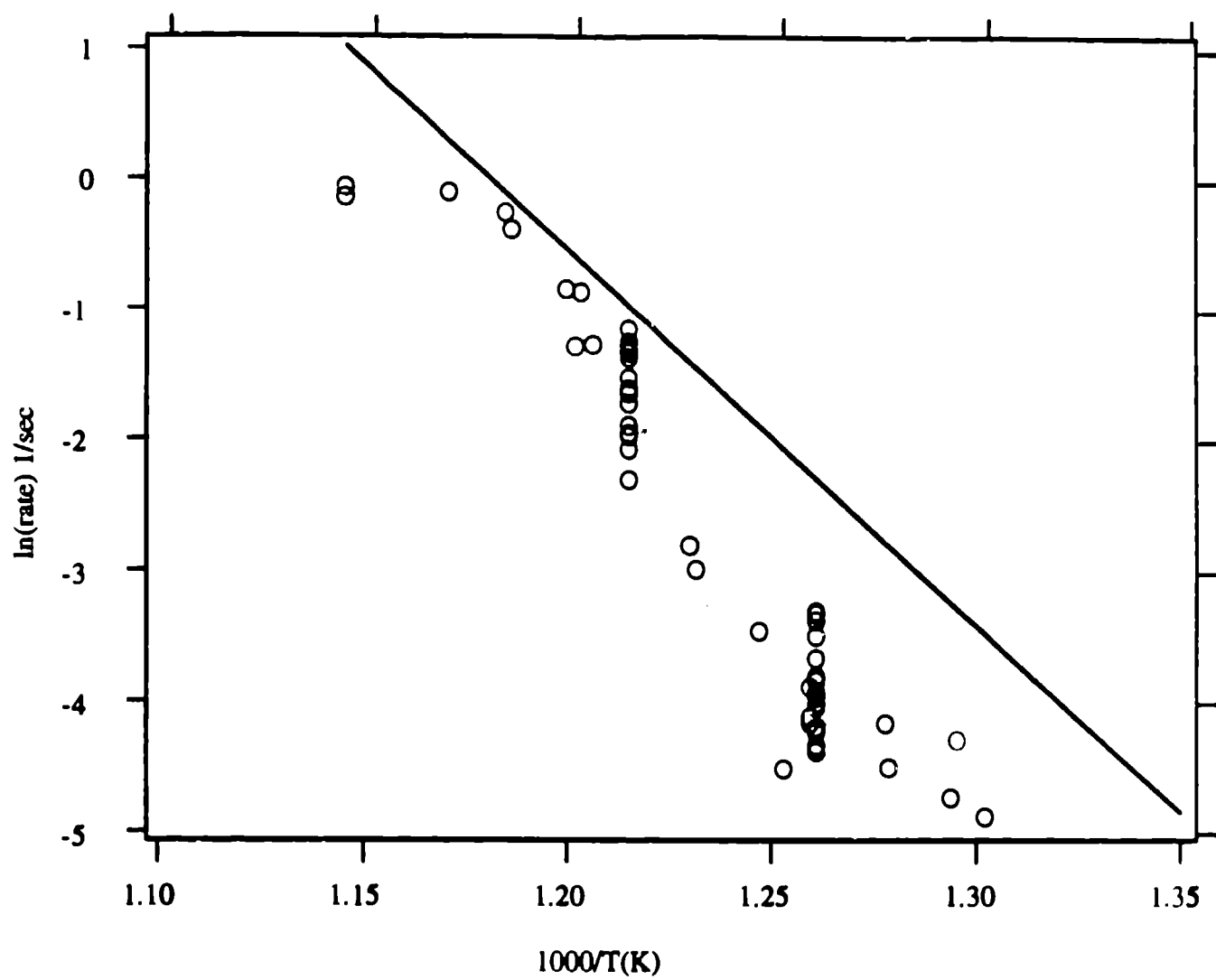


Figure 76. Comparison of theoretical steady state oxidation rate of hydrogen with experiment.

Reference 49 using the values $[H_2] = 10^{-6}$ moles/cm³ and $[H_2O] = 4.25 \times 10^{-3}$ moles/cm³. Note that the steady state analysis gives an upper limit to the oxidation rate. This is because there is an induction time for the reaction to reach steady state which decreases with increasing temperature. At 500 °C the induction time is about 50 seconds whereas at 600 °C it is less than 1 second. The data in Figure 76 were collected at times less than 15 s so the measured rate at 500 °C is well below the steady state value. The theoretical activation energy of 232 kJ is very close to the global steady state energy of 244 kJ found by Holgate (Reference 51). The theoretical value was derived directly from the individual rates given in Table 52.

The hydrogen oxidation rate above does not depend on O₂ concentration but it does depend on the 2/3 power of the H₂ concentration. This is also consistent with experiment. In Figure 77 we show the data from Figure 76 at 550 °C where we plot $[H_2]/[H_2]_0$ vs time where $[H_2]_0$ is the initial concentration of H₂. The data are shown for three different initial concentrations. The three curves shown for the three initial concentrations are found by solving equation (5) involving the 2/3 power law. Note that we can fit the data by assuming one induction time of two seconds for all the data.

In conclusion, we have explicitly derived the steady state activation energy for the oxidation of H₂ in supercritical water and have shown that the oxidation does not depend on the oxygen concentration but depends on the 2/3 power of the hydrogen concentration, in agreement with experimental results. The analysis given here illustrates the simplifications that result whenever steady state approximations are valid. Clearly, in future studies of more complex reaction systems, exploration of potential steady state regimes is highly desirable.

D. MODELING OF CLUSTER DISTRIBUTIONS IN SUPERCRITICAL WATER

The distributions of cluster sizes in water vapor at temperatures below the critical point and in the fluid above the critical point were calculated using equilibrium constants obtained from a thermodynamic model for water clusters. The model uses information such as the enthalpy of vaporization of water, the experimental bond strength of the dimer, a combination of Debye and Einstein temperatures that reproduces the heat capacity of ice, and the theoretical structures and energies of a few small clusters. The calculations were checked by comparing to measured water properties such as density and volume of the saturated steam and densities of the supercritical water. To make the comparisons, we developed an equation of state, a modification of the van der Waals equation of state, that relates pressure, temperature and density in terms of the cluster distribution. Cluster distributions for a variety of temperatures above and below the critical point

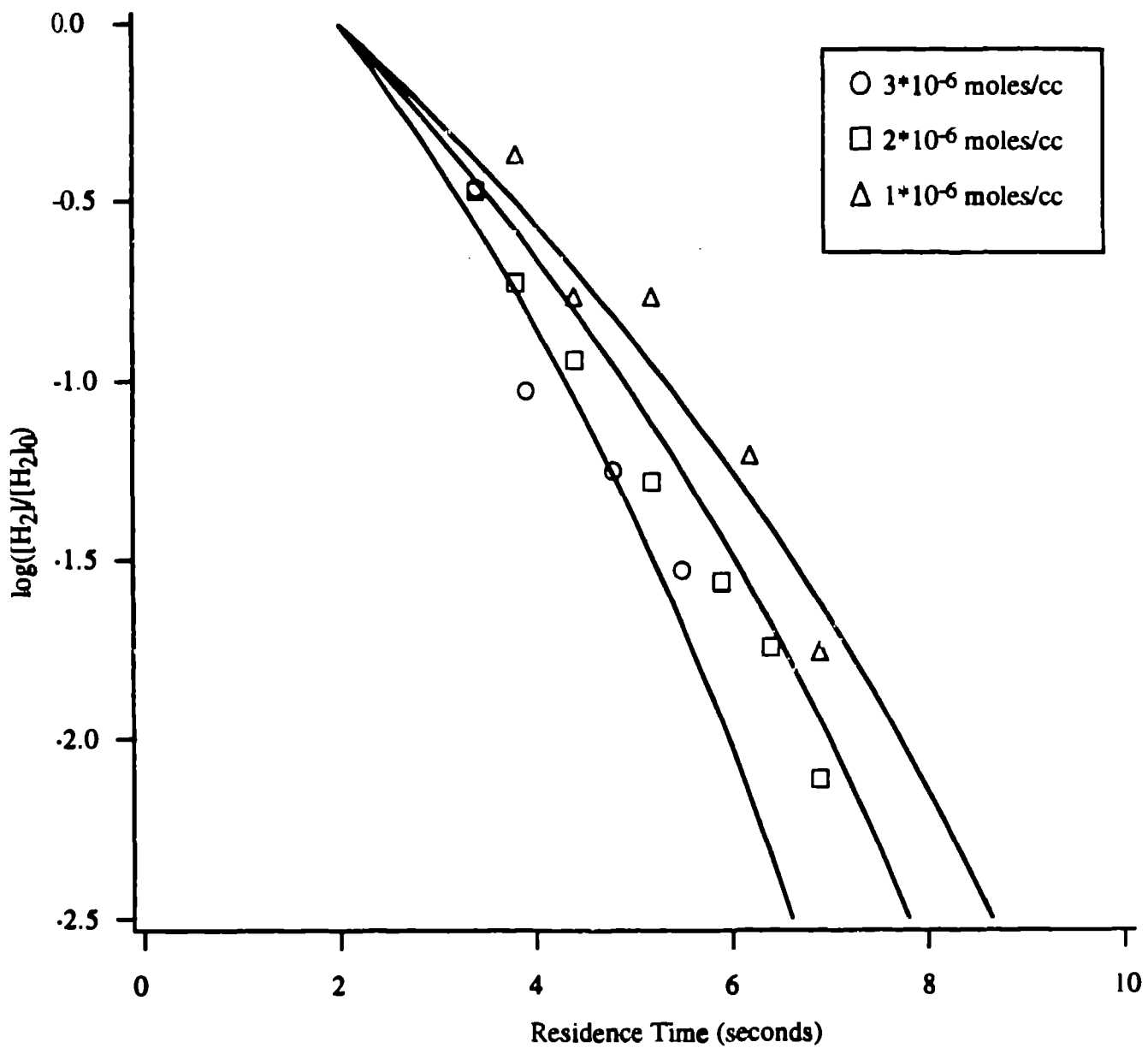


Figure 77. Comparison of theoretical steady state decay of hydrogen concentration $\log([H_2]/[H_2]_0)$ with experiment for three concentrations.

were calculated at a pressure of 246 bar. At low temperatures the calculations with a finite number of clusters (20) show an increased stability above a cluster size near four. If much larger clusters are included, most of the water molecules are found in the largest cluster, i.e., liquid water. Near the critical temperature (647.3 K) the number of molecules in each cluster size is roughly the same. Well above the critical temperature (900 K) the cluster size distribution is monotonically decreasing.

E. MODELING TOOLS FOR SOLVATION FREE ENERGIES IN HYDROTHERMAL SYSTEMS

It has been demonstrated that a dielectric continuum model provides a physically sound approximate description of solvation free energies of charged and polar solutes in complex solutions including aqueous solutions, (Reference 52). Adaptation of these models for application to supercritical aqueous solutions should assist in developing a predictive molecular description of ion-pairing phenomena, corrosion and scale formation, chemical reactivity in solution, and equation of state modeling. These tools should unify the elementary information required by the Advanced Process Simulator for Engineering (ASPEN) computer code, provide new information to fill the gaps within available experimental results, and produce physically sound extrapolations of experimental results into thermodynamic regimes not easily studied experimentally.

The physical idea of the dielectric continuum model is that the molecular medium external to a solute of interest is idealized as a dielectric continuum. The technical difficulty in applying the model is the solution of a known partial differential equation, the Poisson equation for continuous media. We have written and validated a boundary element computer code to solve this equation and thus evaluate solvation free energies, (Reference 53-56). The molecular information required for the solute molecule is (i) the dielectric response of the solvent; (ii) the molecular geometry of the solute; (iii) molecular charge distribution of the solute; and (iv) van der Waals radii used in defining the internal volume of the solute. The code which was written is applicable to arbitrary specification of these parameters and therefore applies to general complex solute molecules for which current alternative molecular theories can be applied.

As an initial validation of this approach, we studied the solvation free energy of the acetamide molecule (CH_3CONH_2) in aqueous solution near the triple point of the solvent. This example was chosen because experimental results and alternative molecular theoretical results were available for comparison, (Reference 57). The input information was taken from that previous theoretical study to provide the clearest comparison. The dielectric model predicted -0.47 eV for the solvation free

energy (the excess, or interaction part of, the chemical potential of the solute). The experimental result is -0.50 eV. The previous molecular theoretical calculation predicted -0.45 eV for the same quantity. Of that latter value, -0.39 eV was regarded as due to classical electrostatic forces. That distinction is not available for the experimental result or the model prediction. In this test, the model was clearly successful in predicting the solvation free energy of moderately complex solute in aqueous solution.

A second validation calculation studied the solvation free energies of alkali-chloride ion pairs in liquid water. Such information can teach us about the likelihood of encounter of charged groups in solution and thus about chemical reaction rates in solution. These particularly simple examples were, however, chosen because of the availability of molecular theoretical information with which to compare our model results. The results for calculated solvation free energies as a function of interionic distance (the so-called *potential of mean force*) are shown in Figure 78. These results depend crucially on our ability to achieve sufficient computational resolution to extract free energetic changes of a few 0.01 eV (1 eV = 23.06 kcal/mol). The results shown are in surprisingly good qualitative agreement with the results of reliable molecular theoretical calculations. For the case of Na⁺... Cl⁻ ion pair, the potential of mean force shows a free energetic barrier at approximately 3.2Å to ion contact at about 2.5Å. For conditions near the triple point of water, this contact ion pair is 'metastable' as is expected physically since close ion pairs are expected to be rare under such conditions. The model results are in remarkable qualitative agreement with available molecular information; the level of quantitative agreement, though quite reasonable, is currently being scrutinized with the objective of refining the parameterization of the model. In this way, we expect to be able to produce the most reliable predictions with this model approach.

With these validation efforts in view, our next application was to the solvation free energy of the carbonate anion (CO₃²⁻) in water as a function of temperature. Carbonate is a solute of interest in hydrothermal processing because it is the product of complete carbon oxidation. The molecular geometric parameters and partial charges necessary for the solvation free energy calculations were acquired from an electronic structure calculation by Joel Kress*. Figure 79 shows as the solid circles the results for that solvation free energy at thermodynamic states on the water *liquid-vapor* coexistence curve for temperatures between the triple temperature and the critical temperature of water. We expect these results, together with calculations in progress for complexes of the carbonate ion with the sodium ion, to be helpful in predicting the concentrations of the various possible complexes of this type.

*Personal communication with Joel Kress of the Theoretical Division at Los Alamos National Laboratory

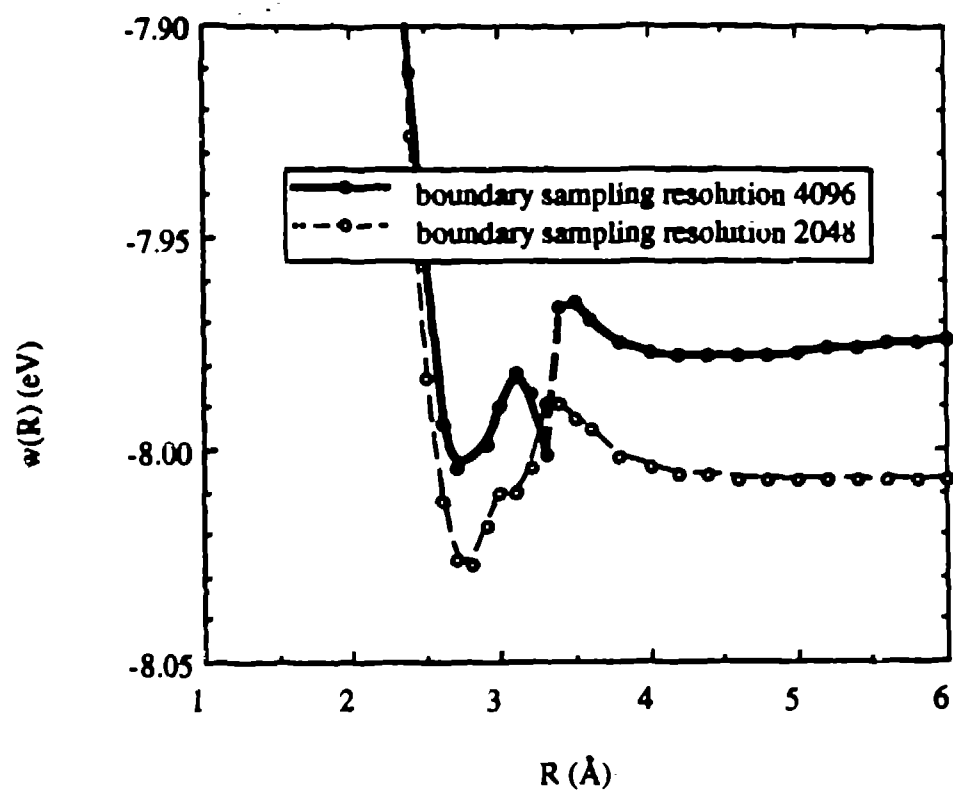


Figure 78. Potential of average force, $w(R)$, for $\text{Na}^+ \dots \text{Cl}^-$ ion pair in water at the water triple point according to the continuum dielectric model. The upper curve obtained with a much higher resolution calculation.

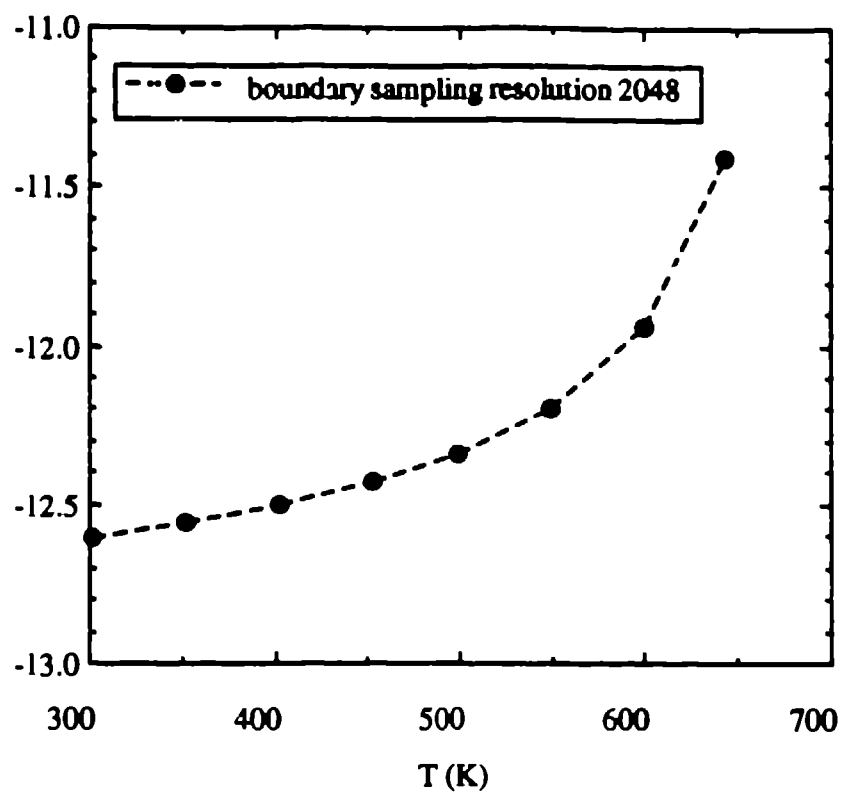


Figure 79. Solvation free energy of the carbonate anion, CO_3^{2-} in water along the coexistence curve as a function of temperature from the triple point to the critical point.

Finally, we have applied our code to the problem of encounter of a Cl^- ion in aqueous solution with a metal wall. In this case the wall effects are incorporated naturally into the dielectric continuum by assigning the static dielectric constant of the metal to be infinite, $\epsilon = \infty$. We expect that close contact would be required for efficient electron transfer and hence efficient corrosion. Subsequent study of how these barriers change with thermodynamic state progressing into supercritical regions should provide insight into the rates of corrosion of reactor walls.

F. REACTOR DESIGN TO MINIMIZE WALL CORROSION

1. Basic Concept

One of the major concerns in designing a reactor for the supercritical water oxidation of wastes is the corrosion that occurs on the reactor walls, seriously shortening the lifetime of the reactor. Given the wide array of wastes, ranging from organics to fuel propellants, that can be treated with this process, it is clearly desirable to lessen or eliminate the corrosion problem in order to enhance its utility.

Corrosion of reactor walls can be caused either by the waste stream, oxidizers, reaction products, or a combination of all three. In practice, it is found that having the oxygen-supercritical water mixture in contact with the walls is a less serious problem than having the waste stream and reaction products in contact with the walls. The reason for this is that the walls can be passivated by electrochemical means against corrosion from the oxidizing stream.

Clearly, the simplest way to deal with the problem is to prevent the waste stream and the reaction products from ever reaching the reactor walls. With this in mind, we can think of a tubular flow reactor. In this reactor, a mixture of supercritical water and oxygen is fed in and flows downstream continuously at a low velocity, e.g., 1 cm/s. The waste stream is then fed in along the axis of the tube in the form of a spray. In the case of a gaseous stream, which is the one we shall consider here, the "spray" will consist of vapor bubbles. These vapor bubbles are of course surrounded by the mixture of supercritical water and oxygen. Given the small dimensions of the bubble (the order of micrometers), it takes a miniscule amount of time (milliseconds) for the vapor to mix with the ambient stream. In this manner, the waste stream mixes well with the oxidizing stream. If the tube is long enough to allow the reaction to proceed to completion, and if the tube is sufficiently wide to prevent the mixed reacting stream from coming in contact with the walls before it leaves the tube, then we will have significantly reduced the corrosion problem.

2. Design Considerations

Typical flow speeds (u_f) are on the order of 1 cm/s. Residence times for the supercritical water oxidation of wastes are typically tens of seconds, $\tau_r \sim 60$ s. Thus the length L_t of the tube we shall need is of the order of $u_f/\tau_r \sim 60$ cm. In a time τ_r , the lateral diffusion (the diffusion constant being $\sim 10^{-3}$ cm² s⁻¹) will have an extent $R_t \sim (D \tau_r)^{1/2} \sim 0.3$ cm. On the other hand, the spray which is injected along the axis will have an angular extent ϕ . In a distance L_t , this translates to a radius of $\phi L_t \sim 3$ cm. This latter number defines the radius of the tube we shall need.

These considerations give us an idea of the dimensions of the tube reactor we need. Later, we shall show that detailed calculations change these numbers somewhat. The changes are primarily due to the fact that in our flow reactor, there are concentration gradients which cause the reaction to proceed at non-uniform rates within the reactor.

The physical picture we have from these considerations is a narrow jet issuing into the center of a cylindrical tube, mixing with the surrounding, flowing oxidizer/supercritical water mixture, and flowing downstream while spreading laterally in a plume as the oxidizing reaction proceeds. We have depicted this in Figure 80.

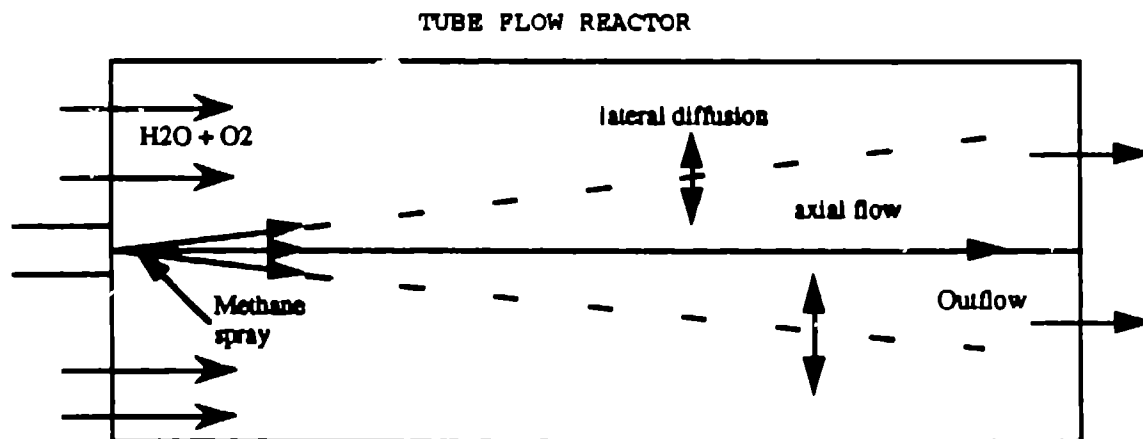


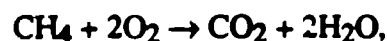
Figure 80. Conceptual set-up of the reactor geometry.

3. Numerical Calculations

As mentioned in the previous two sections, the idea is to shape the reacting flow in our reactor such that it does not touch the walls to avoid corrosion. We have performed numerical simulations of such flows using KIVA-II. This is a Fluid Dynamics code to simulate low speed reactive flows, using a semi-implicit method for advancing in time. While this code is a state-of-the-art tool designed to handle primarily internal combustion engines, it has options for inflow and outflow boundary conditions that allow it to be utilized for our purposes.

As an example of reactive flows confined to the neighborhood of the axis of the tube, we have used methane (CH₄) to simulate the waste stream. Methane is known to cause the carburization of refractory metals according to the reaction CH₄(gas) → C(diss) + 2H₂. As such, methane serves as an example of a stream that can have deleterious effects on the walls of a reactor. The oxidation of methane in our reactor serves to show that by having a confined reactive flow, the reactants as well as the products, along with the very high temperatures that are achieved during exothermic reactions, are not transported to the walls, thereby reducing the likelihood of corrosion.

The global reaction mechanism we used is



with the reaction rate given by Webley and Tester. (Reference 58)

$$\frac{d[\text{CH}_4]}{dt} = -A \exp\left(-\frac{E_a}{RT}\right) [\text{CH}_4] [\text{O}_2]^{2/3},$$

where $A = 10^{11.4} (\text{mol/L})^{-0.65}/\text{s}$, $E_a = 408.8 \pm 85.4 \text{ kJ/mol}$, in the temperature range 450-550°C.

The simulations were performed for a tube 10 cm (diameter) x 25 cm (length). The procedure we followed is to start a flow of oxygen (O₂) and supercritical water (H₂O) into the reactor until all the transients die out and a steady state is reached. At that point we noticed that the velocity pattern was almost uniform, with a narrow boundary layer developed along the walls. The boundary layer increases in width with the distance downstream. This is exactly what one would expect from a uniform flow past a flat plate. We estimated the thickness of the boundary layer expected from a uniform flow past a flat plate, and found it agreed reasonably well with the

numerical results. Had we done the calculation for a longer tube, the boundary layer would have eventually enveloped the entire width of the tube.

Once steady state was reached, we turned on a (gaseous) spray of methane (0.1g/s), which is well mixed with the surrounding flow of oxygen (mass fraction 10%) and supercritical water (mass fraction 90%) at a density of 0.2g/cm^3 . We have done the simulations at sufficiently high temperatures that the water can essentially be treated as a perfect gas. This not only aids in the equation of state to be used, but also ensures a higher rate of destruction (oxidation) of methane. We kept the walls at a constant temperature of 837 Kelvin.

Figure 81 shows the CO_2 concentration profile about 12 s after the methane spray has been turned on. At this point we have not reached a steady-state. We see the beginnings of a flame/blow-torch. The temperature is significantly higher in the central core region where chemical reactions are taking place. One might expect that since the central core region has a higher temperature than the surrounding gas, we would have a Rayleigh-Bernard instability. We note that while this might occur on a very short time scale, we are looking at the reaction zone on the time scale of seconds. This is many orders of magnitude more than the acoustic transit time across the reaction zone. On this sort of a time scale, one can safely expect the pressure to have equilibrated throughout the reaction zone, thereby damping out any instability.

Figure 82 shows the CO_2 concentration profile about 31 s after the methane spray has been turned on. We have now reached a steady-state. The density contours show a definite dip near the axis. In the contours of the mass fractions of the chemical species, we notice that the methane forms a core around which the other species appear to form a halo. We will show in the next section how one can understand this behaviour in terms of a self-similar model for the flame structure in our reactor.

In all the contours, we see that the methane stream and the reaction products never touch the walls. This happens just as we had planned. For this 'test' length of reactor tube, we find that the destruction of methane is about 20%. Thus, if we had a tube of about 125 cm, we would have had complete destruction. We have not made a simulation of a reactor of this length, due to the significant computer time required. However, we did halve the length of the tube to 12.5 cm, and found that the destruction is very nearly halved. Based on these numerical results,

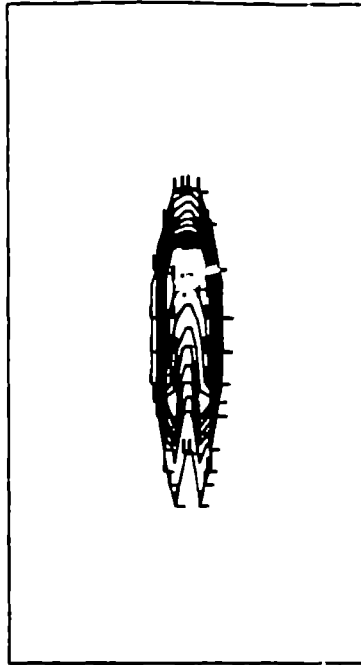


Figure 81. Contours of CO₂ (product) concentration 12 s after the spray of methane was turned on. Steady state has not been reached.

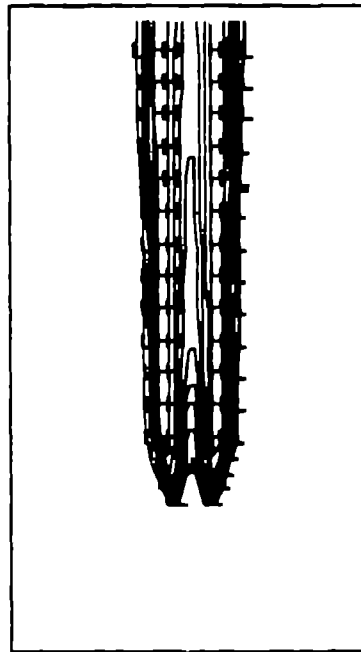


Figure 82. Contours of CO₂ (product) concentration after steady state has been reached (31s).

we feel that a tube of about 150 cm length and a radius of about 10 cm would be sufficient to achieve close to 100% destruction, without the flow reaching the walls of the reactor.

G. PROCESS EVALUATION AND OPTIMIZATION

1. Objective

Several laboratory-scale versions and a few bench-scale versions of the SCWO process exist. Los Alamos National Laboratory (LANL) uses plant design techniques to evaluate the SCWO process and to guide supporting experimental work. In an effort to reduce the number of experiments required, LANL compares several design and operating scenarios for full-scale SCWO plants. Undesirable design and operating conditions are identified, and data are taken at optimal or near-optimal points identified by these simulations.

The tool used for this work is the ASPEN (Advanced System for Process Engineering) computer code, which is normally used for designing chemical plants and refineries. The ASPEN code can produce mass and energy balances for an entire plant flowsheet. The code has many built-in unit operations that can be integrated to form process flowsheets. It also has a large data base of thermophysical properties and many options for estimating vapor-liquid equilibria and phase behavior. The ASPEN code is one of the few commercial simulators that can model solids handling processes.

Based on actual experiments, several simple schemes representing the LANL experimental set-up were analyzed using ASPEN. One set of experiments with methyl ethyl ketone as a surrogate waste provided the basis for six full-scale plant designs. Analyzed on the basis of capital and operating costs, the data indicate which cost factors weigh heaviest on the SCWO process and provide information for finding the optimal plant design and operating conditions.

2. The ASPEN Code

The ASPEN code is an extremely large, flexible computer program that acts as a process flowsheet simulator. It provides building blocks that can be combined to build modules that represent portions of refineries, chemical plants, and waste disposal processes. These building blocks include unit operations such as pumps, reactors, heat exchangers, and distillation columns.

The ASPEN code provides a thermodynamic data base for equilibrium calculations and energy balances. It easily handles normally tedious plant calculations such as recycle matching and provides an accurate material balance for the plant. Other calculations that ASPEN performs are chemical equilibrium calculations (minimization of Gibbs free energy), flash calculations, and pump, turbine, and compressor calculations. This code also establishes design specifications; that is, the engineer can specify a process condition such as stream temperature at a given point in the process and a variable to be manipulated such as a component of the feed stream. The code manipulates the variable (the concentration of the specified component in the feed stream) until the process condition (stream temperature) matches the desired temperature, and can also do equipment sizing and cost analysis.

The ASPEN code has a large, built-in data base of physical thermodynamic properties. It also contains correlations and models for the prediction of physical and thermodynamic properties. These correlations are given for both pure components and mixtures. Predicting physical properties of fluid mixtures is not straightforward unless the mixtures are ideal, which is seldom the case. A package of models that applies to a particular class of components is called a system-option or SYSOP. Los Alamos National Laboratory's version of ASPEN features 12 SYSOPs. The physical property models in each SYSOP are for the fugacity coefficient, enthalpy, Gibbs free energy, entropy, volume or density, viscosity (no solid correlation), thermal conductivity, diffusivity (no solid correlation), and surface tension (liquid correlation only). Of these models, the fugacity coefficient correlation is probably the most important. The version of ASPEN used in this work is ASPEN/SP, a product of Simulation Sciences of Denver, Colorado.

3. Modeling Results

One purpose of this study was to provide heat and material balance information for a commercial-scale (20,000 gallons per day) supercritical water oxidation waste processing unit. This study gives insight into SCWO process optimization and potential plant scale-blems. It also provides information to experimentalists about the relationship of their experiments to the overall plant problem so they can make their experiments more meaningful.

The study was subdivided into two problem sets based on two types of plant design. Problem Set 1 dealt entirely with commercially configured plants. In addition to a supercritical water oxidation reactor, plant flowsheets included peripheral equipment that a commercial plant would require to perform complete waste destruction, including heat exchangers, pumps, turbines,

compressors and knock-out vessels. All problems in Problem Set 2 were based on a plant configuration closely resembling a scaled-up version of one LANL experimental reactor. This plant had a compressor and a pump, but the reactor essentially emulated an electrically heated tube. Problem Set 1 provided insight into the issues of full-scale plant design, construction and operation. Problem Set 2 provided feedback for the experimentalists. Problem Set 2 also provided screening for a large set of problems that will be run later in the Problem Set 1 mode, which is more difficult to set up and run. The ASPEN computer code simulated the plant designs at steady-state operation to provide heat and material balance information for both problem sets.

Problem Set 1 was subdivided into plants that extracted energy as a byproduct and plants that extracted no energy. Plants with no energy extraction furnish the more realistic models because the process conditions used for the energy extraction turbines in the models may be too severe for current commercial turbines. The comparative studies were originally intended to provide incentive for development of those turbines, at least for the higher concentration of hydrocarbons in water. In Problem Set 1, methyl ethyl ketone was used as a surrogate to simulate hydrocarbon-based chemicals such as paint thinner. In this problem set, two times the stoichiometric amount of pure oxygen was used as the oxidant. The calculations showed it is impractical to use this much oxygen in practice; future experiments will be more meaningful if they reflect this information. Six runs were calculated, two each (one with energy extraction and one without) for 2, 10, and 20 wt% methyl ethyl ketone in water.

Several preliminary conclusions can be drawn from the results of Problem Set 1:

- Energy extraction does not pay when the plant feed contains only a small amount of usable energy. In this case, 2 wt% methyl ethyl ketone in water provides a small amount of usable energy. This situation holds for mixtures of other energy-rich compounds such as hydrocarbons in water. Energy extraction is only slightly better (821 kW input versus 879 kW input) than with no extraction. Both cases require net energy input.
- Destruction of hazardous waste solutions containing only 2 wt% methyl ethyl ketone or its heat equivalent in water probably will not be economical. These cases require large heat transfer areas for the reactors—over 10 times that of the 10 wt% methyl ethyl ketone case (based upon heat transfer rates of 8.1×10^6 BTU/hr for the 2 wt% case versus 0.64×10^6 BTU/hr for the 10 wt% case). Water waste

solutions with low heat values require large energy inputs to keep the reaction going, and large energy inputs normally require large heat transfer areas.

- If energy extraction is not the goal, the 10 wt% methyl ethyl ketone case appears to be a good choice. It requires little energy input and a small heat exchange area. If energy extraction is the goal, one can get about as much energy out of the 10 wt% energy extraction case as must be put into the 10 wt% nonextraction case. This level of energy extraction does not justify the extra equipment costs.

Note that the above analyses are strongly dependent upon the heating value per pound of the waste.

Conclusions that may be drawn from the results of Problem Set 2 are as follows:

- Pumping liquid oxygen to process pressures requires less energy than compressing gaseous oxygen to process pressures. How much less energy depends on pump efficiency. A small penalty is paid in energy input and heat exchange area to heat and vaporize the cold liquid.
- Air costs more to compress and heat because more inert gas is present. The effect of heating the inert gas will be different in systems when a greater weight-percent of organic matter is present in the feed.
- The difference between methyl ethyl ketone and the other organics comes from different molecular weights and heating values. Another difference between the methyl ethyl ketone cases and the other organics is the difference in the amount of oxygen required to meet the $1.1 \times$ stoichiometric requirement. This difference affects the compression costs.

4. Conclusions

In addition to the information obtained from this study, mass and energy balances were computed that allow designers to size, specify, and select equipment (or at least anticipate scale-up problems) for these plants. We developed a framework that will allow us to continue efforts to determine optimum operating conditions. We also have a framework on which to build better cost analyses. Even though the cost analysis presented here is preliminary, it provides a first step in the search for optimal plant configurations and operating conditions.

Important things we learned from this study include the following:

- **We should think hard about using a higher weight-percentage of organic matter as a base case. The 2 wt% organic base case has a high operating cost.**
- **Energy extraction is not economical at 20 wt% methyl ethyl ketone (or equivalent hydrocarbon) and below. The calculation trends indicate that above 20%, energy extraction may have an economic payoff.**
- **With the current set of plant designs, purchased oxygen represents the most expensive single operating cost. Using two times stoichiometric oxygen is too expensive and probably unnecessary. The costs of manufacturing oxygen on-site will be studied next as an alternative to purchasing.**
- **In general, operating costs represent a larger share of overall costs than capital equipment costs. Of the capital equipment costs, equipment such as pumps, compressors, and turbines represent a bigger investment than the capital costs of reactors and heat exchangers. We should keep these points in mind as we try to improve the process.**

SECTION X

CONCLUSIONS

A. SCWO CHEMISTRY

In general the chemistry of oxidation of energetic materials in supercritical water is very similar to that found previously for other classes of organics. We have established conditions for which the hydrocarbon elements of all the energetic compounds investigated thus far are completely oxidized to CO_2 and H_2O . The temperature, residence time and oxidant concentration necessary to achieve complete oxidation vary, depending on the nature of the energetic material. Our results indicate that complete oxidation is always achievable using excess oxidant and operating the linear reactor at $600\text{ }^\circ\text{C}$ (11-s residence time). Reasonable carbon balances are obtained for all the energetic materials investigated under these conditions, including PETN, HMX, TNT, RDX, NQ, NM, NG and UDMH. Most of the carbon is detected as CO_2 , with some small fraction remaining in solution as inorganic carbon (CO_3^{2-} or HCO_3^-). The exception is NQ, which produces large quantities of inorganic carbon.

The conditions that produce these results were deliberately "extreme" to ensure complete oxidation. In many cases we have not adequately explored the dependence of the chemistry on oxidant concentration and temperature to determine optimum conditions. Minimization of oxidant concentration is particularly important since the oxidant represents a large fraction of the process cost and if present in excess may enhance corrosion or cause the formation of undesirable products. Furthermore, we have very few data for one variable, the reactor residence time. Less-extreme conditions (e.g., lower temperatures and 1:1 oxidant stoichiometries) may be sufficient to achieve complete oxidation given longer residence times.

Without added oxidant, products of incomplete oxidation were often observed, including CO , CH_4 and HCN . These products are highly undesirable because of their toxicity and/or flammability. Therefore a necessary part of process control is online analysis for the detection of products of incomplete oxidation in the event of loss of oxidant or other such failure. The criteria necessary for online analysis are ppm sensitivity, specificity for multiple components of complex mixtures and rapid (seconds) response. The gaseous effluent diagnostics used in this work, FTIR and mass spectroscopy, meet these criteria and are thus suitable for this purpose.

The nitrogen chemistry of energetics is considerably more complicated, varying widely depending on the nature of the starting material. The nitrogen is always distributed among a group of products, N_2 , N_2O , NO_2^- , and NO_3^- , having formal oxidation states of N varying from 0 to +5. For most of these reactions, quantitative data have been obtained for all products except N_2 . The latter is implicated as the major N product in many of the reactions by elimination of other possible products. Qualitative data (MS and GC) indicate N_2 production in the case of NM, NQ, and TNT. The production of N_2 has been quantified in the reactions of N_2H_4 and UDMH using gas chromatography.

No obvious correlation exists between the nitrogen content or the type of nitrogen groups (e.g., NO_2 or NH_2 groups) of a particular energetic material and the distribution of nitrogen products (N_2 , N_2O , NO_2^- and NO_3^-). It is possible, however, to vary the distribution of products in the different oxidation states by varying the temperature and the oxidant concentration. The clearest example of this variability is NO_x^- production in the reactions of TNT. When a large excess of oxidant is employed at 600 °C, a significant fraction of the initial N (74 percent) is converted to NO_x^- . This fraction is much less (12 percent) for a small (fivefold) excess of oxidant and yet complete oxidation of the carbon still occurs. The same trend is observed for the oxidation of RDX with excess H_2O_2 (10 percent NO_3^-) and with oxygen balance (no NO_3^-). These results indicate that significant control over the oxidation chemistry is possible through the precise tuning of reaction parameters.

The type of oxidant can also have a dramatic effect on the nitrogen product distribution. A case in point is hydrazine. The use of H_2O_2 as oxidant produces primarily N_2 and only trace amounts of nitrate, nitrite and N_2O . Nitrate was also explored as an oxidizer since N_2O_4 is usually used as the oxidizer for hydrazine in liquid fueled rockets and it disproportionates into nitric and nitrous acid when dissolved in water. In contrast to the H_2O_2 case, substantially different nitrogen chemistry is observed with either HNO_3 or $NaNO_3$ oxidizer; the primary products are N_2 and N_2O . Experiments with isotopically labeled HNO_3 indicate that the N_2O is produced from the combination of an NO group of NO_3 with a N from H_2N_4 . Clearly the reaction with H_2O_2 is cleaner, although N_2O_4 (or NO_3) would also be an effective oxidizer for both hydrazine and UDMH.

The destruction chemistry of AP in SCW is unique among the energetic materials since AP has no carbon and is a strong oxidant. The chemistry is best described by the following equation:



Conditions have been determined for which 99.6 percent of the ClO_4^- is destroyed. The Cl is converted into Cl^- , formally reduced from 7^+ to 1^- , and excess oxygen is produced in the reaction. Further evidence for the highly oxidizing nature of this reaction is provided by the strong oxidative corrosion of the C-276 and 316 stainless reactors. The addition of reducing equivalents, in the form of a fuel such as a hydrocarbon, may improve the destruction of AP as well as reduce the reactor corrosion. The nitrogen is distributed between N_2 and N_2O , with no formation of higher oxides or NO_x^- . In contrast to thermal decomposition of solid AP, no harmful products such as Cl_2 or NOCl are formed in the SCWO reactions.

B. INCREASING THROUGHPUT OF EXPLOSIVES

A critical issue in scaling up SCWO treatment of energetic materials to enable a practical process is introduction of significant quantities of explosives into the reactor. We have examined three potential approaches to this problem. The least attractive approach appears to be pre-dissolving the explosive in an organic co-solvent. While convenient for introducing large concentrations of explosives, the co-solvent is partially oxidized in the process, creating numerous byproducts that must subsequently be separated and processed. This disadvantage could be overcome by using a co-solvent that is inert to oxidation, such as supercritical CO_2 . We have found, however, that many explosives and propellant components are only very slightly soluble in SCCO_2 .

A second approach we have explored is to introduce high concentrations of energetics as aqueous slurries. Results on the thermal decomposition of aqueous slurries of TATB suggest somewhat unpredictable behavior. The source of this unpredictability is not presently known; however, we suspect that it may be a mixing problem that leads to self-heating and faster reactions. These experiments have been limited to a static batch reactor with no attempt to stir or agitate the slurry. Experiments with a double base propellant (NG/NC) and with pure HMX gave more predictable results. In both of these cases it was found that water significantly moderated the decomposition compared to the dry material and also modified the product distribution.

We have also attempted to pump slurries mechanically, which may prove to be the greatest hazard associated with their handling. We have designed and constructed a slurry pumping reactor which can be operated remotely at a firing site. We have pumped slurries of a simulant, melamine, and an actual explosive, HMX. We find that the most critical factor in successful slurry pumping is the particle size. With our reactor design, it was necessary to use particle sizes less than $50 \mu\text{m}$

to avoid accumulation and plugging of the reactor. Modeling studies indicate that a combination of larger reactor pipe diameter and faster flow rates would allow the use of larger particle size.

Finally, the most promising approach appears to be pretreatment of the energetic material to increase its solubility in water. Our effort has focused on degradation of the explosive via base-catalyzed hydrolysis at elevated temperatures. These reactions produce water-soluble products that are further processed in SCW to achieve complete destruction of the energetic material and its hydrolysis byproducts. This approach has been successfully demonstrated for NQ, NC, NG, TNT, HMX, RDX and propellants including PBX 9404 and class 1.1 aluminum containing formulations (CYH). We have processed large amounts (up to 500 g pieces) at low temperatures (< 150 C) and pressures (< 60 psi) to produce water-soluble, nonexplosive products. We find that one mole of base is consumed per mole of NO_x groups in the explosives. For class 1.1 propellant formulations, additional base is consumed in reactions with the Al and AP. We find that 1 mole of base is consumed for each mole of Al and AP. Because this approach allows the processing of large concentrations, we have demonstrated very high destruction efficiencies of the starting materials. In most cases, the final products of the combined hydrolysis/SCWO process are identical to those obtained with SCWO alone.

C. REACTOR CORROSION

One of the most critical issues for practical application of an SCWO process to the treatment of energetic materials is reactor wear caused by corrosion. Corrosion of the C-276 reactor by most of the energetic materials does not appear to be a problem. The exception is AP, which caused severe corrosion of the C-276 and 316 stainless reactors. For laboratory-scale reactors, this problem has been solved by the use of a gold liner in the SCW region, which reduces corrosion to acceptable levels.

D. SALT SOLUBILITY

Efficient hydrothermal processing of PEPs requires high starting concentrations which results in the formation of high salt concentrations. Information regarding the solubility behavior of salts formed in hydrothermal processing is essential to control plugging, corrosion, phase behavior and the chemistry related to these processes. The salts produced in hydrothermal processing that are of primary concern are carbonates and aluminates. Carbonates are formed from the oxidation of carbon at pH 5 or greater (carbonate is also referred to as TIC or inorganic carbon in this report). Aluminates are formed from the base hydrolysis of class 1.1 propellants. The

solubilities of these species are highly dependent on pressure and temperature (which determine density). For example, at 450 °C, doubling the pressure from 5000 psia to 10,000 psia increases the solubility over 100-fold. The solubility of aluminates is easily controllable using pH. Under most hydrothermal processing conditions aluminates are highly soluble and should not present any processing difficulties. Carbonates are much less soluble and tend to plug the reactors. Our results indicate that carbonate solubility is significantly enhanced at high pressures (< 10,000 psia) and at high sodium hydroxide concentrations, presumably due to the creation of a melt phase. Our results suggest that it is possible to control the solubility of carbonates to prevent plugging and other harmful effects by operating at high pressure and hydroxide concentration.

SECTION XI

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